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A Classification of Existing and Emerging Hydrogen Storage Technologies

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Abstract—Hydrogen as an energy carrier is expected to play a significant role in the energy systems of the future. Storing hydrogen at utility scale is a relatively new application for which technologies are yet to mature. This paper provides a review of the existing and emerging hydrogen storage technologies. The technologies are categorized based on the phase of storage - gas, liquid or solid - and the type of bonds - compound or free hydrogen. For each category, the storage technologies are compared based on technological operational parameters, technology efficiency, safety, and economic projections.

Index Terms—hydrogen, energy carrier, grid balancing service, hydrogen storage technologies, comparison criteria

I. Introduction

The decarbonization of energy systems entails a shift from greenhouse gas emitting fossil-based sources towards environmentally-friendly renewable energy sources (RES) [1] [2]. RES energy production, however, is dependent on primary intermittent energy sources such as wind and solar irradiation. As a result, large scale integration of RES can lead to a higher level of uncertainty in planning and operation of energy systems. One way to handle this problem is to increase flexibility in the system through energy storage systems.

Energy storage technologies are generally capital intensive. They are mostly built from materials that are limited such as lithium, obtained through harmful mining [3]. Therefore, there is a need for alternative energy carriers to support a smoother transition considering various challenges associated with transport, storage and even end-user consumption.

Hydrogen is considered a promising alternative to natural gas that can replace its application while addressing challenges associated with transport and storage at utility scale [4]. Hydrogen's potential has already been examined and investigated in various applications including heavy industries such as refineries, space applications [5] [4], heavy-duty transport [6] and chemical industries [7].

However, there are numerous technical, economic and legal challenges to come over before hydrogen economy becomes operational [8]. Starting with hydrogen production: only 4% of the global hydrogen production today is obtained from non-potable water resources using RES produced electricity - so-called Green Hydrogen [9] [4]. Shifting to 100% Green Hydrogen production requires an unrealistically massive amount of investment in RES which is deemed infeasible at least in the foreseeable future, thus a limiting factor [10]. Despite the availability of RES, the process of large-scale hydrogen production from non-potable water resources can yield a

significant amount of concentrate, necessitating appropriate management [11]. In addition, a hydrogen economy would require a new hydrogen infrastructure, but creating this induces costs and possibly other unforeseen consequences [12].

Regardless of the method of production, another major technological challenge is hydrogen storage [13]. That is, an adequate storage technology that can be employed at utility scale is yet to be developed. At the production side, hydrogen storage technologies are needed to store the substantial amount of hydrogen that is expected to be produced in the future. At the distribution level, hydrogen storage technology is mostly expected to provide auxiliary services, especially to the power system. That is, it can be used to provide *grid balancing services* in the short-run [14], and long-term seasonal storage services (i.e., level out the variation in energy consumption and production systems) in the long-run [15].

Most of the hydrogen storage technologies proposed in literature are not yet ready to be deployed in the real-world, for various reasons. This is mainly due to hydrogen's explosive nature [16] and the high investment costs [17].

Hydrogen storage technologies have been widely investigated in literature from purely technological and economic prospective. However, several other aspects related to storage, efficiency and safety have not been in the focus of existing literature. This paper aims to take upon those aspects. Section II provides an overview of available hydrogen storage technologies, categorized by form and subsequently phase of storage. The technologies are then analyzed in Section III, based on four criteria: operational conditions, storage efficiency, safety and economic projections. Section IV concludes the paper.

II. OVERVIEW OF TECHNOLOGIES

Hydrogen can be stored in 3 different phases: gas, liquid or solid. It can be stored either as free state hydrogen or as a compound containing hydrogen molecules. In light of this description, six categories of hydrogen storage technologies are defined: Free Hydrogen Gas (FHG), Free Hydrogen Liquid (FHL), Free Hydrogen Solid (FHS), Compound Hydrogen Gas (CHG), Compound Hydrogen Liquid (CHL), and Compound Hydrogen Solid (CHS). The hydrogen storage technologies are classified accordingly and discussed in the following.

A. Free State Hydrogen Storage

Hydrogen is in its free state when hydrogen atoms are stored without modifying the chemical structure, thus remaining H2.

1) Gas Phase: Hydrogen is a gas at room temperature. Hydrogen storage in its gaseous state requires compression due to its extremely low density (0.089 kg/m3) under normal conditions [18] [19]. The storage pressure is restricted by the safety regulation and other operational considerations [20].

The utility scale storage systems that are available today do not exceed 100-200 bar of pressure. Higher pressure increases the hydrogen density inside the tank to 7,8 kg/m3, and induces high energy requirements and operation costs. Compressed hydrogen gas storage can be divided into 2 categories:

- above-ground storage technologies that make use of metallic vessels [20] or small-scale glass structures. The latter has been introduced recently and enables storage at very high pressures up to 1000 bar [21] [22] [23],
- below-ground storage technologies that make use of existing geological features such as existing salt cavities, retired oil/gas reservoirs, aquifers, or pipelines [20].
- 2) Liquid Phase: Liquid hydrogen (or cryogenic hydrogen) storage is attracting more attention due to the high hydrogen content, and relatively low risks corresponding to the low storage temperature and pressure [24]. The main disadvantage of cryogenic hydrogen is the high investment and operational costs corresponding to the higher energy requirement [19].

The energy requirement for operating liquid storage is more than 50% higher than of high-pressure gas storage technologies [19]. This links to the liquefaction of hydrogen, for which the gas needs to be cooled to approximately 20°K at normal pressures (1 bar) or higher [25]. The liquefaction process increases the density of hydrogen to approximately 70 kg/m3 (at 1 bar) [20]. Besides the relatively high energy requirement, liquefaction entails substantial installation costs due to the unsuitability of existing infrastructure and availability issues [26]. Even more importantly, part of the hydrogen is lost to the environment as boil-off, raising safety issues [22].

Liquid hydrogen can be stored in specially designed cryogenic storage vessels, both for terrestrial and marine applications [22] [26]. These should be suitable for operation at extremely low temperatures and be able to maintain the pressure at which the gas is liquefied [27].

3) Solid Phase: Solid state storage of hydrogen occurs through physisorption. In this case, hydrogen itself is not in solid form but rather the adsorbent. Hydrogen molecules stick to the surface of the solid adsorbent. This type of hydrogen storage is extensively investigated due to its promising properties such as fast kinetics, good reversibility and high storage capacity [18]. The main disadvantage of solid state storage lies in complex operation, and space. Several exogenous factors such as temperature and pressure should be adjusted optimally to achieve the desired hydrogen density (i.e., energy density) in solid-state storage [20]. That is, the exothermic reaction needs appropriate heat management to reach higher adsorption rates, and additives to make the process more effective. In addition, even though hydrogen can be stored using adsorbents, the adsorbents themselves also need to be stored. For example in a so-called Adsorptive Hydrogen Storage Tank [28]. The extra space makes it difficult to apply and adjust pressure [29].

Suitable adsorbents are Metal Organic Frameworks (MOFs), Carbon structures (e.g. Activated Carbon (AC), Graphite (G) and Carbon Nanofibres (CN)), and Zeolites [30].

B. Compound Hydrogen Storage

Hydrogen can also be stored as a compound, bonding it to another chemical. It can form gas, liquid or solid compounds.

1) Gas Phase: The most well-known gaseous compounds in which hydrogen can be stored are ammonia (NH3) and methane (CH4). Ammonia (NH3) is a specially interesting alternative due to its relatively high hydrogen storage density and the broad range of applications [31]. Ammonia can be used directly [18], in a fuel cell or combustion engine, or indirectly, by converting it to hydrogen, requiring extra purification steps [22]. Ammonia advantageously makes CO2free energy but can release other GHGs during combustion [32]. Liquefying ammonia leads to higher volumetric energy densities, beneficial for transportation and storage purposes [33]. Storage can occur in tanks at low temperature (-33,4°C) or in the existing propane infrastructure [22]. The main drawback of ammonia lies in the production process. It is mostly produced through the Haber-Bosch process, conducted at a high temperature and pressure, and requiring a specific catalyst to facilitate the process [34], [35].

Methane (CH4) is the "carbon-based carrier with the highest storage capacity" for hydrogen [22]. Production occurs through the Sabatier reaction [36], requiring pure CO2 as input. Despite this benefit, the CO2 used in the methanation process has to be purified before use. Besides, heat recovery should be applied. These extra steps result in higher costs due to higher energy and land requirements. In addition, recovering hydrogen from CH4 is hard and costly. It can be done through the Steam Methane Reforming (SMR) process, which produces so-called Grey Hydrogen and CO2 [37], or through the Catalytic Decomposition of Methane (CDM), a greener yet not commercially available option. These disadvantages make methane more viable as another energy carrier rather than as a medium for storing hydrogen [22].

2) Liquid Phase: Hydrogen can also be stored in compounds that are liquid at ambient temperatures [18]. Most well-known alternatives in this category are liquid organic hydrogen carriers (LOHCs) including Methanol and Formic Acid. LOHCs have a great capacity to store hydrogen, release little heat during production and are safe and abundant. The delivery of LOHCs to the end-users is rather simple as they are compatible with the technical characteristics of the existing fuel distribution infrastructure [18] [22]. The key disadvantage of LOHCs lies in high production costs, mainly due to the high temperatures and pressures, and catalysts needed [18].

Formic Acid (HCOOH) is an advantageous option because of its relatively high density, resulting in a considerable volumetric hydrogen storage capacity. It is associated with low flammability and toxicity, meaning that it is less likely to cause harm to living organisms and the environment. Compared with other liquid carriers, formic acid is rather easy to transport and store [38]. The problem is, it has limited applications, partly

due to its corrosive nature (requiring costly infrastructure adjustments), and partly due to the chemically unfavorable production process. In addition, it has a relatively low energy density when used directly as a fuel [39].

Methanol (CH3OH) also has a number of advantages: promising formation reaction rates, and a lower production cost. It can be used both as a hydrogen carrier (hydrogen is easily released from methanol) or directly as a fuel [40]. Methanol has a higher energy density as a fuel compared to Formic Acid, though lower than gasoline [39], [41]. The main disadvantage of methanol lies in its flammability (it burns with near-invisible flame) and toxicity [42], [43].

Another liquid hydrogen carrier is Syncrude, a mixture of long chain hydrocarbons showing similarities to crude oil [22]. Because of this characteristic, the existing infrastructure can be used for distribution. Syncrude can be produced from CO2 and hydrogen directly and indirectly [44]. However, the production process (Fischer-Tropsch synthesis [45]) is still complex and requires further improvement regarding reaction specifics.

3) Solid Phase: Hydrogen can react with other chemicals to form a solid via the process of absorption. Most common solid absorbents are Metal hydrides, divided into three groups: elemental, intermetallic and complex hydrides [20]. Metal hydrides are considered a safe medium for storing hydrogen due to the low operation temperatures and endothermic reaction [46]. Shortcomings that hinder large-scale application of this technology are e.g. relatively slow kinetics, high (hydrogen release) temperatures and low reversibility [47].

Adsorption technologies can be improved by surface modification and combining elements. Elemental hydrides are binary compound materials made of bonds between hydrogen and 1 other metal [48]. The most promising examples are magnesium hydride (MgH2) and aluminium hydride (AlH3). Intermetallic hydrides can be seen as an improved example of elemental hydrides with an extra element (largely rare earth and transition metals). The final compound takes the chemical formula of AxByHz [49]. These combinations improve hydrogen storage capacities, at the expense of higher material and thus investment costs. Finally, complex hydrides are formed through a reaction of two hydrides, for example, LiBH4, NaAlH4 and LiNH2 [22]. The highest storage densities are reached when boron (B) functions as the central atom. Hydrogen can be released under mild conditions, but hydrogen uptake - the amount of hydrogen that can be adsorbed or absorbed by a material per unit mass or volume - is a lot harder to achieve and requires significant costs and effort [50].

III. ANALYSIS OF CHARACTERISTICS

This section presents an analysis of the different hydrogen technologies with regard to the 4 comparison criteria. First, technological operational conditions are reviewed. Then technology efficiency, and safety. And lastly, economic projections.

A. Technical Operational Conditions

Operational conditions refer to the specifications regarding temperature, pressure and additive requirement needed for hydrogen storage, uptake and release. The simplest condition to maintain the operation is when hydrogen is stored at room temperature (about 21°C) and under normal pressure (1 bar), as this requires the least maintenance and safety measures.

Table I & II present the operational conditions for storage (maintaining hydrogen in the medium) and for uptake and release (forcing hydrogen in and out of the medium) of hydrogen respectively. A ? refers to a lack of information. Remarks are added in italic.

TABLE I: Hydrogen Storage Parameters

| Cat. | Option | Pressure | Temperature | Add. | |
|------|---------------|----------------|---------------------|----------|--|
| | | bar | °C | | |
| | Compressed | 350-700 [51] | normal [51] | No | |
| FHG | H2 gas | | | | |
| | Glass struct. | 1000+ [22] | -40 - 60 [23] | No | |
| FHL | Liquid H2 | 1 [25] | -253 [20] [13] | No | |
| | MOFs | 1 [18] | cryogenic [18] | Yes [18] | |
| | (MOF-5) | | | | |
| | Carbon | high [18] | cryogenic [18] | Yes [18] | |
| | struct. | 00 [20] | 25 [20] | 37 [10] | |
| EHC | - AC | 80 [29] | 25 [29] | Yes [18] | |
| FHS | - G - CN | 100 [29] | 25 [29] | Yes [18] | |
| | | 120 [29] | 27 [29] | Yes [18] | |
| | Zeolites | ? | room T [18] [52] | Yes [18] | |
| | Adsorption | 40 [20] | -176 [20] | Depend. | |
| | (general) | | | on type | |
| | | | | sorbent | |
| | Ammonia | normal / 8-10 | -33,4 / ambient | Yes [18] | |
| CHG | | [31] [5] | [31] [5] | | |
| | Methane | N.A. | | | |
| | Syncrude | Similar to | Similar to | Yes [22] | |
| | | existing fuels | existing fuels | | |
| | | [22] | [22] | | |
| CHL | Methanol | 1 [31] [5] | 25 [31] [5] | Yes [22] | |
| | (LOHC) | 105 5201 | 100 100 5203 | 77 [22] | |
| | Formic Acid | 105 [20] | 100-180 [20] | Yes [22] | |
| | (LOHC) | 10.40.5521 | 20.5521 | 77 [22] | |
| | Metal Hydr. | 10-40 [53] | 20 [53] | Yes [22] | |
| CHS | - Elemental | [20] | [20] | Yes [20] | |
| | - Intermetal. | 50 [20] | 80 [20] | | |
| | - Complex | 100 [54] | 200 [54] | Yes [20] | |

From Table I it can be observed that there is no technology that enables storing hydrogen at room temperature and normal pressure. The least complicated way to store hydrogen are represented by the options with 2 optimal conditions: Compressed H2 Gas (normal temperature & no additives), Liquid H2 (normal pressure & no additives), Ammonia (normal pressure & temperature) and Methanol (normal pressure & temperature).

Methane is a special case. Methane storage and transport is a well established practice (natural gas). However, methane is almost never considered as a hydrogen carrier but rather as an energy carrier. This refers mainly to the relatively hard and costly process of hydrogen release, but also to the extra steps required to adequately store hydrogen in it.

Table II shows a wide variety of processes and associated conditions for hydrogen storage. Although comparing is difficult, one can observe that for both Compressed H2 Gas and Liquid H2 the hydrogen uptake and release processes are

unnecessary, making those options relatively beneficial. Once again methane is special in that it has an unfavorable hydrogen release process. Note that Syncrude is usually considered an end product and thus no hydrogen storage medium. In some cases - mostly for groups of hydrogen carriers like MOFs there is still a lack of information.

TABLE II: Hydrogen Uptake & Release Parameters

| | | H2 | Uptake | H2 Release | | 1 |
|------|--------------------------|------------------------------|------------------------------------|----------------------------------|---|------------------------------|
| Cat. | Option | P | T | P | T | Add. |
| | _ | bar | °C | bar | °C | |
| FHG | Compr. H2 gas | N.A. | N.A. | N.A. | N.A. | N.A. |
| | Glass struct. | N.A. | N.A. | N.A. | N.A. | N.A. |
| FHL | Liquid H2 | N.A. | N.A. | evap. [55] | evap. [55] | N.A. |
| | MOFs MOF-5 | 1 [18] | cryog. [18] | ? | ? | ? |
| | Carbon struct. | ? | ? | ? | ? | Yes |
| | - AC | 30 [56] | -196 [56] | ? | ? | Yes [56] |
| FHS | - G | 113,5 [56] | room T ~ 20 [56] | ? | ? | Yes [56] |
| | - CN | 101 [56] | room T ~ 20 [56] | ? | ? | Yes [56] |
| | Zeolites | ~100 [52] | 350 [18] | 1,5 [52] | ? | Yes [18] |
| CHG | Ammonia | 100- 300 [22] [24] | 400-500 [24] [31] | 250 [57] | 400-700 [31] [57] | Yes [22] [31] [24] |
| | Methane | <100 [58] | 250-400 [22] | ? [22] | ? [22] | Yes [22] |
| CHL | Syncrude | 10-40 [22] | 200-250 (<i>LTFT</i>) [22] | ? | ? | ? |
| | Methanol (LOHC) | 40-60 [59] | ~140 [59] | 25-50 [24] [22] | 200-300 [24] [22] | Yes [31] |
| | Formic Acid (LOHC) | 120 [60] | 120 [60] | depend. on CO2 recov. | 50-100 [20] [55] | Yes [60], Ru- based |
| CHS | Metal Hydr. | depend on type [22] | depend on type [22] | 1.5 [54] (compl. hydr.) | <180 (compl.) [54] ≥300 (MgH2) [18] [20] | Yes [22] |

B. Technology Efficiency

This section focuses on how far the different hydrogen storage technologies have progressed. This assessment is carried out considering various factors including: the scale of application, hydrogen content (in wt%), volumetric (in kWh/L) & gravimetric densities (in kWh/kg), round-trip & conversion efficiencies. Scale of application refers to the scale at which the technology currently is employed. It ranges from 1=large scale (e.g. energy grids), 2=medium scale, 3=small scale (usually laboratory scale), 4=very small scale (microscale) to 5=not realistic. The hydrogen content of a storage option

describes what percentage of the weight consists of hydrogen. Volumetric and Gravimetric Density show the available energy per unit of volume or weight respectively. Volumetric Density can change depending on the applied pressure, whereas Gravimetric Density is a material property. Round-trip efficiency (or storage efficiency) is the percentage of energy input that can be retrieved again. Conversion efficiency is the effectiveness of the conversion - generally converting hydrogen in a compound - expressed as a percentage.

It is assumed that a desirable hydrogen storage technology should have widespread availability, high H2 content, high densities (especially volumetric), and high efficiencies. These factors are considered to determine the most favorable hydrogen storage technology. Results are summarized in Table III.

Table III shows that ammonia exhibits high scores across a majority of dimensions, with Methanol following closely behind. Thus, CHG appears to be the best performing category. One can also see that Liquid H2 has quite a high gravimetric density, but has rather low round-trip and conversion efficiencies. Likewise, methane has a high H2 Content but has a rather low volumetric density. On the other hand, most FHS technologies score very low regarding H2 Content. Note that there is a lack of data on some technologies including MOFs, carbon structures, zeolites, metal hydrides.

C. Safety

The safety level of different hydrogen technologies is evaluated based on the explosiveness and toxicity of the storage medium. The result is given in Table IV. A +/++ refers to reported high levels of explosiveness or toxicity. A - refers to the characteristic not being observed. A ? shows a lack of information. In the far right column important remarks regarding the safety of the storage options are reported.

Table IV shows that flammability is an issue for compressed hydrogen gas, liquid hydrogen, methane, methanol, and metal hydrides, followed by a lower level of explosiveness for ammonia and possibly syncrude. Toxicity is mainly a problem for ammonia, but also, albeit less extreme, for MOFs and methanol. The most promising options in this regard are thus carbon structures or formic acid for hydrogen storage as they both have no reported explosiveness and toxicity claims.

D. Economic Projections

The most prominent factor that determines the success of any technology finding its way in practice is its economic projection. Therefore, an estimated calculation of costs per technology option is provided in Table V. These relate to levelized costs of hydrogen storage (LCHS) solely. LCHS refers to the capital and operational cost of the hydrogen storage system expressed per unit of hydrogen stored. Other costs are considered beyond the scope of this paper. The values are calculated for storage of 1 ton of hydrogen, a realistic future objective. The results are shown in Table V. From an investment perspective, it is evident that technologies with lower investment and/or operational costs are preferred.

TABLE III: Technology Efficiency Parameters

| Cat. | Option | Scale | H content | Vol.Dens. | Grav.Dens. | Round-trip Eff. | Conv. Eff. |
|------|----------------|-------------|----------------|---------------------|----------------------|-----------------|---------------------|
| | | - | wt% | kWh/L | kWh/kg | % | % |
| FHG | Compr. H2 Gas | 1 [22] | 13 [29] | 1,32 [18] | 33,3 [22] | 95-98 [19] | 72,4 [5] |
| | Glass struct. | 4 [22] | 10-14 [13] | ? | ? | ? | ? |
| FHL | Liquid H2 | 2-1 [13] | Size dependent | 2,36 [22] | 33,3 [22] | ~53 [5] | 44,7 [5] |
| | MOFs (MOF-5) | 3 [13] | 4,5 [18] | 0,021 kg H2/L [18] | 0,038 kg H2/kg [18] | ? | ? |
| | Carbon struct. | 3 [13] | 8 [13] | ? | ? | ? | ? |
| FHS | - AC | 3 [13] | 5,5 [29] | ? | ? | ? | ? |
| 1115 | - G | 3 [13] | 4,48 [29] | ? | ? | ? | ? |
| | - CN | 3 [13] | 6,5 [29] | ? | ? | ? | ? |
| | Zeolites | 3 [13] | 9,2 [13] | ? | ? | ? | ? |
| CHG | Ammonia | 1 [22] [31] | 17,8 [18] | 3,53 [31] | 5,17 [31] | 99,3 [5] | Haber-Bosch: 76 [5] |
| CHO | | | | | | | NH3 to H2: 69 [57] |
| | Methane | 5 [22] | 25 [22] | 0,0105 [61] | 15,4 [61] | 95 [5] | Methanation: 87,9 |
| | | | | | | | [5] |
| | Syncrude | 1 [22] | ? | 10 [62] (crude oil) | 3,53 [63](crude oil) | ? | Power-to-fuel: 46- |
| CHL | | | | | | | 67 [64] |
| CIL | Methanol | 3 [22] | 12,5 [22] | 3,3 [22] | 8,64 [63] | 95 [5] | 83,5 [5] |
| | (LOHC) | | | | | | |
| | Formic Acid | 3 [22] | 4,4 [13] | 1,79 [22] | ? | ? | 48 (+Ru-catalyst) |
| | (LOHC) | | | | | | [60] |
| | LOHCs | 1-3 [22] | ? | ? | ? | ~71 [65] | ? |
| | Metal Hydr. | 4-3 [22] | max 12,6 [13] | dependent on type | 0,50 [53] | ~78 [65] | ? |
| CHS | - Compl. | 4-3 [22] | 18,5 [66] | 0,71 [18] | ? | ? | ? |
| | - MgH2 | 4-3 [22] | 7,66 [66] | 5,55kg/100L [66] | ? | ? | ? |

TABLE IV: Safety Assessment

| Cat. | Option | Explosive | Toxic | Remarks |
|------|-----------------------|-----------------|----------------|---|
| FHG | Compressed H2 gas | ++ [67] | - [68] | Asphyxiant [68] |
| FHL | Liquid H2 | ++ [67] [27] | - [68] | Frostbite [27] [67] |
| | MOFs | ? [69] | + [69] [70] | Many forms [69] [70] |
| FHS | Carbon structures | - [71] [72] | - [71] [72] | Weakly explosive / health hazard [73] |
| | Zeolites | ? [74] | ?/- [74] | Little info |
| CHG | Ammonia | + [75] | ++ [75] | Corrosive / Environ- mental hazards [75] |
| | Methane | ++ [76] | - [76] | |
| | Syncrude | +? [77] | -? [77] | Based on crude oil [22] / Health and environmental haz. |
| CHL | Methanol (LOHC) | ++ [78] | + [78] | Health hazard [78] |
| | Formic Acid (LOHC) | - [79] | - [79] | Corrosive [79] |
| CHS | Metal Hydr. | ++ [80] [81] | ? [81] | Taken as a group |

It should be noted that the values listed in Table 5 are not complete. Costs related to chemical processes (hydrogen uptake and release) and material costs are not included. Moreover, most technologies require some development as the costs are still quite high. This especially counts for MOFs and Formic Acid. Costs are relatively low for Metal Hydrides and above-ground Compressed H2 Gas storage.

IV. CONCLUSION

This paper provides a comprehensive overview of the existing and emerging hydrogen storage technologies. Special

TABLE V: Economic Projections

| Cat. | Storage Option | Costs | Remarks |
|------|-------------------|--------------|--------------------------|
| | | \$/ton | |
| | Compressed H2 gas | 1810 [82] | Compression + Storage |
| FHG | - Salt caverns | 1610 [22] | LCHS |
| 1110 | - Above ground | 140-330 [65] | |
| | Glass structures | ? | No info available |
| FHL | Liquid H2 | 1686-1905 | Liquefaction / Liquefac- |
| TILL | | [22] [57] | tion + Storage |
| | MOFs | 490000 [18] | |
| FHS | Carbon structures | ? | No info available |
| ĺ | Zeolites | ? | No info available |
| | Ammonia | 3510 [65] | LCHS Air Seperation |
| CHG | | | Unit [5] |
| | Methane | ? | No info available |
| | Syncrude | 1523 [64] | Calculated from €/lDE |
| | Methanol (LOHC) | 2250 [65] | LCHS |
| | Formic Acid | 23160 [60] | Levelized costs (ecFA |
| CHL | (LOHC) | | + LCO2), described as |
| CIIL | | | Scenario 3 in article by |
| | | | Kim et al. (2022), con- |
| | | | taining production and |
| | | | transportation |
| | GENERAL LOHC | 1200 [65] | LCHS |
| CHS | Metal Hydrides | 700 [65] | LCHS |

attention is given to non-economic characteristics: technical operational conditions, technology efficiency and safety.

The technical operational conditions show that Compressed Hydrogen Gas storage is the most promising technology. It stores free hydrogen, requiring no additional chemical reactions for uptake and release of hydrogen. Hydrogen is stored at normal temperature without additives. On the downside, it requires an elevated pressure of 350-700 bar, raising safety concerns.

The technologies are also assessed based on scale, energy

content, and efficiency. In this regard, ammonia is the most suitable technology. The technology is readily available at a large scale, and especially suitable for transport. It has a high hydrogen content (17,8 wt%), high storage efficiency (99,3%), medium conversion efficiencies (ranging from 25% to 76%) and a relatively high volumetric density (3,53 kWh/L).

The level of safety is assessed based on flammability and toxicity. From this point of view, Carbon structures and Formic Acid are most suitable because neither are flammable nor toxic. However, Formic Acid is corrosive, negatively impacting its storage possibilities. Powdered carbon structures exhibit low explosive potential and are classified as irritants and suspected carcinogens.

Lastly, regarding economic projections, it is difficult to draw any conclusion. This is because research in this field is relatively new. As a result, there is limited clarity and data availability which makes the assessment prone to error. This aspect can be further investigated in the future.

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