

# **The Effect of Trace Elements on the Metabolism of Methanogenic Consortia**

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# **The Effect of Trace Elements on the Metabolism of Methanogenic Consortia**

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## Abstract

Jiang B. (2006) **The Effect of Trace Elements on the Metabolisms of Anaerobic Microbial Consortia**. PhD Thesis, Wageningen University, Wageningen, The Netherlands. p122.

Trace metals are essential for the growth and metabolism of anaerobic microorganisms, due to their roles in key enzymes or cofactors of metabolic pathways. The requirement of trace metals has been recognized. But, proper dosing of these metals in anaerobic treatment system as nutrient still is a great challenge, since dosing of a metal at a high concentration is toxic for growth of microorganisms, and dosing of a specific metal may lead out-compete of one group of microorganisms by the other. In order to obtain knowledge for optimization of metal dosing of anaerobic treatment system, the influence of trace metals, like cobalt, nickel, tungsten and molybdenum on the conversion of methanol and propionate were studied in this research.

By using cobalt-sufficient medium, a methanogenic enrichment culture was enriched from a thermophilic lab-scale UASB reactor fed with methanol as carbon and energy source. From which a novel thermophilic obligate methylotrophic methanogenic archaeon, strain L2FAW<sup>T</sup>, was isolated and characterized as *Methanomethylovorans thermophila*. The growth of strain L2FAW<sup>T</sup> on methanol is stimulated by the addition of cobalt; the optimal cobalt concentration is 0.5 to 2  $\mu\text{M}$ . therefore, cobalt is important for direct methanol conversion by this methanogen.

On the other hand, a syntrophic coculture of methanol degradation was enriched from the same sludge by using cobalt deficient medium, which consisted of a homoacetogen and a hydrogenotrophic methanogen. This coculture degrades methanol partially to acetate and partially to methane, depending on the presence of cobalt. Acetate is the main product when cobalt is present at high concentration; otherwise methane is formed as dominant products. Therefore, cobalt plays a role in the regulation of the pathway of methanol conversion. The optimal cobalt concentration of the coculture for complete methanogenesis from methanol is about 0.1  $\mu\text{M}$ . A thermophilic spore-forming bacteria, strain AMP, was isolated from the coculture, and it is most closely related to *Moorella thermoacetica* based on 16S rRNA analysis. Despite its high DNA-DNA homology with *M. thermoacetica*, strain AMP differs from *M. thermoacetica* on its inability to use glucose, formate and  $\text{H}_2/\text{CO}_2$ , and its unique hydrogenogenic growth on CO. Moreover, strain AMP can grow on formate in a coculture with a hydrogenotrophic methanogen. It is described for the first time that a bacterium can grow on the conversion of formate to  $\text{H}_2$  and bicarbonate provided that hydrogen is consumed by a methanogen.

The effect of cobalt and nickel on the corrinoid and F430 content and on growth of *Methanosarcina barkeri* on methanol was studied. Cobalt and nickel limitation was achieved and competition between cobalt and nickel uptake was observed. Uptake efficiency of cobalt was high at low cobalt concentration and decreased when the cobalt concentration in the medium was increased. Corrinoid and F430 content correlated positively with the cell content of the corresponding metal, but incorporation in the corrinoid and F430 was significant less at low cell metal contents, ranging from 35% to 80% for corrinoid and 5% to 15% for F430.

The trace elements tungsten and molybdenum play an essential role in the growth of anaerobic microorganisms. Depletion of tungsten and/or molybdenum in the media did not affect axenic growth of *Syntrophobacter fumaroxidans* on propionate+fumarate, indicating under these conditions this organism does not have a high tungsten or molybdenum requirement. However, growth of *Methanospirillum hungatei* on either formate or hydrogen and carbon dioxide required tungsten, and molybdenum can replace tungsten to some extent. Growth of the *Syntrophobacter-Methanospirillum* coculture on propionate is significantly affected by the addition of these two metals. Measurement of enzyme levels in cell extracts of syntrophically grown cells indicated that the levels of hydrogenase and formate dehydrogenase activity were correlated with the methane formation rates by the cocultures, which suggests both hydrogen and formate play important role in syntrophic propionate oxidation.

# *Chapter 1*

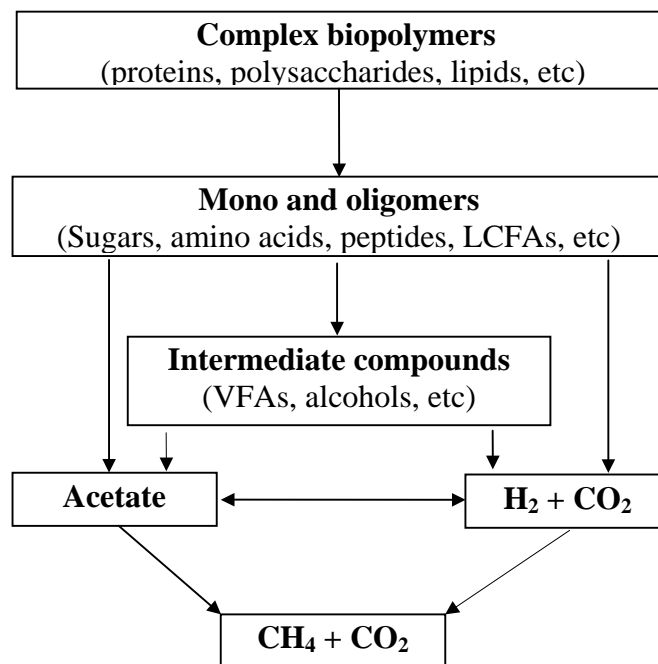
## **General introduction**

## Anaerobic environmental technology

### Anaerobic wastewater treatment

Anaerobic treatment of wastewater is presently accepted as a proven technology (94, 139). Interest in anaerobic treatment of industrial wastewater is increasing rapidly, primarily due to the positive energy balance of the anaerobic treatment process, the low excess sludge production and the development of inexpensive and high rate treatment systems. Various advanced anaerobic treatment configurations have been developed, such as the packed bed, fixed film, expanded/fluidized bed, membrane and upflow anaerobic sludge blanket reactor (72).

**Fig. 1** Flow of carbon in the anaerobic digestion of organic matter, after Gujer & Zehnder (51). LCFAs: long chain fatty acids; VFAs: volatile fatty acids.



Anaerobic digestion is a microbial process in which organic matter is decomposed in the absence of molecular oxygen or other inorganic electron acceptors. The main products of this process are methane, carbon dioxide, ammonium and hydrogen sulfide. Anaerobic digestion can be distinguished in four stages, hydrolysis, fermentation, acetogenesis and methanogenesis (51). Methanogenesis is characterized by a sequence of reactions performed



by different physiological types of anaerobic microorganisms: primary and secondary fermenters acetogenic bacteria and methanogens (51). The last two trophic groups are key players in the anaerobic mineralization of organic matter. Methanogens are specialized in the use of  $\text{H}_2/\text{CO}_2$ , formate and acetate as substrates. Consumption of these products is essential for acetogenic bacteria to oxidize products of the fermentation process, like butyrate and propionate. The conversion of these compounds to the methanogenic substrates is thermodynamically unfavorable (112, 114, 122).

Propionate is an important intermediate in the complete decomposition of complex organic matter under methanogenic conditions. It is formed by fermentative bacteria and accounts for up to 15% of total methanogenesis (51). Conversion of propionate by acetogenic bacteria to acetate,  $\text{CO}_2$ ,  $\text{H}_2$  and or formate, can only proceed if the products, hydrogen and formate, are removed efficiently by methanogens (112, 122). Therefore, syntrophic propionate oxidation plays an important role in methanogenic decomposition, and in maintaining bioreactor stability and performance.

Most of the known syntrophic propionate-oxidizing bacteria belong to the *Syntrophobacter* genus. These bacteria degrade propionate via the methyl-malonyl-CoA pathway (103). To dispose of electrons released from this pathway, acetogens reduce protons to  $\text{H}_2$  or bicarbonate to formate by means of hydrogenase ( $\text{H}_2$ ase) and formate dehydrogenase (FDH). These electron carriers are oxidized again by methanogens. Interspecies electron transfer by syntrophic propionate-oxidizing consortia has been studied extensively, but it is still unclear whether electrons are transferred mainly as hydrogen or as formate (112, 122). Unlike syntrophic butyrate and ethanol oxidation bacteria, *Syntrophobacter* species can only oxidize propionate in coculture with methanogens that can utilize both  $\text{H}_2$  and formate, such as *Methanospirillum hungatei* and *Methanobacterium formicicum*, but not with *Methanobrevibacter* strains that only utilize  $\text{H}_2$  (34). Therefore, besides  $\text{H}_2$  transfer also formate transfer was considered as a possible mechanism (14, 27, 127). Biochemical evidence for interspecies formate transfer was obtained for a co-culture of *S. fumaroxidans* and *M. hungatei* (28, 35). Both microorganisms possess both  $\text{H}_2$ ases and FDHs, and exhibit high activities of these enzymes during axenic growth on formate and during syntrophic growth on propionate (27).

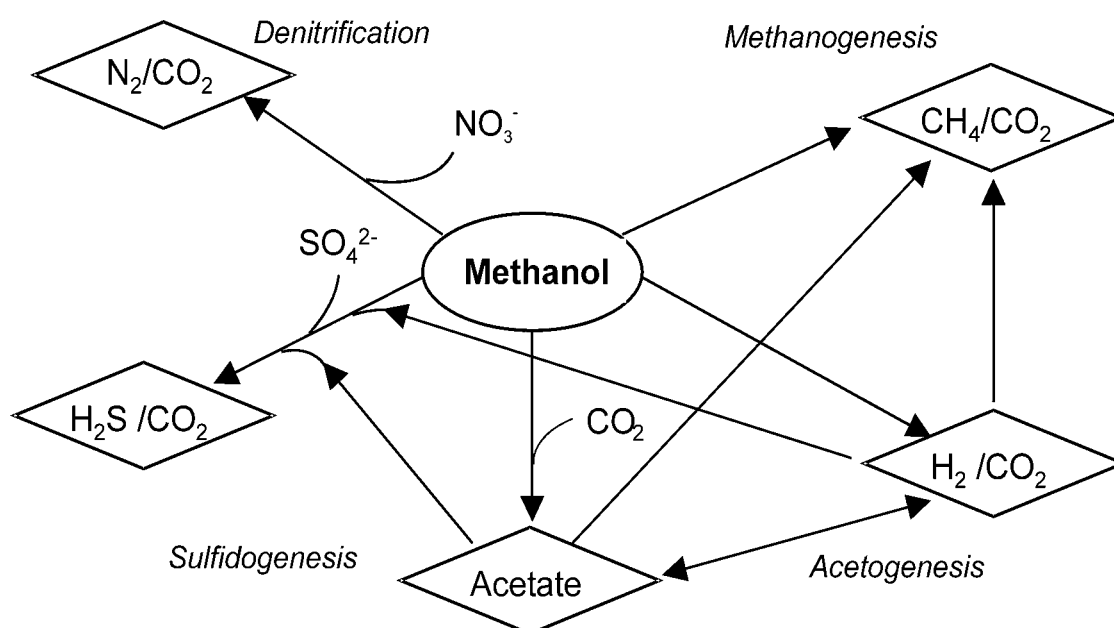
*Thermophilic anaerobic wastewater treatment*

The possibility of the anaerobic treatment technology could be extended if the process could be applied at high temperature ( $>50^{\circ}\text{C}$ ). At high temperature the reaction rates proceed much faster than under mesophilic conditions, so that the loading rates of anaerobic bioreactors can be substantially higher (1, 144). Thermophilic treatment could be an attractive alternative of mesophilic treatment, particularly when the wastewater is discharged at high temperatures. Wastewater treatment in agro-industrial processes at high temperature may be useful in closed water circuits, since it avoids the cooling of the process water and thus allows reuse of water without additional heating (71, 133). However, up to now, only a very few thermophilic anaerobic systems are in operation at full-scale. That is because at thermophilic conditions the start-up of a reactor takes much longer and the process is more sensitive to environmental conditions, e.g. temperature and pH changes, shock loading, feed interruptions, etc. (132).

*Anaerobic conversion of methanol*

Methanol is a one-carbon compound. It is formed during biodegradation of methoxylated aromatics and pectin by fungi and bacteria (96, 113). Methanol is a main

**Fig. 2** Four potential degrading processes and end-products of methanol conversion under anaerobic conditions.



pollutant in the evaporator condensate of pulp and paper industries (85) and in some other chemical and food industries, e.g. coal-gasification plants (86), in landfill leachates (134) and in wastewater of potato-starch factories (88). When a cheap and efficient organic electron donor is required, methanol is often selected as a substrate, for example, in sulfate reduction, denitrification and dehalogenation processes (129, 138).

**Table 1.** Stoichiometries and Gibbs free energy changes of selected biological reactions involved in the anaerobic degradation of methanol at 25°C and 55°C. Values of  $\Delta G'$  were calculated after Amend and Shock (2).

Reactions			$\Delta G'$ kJ/reaction	
			25°C	55°C
<b>Methanogens</b>				
1	$4 \text{ CH}_3\text{OH} \rightarrow 3\text{CH}_4 + \text{HCO}_3^- + \text{H}^+ + \text{H}_2\text{O}$		-313	-319
2	$\text{CH}_3\text{OH} + \text{H}_2 \rightarrow \text{CH}_4 + \text{H}_2\text{O}$		-113	-112
3	$\text{HCO}_3^- + 4 \text{ H}_2 + \text{H}^+ \rightarrow \text{CH}_4 + 3\text{H}_2\text{O}$		-136	-125
4	$\text{CH}_3\text{COO}^- + 2\text{H}_2\text{O} \rightarrow \text{CH}_4 + \text{HCO}_3^-$		-31	-35
<b>Acetogens</b>				
5	$4 \text{ CH}_3\text{OH} + 2 \text{ HCO}_3^- \rightarrow 3\text{CH}_3\text{COO}^- + \text{H}^+ + 4 \text{ H}_2\text{O}$		-219	-214
6	$\text{CH}_3\text{OH} + 2\text{H}_2\text{O} \rightarrow 3\text{H}_2 + \text{HCO}_3^- + \text{H}^+$		+23	+13
7	$\text{CH}_3\text{COO}^- + 4\text{H}_2\text{O} \rightarrow 2\text{HCO}_3^- + \text{H}^+ + 4\text{H}_2$		+104	+90
<b>Sulfate and nitrate reducers</b>				
8	$4 \text{ CH}_3\text{OH} + 3\text{SO}_4^{2-} \rightarrow 3\text{HS}^- + 4\text{H}_2\text{O} + 4\text{HCO}_3^- + \text{H}^+$		-363	-373
9	$5\text{CH}_3\text{OH} + 6\text{NO}_3^- \rightarrow 3\text{N}_2 + 5\text{HCO}_3^- + \text{OH}^- + 7\text{H}_2\text{O}$		-3207	-3207

Possible anaerobic degradation pathways of methanol are shown in Fig. 2. Reaction stoichiometries and Gibbs free energy changes at mesophilic and thermophilic conditions are shown in Table 1. Four distinct groups of anaerobic microorganisms are able to grow on methanol, namely denitrifiers, sulfate-reducing bacteria (SRB), methanogenic archaea (MA), and homoacetogenic bacteria (HAB) (83, 89, 128, 137). All four groups of microorganisms may compete for the available methanol in the mixed communities, depending on the availability of electron acceptors.

Indirect methanogenesis from methanol is occurring when methanol is first converted to either acetate or  $\text{H}_2$  by HAB (109, 130), and then acetate or  $\text{H}_2$  is used by MA (3) or SRB

(26). Indirect methanol degradation via  $H_2$  as intermediate is unfavorable under standard conditions (Table 1), thus the  $H_2$  level has to be kept low (112, 114, 122). In this respect, the different microorganisms involved depend on each other to degrade methanol, which is called a syntrophic relationship (112, 122). Since utilization of methanol by MA and HAB is independent on electron acceptors, these microorganisms metabolically interact with each other directly or indirectly.

### *Biotechnology of anaerobic treatment of methanol-containing wastewater*

Much research was conducted to investigate the feasibility of anaerobic treatment of methanol containing wastewater. Feasibility of anaerobic treatment of methanolic wastewater was doubted. These doubts concerned the operation of a stable anaerobic treatment process due to unpredictable accumulation of volatile fatty acids (VFAs) in the effluent that may cause the failure of the treatment process (46, 74).

Lettinga and co-workers (46, 73, 74) concluded that environmental factors, such as the cobalt concentration level, the methanol concentration inside the reactor, the presence of exogenous bicarbonate and high concentrations of undissociated VFA, determine the stability of methanogenesis from methanol and the predominance of homoacetogens or methanogens. When bicarbonate and trace metals were applied together, VFAs accumulate in the effluent, consequently, methane production ceases due to a drop of pH (46, 73, 74). When the concentrations of cobalt, bicarbonate and methanol were kept low, methanogens predominated and methanol was converted directly to methane by methylotrophic methanogens and not via the intermediate formation of VFA or  $H_2$ . Under other conditions, homoacetogenesis predominated, resulting in the formation of acetate (45). It was found that *Methanosarcina* species dominated under mesophilic conditions in a reactor fed with methanol, indicating direct methanogenesis from methanol (11). If the pH was maintained between the 5.0-6.0, hydrogenotrophic methanogens survived and grew, indicating that methanol was converted syntrophically to methane through  $H_2$  and  $CO_2$  (9, 10). The predominant methanogens in the granular sludge from this reactor resembled the hydrogenotrophic *Methanobacterium* and *Methanobrevibacter*, *Methanosarcina* and acetoclastic *Methanosaeta* (11). From this, the authors concluded that methanol was not converted to methane directly, but was also converted through the intermediate formation of acetate and  $H_2/CO_2$ .

Feasibility of thermophilic treatment of methanol-containing wastewater was studied recently (99, 100). Good reactor performance was achieved at organic loading rates (OLR) up to 47.3 g COD/L/day in a bicarbonate buffered medium. About 93% of the methanol was converted to methane, with little acetate accumulation (99). By using specific inhibitors and nuclear magnetic resonance (NMR) spectroscopy, it was found that half of the methanol was directly converted to methane by methylotrophic methanogens and the other half via the intermediates of  $H_2$  and acetate (101). This was confirmed by analysis of the microbial composition of the sludge: the most abundant bacteria and archaea were most closely related to *Moorella glycerini*, *Methanothermobacter thermoautotrophicus* strains and *Methanomethylovorans hollandica* (105). Moreover, it was also found that the cobalt requirement of the thermophilic mixed consortium was lower than that of a mesophilic-methylotrophic consortium (98).

### Anaerobic microorganisms involved in methanol conversion

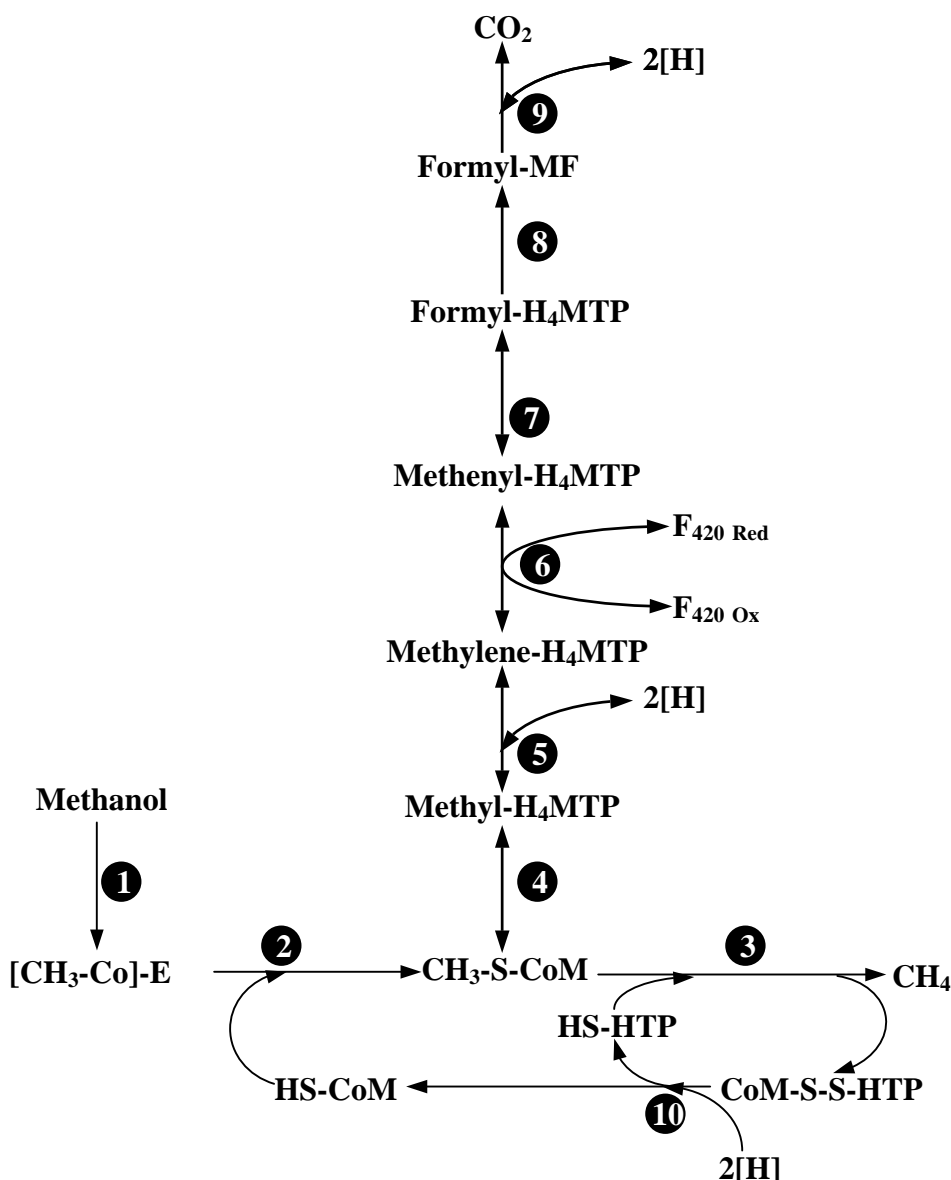
A major part of thesis was focused on thermophilic methanol conversion. Therefore, the microorganisms involved in mainly thermophilic methanol degradation are addressed here.

#### *Thermophilic methanogenic archaea*

Methanogenic archaea are microorganisms that use only a few substrates for methane formation, such as  $H_2/CO_2$ , acetate and C1-compounds, like formate, methanol and methylated amines (43). Most thermophilic methanogenic archaea can only utilize  $H_2/CO_2$  and (or) formate as substrate, such as species in genera *Methanothermobacter* and a few species of the genus *Methanobacterium*, *Methanocaldococcus* and *Methanosarcina* (135). A few methanogens can utilize acetate for methane formation, like *Methanosaeta thermophila* (93) and *Methanosarcina thermophila* (145). Methanogens capable of methanol utilization almost exclusively belong to the family *Methanosarcinaceae*. Besides the two thermophilic halophilic obligate methylotrophs, *Methanohalobium evestigatum* and *Methanosalsum zhilinae*, *Methanosarcina thermophila* is the only thermophilic freshwater species that can utilize  $H_2/CO_2$ , acetate and methanol. *Methanosarcina thermophila* and most *Methanosarcina*

species were isolated from anaerobic bioreactors. *Methanothermobacter* species are ubiquitously present in a number of environments such as anaerobic digesters, hot springs and sediments (135).

All methanogenic Archaea examined to date rely on methanogenesis as their sole means of energy conservation (43). Methanogens growing on different methanogenic substrates use a common methanogenic pathway (Fig. 3). This pathway is unique since it has several unique coenzymes, like coenzyme-M (HS-CoM), factor F420 and F430, methanofuran, tetrahydromethanofuran and 7-mercaptoheptanonylthreonine phosphate, which are not commonly present in other groups of microorganisms (108). Activation of methanol in this pathway (reduction route) is carried out by two corrinoid-containing methyltransferases, resulting in a methylated coenzyme-M (23). Methane formation from methyl-CoM is catalyzed by methyl CoM reductase, an enzyme that contains F430. In order to provide reducing equivalents for reduction of methanol to methane, one quarter of methanol has to be oxidized to CO<sub>2</sub>. The mechanism of methanol conversion is still not clear yet. An overall pathway is depicted in Figure 3. Several alternatives are possible (63), in which methanol is oxidized to methenyl-H<sub>4</sub>MTP by a methanol dehydrogenase and an unknown methyl-carrier. Interestingly, in such a pathway, corrinoid seems not necessary (12). During methanol conversion, a sodium-gradient is generated by methyl transfer from CH<sub>3</sub>-H<sub>4</sub>MPT to HS-CoM. The sodium-gradient is the driving force for the synthesis of ATP, reverse electron transfer, and solute uptake (7, 13). Recently, an energy conserving hydrogenase was found in *Methanosarcina barkeri*, which could drive a reverse electron transfer process to provide reducing equivalents for the reduction of ferredoxin with H<sub>2</sub> (84).



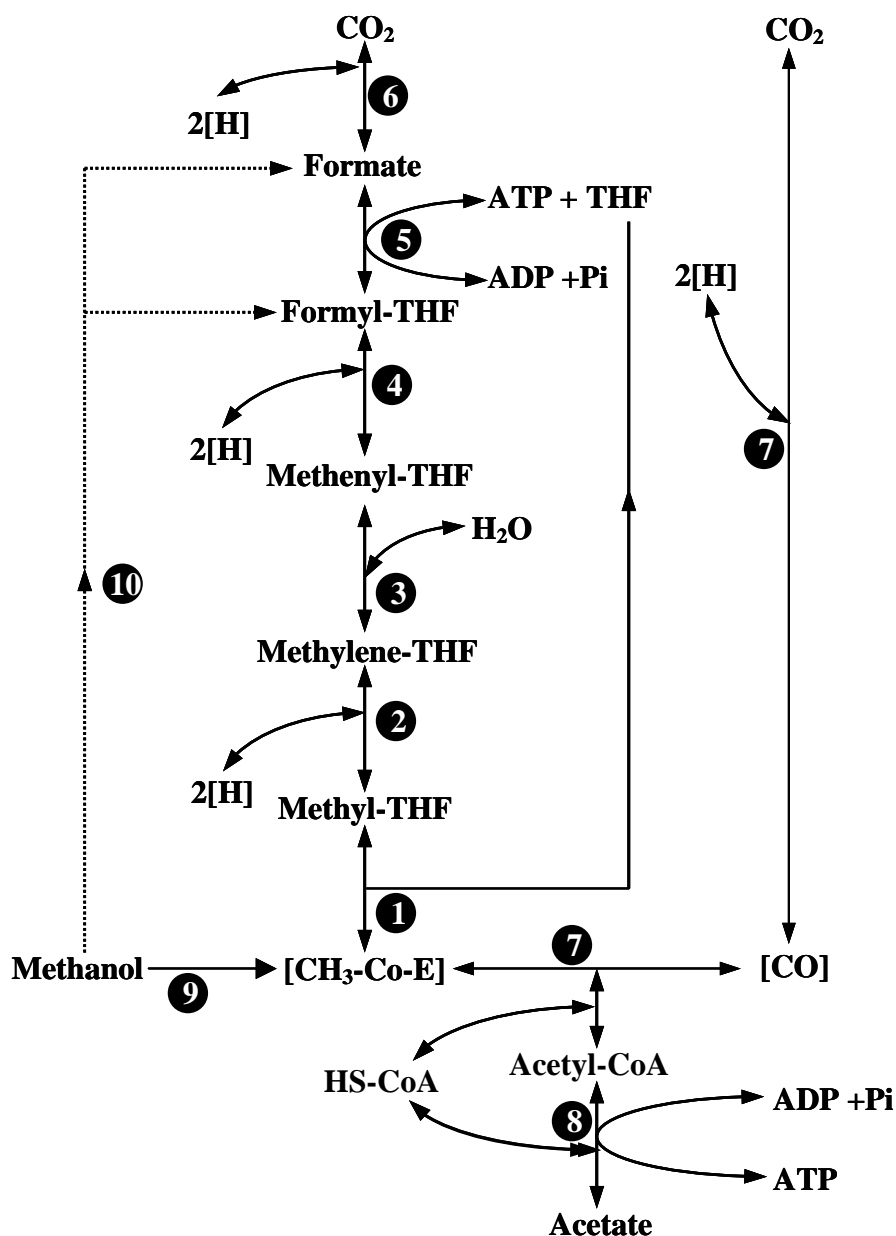
**Fig 3.** Methanogenic pathway from methanol, after (87) and (24). Abbreviations: MF, methanofuran;  $\text{H}_4\text{MTP}$ , tetrahydromethanopterin;  $\text{F}_{420}$ , a 8-hydroxy-5-deazaflavin derivative;  $\text{HS-CoM}$ , coenzyme M;  $\text{HS-HTP}$ , 7-mercaptoheptanonylthreonine phosphate;  $[\text{CH}_3\text{-Co}]\text{-E}$ , corrinoid bound methyl group. Enzymes indicated by 1, methanol:5-hydroxybenzimidazolylcobamide methyltransferase; 2, methylcobamide: $\text{HS-CoM}$  methyltransferase; 3, methyl-S-CoM reductase; 4, methyl- $\text{H}_4\text{MTP}$ : $\text{HS-CoM}$  methyltransferase; 5, methylene- $\text{H}_4\text{MTP}$  reductase; 6, methylene- $\text{H}_4\text{MTP}$  dehydrogenase; 7, methylene- $\text{H}_4\text{MTP}$  cyclohydrolase; 8, formylmethanofuran: $\text{H}_4\text{MTP}$  formyltransferase; 9, formylmethanofuran dehydrogenase; 10:  $\text{F}_{420}\text{H}_2$ :heterodisulfide oxidoreductase.

*Thermophilic homoacetogens*

Homoacetogenic bacteria are a group of bacteria that utilize the reductive acetyl-CoA pathway to form acetate (37). They are versatile anaerobes in terms of their substrate profile (36). In the acetyl-CoA pathway CO<sub>2</sub> acts as a sink for reducing equivalents generated in the oxidation of carbohydrates, organic acids, C1 compounds or hydrogen. Around 100 species of homoacetogenic bacteria divided over 21 genera in the *Bacillus-Clostridium* subphylum have been described (22, 37). Well-studied mesophilic methylotrophic utilizing homoacetogens are *Sporomusa ovata*, *Eubacterium limosum*, and *Acetobacterium woodii*. The best-characterized thermophilic methanol-degrading homoacetogens are the heat-resistant spore-producing species *Moorella thermoautotrophica* (140) and *Moorella thermoacetica* (47). Based on which cation is used for energy conservation, homoacetogens are divided into two groups: proton-dependent homoacetogens, like *Moorella* and *Sporomusa* species (49, 62), and sodium-dependent homoacetogens, represented by *Acetobacterium woodii* and *Thermoanaerobacter kivui* (55, 142).

Homoacetogens use the acetyl-CoA pathway (Fig.4) for both catabolism and carbon fixation of C1 compounds, like CO, formate and methanol (37, 76). It is also used by other microorganisms, like sulfate reducing bacteria and methanogens for synthesis of biomass (19, 70, 103). It is also found that the acetoclastic methanogen, *Methanosarcina acetivorans* C2A during growth on carbon monoxide might employ this pathway for energy conservation as an alternative for the methanogenic pathway (107). Therefore, acetyl-CoA pathway is important for all kinds of microorganisms. The key enzymes in the acetyl-CoA pathway are formate dehydrogenase (FDH), methyltransferase and carbon monoxide dehydrogenase/acetyl-CoA synthase complex (CODH/ACS). Formate dehydrogenases contain either tungsten or molybdenum, depending on the species (38), growth substrates (92) or availability of these two metals (8, 18). CODH/ACS complex contains nickel and iron, and has both CO oxidation and acetyl-CoA synthesis activities (76). Tetrahydrofolate is the C1-carrier in the acetyl-CoA pathway (57). It is still unclear how methanol enters this pathway, but likely a corrinoid-containing methyltransferase is involved (130). Alternatively, methanol could be oxidized by a methanol dehydrogenase. In *Moorella thermoautotrophica* oxidation of methanol to formate is done with a methanol dehydrogenase that contains paraquinoline quinone (PQQ) as the prosthetic group (141).





**Fig 4.** Acetate formation from methanol via the acetyl-CoA pathway in homoacetogens, modified after (54). Abbreviations: THF, tetrahydrofolate; HS-CoA, coenzyme A;  $CH_3\text{-Co-E}$ , corrinoid bound methyl group. Enzymes indicated by 1, methyltransferase; 2, methylene-THF reductase; 3, methylene-THF dehydrogenase; 4, methenyl-THF cyclohydrolase; 5, formyl-THF synthetase; 6, formate dehydrogenase; 7a, carbon monoxide dehydrogenase; 7b, acetyl-CoA synthase; 8, phosphotransacetylase and acetate kinase; 9, methyltransferase (130); 10, methanol dehydrogenase (141).

### *Syntrophic degradation of methanol*

Conversion of methanol by homoacetogens results in the formation of acetate that is used by aceticlastic methanogens, such as *Methanosaeta* species (93). However, it is also possible that homoacetogens convert methanol to  $H_2/CO_2$ , when the  $H_2$  partial pressure is kept low by hydrogenotrophic methanogens or sulfate reducers. As methanol oxidation to hydrogen is thermodynamically unfavorable at standard conditions, consumption of  $H_2$  is essential for syntrophic methanol degradation via  $H_2$  (112, 122). The first syntrophic methanol degrading co-culture was enriched in an attempt to isolate a vitamin B<sub>12</sub> producer, and consisted of *M. thermoautotrophica* strain Z-99 and *Methanobacterium thermoformicum* strain Z-245 (97). Such syntrophic methanol conversion was also observed for some other homoacetogens, like *Butyribacterium methylotrophicum*, *Sporomusa ovata*, *Acetobacterium woodii* and *Moorella mulderi* (3, 54), or by a fermentative bacterium *Thermotoga lettingae* (4). Besides methanogens, sulfate reducers (26, 54) and iron reducing bacteria can be syntrophic partners (25).

### **Trace metals as nutrients in microorganisms**

Certain metals play a fundamental role in microbial growth and metabolism, but they may also be toxic to microbial life at higher concentrations (59, 95). A rough estimation of the required amount of trace metals can be obtained from the cell composition of intact microorganisms (45, 111). The requirement of trace metals is dependent on their role in certain enzymes and cofactors in the metabolic pathways of microorganisms (95). Table 2 lists common trace metals required for growth of methanogenic archaea, homoacetogenic bacteria and sulfate-reducing bacteria. Among them, cobalt (24, 130), nickel (33, 76, 104), tungsten (77) and molybdenum (38) are important metals in the methanogenic and homoacetogenic pathways. Most metals exist as a metal center in enzymes or as cofactor, for example, cobalt in corrinoid, nickel in F430, hydrogenase and carbonmonoxide dehydrogenase. Other metals cannot replace these metals. However, tungsten and molybdenum can replace each other in formylmethanofuran dehydrogenase (8, 56).

**Table 2.** Selected trace elements in enzymes of anaerobic microorganisms and their functions. MA: methanogenic archaea; HAB: homoacetogenic bacteria; SRB sulfate-reducing bacteria

Enzymes or groups	Metals	Exist form	Affected groups	Reactions	Reference
Methyltransferase	Co	Corrinoid	MA, HAB	$\text{MeOH} + \text{CoM} \rightarrow \text{CH}_3\text{-CoM}$	(24, 130)
Methyl-CoM reductase	Ni	F <sub>430</sub>	MA	$\text{CH}_3\text{-CoM} + 2[\text{H}] \rightarrow \text{CH}_4 + \text{CoM}$	(33)
Formylmethanofuran dehydrogenase	W, (Se, Fe) Mo, (Se, Fe)	Tungstopterin Molybdopterin	MA	$\text{CO}_2 + \text{MFR} \rightarrow \text{CHO-MFR} + \text{H}_2\text{O}$	(56)
Carbon monoxide dehydrogenase	Ni, Fe	Fe-Ni-S	MA, HAB, SRB.	$\text{CO} + \text{H}_2\text{O} \leftrightarrow \text{CO}_2 + 2\text{e}^- + 2\text{H}^+$	(70, 76, 103)
Hydrogenase	Fe Fe, Ni, Se.	Fe-S Fe-S-Se	MA, HAB, SRB.	$\text{H}_2 \leftrightarrow 2\text{e}^- + 2\text{H}^+$	(53, 104)
Formate dehydrogenase	W, (Se, Fe) Mo, (Se, Fe)	Tungstopterin, Molybdopterin	MA, HAB, SRB	$\text{HCOOH} \leftrightarrow \text{CO}_2 + 2\text{e}^- + 2\text{H}^+$	(77, 82, 103)
Carbonic anhydrase	Zn,		MA, HAB	$\text{CO}_2 + \text{H}_2\text{O} \leftrightarrow \text{HCO}_3^- + \text{H}^+$	(121)
Nitrogenase	Mo		MA	$\text{N}_2 + 8\text{H}^+ + 8\text{e}^- + 16\text{ATP} \rightarrow 2\text{NH}_3 + \text{H}_2 + 16\text{ADP} + 16\text{P}_i$	(78, 110)
Superoxide dismutase	Cu, Zn		MA	$\text{H}_2\text{O}_2 \rightarrow \text{O}_2 + 2\text{e}^- + 2\text{H}^+$	(17, 64)
Cytochrome	Fe	Haem, Fe-S	HAB, SRB	Electron transfer chain	(62)
Ferredoxin	Fe	Fe-S	MA, HAB, SRB	Electron transfer chain	(123)

*Cobalt in corrinoid of methyltransferase*

Corrinoid sometimes is referred to as cobalamin, or vitamin B<sub>12</sub>. The catalytic center of the corrinoid is the cobalt ion (124)(Fig. 5). Up to 8 different corrinoid structures have been characterized from anaerobic microorganisms; their occurrence differs from species and the metabolic substrate that is used (124). Synthesis of corrinoid compounds has been studied in most detail in *Propionibacterium shermanii*. Synthesis of corrinoid requires at least 25 enzymes and more than 40 catalytic steps (106). Up to 98% of the total cobalt content may be present in corrinoid (126). The corrinoid content of methanogens and homoacetogens differs dependent on the species, growth substrate and cultivation condition; highest values were obtained when grown on methanol (48, 69, 124). Vitamin B<sub>12</sub> production by *M. barkeri* was intensively studied (91, 118-120).

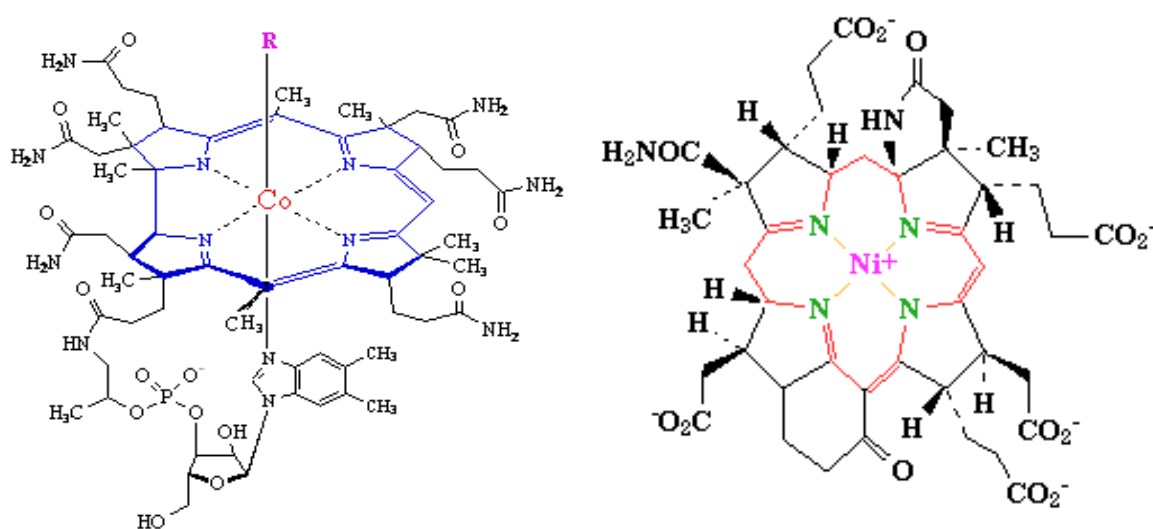


Fig. 5 Structures of corrinoid compounds and cofactor F430 (from (124) and (117), respectively)

Corrinoid-dependent methyl transfer reactions are important in methanogenesis and homoacetogenesis (24, 125, 130). In methanogens, a corrinoid derivate, cofactor III in super reduced Co (I) form accepts the methyl group from methyl-H<sub>4</sub>-MTP or methanol, resulting in a methyl-Co(III) intermediate. This intermediate reacts with HS-CoM, resulting in the formation of methyl-CoM and regenerated Co(I) (7). A similar corrinoid-dependent methyl transfer reaction occurs in homoacetogens, except that the methyl donor and methyl acceptor are methyl-THF and carbon monoxide, respectively (76, 130).

*Nickel in cofactor F430 of methyl-CoM reductase*

Nickel has been found in many enzymes, including urease, hydrogenase, carbon monoxide dehydrogenase of all kinds of microorganisms, and the methyl-CoM reductase of methanogens (53). F430 is a yellow nickel containing tetrapyrrole that does not show fluorescence (116). F430 has a similar structure as corrinoid (Fig. 5). They share almost the same biosynthesis route till the last step before the insertion of the metal (30, 31). Up to 70% of the labeled nickel taken up by *Methanothermobacter thermoautotrophicus* was found to be present in this cofactor (32). Ni(I) in F430 can be methylated to form methyl-Ni(III), which is spontaneously converted to methane and Ni(II)-F430 (50, 61).

*Tungsten and molybdenum in formate (formylmethanofuran) dehydrogenase*

Molybdenum and tungsten are essential trace elements for growth of a variety of microorganisms, including methanogenic and hyperthermophilic archaea, gram-positive bacteria, sulfate reducers and nitrogen-fixing bacteria (38, 56, 70, 103). Enzymes containing these elements usually catalyze oxidation reactions, such as formate dehydrogenase (FDH), formylmethanofuran dehydrogenase (FMDH). The metal ion is associated with either one or two pterin derivatives to form a cofactor in the enzymes (65). FDH catalyzes the first reaction of CO<sub>2</sub> reduction to formate in the acetyl-CoA pathway (76), and is also important for syntrophic propionate oxidation (103). Formylmethanofuran reductase is an analogue of FDH in methanogens, using methanofuran as formyl group acceptor for CO<sub>2</sub> reduction (56). The stimulation effect of tungsten and molybdenum on homoacetogens and methanogens is mainly related to these two enzymes (65). Isoenzymes with either tungsten or molybdenum can be found in the same species (18, 38). Antagonistic effects were also described (82, 143). Most interestingly, it was found that tungsten could replace molybdenum in the Mo-isoenzymes of FMDH, but replacement of tungsten by molybdenum results in inactive isoenzymes (8, 115). This is the only example that the metal center in enzymes can be replaced by another metal functionally.

*Metal speciation and metal uptake*

Although essential metals can be added to the growth medium as simple metal salts, the metal ions may be present in the final medium in different forms depending on the chemical properties and concentrations of anions and complexing agents present and the pH.

Under anaerobic conditions, sulfide, carbonate and phosphate may be present at a high concentration. Due to binding with metals to form precipitates, they have a strong effect on metal speciation, metal uptake and growth of microorganisms (20, 21, 58). To keep metals in soluble form, organic ligands, such as EDTA and NTA are often added to the medium (15, 52). As a strategy to facilitate uptake, microorganisms secrete organic products, which have a similar role as the added organic ligands (5, 6, 42). A good example of microbially produced ligands is given by the siderophores secreted by aerobic bacteria to facilitate specifically the uptake of iron (75, 80). Such specific metal ligands are rarely described for anaerobes (16, 44). Due to weak metal binding of most (characterized) compounds, excreted ligands are unlikely effective at low metal concentration (16).

It is generally accepted that only free metal ions can be transported across the cytoplasmic membrane. It is also reported that labile (131), lipophilic and even hydrophilic complexes can be transported (102). Metal ions are taken up by microorganisms via a wide variety of transport systems. Transporters are categorized into two groups: non-specific transporters and specific high affinity transporters (40, 66, 68). Non specific transporter can transport all divalent cations with quite low affinity in a sequence of preference  $Mg^{2+} > Co^{2+} > Zn^{2+} > Mn^{2+} > Ni^{2+} > Ca^{2+}$  (60, 90, 136). Therefore, cobalt and nickel uptake is affected by the presence of magnesium (90). When metals are at a growth-limiting concentration, microorganisms express specific high affinity transporters for uptake. Typically ABC transporters and trans-membrane permeases possess an affinity below the  $\mu M$  range (29, 39-41, 67). All these transporters are affected by certain metals at high concentrations, e.g. nickel uptake by the specific transporters, Nik and HoxN, is inhibited by cobalt (29, 41). Uptake of anions, like tungstate and molybdate, is not well studied. They can be transported via a non-specific sulfate transport system and a specific ABC transport system (79, 81).

### **Synopsis of the thesis**

The objective of the research presented in this thesis was to study microbial aspects of methanogenesis with methanol, and the role of metals on the metabolism of the microorganisms involved. This information is essential to optimize trace metal dosing in anaerobic bioreactors and to steer metabolic pathways in mixed anaerobic microbial communities.

Under moderately thermophilic conditions, direct methanogenesis from methanol by methylotrophic methanogens and indirect methanogenesis from methanol by homoacetogens and hydrogenotrophic methanogens are both important. This indirect methanogenesis from methanol requires less cobalt. Therefore, the first part of the thesis was focused on the isolation and characterization of the microorganisms in sludge of a methanol-fed anaerobic bioreactor operated at 55°C. **Chapter 2** described a novel thermophilic methylotrophic methanogen, *Methanomethylovorans thermophila* strain L2FAW. In **Chapter 3**, a novel carboxydutrophic hydrogenogenic homoacetogen, *Moorella hydrogenoformans* strain AMP was described. Strain AMP grows on formate in a syntrophic association with a methanogen, *Methanothermobacter* strain NJ1 (isolated from the same enrichment culture). This is described in **Chapter 4**. In the second part of the thesis, the effect of metals on the metabolism of specific microorganisms was studied. In **Chapter 5**, the effect of cobalt and nickel on the growth of *Methanosarcina barkeri* under conditions of well-defined metal speciation was studied. The relationship between growth rate, cell metal and cofactor content were investigated as well. In **Chapter 6**, the effect of tungsten and molybdenum on the interspecies electron transfer on syntrophic propionate oxidation was studied. Finally, the results obtained in this thesis are discussed in **Chapter 7**.

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## *Chapter 2*

***Methanomethylovorans thermophila* sp. nov., a  
thermophilic methylotrophic methanogen from an  
anaerobic reactor fed with methanol**

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## Summary

A novel thermophilic obligate methylotrophic methanogenic archaeon, strain L2FAW<sup>T</sup>, was isolated from a thermophilic lab-scale UASB reactor fed with methanol as carbon and energy source. Cells of strain L2FAW<sup>T</sup> were non-motile, irregular cocci of 0.7-1.5 µm, occurring mainly single, or in clusters of two or four cells. Cells stained Gram-negative and lysed immediately in 0.1% (w/v) SDS. Growth was inhibited by chloramphenicol and tetracycline, but not by penicillin, bacitracin, spetinomycin, vancomycin and kanamycin. Methanol, and mono-, di- and tri-methylamine were used as substrates, but H<sub>2</sub>/CO<sub>2</sub>, formate, acetate, propanol, dimethyl sulfide and methanethiol were not. The temperature range for growth was 42-58°C, with an optimum at 50°C. Fastest growth was observed at a salinity below 100 mM NaCl, no growth occurred above 300mM NaCl. The optimal pH for growth was 6.5; growth was observed from pH 5 to 7.5. The G+C content of its genomic DNA was 37.6 mol %. Analysis of the 16S rRNA gene sequence and the partial methyl-CoM reductase gene sequence revealed that the organism was phylogenetically closely related to *Methanomethylovorans hollandica* DMS1<sup>T</sup> (98% similarity for 16S rRNA gene and 91% similarity for methyl-CoM reductase gene). The DNA-DNA homology between L2FAW<sup>T</sup> and *M. hollandica* DMS1<sup>T</sup> was 46%. Based on these results, the novel species *Methanomethylovorans thermophila* strain L2FAW<sup>T</sup> is proposed (DSM 17232=ATCC BAA-1173). Genbank accession numbers for the 16S rRNA gene and mcrA gene sequences of *M. thermophila* L2FAW<sup>T</sup> are AY672821 and AY672820, respectively.

**Key words:** *Methanomethylovorans thermophila* sp. nov., methanogen, methylotrophic, thermophilic, methanol.



## Main text

The utilization of methylated substrates among methanogenic archaea is almost exclusively restricted to the family of *Methanosarcinaceae*. The only exceptions are members of the genus *Methanosphaera* that can only convert methanol in the presence of H<sub>2</sub>. The family of *Methanosarcinaceae* comprises eight genera: *Methanococcoides*, *Methanohalobium*, *Methanohalophilus*, *Methanolobus*, *Methanomethylovorans*, *Methanimicrococcus*, *Methanosalsum*, and *Methanosarcina*. The genus *Methanosarcina* includes the most versatile species among all methanogens capable of using H<sub>2</sub>/CO<sub>2</sub>, acetate, and methylated compounds (methanol, methylated amines and in some cases methylated sulfides) (Boone *et al.*, 1993). The only member of *Methanimicrococcus*, *M. blatticola* (formerly *Methanomicrooccus blatticola*), resembles the *Methanosphaera* species in that it can only utilize methanol (or methylated amines) by complete reduction in the presence of H<sub>2</sub> (Sprenger *et al.*, 2000). The members of the other six genera are all obligate methylotrophs, utilizing methanol, methylated amines and in some cases methylated sulfides. All species from the genus *Methanomethylovorans* are typical freshwater isolates (indicated by their low salt tolerance), whereas the other obligate methylotrophs are generally regarded as halophiles (Garcia *et al.*, 2000).

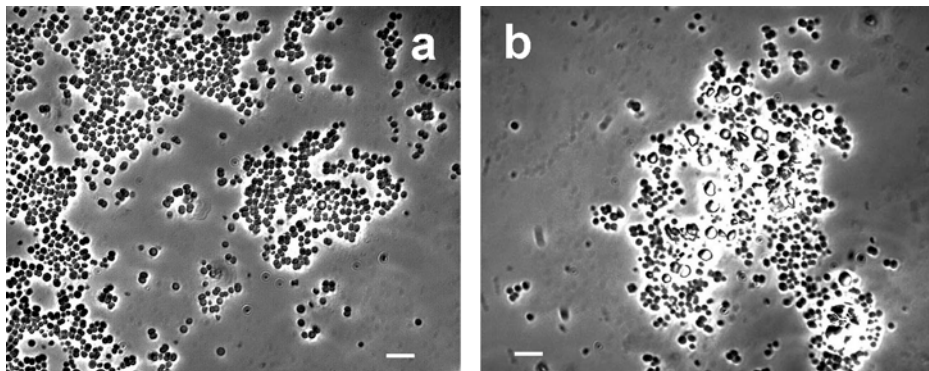
The genus of *Methanomethylovorans* was recently described in 1999, representing a group of freshwater species that can utilise methanol, methylated amines, dimethyl sulfide (DMS) and methanethiol (MT) for methanogenesis (Lomans *et al.*, 1999). *Methanomethylovorans hollandica* DMS1<sup>T</sup> was isolated from a eutrophic freshwater pond sediment in the Netherlands (Lomans *et al.*, 1999). It is the only validated species in the *Methanomethylovorans* genus. *Methanomethylovorans* sp. strain ZB was isolated from Baldegger Lake in Switzerland (Simankova *et al.*, 2003), where the temperature is only 5-6°C throughout the year. The third species, *Methanomethylovorans victoria* was isolated from the sediment of the eutrophic Lake Victoria in Mwanza of East Africa (Muyodi, 2000). *Methanomethylovorans* species were also detected in samples from rice field soils (Lueders *et al.*, 2001), oil contaminated groundwater (Watanabe *et al.*, 2002), freshwater sediments (Lomans *et al.*, 2001), sludge of an anaerobic baffled reactor treating industrial dye waste (Plumb *et al.*, 2001) and in a bioreactor treating dichloropropan-contaminated wastewater (Schlotelburg *et al.*, 2002). The three *Methanomethylovorans* strains described were all

enriched on either trimethylamine (TMA) or DMS and are all mesophilic (growth above 40°C was not possible). In this paper, the isolation and characterization of a novel thermophilic strain L2FAW<sup>T</sup> from thermophilic sludge of an anaerobic bioreactor are described. It is proposed that this strain represents a novel methylotrophic species, *Methanomethylovorans thermophila* sp. nov.

Strain L2FAW<sup>T</sup> was isolated from a methanol degrading enrichment culture, which was obtained from a thermophilic anaerobic reactor (Paulo *et al.*, 2002) and routinely maintained by successive transfers on methanol for about two years in our laboratory. The bicarbonate buffered mineral medium used in this study was prepared as described before (Stams *et al.*, 1993). The gas phase consisted of N<sub>2</sub>/CO<sub>2</sub> (80:20 v/v) at a pressure of 170 kPa. Substrates were added from 1 M stock solutions to give a final concentration of 25 mM, unless indicated otherwise. The enrichment culture consisted of only two morphologically distinct microorganisms; a dominant irregular cocci and some short-rods. Attempts to isolate the methanogenic cocci from this enrichment culture by different techniques (petri-dish, roll-tube, deep agar and soft agar) were not successful. The rod-shaped contaminant was not eliminated by serial dilution up to 10<sup>-8</sup>, even not after the addition of vancomycin. Modifications were made to the deep agar technique, keeping agar medium liquefied after inoculation. Visible colonies developed after two weeks of incubation at 55°C. The well-separated colonies were picked-up by hypodermic needles after cooling the agar at room temperature, and dilution series were made for further purification. The strain isolated from the highest dilution (10<sup>-8</sup>) was designated as strain L2FAW<sup>T</sup>.

The colonies of strain L2FAW<sup>T</sup> in deep liquefied agar were smooth milk-white spheres that reached a diameter of 1 mm after 2 weeks of incubation at 55°C. Cells of strain L2FAW<sup>T</sup> were non-motile irregular cocci with a diameter of 0.7 to 1.5 µm, occurring mainly single or in clusters consisting of two to four cells (Fig. 1a). Big aggregates, which are typical for *Methanosarcina* species were rarely observed. At the end of the exponential phase, cells became bigger, and eventually lysed (Fig. 1b). During active methanogenesis on methanol, the culture broth gradually turned from light yellow to greenish, which, upon exposure to air, became reddish-brown. This observation indicates that strain L2FAW<sup>T</sup> produced reduced

forms of corrinoids ([Co-II]-B<sub>12</sub>), which were oxidized to red corrinoids ([Co-III]-B<sub>12</sub>) with oxygen as observed for *Methanosarcina barkeri* (Mazumder *et al.*, 1987).



**Figure 1.** Phase contrast micrograph of strain L2FAW<sup>T</sup> grown on methanol. Bar: 10 µm. a: irregular single cocci or clusters of two or four cells in the early exponential phase; b: Larger cells eventually lysed at the end of the exponential phase.

Cells of L2FAW<sup>T</sup> stained Gram-negative. They lysed immediately upon the addition of SDS at a concentration of 0.1% (w/v) or Triton X-100 at a concentration of 4% (w/v), but resisted an osmotic stress in demi-water for 20 minutes, indicating that a proteinaceous cell wall was present (Boone & Whitman, 1988). Growth of strain L2FAW<sup>T</sup> was inhibited by the addition of chloramphenicol (100 µg ml<sup>-1</sup>), tetracycline (100 µg ml<sup>-1</sup>), but not by penicillin (2 mg ml<sup>-1</sup>), bacitracin (10 µg ml<sup>-1</sup>), spetinomycin (100 µg ml<sup>-1</sup>), vancomycin (100 µg ml<sup>-1</sup>) and kanamycin (100 µg ml<sup>-1</sup>).

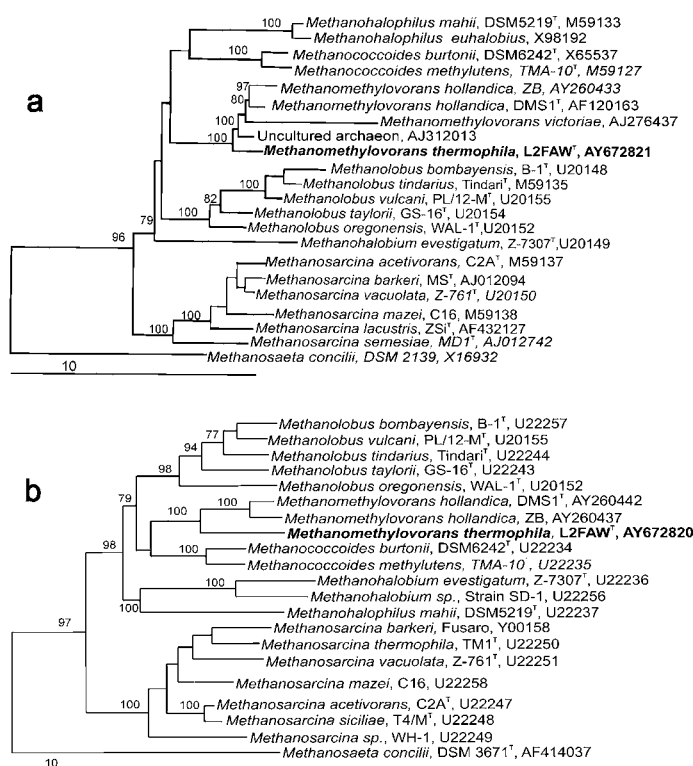
Strain L2FAW<sup>T</sup> could only use methanol, TMA, dimethylamine and methylamine for growth. H<sub>2</sub> was produced in trace amounts (80 to 160 Pa) during growth on methanol. Neither H<sub>2</sub>/CO<sub>2</sub> (headspace, 80:20, 170 kPa), CO/CO<sub>2</sub>/N<sub>2</sub> (headspace, 20:20:60, 170 kPa), formate, 2-propanol nor acetate supported growth, nor were they co-utilized together with methanol. The strain did not utilise a mixture of acetate and hydrogen. The addition of hydrogen in the headspace (170kPa) resulted in a slower growth on methanol. When transferring methanol-grown cultures into TMA-containing medium, a lag phase of about three days was observed. The lag phase became shorter with subsequent transfers on TMA. The same was observed when transferring TMA-grown culture back to methanol. An

increased lag phase was not observed when transferring the culture adapted to one methylated amine, to another methylated amine. These results confirm previous findings, that the enzymes involved in methanol and methylated amines degradation are different and have to be induced (King, 1984). DMS and MT were also tested, but no growth of strain L2FAW<sup>T</sup> was observed at the concentrations tested (2mM and 200μM for DMS and MT, respectively). These two substances also could not be co-metabolised during growth on methanol (5 mM) or TMA (5 mM).

Strain L2FAW<sup>T</sup> was isolated using mineral medium. Yeast extract or peptone (0.2%, w/v) slightly stimulated growth, but were not necessary. The temperature range for growth was from 42 to 58°C, with an optimum at 50°C. Growth was not observed at 37°C and 60°C. Growth was optimal up to a NaCl concentration of 100 mM. No growth and methane formation was observed at 300 mM NaCl or higher. Strain L2FAW<sup>T</sup> could grow at a pH from 5.0 to 7.5. The optimal pH was about 6.5. Remarkably, the growth rate of strain L2FAW<sup>T</sup> at pH 5.0 was still relatively high (55% of maximum at pH 6.5), which could be important in the resistance to acidification due to acetate formation by homoacetogens in anaerobic bioreactors (Yamaguchi *et al.*, 1989). Addition of extra cobalt stimulated growth of strain L2FAW<sup>T</sup>, the optimal concentration of cobalt in the mineral medium was between 0.5 and 2 μM. Further increase of the cobalt concentration was inhibitory. Thus, strain L2FAW<sup>T</sup> is a thermophilic, slightly acidophilic, methylotrophic freshwater methanogen. At optimal conditions, the maximal specific growth rate is 0.05 hr<sup>-1</sup>.

For the phylogenetic analysis, a bead-beating and phenol-chloroform based extraction method was used to extract DNA from strain L2FAW<sup>T</sup> (Zoetendal *et al.*, 1998). The 16S rRNA gene was amplified with a GeneAmp PCR System 2400 thermocycler (Perkin-Elmer Cetus, Norwalk, Conn.) using the primer set 7f and 1492r and *Taq* DNA polymerase (Invitrogen, Breda, The Netherlands). The amplified fragment of 16S rRNA gene was cloned into *E. coli* JM109 (Invitrogen, Breda, The Netherlands) using the pGEM-T Easy Vector System (Promega, Madison, WI). Randomly selected recombinant clones were reamplified by PCR with the vector specific primers T7 and Sp6 (Promega, Madison, WI) and sequenced using a sequencing kit (Amersham, Slough, United Kingdom) and T7 and Sp6 IRD800-labelled sequencing primers according to the manufacturer's instructions (MWG-Biotech,

Ebersberg, Germany). The DNA fragment of the methyl coenzyme M reductase (*mcrA*) gene was sequenced by the primer set of ME1 (5' – GC (AC) ATG CA (AG) AT (ACT) GG (AT) ATG TC –3') and ME2 (5' – TCA T (GT) G C (AG) T AGT T (AGT) G G (AG) T AGT- 3') as described previously (Hales *et al.*, 1996). The partial 16S rRNA gene (1363 bp) and *mcrA* gene sequence (739 bp) obtained were compared to sequences deposited in Genbank by Blast search tool (Benson *et al.*, 2004). According to the sequence similarity of the 16S rRNA gene, the closest related species of strain L2FAW<sup>T</sup> were *Methanomethylovorans hollandica* DMS1<sup>T</sup> (98%), *Methanomethylovorans* sp. strain ZB (98%), and *Methanomethylovorans victoriae* (97%). Other related methanogenic species were



**Figure 2.** Phylogenetic trees of 16S rRNA gene (a) and *mcrA* (b) gene sequences showing the relationship between strain L2FAWT and members from *Methanomethylovorans*, *Methanobrevibacter*, *Methanosarcina*, and *Methanococcoides* constructed using the neighbour-joining method (Saitou & Nei, 1987). Bootstrap values for both trees were calculated using neighbour-joining analysis after 1000 replicate data sets and re-evaluated by SeqBoot and DNAPARS implemented in Phylip package (Felsenstein, 1993). *M. concilii* is used as outgroup. The bar indicated represents 10 % sequence divergences.

*Methanolobus oregonensis* (94%), *Methanolobus taylorii* (94%), *Methanosarcina lacustris* (94%), *Methanosarcina mazei* (93%), *Methanococcoides burtonii* (93%), and *Methanohalophilus euhalobius* (93%). The similarities of *mcrA* gene sequence with *M. hollandica* and *Methanomethylovorans* sp. ZB were 91% and 90%, respectively. Deduced amino acid similarity between the two methyl-CoM reductases was 88%. The values to other species were below 82%. The 16S rRNA gene and *mcrA* gene sequences are accessible in Genbank with the accession number of AY672821 and AY672820, respectively.

The sequences from the 16S rRNA gene and *mcrA* gene of strain L2FAW<sup>T</sup> and from other related methanogens were aligned by ClustalV embedded in ARB package (Strunk & Ludwig, 2000). Phylogenetic trees (Fig. 2) were constructed using the neighbour-joining method (Saitou & Nei, 1987). Bootstrap values for the trees with the 16S rRNA gene and *mcrA* gene sequences were calculated using neighbour-joining analysis after 1000 replicate data sets and re-evaluated by SeqBoot and DNAPARS implemented in Phylip package (Felsenstein, 1993). The whole genomic DNA of strain L2FAW<sup>T</sup> was isolated by the method of Marmur (Marmur, 1961). The mol% G+C content of genomic DNA of strain L2FAW<sup>T</sup> was 37.6, determined by thermal denaturation using a Pye Unicam SP 1800 spectrophotometer as described by Owen (Owen *et al.*, 1969). DNA-DNA homology between *M. hollandica* DMS1<sup>T</sup> and strain L2FAW<sup>T</sup> was 46%, determined by using the reassociation method described by De Ley (De Ley *et al.*, 1970).

The 16S rRNA gene and *mcrA* gene sequence analysis revealed that strain L2FAW<sup>T</sup> clustered in *Methanomethylovorans* genus with highest similarity to the only validated species in this genus, *M. hollandica* DMS1<sup>T</sup> (DSM15976). Similar to *M. hollandica* DMS1<sup>T</sup>, strain L2FAW<sup>T</sup> is also a freshwater species, which is a major characteristic of members of the *Methanomethylovorans* genus as compared to the other closest genera, *Methanolobus*, *Methanococcoides*, *Methanohalobium* and *Methanohalophilus* (Lomans *et al.*, 1999). Strain L2FAW<sup>T</sup> differs from *M. hollandica* DMS1<sup>T</sup> and other isolated *Methanomethylovorans* strains by its cell wall composition, cell morphology, substrate spectrum, optimal temperature and its G+C content of genomic DNA (Table 1).

Besides methanol and methylated amines, *M. hollandica* DMS1<sup>T</sup> and *Methanomethylovorans* sp. ZB can also utilise DMS and MT for growth (Lomans *et al.*, 1999; Simankova *et al.*, 2003). Utilization of MT and DMS was not reported for *M. victoria*. Strain L2FAW<sup>T</sup>, however, cannot grow on DMS and MT nor co-utilise them together with methanol or TMA (Table 1). It is unlikely that strain L2FAW<sup>T</sup> lost its ability to degrade DMS and MT due to long term cultivation on methanol, since no methane was produced from the original enrichment culture and from the seed sludge of the UASB reactor when DMS or MT were tested as substrates (results not shown). The inability to use DMS and MT at lower concentrations (200 µM), and even when other reducing agents, such as cysteine or titanium citrate, or when complex medium (addition of yeast extract and peptone, supplement with extra iron and cobalt) were used, indicated that the inability to use DMS or MT is not due to the toxicity of DMS, MT and sulphide on the growth of strain L2FAW<sup>T</sup> on DMS and MT or lack of essential nutrients.

The results of bootstrap analysis showed a clear branching of strain L2FAW<sup>T</sup> from other *Methanomethylovorans* species and *Methanosarcina* genus. DNA matrix distance analysis of 16S rRNA gene showed the average distance of strain L2FAW<sup>T</sup> to all members of genera *Methanolobus*, *Methanococcoides*, *Methanohalobium* were  $0.066 \pm 0.006$ ,  $0.073 \pm 0.006$  and  $0.084 \pm 0.001$ , respectively. This value for strain L2FAW<sup>T</sup> to the members of *Methanomethylovorans* was  $0.022 \pm 0.001$ . Springer *et al* (1995) suggested that, based on phylogenetic analysis of 16S rRNA gene and the *mcrA* gene sequences from the family of *Methanosarcinaceae*, distance values lower than  $0.0214 \pm 0.0065$  indicated intergeneric relationship whereas values higher than  $0.0907 \pm 0.0096$  represented different genera within this family. Thus, it is clear that strain L2FAW<sup>T</sup> is a novel species of the *Methanomethylovorans* genus. We propose *Methanomethylovorans thermophila* for this novel species, and strain L2FAW<sup>T</sup> as the type strain.

Only a few thermophiles are described in the family of *Methanosarcinaceae*. Two thermophilic obligated methylotrophs, *Methanohalobium evestigatum* (Zhilina & Zavarzin, 1987) and *Methanosalsum zhilinae* (Mathrani *et al.*, 1988), which is the only species in corresponding genus, are halophiles. The first thermophilic species described in this family, *Methanosarcina thermophila* (Zinder & Mah, 1979) that can utilize methanol, acetate and

H<sub>2</sub>/CO<sub>2</sub>, is affiliated with other mesophilic species in the genus *Methanosarcina*. Two other thermophilic strains of *Methanosarcina* have been described, which can utilize acetate and methanol but not H<sub>2</sub>/CO<sub>2</sub> (Ollivier *et al.*, 1984; Touzel *et al.*, 1985). *Methanomethylovorans thermophila* strain L2FAW<sup>T</sup> described here, is a thermophilic, obligated methylotrophic, freshwater species affiliated with other mesophilic species in the genus *Methanomethylovorans*.

**Table 1.** Characteristics of *Methanomethylovorans* strains and *Methanococcoides burtonii*

<b>Characteristics</b>	<b>Strain L2FAW<sup>T∞</sup></b>	<b><i>M. hollandica</i> DMS1<sup>T*</sup></b>	<b><i>M. hollandica</i> Strain ZB<sup>†</sup></b>	<b><i>M.</i> victoria<sup>‡</sup></b>	<b><i>M. burtonii</i><sup>§</sup> DSM6242<sup>T</sup></b>
<b>Habitat</b>	UASB reactor	eutrophic lake	cold lake	eutrophic lake	cold lake
<b>Cell size (µm)</b>	0.7-1.5	1-1.5	1.0-1.7	0.5-1.2	0.8-1.8
<b>Cell shape</b>	single	aggregates	Clusters (2-4)	Clusters (2-4)	Single/Clusters (up to 4)
<b>SDS sensitivity (w/v)</b>	lysed at 0.1%	not lysed at 1%	n.d.	not lysed at 1%	lysed at 0.1%
<b>Temp. range (opt.T)</b>	42-58°C (50°C)	12-40°C (37°C)	1-38°C	n.r.	6-30 (23.4°C)
<b>NaCl range (mM)</b>	0 to 200	0-300	n.r.	n.r.	200-600
<b>Opt. pH</b>	6.5	6.5-7.0	n.r.	n.r.	7.7
<b>G+C %</b>	37.6	34.4 <sup>∞</sup>	n.r.	n.r.	39.6
<b>Methanol</b>	+	+	+	n.r.	+
<b>Methylated amines</b>	+	+	+	+	+
<b>Dimethyl sulfide</b>	-	+	+	n.r.	-
<b>Methanethiol</b>	-	+	+	n.r.	-

<sup>∞</sup>: this study; <sup>\*</sup>: Lomans *et al.*, 1999; <sup>†</sup>: Simankova *et al.*, 2003; <sup>‡</sup>: Muyodi, 2000; <sup>§</sup>: Franzmann *et al.*, 1992. + or – indicates that the growth is positive or negative on this substrate; n.r.: not reported.



### **Description of *Methanomethylovorans thermophila* sp. nov.**

*Methanomethylovorans thermophila* (Me.tha.no.me.thy.lo'vo.rans. M. L. n. *methanum*, methane; M. L. n. *methylum*, methyl; L. adj. *vorans*, devouring; M. L. n. *Methanomethylovorans*, methane producing, methyl group consuming; L. adj. *thermophila*, ther.mo.phi'la. Gr. adj. *thermos* hot; Gr. adj. *philos* loving; N.L. fem. adj. *thermophila* heat-loving). Cells are irregular, non-motile and coccoid with a diameter of 0.7 to 1.5 µm. Cells occur single or sometimes in clusters of two or four cells. Cells lyse in 0.1% (w/v) SDS. Cells stain Gram negative. Temperature range for growth is from 42 to 58°C with the optimum at 50°C. The strain is slightly acidophilic (pH range 5 to 7.5 with optimum at pH 6.5) and has a low salt tolerance (lower than 0.3 M NaCl). Methanol and methylated amines are the only catabolic and methanogenic substrates. Type strain L2FAW<sup>T</sup> (DSM 17232=ATCC BAA-1173) was isolated from UASB bioreactor treating paper mill wastewater.

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# *Chapter 3*

## **Novel one-carbon metabolism of *Moorella hydrogenoformans* sp. nov., isolated from a methanogenic bioreactor**

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## Summary

A thermophilic spore-forming bacterium, strain AMP, was isolated from a thermophilic methanogenic bioreactor that was fed with methanol as sole substrate. Strain AMP was affiliated with the *Moorella* genus based on 16S rDNA sequence analysis, but it had a unique one-carbon metabolism compared with other *Moorella* species and other homoacetogenic species. In pure culture it grew homoacetogenically on methanol, but not on formate and H<sub>2</sub>/CO<sub>2</sub>. Hydrogenase and formate dehydrogenase activities were detected, but cytochrome *b* was not present in cell-free extracts of strain AMP. This might be the reason for the inability to grow on formate and H<sub>2</sub>/CO<sub>2</sub>. Growth on formate, but not on H<sub>2</sub>/CO<sub>2</sub> was obtained in the presence of thiosulfate as electron acceptor. Unlike other *Moorella* species, strain AMP grew hydrogenogenically on CO, indicating the presence of an energy-conserving hydrogenase. The G+C content of genomic DNA is 57.3 mol%. The DNA-DNA homology showed 75.2±4.7% similarity to *Moorella thermoacetica* DSM 521<sup>T</sup>. We propose that strain AMP represents a novel species within the *Moorella* genus. *Moorella hydrogenoformans* was assigned to this novel species with strain AMP<sup>T</sup> as its type strain. Genbank accession number of 16S rDNA gene sequence of *M. hydrogenoformans* AMP<sup>T</sup>: AY884087.

## Introduction

Around 100 species of homoacetogenic bacteria divided over 21 genera in the *Bacillus-Clostridium* subphylum have been described (6, 9). Homoacetogens have the ability to form acetate through the reductive acetyl-CoA pathway. In this pathway CO<sub>2</sub> acts as a sink for reducing equivalents generated in the oxidation of carbohydrates, organic acids, C1 compounds or hydrogen (9). ATP is conserved in this pathway by substrate level phosphorylation in the last step, but ATP has to be invested to activation of formate (formed from CO<sub>2</sub>) to formyl-tetrahydrofolate (21). Additional ATP is formed via chemiosmotic processes that involve proton or sodium translocation across the cytoplasmic membrane. Hydrogenase (H<sub>2</sub>ase), the bifunctional carbon monoxide dehydrogenase and acetyl-CoA synthase complex (CODH/ACS), formate dehydrogenase (FDH) and corrinoid-containing methyltransferase are key enzymes in the metabolism of homoacetogens.

*Moorella* is a genus of Gram-positive, sporeforming homoacetogens. This genus consists of four validated species and several undescribed strains. Most *Moorella* species grow on diverse sugars, organic acids, C1 compounds and H<sub>2</sub>/CO<sub>2</sub>. However, *M. glycerini* is not able to grow on methanol, formate and H<sub>2</sub>/CO<sub>2</sub> (34). In this report, we describe a novel *Moorella* species. This bacterium grows homoacetogenically on methanol, but is not able to grow homoacetogenically on H<sub>2</sub>/CO<sub>2</sub>, CO or formate. Remarkably, the bacterium is able to grow hydrogenogenically on CO, a property of facultative anaerobic phototrophs (3, 7, 46), some strictly anaerobic thermophilic anaerobes (36, 38, 39, 42, 43) and an archaeon (37). The novel strain is able to grow on formate, but not on H<sub>2</sub>/CO<sub>2</sub>, with thiosulfate as electron acceptor. To emphasize the novel physiological features the strain is described as a novel species within the genus *Moorella*, *Moorella hydrogenoformans*.

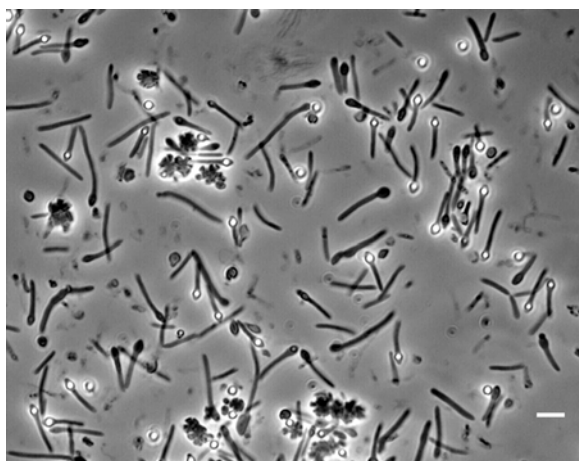
## Material and Methods

### *Source of microorganisms*

Strain AMP, described here, was isolated from a methanol-degrading enrichment culture (27). Strain NJ1, resembled to *Methanothermobacter thermoautotrophicus*  $\Delta H$ , was isolated from the above mentioned enrichment culture with  $H_2/CO_2$  (reported also in this report). *Moorella thermoacetica* DSM 521 was obtained from the Deutsche Sammlung für Mikroorganismen und Zellkulturen (DSMZ, Braunschweig).

### *Media and growth conditions*

A bicarbonate buffered mineral medium was prepared as described previously (40). Vitamin  $B_{12}$  and when indicated,  $CoCl_2$  were omitted from this medium. Routine cultivation was carried out in 127-ml serum bottles with 50 ml medium and a  $N_2/CO_2$  (80:20) gas phase at a pressure of 170 kPa.  $CO$  or  $H_2$  replaced  $N_2$  when used as substrates. Methanol (40 mM) was used as sole carbon and energy source for enrichment and isolation. Substrates and electron acceptors were added from neutralized sterile stock solutions to a final concentration of 10 mM or an otherwise indicated concentration. For solid media, agar (Difco) was added (8 g/L) to the liquid medium. Yeast extract and peptone (Difco) were amended at concentrations of 0.2 g/L when indicated. Temperature of incubation for enrichment and isolation was 55°C. Other cultivation experiments were performed at 65°C. Strain NJ1 was routinely cultivated in the same medium using  $H_2/CO_2$  as substrate. Coculture experiments were performed by inoculating cultures of strain NJ1 and strain AMP at an inoculum size of 5% each.



**Fig. 1.** Phase contrast microscopic picture of strain AMP grown on methanol, showing vegetative cells, sporulating cells and mature spores. Bar indicates 5  $\mu m$ .



### *Isolation procedure*

By using cobalt-deficient media, a methanol-degrading enrichment culture was obtained that consisted of spore-forming bacteria and rod-shaped methanogens (27). The spore-forming bacterium was isolated by repeated serial dilutions in liquid methanol-containing media (with addition of  $\text{CoCl}_2$ ) using an autoclaved ( $121^\circ\text{C}$  for 1 h.) culture as inoculum. The highest dilution with growth was diluted in soft agar (Difco, 8 g/L). Well-separated colonies were picked up and used as inoculum for serial dilutions in liquid medium with bromoethanesulfonate (Bres, 10 mM) and penicillin G (2mg/ml). The pure culture that was obtained in the highest dilution was designated strain AMP. Purity of the isolate was confirmed by phase contrast microscopy and by incubations in anaerobic Wilkens-Chalgren broth (Oxoid, Basingstoke, UK) amended with thiosulfate and pyruvate.

### *Physiological characterization*

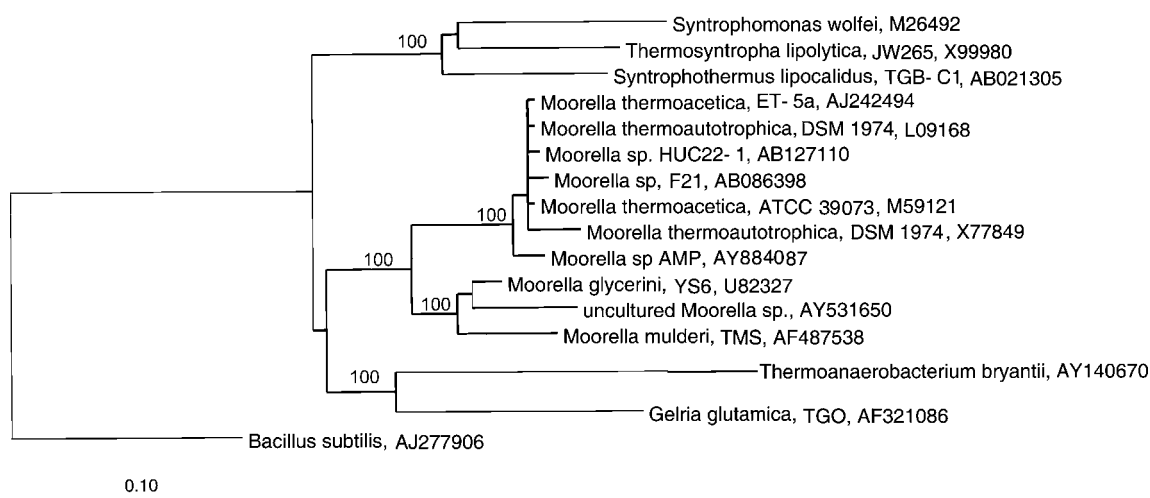
Electron donor and electron acceptor utilization by strain AMP was tested in the described mineral medium (with  $\text{CoCl}_2$ ) or undefined DSM medium 60 ([www.dsmz.de](http://www.dsmz.de)) amended with single and mixed substrates as described in the text. Growth on a substrate was confirmed by substrate consumption, product formation, increase of culture turbidity and subsequent transfers in fresh media.

Optimal growth conditions were tested in bicarbonate buffered media with methanol (40 mM) as substrate. pH values from 5.0 to 9.0 were obtained by the addition of a calculated amount of 1M HCl or 1M NaOH. Cultures were incubated at a temperature range from  $37^\circ\text{C}$  to  $75^\circ\text{C}$ . To test optimal salt concentrations, NaCl was added to the final concentration of 10 mM to 500 mM. Gram staining was made according to a standard method (13).

### *Phylogenetic analysis*

DNA of strain AMP was extracted as described previously (51). 16S rDNA was amplified using the 7f and 1492r primer set (Invitrogen, Breda, The Netherlands). The pGEM-T Easy vector system was used to clone amplified 16S rDNA fragments into *E. coli* strain JM109 (Promega, Madison, WI). Randomly selected recombinant clones were reamplified by PCR with the vector specific primers T7 and Sp6 (Promega, Madison, WI). Reamplified 16S rDNA fragments were sequenced according to the manufacturer's

instructions (Amersham, Slough, United Kingdom) with IRD800-labelled sequencing primer sets Sp6 and T7 (Promega, Madison, WI), 533f and 1100r (20).



**Fig. 2.** Phylogenetic tree based on 16S rDNA sequence analysis showing the position of strain AMP within the *Moorella* genus and relationship to selected bacteria using neighbour-joining method (30) embedded in ARB package (41). The bar represents 10 % sequence divergences.

Obtained 16S rDNA sequences (1528 bp) were compared to sequences deposited in the NCBI database (2). 16S rDNA sequences were aligned using ARB software package (41). Phylogenetic trees based on 16S rDNA sequences were constructed using the neighbor-joining method (30). Bootstrap values were calculated using neighbour-joining analysis of 1000 replicate data sets by SeqBoot and subsequent re-evaluation by DNAPARS, both implemented in the Phylip software package (10).

The G+C content of genomic DNA was determined at the identification service of the DSMZ (Braunschweig, Germany). The DNA was isolated according to Visuvanathan et al. (47) and purified as described by Cashion et al. (5). The G+C content was determined by HPLC analysis (24, 44). DNA homology was determined using the reassociation method described by De Ley et al. (8).

### Enzyme assays

Cells of strain AMP were cultivated on either methanol or methanol plus CO. Cells were harvested in the late logarithmic phase by centrifugation and cell free extracts were

prepared under anoxic conditions by osmotic shock and sonication using lysozyme as described previously (22). Soluble fractions and membrane fractions were obtained by ultracentrifugation of cell free extracts (15). Carbon monoxide dehydrogenase (CODH), formate dehydrogenase (FDH) and hydrogenase ( $H_2$ ase) activities were assayed in 50 mM Tris-HCl (pH 8.5) containing benzylviologen (BV, 5 mM) and dithiothreitol (DTT, 1 mM) at 55°C in a U2010 spectrophotometer (Hitachi, Japan) as previously described (15).  $H_2$ -evolution activity (MV- $H_2$ ) was assayed in 50 mM MOPS/KOH buffer at pH 7.0 and 2mM DTT with reduced methyl viologen (MV, 2 mM) according to Soboh et al. (35).

### *Analytical methods*

Organic acids were measured by HPLC (40). Gases and alcohols were measured by gas chromatography (1, 14), and nitrate, thiosulfate, sulfate were analysed by a HPLC system equipped with an Ionpac AS9-SC column and ED 40 electrochemical detector (Dionex, Sunnyvale, Calif.) (32). Cell dry weights were analysed as previously described (31). Sulfide was analysed by the method of Trüper and Schlegel (45). To detect the cytochrome *b*,  $O_2$ -oxidized membrane fractions were reduced by sodium dithionite, and the reduced-minus-oxidized spectra were recorded with a dual-beam spectrophotometer (Hitachi U2010, Japan) as described by Fröstl et al. (12). Protein was determined according to the Bradford method with bovine serum albumin as a standard (4).

## **Results**

### *Enrichment and isolation*

In previous work we studied the effect of cobalt on methanol conversion in a laboratory scale anaerobic bioreactor operated at 55°C (27, 28). We obtained methanol-degrading enrichment cultures with and without  $CoCl_2$  as cobalt source in the medium. Typically, a sarcina-type of methanogen was enriched in cobalt containing media, which can utilize methanol directly for methanogenesis. This methanogen was described recently (16). However, enrichment in the absence of cobalt resulted in a coculture consisting of rod-shaped microorganisms, some of which showed autofluorescence and others that formed spores. That

coculture formed methane as end product from methanol. To obtain the microorganisms in pure culture we continued cultivation of the enrichment culture in cobalt-amended media ( $\text{CoCl}_2$ , 0.5  $\mu\text{M}$ ). This resulted in faster growth and a dominance of the spore-forming, rod-shaped microorganism. In that culture, acetate was the main product of methanol utilization instead of methane (27). The spore-forming bacterium, strain AMP, was isolated after repeated dilutions series in liquid media and one dilution series in deep agar. From the same medium, a methanogenic strain was also isolated with  $\text{H}_2/\text{CO}_2$  as substrate, which designated NJ1.

#### *Morphology and optimal growth conditions*

Strain AMP is a rod shaped, Gram-positive, spore-forming bacterium. Cells of strain AMP grown on methanol were 0.4 to 1.2  $\mu\text{m}$  wide, and 5 to 14  $\mu\text{m}$  long. In old cultures, round swollen terminal endospores were observed. Exponentially growing cells were generally longer than sporulating cells (Fig. 1). Cells were shorter and spores were hardly observed when grown on pyruvate or lactate.

Strain AMP grew at a temperature range of 42°C to 75°C with optimal growth between 60°C and 65°C. Growth was observed in a pH range of 5.0 to 8.5 with fastest growth at pH 6.9. Growth rates remained unchanged when NaCl concentrations were below 150 mM. Lower growth rates were observed with NaCl concentrations above 200 mM, while no growth occurred at a NaCl concentration of 400 mM or higher.

#### *Phylogeny of strain AMP*

The 16S rDNA gene sequence of strain AMP (1528bp) was sequenced and is accessible under Genbank accession number AY884087. Based on 16S rDNA sequence analysis strain AMP is closely related to *Moorella thermoacetica* strains HUC22-1 (98.7%), ET-5a (98.4%), DSM 521<sup>T</sup> (98.3%) and F21 (97.8%), as well as to *Moorella thermoautotrophica* strain DSM1794 (98.2%). Strain AMP was distantly related to other *Moorella* species; *M. glycerini* (94.5%) and *M. mulderi* (91.5%). Neighbor-joining tree based on 16S rDNA sequences indicated that strain AMP fell into the cluster of the genus *Moorella* (Fig. 2). The G-C content of genomic DNA was 57.3 mol%. The DNA-DNA hybridisation showed 75.2±4.7% (duplicate measurements) similarity to *M. thermoacetica* DSM 521<sup>T</sup>.

**Table 1.** Main characteristics of strain AMP related to other *Moorella* species<sup>a</sup>.

	Strain AMP	<i>M.</i> <i>mulderi</i>	<i>M.</i> <i>glycerini</i>	<i>M. thermo-</i> <i>autotrophica</i>	<i>M.</i> <i>thermoactica</i>
<b>Opt. Temp (°C)</b>	65	65	58	55-58	55-60
<b>Opt. pH</b>	6.9	7.0	6.3	5.7	6.9
<b>G-C% (mol%)</b>	57.3	53.6	54.5	53-55	53-55
<b>Similarity of 16S rDNA, %)</b>	100	91.5	94.5	98.2	98.3
<b>Electron donor</b>					
<b>Glucose</b>	-	+	+	+	+
<b>Fructose</b>	±	+	+	+	+
<b>Pyruvate</b>	+	+	+	+	+
<b>Lactate</b>	+	+	+	+	+
<b>Glycerol</b>	-	-	+	-	-
<b>Methanol</b>	+	+	-	+	+
<b>Formate</b>	±	+	-	+	+
<b>H<sub>2</sub>/CO<sub>2</sub></b>	-	+	-	+	+
<b>CO/CO<sub>2</sub></b>	+(to H <sub>2</sub> )	na <sup>c</sup>	na <sup>c</sup>	+(to acetate)	+(to acetate)
<b>Electron acceptor</b>					
<b>Nitrate</b>	-	-	-	+	+
<b>S<sub>2</sub>O<sub>3</sub><sup>2-</sup></b>	+	+	+	+	+
<b>Fumarate</b>	-	-	+	-	-

<sup>a</sup> Characteristics of other *Moorella* species were obtained from (1) and from (11), (49) and (34).<sup>b</sup> +, - or ± indicates that growth is positive, negative or weak.<sup>c</sup> not analysed

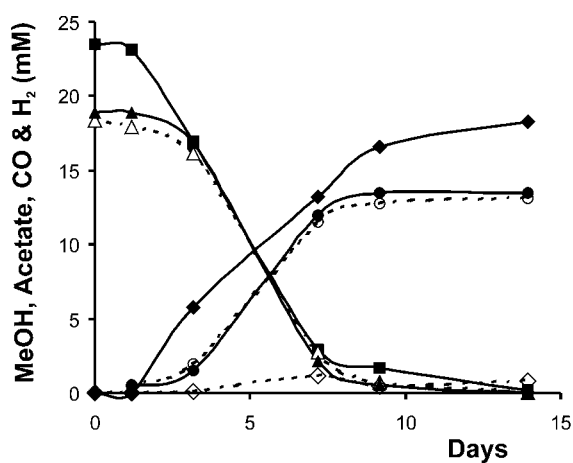
### Substrate utilization

Strain AMP has a different substrate profile than *M. thermoacetica* and *M. thermoautotrophica* (Table 1). It grew on pyruvate, lactate, mannose, methanol (40 mM), vanillate (5 mM), vanillin (5 mM), and CO/CO<sub>2</sub> (headspace, 80:20, 170 kPa). Acetate was the major end product after growth of strain AMP on the mentioned substrates (except on CO/CO<sub>2</sub>) with little amount of H<sub>2</sub> and formate formation (Table 2 and data not shown). We did not analyze the formation of aromatic compounds from vanillate and vanillin. The following substrates were tested, but not utilized by strain AMP: H<sub>2</sub>/CO<sub>2</sub> (headspace, 80:20,

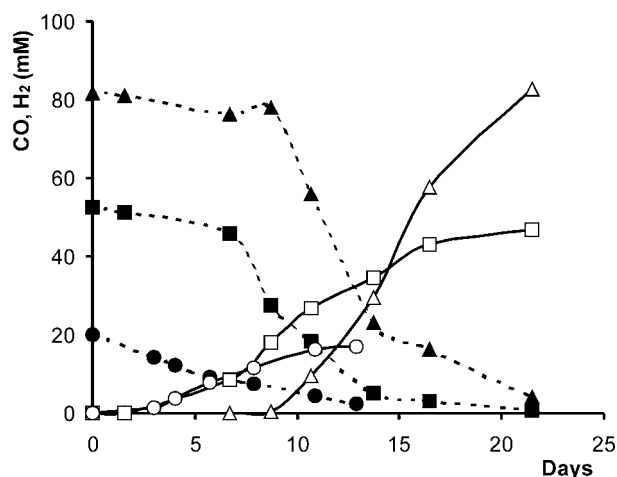
170kPa), acetate, ethanol, n-propanol, glycerol, glucose (5 mM), melibiose (5 mM), raffinose (2 mM), rhamnose (2 mM), trehalose (5 mM), arabinose, cellobiose, cellulose, galactose, lactose, maltose, xylose, mannitol, melezitose, ribose (5 mM), sorbitol, starch (0.5 g/L), sucrose, benzoate. Similar to other *Moorella* species, thiosulfate was used as electron acceptor by strain AMP. This resulted in the formation of sulfide as major product. Remarkably, formate and fructose only provided measurable growth in the presence of thiosulfate. When methanol or lactate was used as electron donors, nitrate, sulfate, and fumarate were not reduced by strain AMP.

### Methanol metabolism of strain AMP

Methanol was readily utilized as energy and carbon source by strain AMP (Fig. 3). The ratio of acetate formed to methanol consumed was 0.74. In the presence of CO or formate, this ratio increased to 1.09 and 1.02, respectively (Table 2). The consumption of 40 mM methanol by strain AMP took 6 days when cobalt was present at a concentration of 0.5  $\mu\text{M}$ ; it took more than 16 days to convert the same amount of methanol to acetate when cobalt was not added (Table 3). In that case the residual cobalt concentration was about 0.025  $\mu\text{M}$ . In the presence of *Methanothermobacter* strain NJ1, more methane and less acetate was formed when cobalt was not added (Table 3). The 16S rDNA of strain NJ1 was 99.5% similar to *M. thermoautotrophicus* strain  $\Delta\text{H}$ . Strain NJ1 was not able to grow on methanol, formate or acetate (results not shown). The constructed coculture converted methanol four times faster in the presence of cobalt compared that in the absence of cobalt.



**Fig. 3.** Conversion of methanol (20 mM) and CO (34 kPa) by strain AMP. Methanol; dashed lines and open symbols. Methanol and CO; solid lines and closed symbols. Symbols: acetate:  $\circ$ ,  $\bullet$ ; methanol:  $\Delta$ ,  $\blacktriangle$ ; CO:  $\square$ ,  $\blacksquare$ ;



**Fig. 4.** Conversion of CO (dashed lines, open symbols) by strain AMP coupled to H<sub>2</sub> formation (solid lines and closed symbols) at 20% (●, ○), 50% (■, □) and 80% (▲, △) CO.

#### *CO metabolism of strain AMP*

Acetate was not the main product when strain AMP was inoculated in a mineral medium with 34 kPa (20%) CO in the headspace. Instead, 18.5 mM H<sub>2</sub> and comparable amount of CO<sub>2</sub> were produced from 19.4 mM CO (Fig 4); acetate formation was not detectable (<0.2 mM). Conversion of CO was considerably slower than conversion of methanol (Figure 3 and 4). With CO as substrate, the optical density of the culture at 600 nm (OD<sub>600</sub>) increased from 0.025 to 0.086, which indicated that the conversion was coupled to the growth. Chemolithotrophic growth of strain AMP on CO coupled to H<sub>2</sub> evolution was confirmed by subcultivation in 6 successive transfers into fresh mineral medium with CO as sole energy and carbon source. Strain AMP grew also at CO level of 85 kPa (50%) and 136 kPa (80%) and formed H<sub>2</sub> as major product. Acetate was detected, but its concentration was always below 1 mM. Strain AMP showed a faster conversion rate at higher partial pressure of CO, but the lag phase was also longer. Strain AMP could also be subcultured at high CO concentrations, but the lag phase remained long.

As methanol results in acetate formation and CO in hydrogen formation, we investigated mixed substrate utilization by strain AMP. Fig. 3 shows methanol and CO consumption in cultures inoculated with CO adapted cells. Production of acetate and consumption of methanol in the culture with methanol and CO were similar as on methanol alone. In addition, H<sub>2</sub> was produced stoichiometrically from CO. However, if methanol-

grown cells were grown on methanol in the presence of 136 kPa CO, more acetate was formed. In this case less hydrogen was formed from CO (Table 2). CO conversion to H<sub>2</sub> also occurred when cells of strain AMP grew on pyruvate, lactate or formate, and when thiosulfate was present as electron acceptor (Table 2). Higher ratios of acetate produced to substrate consumed were measured when pyruvate or lactate was the substrate together with CO (data not shown and Table 2). Growth rates on methanol or pyruvate in the presence or absence of CO were similar, while the growth rate on lactate in the presence of CO was lower (data not shown).

FDH, H<sub>2</sub>-ase, CODH and H<sub>2</sub>-evolution activities were detected in cell-free extracts prepared from cells grown on methanol or methanol/CO. FDH levels were not affected by the presence of CO, which remained around 3 U/mg protein. H<sub>2</sub>-ase levels decreased from 28 to 9 U/mg protein and CODH levels increased from 60 to 92 U/mg protein when cells grew in the presence of CO. The difference-spectrum of reduced vs. oxidized membranes obtained from cells cultivated with either methanol or methanol/CO showed no absorption peak around 430 and 560 nm, indicating that cytochrome *b* was not present in the cell membrane fraction. Similarly, we could not detect cytochrome *b* peaks in the cytoplasm fractions.

#### *Formate metabolism by strain AMP*

Fast growth and formate conversion were observed when strain AMP was inoculated into mineral medium with formate and thiosulfate as substrates (Fig. 5); 3.0 mM sulfide, 2.4 mM H<sub>2</sub> (4750 Pa) and 8.1 mM acetate were formed from 47.5 mM formate in 15 days (Fig. 5 and Table 2). Formate was not consumed when thiosulfate was replaced by sulfate, nitrate or fumarate. In the absence of thiosulfate, H<sub>2</sub> gradually built up to a partial pressure of 2000 Pa in 40 days. Removal of H<sub>2</sub> from the headspace by replacing headspace resulted again in a built up of H<sub>2</sub> back to 2000 Pa, indicating that accumulation of H<sub>2</sub> is inhibitory for the conversion of formate (data not shown).

### **Discussion**

Previously, a syntrophic methanol degrading enrichment culture was obtained by using cobalt limited mineral media (27). An obligate hydrogenotrophic methanogen, strain NJ1 and the methanol-utilizing strain AMP described here were isolated from this enrichment.



This coculture resembled the first described syntrophic methanol-degrading coculture consisting of *Moorella thermoautotrophica* strain Z-99 and *Methanobacterium thermoformicicum* strain Z-245, but this coculture was enriched at a high cobalt concentration of 540  $\mu\text{M}$  (26). In our experiments incubations in cobalt sufficient medium (0.5  $\mu\text{M}$ ) resulted in the isolation of a methylotrophic methanogen (16). The effect of cobalt on growth of strain AMP is not exactly clear. We speculate that in the presence of cobalt strain AMP like other homoacetogens employs a corrinoid-containing methyltransferase for methanol degradation. The cofactor-bound methyl group can supply methyl group for acetate synthesis via the acetyl-CoA pathway. It might be that a methanol dehydrogenase is involved in the oxidation of methanol in the absence of cobalt, resulting in the formation of formaldehyde that cannot enter the acetyl-CoA pathway but can be oxidized to  $\text{CO}_2$ . In *M. thermoautotrophica* a methanol dehydrogenase with pyrroloquinoline quinone as the prosthetic group is present (50), which is an indication that such an enzyme might also exist in strain AMP.

Strain AMP is a homoacetogen as indicated by the product profile, the existence of CODH (9) and its phylogeny. However, unlike many other homoacetogens strain AMP could not grow homoacetogenically on  $\text{H}_2/\text{CO}_2$  or formate as sole substrates. Growth of *Moorella* and *Sporomusa* species on  $\text{H}_2/\text{CO}_2$  or formate depends on  $\text{H}_2$ -ase and FDH, and a membrane electron transport chain that comprises cytochrome *b* for energy conservation (19, 21).  $\text{H}_2$ -ase and FDH activities were detected in strain AMP, but cytochrome *b* was not found. The absence of cytochrome *b* may be the reason why strain AMP cannot grow homoacetogenically on  $\text{H}_2/\text{CO}_2$  or formate. A cytochrome *b*-deficient mutant of *Sporomusa sphaeroides* BK824 (17) and *M. thermoacetica* (12) that fails to express cytochrome *b* in the presence of nitrate, were also not able to grow on these substrates as sole energy and carbon sources. However, in *Acetobacterium woodii* and *Thermoanaerobacter kivui*, energy is conserved via a sodium ion gradient, which do not require cytochrome *b* for electron transport (25). It is remarkable that strain AMP cannot grow homoacetogenically on formate, while acetate is formed when grown in the presence of thiosulfate or CO. This may reflect that an energy substrate is required to metabolize formate.

**Table 2.** The effect of thiosulfate, CO and formate on the conversion of methanol, pyruvate and lactate by strain AMP.

Methanol grown culture was used as inoculum for all the incubations.

1 <sup>st</sup> substrate consumed (mM)	2 <sup>nd</sup> substrate consumed (mM)	S <sub>2</sub> O <sub>3</sub> <sup>2-</sup> addition (mM)	Biomass mg dry weight/ mol C of 1 <sup>st</sup> substrate	Products (mM)				Recovery		Acetate/ Substrate <sup>c</sup>	
				Acetate	H <sub>2</sub> <sup>a</sup>	HS <sup>-</sup>	Formate	[H] % <sup>b</sup>	C % <sup>c</sup>		
Methanol (38.7)	-	-	2.84	27.7	0.1	n.d.	1.8	84	98	0.74	(0.75)
Methanol (39.2)	CO (108.3 <sup>a,e</sup> )	-	3.82	36.2	60.2	n.d.	0.4	93	94	1.09	(1.0)
Methanol (39.8)	-	20	4.77	17.9	0.5	3.2	n.d.	107	76	0.56	(0)
Methanol (39.4)	Formate (48.3)	n.a.	4.82	31.8	1.8	n.d.	n.a.	81	85	1.02	(1.0)
CO (116)	-	-	0.78	1.9	92.0	n.d.	2.0	97	93	0.02	(0.25)
CO (113)	-	20	1.19	0.2	62.9	0.7	3.1	81	99	0.002	(0)
Lactate (16.5)	-	n.a.	3.49	17.4	1.6	n.d.	0.3	104	99	1.23	(1.50)
Lactate (16.4)	CO (34.5)	-	2.68	20.3	14.5	n.d.	4.9	86	97	1.55	(1.67)
Lactate (16.5)	-	20	2.36	17.0	1.3	4.2	0.4	115	104	1.13	(0)
Formate (53.0)	CO (30)	-	1.69	9.9	20.4	n.d.	n.a.	89	79	0.21	(0.25)
Formate (47.4)	-	20	3.56	8.8	2.4	3.0	n.a.	85	105	0.20	(0)

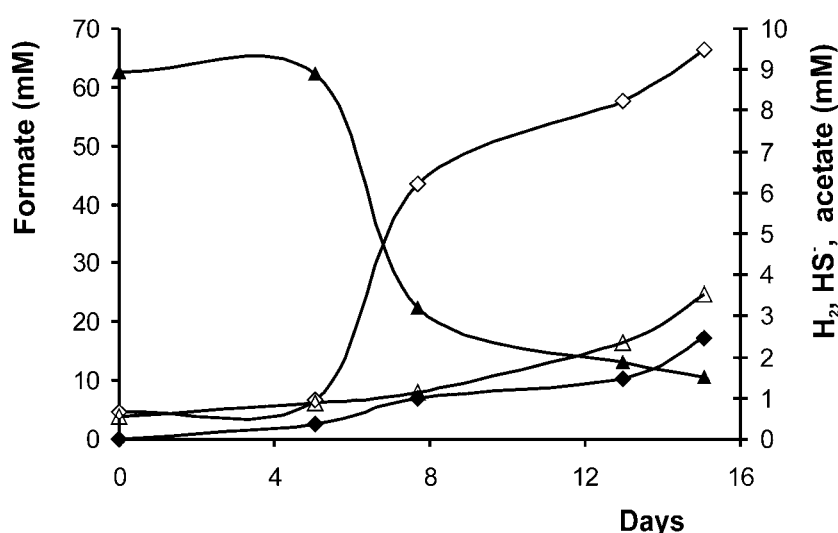
<sup>a</sup> expressed in as mM (mmol/L medium).<sup>b</sup> electrons produced were calculated using available electrons in the products and substrate based on half reactions.<sup>c</sup> CO<sub>2</sub> was estimated based on stoichiometry of the reaction.<sup>d</sup> calculated after correction of biomass formation from corresponding substrate consumed. Theoretic values are in brackets.<sup>e</sup> CO at around 110 mM and 30 mM equivalent to 136 kPa and 34 kPa, respectively.

-: no addition. n.d.: measured but not detected. n.a.: not applicable.

Strain AMP produced high amounts of H<sub>2</sub> during growth on CO, even when thiosulfate is present as electron acceptor (Fig. 5, Table 2). When CO was the sole substrate H<sub>2</sub> was formed stoichiometrically according to:  $\text{CO} + \text{H}_2\text{O} \rightarrow \text{CO}_2 + \text{H}_2$  ( $\Delta G^{\circ'} = -20$  kJ), indicating carboxydutrophic hydrogenogenic growth of strain AMP. *Carboxydotherrmus hydrogenoformans* was identified as the first strict anaerobic moderately thermophilic bacterium capable of CO oxidation and H<sub>2</sub> evolution (42). *C. hydrogenoformans* produces H<sub>2</sub> via a monofunctional CODH, an energy conserving hydrogenase (ECH) and a ferredoxin-like protein B that mediates electron transfer between CODH and ECH (33, 35). *M. thermoacetica* also produces high amount of H<sub>2</sub> in the presence of CO during growth on glucose (23). However, in this strain H<sub>2</sub> was not derived from CO oxidation, since in the absence of glucose no H<sub>2</sub> was formed from CO. It was speculated that in *M. thermoacetica* CO just acted as an inhibitor of the CODH-acetyl CoA synthetase (ACS) complex, which resulted in a shift from acetate formation to hydrogen formation (18). It was also concluded that this H<sub>2</sub> production did not result in energy conservation (9, 18). Unlike *M. thermoacetica*, strain AMP is able to couple CO oxidation and H<sub>2</sub> evolution to growth as occurs in other carboxydutrophic H<sub>2</sub>-producing anaerobes. H<sub>2</sub> was also produced when strain AMP grew on CO plus lactate, CO plus methanol and CO plus formate (Table 2), suggesting that both bifunctional CODH/ACS complexes and monofunctional CODH/ECH complexes are present in strain AMP. These complexes seem to function simultaneously or separately depending on the substrates that are provided.

The cell morphology, Gram staining, formation of spores and 16S rDNA sequence analysis revealed that strain AMP is a *Moorella* species. It is closely related to *M. thermoacetica* and *M. thermoautotrophica* with 98-99 % similarity based on 16S rDNA sequence analysis. The DNA-DNA similarity of strain AMP and *M. thermoacetica* DSM 521<sup>T</sup> is 75.2±4.7%, which is just above the threshold value of 70% for the definition of species according to the recommendation of the ad hoc committee (48). However, strain AMP differs from these two species and *M. mulderi* (1) in its inability to grow fermentatively on glucose, H<sub>2</sub>/CO<sub>2</sub>, and formate. Similar to *M. mulderi* and *M. glycerini* (34), strain AMP was unable to use nitrate as electron acceptor. In contrast to *M. glycerini*, strain AMP was unable to grow on glycerol and reduce fumarate (Table 1). Like *M. thermoacetica* and *M. thermoautotrophica* strain AMP could grow on CO, but the end product is H<sub>2</sub> rather than

acetate, which is the main end product of the other two *Moorella* species. Carboxydotrophic hydrogenogenic growth is only found in less than ten obligate anaerobic bacteria and one archaeon. Only a few are obligate carboxydotrophic (39, 43), while others can also grow heterotrophically on carbohydrates (29, 36, 38). None of them had been reported to show homoacetogenic growth. Thus, strain AMP is the first homoacetogenic bacterium capable of carboxytrrophic hydrogenogenic growth. The G + C content of strain AMP genomic DNA is 57.3 mol%, which is higher than that of the other *Moorella* species (53 to 55 mol%). Although strain AMP clustered in the genus *Moorella* (Fig. 2), it was separated from the sub-cluster of all strains of *M. thermoacetica* and *M. thermoautotrophica* and the sub-cluster of *M. glycerini* and *M. mulderi*. Based on the unique physiological properties, we proposed that strain AMP represent a novel species of the *Moorella* genus. Because of this characteristic hydrogenogenic CO metabolism, we proposed the name of *Moorella hydrogenoformans*.



**Fig. 5.** Formate conversion by strain AMP in the presence of 20 mM thiosulfate as electron acceptor. Symbols: formate: ▲; acetate: ◇; H<sub>2</sub>: ◆; HS<sup>-</sup>: △.

**Table 3.** The effect of cobalt and *M. methanoautotrophicus* strain NJ1 on methanol conversion by strain AMP.

Micro-organism(s)	Co <sup>2+</sup> addition	Methanol consumed (mM)	Days to consume	Main products (mM)		
				Acetate	CH <sub>4</sub> <sup>a</sup>	H <sub>2</sub> <sup>a</sup>
Strain AMP	+	41	5	30	-	0.9
	-	40	16	29	-	4.6
Strain AMP + Strain NJ1	+	42	7	20	6.4	<0.01
	-	42	30	2.2	28	0.4

<sup>a</sup> expressed in mmol/L medium**Description of *Moorella hydrogenoformans* sp. nov.**

*Moorella hydrogenoformans* sp. nov. (hy.dro.ge.no.fo'r.mans. M.L.n. hydrogenium hydrogen, L.adj. formans forming; M.L.adj. hydrogenoformans hydrogen-forming). Cells are gram-positive, long-rods, 0.4-1.2 × 5-14 µm, occurring in single. Forms swollen end spores. Strict anaerobic and thermophilic. Grows fastest at temperature between 60 to 65°C, pH 6.9 and salt concentration below 200 mM with ranges of 42-75°C, pH 5.0 to 8.5 and below 400 mM. Utilizes methanol, pyruvate, lactate, mannose, vanillate and vanillin, forming acetate as the main reduced end product. Grows weakly on fructose. Reduces thiosulfate, but not nitrate, sulfate or fumarate. Does not grow (in the absence of thiosulfate) on H<sub>2</sub>/CO<sub>2</sub>, formate, glucose, acetate, ethanol, n-propanol, glycerol, melibiose, raffinose, rhamnose, trehalose, arabinose, cellobiose, cellulose, galactose, lactose, maltose, xylose, mannitol, melezitose, ribose, sorbitol, starch, sucrose and benzoate. Grows hydrogenogenically on 100% CO. G + C content of genomic DNA is 57.3 mol%. Strain AMP<sup>T</sup> as its type strain. Genbank accession number for the 16S rDNA gene sequence of *M. hydrogenoformans* AMP<sup>T</sup> is AY884087.

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# *Chapter 4*

## **Syntrophic growth on formate of a coculture of *Moorella hydrogenoformans* and *Methanothermobacter* sp. NJ1**

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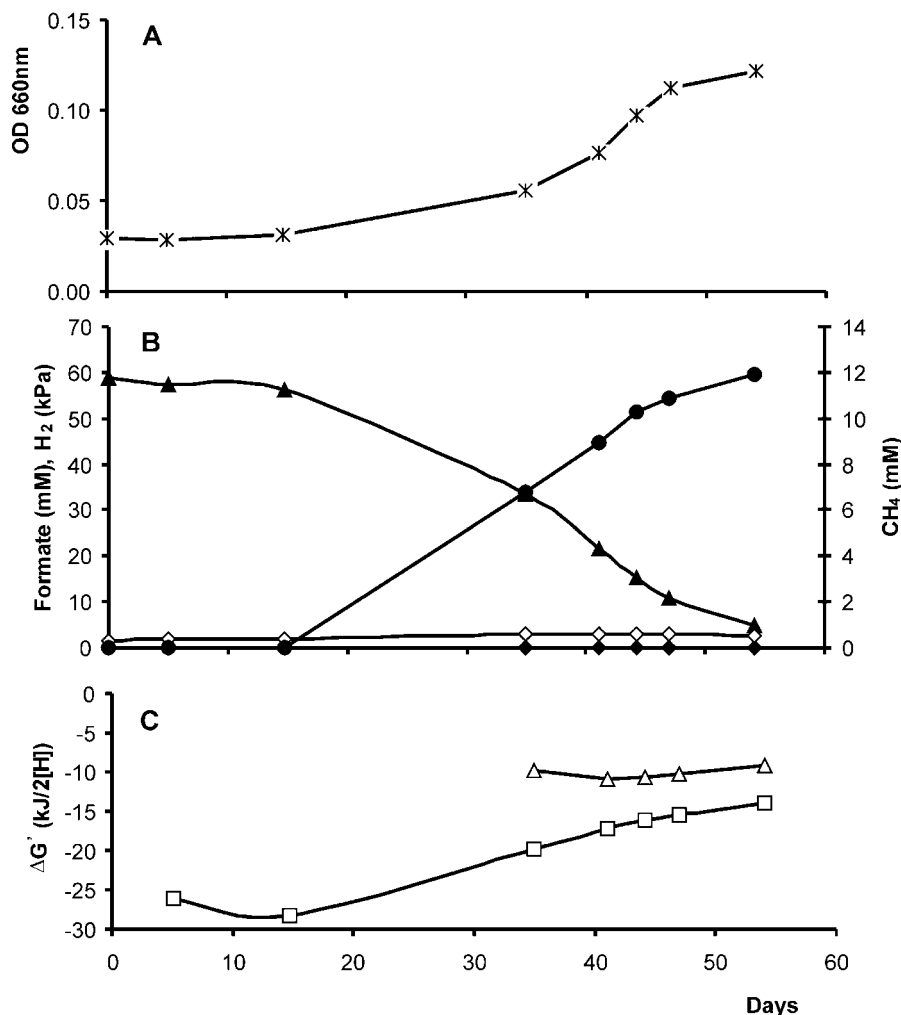
Prepared for submission

Syntrophic associations of acetogenic bacteria and methanogenic archaea operate at the limits of what is thermodynamically possible<sup>1</sup>. Key is the interspecies transfer of electrons with formate and hydrogen as substrates for the methanogens<sup>2</sup>. Contrary requirements of acetogens and methanogens for growth sustaining conditions keep the formate and hydrogen concentrations low and within a narrow range<sup>3</sup>. A niche for organisms growing on the conversion of formate to hydrogen - or vice versa - is therefore unlikely. Here we report growth on formate by a syntrophic consortium of a *Moorella* species with a hydrogen-consuming *Methanothermobacter* species. In pure culture neither *M. hydrogenoformans* nor the methanogen can grow on formate. The co-culture grows slowly with an estimated doubling time of about 17 days and reaches cell densities of  $7.5 \times 10^7$  per ml with 60 mM formate. Based on genomic data we hypothesize that the *Moorella* sp. conserves energy from the mineralization of formate via a special formate-hydrogen-lyase system encompassing an energy conserving hydrogenase. These results imply the existence of a previously unrecognized microbial guild.

The possibility that life exists on mars and other extraterrestrial bodies has triggered a search for the limits of life on earth<sup>4-6</sup>. Much attention is thereby paid to the environmental conditions that limit microbial growth and activity, such as high salt concentrations, high pressure, high and low pH, high and low temperatures, and combinations thereof<sup>6-12</sup>. Less attention is being given to the thermodynamic limits of microbial life. These limits are approached in methanogenic environments, where syntrophic associations of acetogenic bacteria and methanogenic archaea obtain energy for growth from catalyzing pathways that operate close to thermodynamic equilibrium ( $\Delta G' \sim 0$  kJ/mol.)<sup>1,2</sup>. Methanogenic ecosystems are generally schematized as four different functional groups (or guilds) of bacteria and archaea. Primary fermenters convert complex material into substrates for a second group of fermenters, also known as acetogens, which obligately depend on two groups of methanogens, one that uses hydrogen and formate, and another that uses acetate<sup>2,3</sup>. For thermodynamic reasons growth of the acetogens is sustainable only through the removal of their waste products by the methanogens. Hydrogen is the main electron carrier in such syntrophic associations, but formate is important too, especially in associations where electron fluxes are high<sup>13-15</sup>. It seems logical that formate and hydrogen are in thermodynamic equilibrium<sup>16,17</sup>, but this is not always the case. Measurements in a shallow methanogenic aquifer in Denmark have indicated a potential energy gain of 5 to 10 kJ/mol per electron for the conversion of formate to H<sub>2</sub> and bicarbonate<sup>18</sup>. This implies a previously unrecognized niche for organisms that are able to catalyze this reaction.

Cleavage of formate to H<sub>2</sub> and bicarbonate has been described by using a coculture of *Desulfovibrio vulgaris* JJ and *Methanobacterium bryantii*<sup>19</sup>, but it has never been shown that this can be coupled to growth. Here we describe for the first time that a bacterium is able to grow on the conversion of formate to H<sub>2</sub> and bicarbonate provided that hydrogen is consumed by a methanogen. The bacterium was obtained in a study on the effect of cobalt on methanol conversion in a bioreactor operated at 55°C. In the presence of cobalt a novel methanogen was enriched. In the absence of cobalt methanol consumption was sluggish. Under these conditions a methanol-degrading co-culture was enriched consisting of a *Moorella* species, strain AMP, and a *Methanothermobacter* species, strain NJ1<sup>20</sup>. Pure cultures of these two microorganisms were obtained in media to which cobalt had been added. Based on 16S rRNA sequence analysis strain AMP was closely related to *Moorella thermoacetica* and *Moorella thermoautotrophica*. However, it had the special property of growth on CO with H<sub>2</sub> rather than acetate as end product. This led us to propose a novel species, *Moorella*

*hydrogenoformans*. Strain NJ1 was a hydrogen utilizing methanogen; its 16S rRNA was 99.5% similar to *Methanothermobacter thermoautotrophicus* strain  $\Delta$ H.

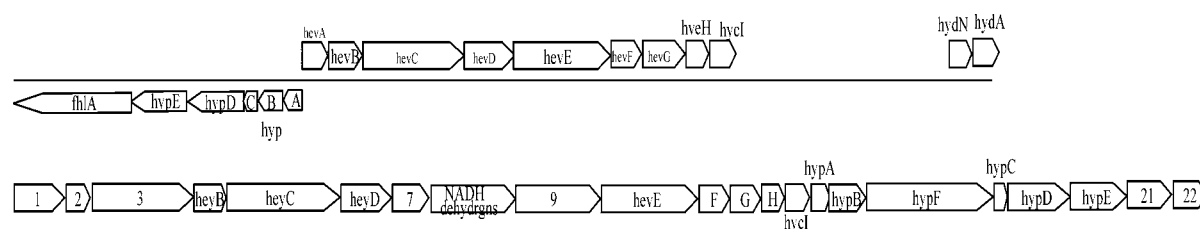


**Figure 1 | Syntrophic growth on formate by a co-culture of *Moorella hydrogenoformans* strain AMP and *Methanothermobacter thermoautotrophicus* strain NJ1.** Symbols: ▲: formate; ●: methane; ◇: acetate; ◆: H<sub>2</sub> in Panel B; □: Gibbs free energy changes for H<sub>2</sub> formation from formate, and Δ: Gibbs free energy changes for methane formation in Panel C.

*M. hydrogenoformans* grew on formate when thiosulfate was added as electron acceptor, but did not grow when thiosulfate was replaced by sulfate, nitrate or fumarate<sup>20</sup>. In the absence of thiosulfate, H<sub>2</sub> gradually accumulated to a partial pressure of 2000 Pa. Removal of H<sub>2</sub> from the headspace via flushing again resulted in accumulation of H<sub>2</sub>. These observations indicate that accumulation of H<sub>2</sub> was inhibitory to the conversion of formate.

Therefore we tested whether *Methanothermobacter* strain NJ1 could serve as alternative electron acceptor. A co-culture of *M. hydrogenoformans* and *Methanothermobacter* sp. NJ1 grew on formate as sole carbon and energy substrate (Figure 1A and B), while the individual pure cultures did not grow in formate-containing media (data not shown). In the coculture  $0.61 \pm 0.04$  mmol  $\text{CH}_4$  was produced by consumption of  $2.71 \pm 0.13$  mmol formate within 60 days, which is consistent with stoichiometric reaction of  $4 \text{HCOO}^- + \text{H}_2\text{O} + \text{H}^+ \rightarrow \text{CH}_4 + 3\text{HCO}_3^-$ , resulting a total cell number increase from  $9 \pm 2.8 \times 10^6$  to  $7.5 \pm 1.4 \times 10^7$  cells/ml and estimated doubling time of  $17 \pm 1$  days. In the co-culture, hydrogen levels were between 10 and 150 Pa. Under these conditions the Gibbs free energy changes in the coculture ranged between -14 and -28 kJ/mol  $\text{H}_2$  for *Moorella* and around -11 kJ/mol  $\text{H}_2$  for the methanogen (Figure 1C). Apparently, both microorganisms are metabolizing close to the thermodynamic limits, as found by Jackson & McInerney for syntrophic degradation of butyrate and benzoate<sup>1</sup>. Taken together these data indicate that interspecies hydrogen transfer is essential to sustain growth of the co-culture and that *M. hydrogenoformans* can grow by the conversion of formate to  $\text{H}_2$  and bicarbonate when the hydrogen concentration is kept low.

**Figure 2 | Comparative structures of formate hydrogenlyase genes in *E. coli* K12<sup>23</sup> (upper) and *Moorella thermoacetica* (bottom).** Predicted functions of genes in contig302 of draft genome sequence of *Moorella thermoacetica* were obtained using The Integrated Microbial Genomes (IMG) System<sup>27</sup> with permission of US Department of Energy Joint Genome Institute. Genes with no homologues in *E. coli* are predicted as 1: Formate/Nitrate transporter; 2: Nitrate reductate; 3: Molybdopterin oxidoreductase:Molybdopterin dinucleotide-binding region; 7: NADH-ubiquinone oxidoreductase, chain 4L; 9: NADH dehydrogenase (quinone); 21: Formate dehydrogenase, subunit FdhD; 22: Molybdopterin-guanine dinucleotide biosynthesis protein A.



*M. hydrogenoformans* is able to grow in pure culture on carbon monoxide<sup>20</sup>. Carbon monoxide is converted into  $\text{H}_2$  and  $\text{CO}_2$  in a similar fashion as described for *Carboxydotherrmus hydrogenoformans* and several other gram-positive bacteria<sup>21</sup>. The energetics of CO conversion ( $\text{CO} + 2\text{H}_2\text{O} \rightarrow \text{H}_2 + \text{HCO}_3^- + \text{H}^+$ ;  $\Delta G^\circ = -15.4$  kJ at  $25^\circ\text{C}$  and

$\Delta G^{\circ} = -12.4$  kJ at  $65^{\circ}\text{C}$ ) is more favorable than the energetics of formate conversion ( $\text{HCOO}^- + \text{H}_2\text{O} \rightarrow \text{H}_2 + \text{HCO}_3^-$ ;  $\Delta G^{\circ} = 1.1$  kJ at  $25^{\circ}\text{C}$  and  $\Delta G^{\circ} = -1.6$  kJ at  $65^{\circ}\text{C}$ ). Thus CO can be removed to low concentrations, even if the partial pressure of  $\text{H}_2$  is high, especially when the bicarbonate concentration is kept low (Henstra, unpublished results). In *Carboxydotherrmus hydrogenoformans* there is compelling evidence that the organism conserves energy via a novel carbon-monoxide-hydrogen-lyase. The key for energy conservation is that the hydrogenase part of the enzyme complex is located at the cytoplasmic site of the cell membrane<sup>22</sup>. We propose that *M. hydrogenoformans* conserves energy from the formate-hydrogen-lyase reaction via an analogous enzyme complex with an energy conserving hydrogenase located at the cytoplasmic side of the cell membrane. Support for this hypothesis was obtained via an analysis of the genome of *Moorella thermoacetica*. This is the closest relative of *Moorella hydrogenoformans* with 98 % homology at the 16S rRNA level, and its genome sequence has recently become available (<http://www.jgi.doe.gov/>). In *M. thermoacetica* the genes encoding for the constituents of the presumed energy conserving formate-hydrogen-lyase complex are all located in one open reading frame with 22 genes (Figure 2). It has high similarity with formate-hydrogen-lyase complex in *E. coli*, which generates energy by production of  $\text{H}_2$  from formate oxidation<sup>23</sup>. But, it is never reported that *E. coli* can grow on formate as sole energy source by this life style. Since we could not find similar formate-hydrogen-lyase complex genes in the draft genome of *Desulfovibrio vulgaris*, the mechanism of syntrophic formate oxidation by this organism remains unclear. Based on these findings it would seem prudent to also test *M. thermoacetica* for its ability to grow syntrophically on formate, but this was pointless because *M. thermoacetica* can grow on formate in pure culture by virtue of its ability to convert formate into acetate ( $4\text{HCOO}^- + \text{H}^+ \rightarrow \text{CH}_3\text{COO}^- + 2\text{HCO}_3^-$ ;  $\Delta G^{\circ} = -99.7$  kJ at  $25^{\circ}\text{C}$  and  $\Delta G^{\circ} = -95.2$  kJ at  $65^{\circ}\text{C}$ ). Indeed *M. thermoacetica* is the model organism with which the pathway for the formation of acetate from hydrogen and formate was elucidated first.

This research describes the construction of an anaerobic microbial consortium that grows on a simple substrate, which from a biochemical and thermodynamic point of view would not seem to be an obvious substrate for syntrophic growth. In nature formate oxidizers have to compete with methanogens that can directly convert formate to methane, and have more energy available than the organisms that convert formate to hydrogen. The detour via hydrogen calls for the introduction of a new microbial guild consisting of bacteria that sponge



on substrates that can also be used by methanogens. Syntrophic acetate oxidizers are other members of this guild<sup>24</sup>. Anaerobic sediments are the habitats where these organisms find their niche<sup>25</sup>.

## ACKNOWLEDGEMENTS

These sequence data of *Moorella thermoacetica*, *Carboxydotherrmus hydrogenoformans* and *Desulfovibrio vulgaris* were produced by the US Department of Energy Joint Genome Institute (<http://www.jgi.doe.gov/>) and The Institute for Genomic Research (<http://www.tigr.org>), respectively.

## METHODS

Strains of *Moorella hydrogenoformans* sp. AMP and *Methanothermobacter* sp. NJ1 were isolated as described previously<sup>20</sup> and maintained routinely on methanol and H<sub>2</sub>/CO<sub>2</sub>, respectively. Media and growth conditions were as described previously<sup>20</sup>. For the coculture study, pre-grown pure culture of *Moorella hydrogenoformans* on methanol and *Methanothermobacter* sp. strain NJ1 on H<sub>2</sub>/CO<sub>2</sub> were inoculated (10%, inoculate size) into fresh mineral medium with 60 mM formate as sole energy source. Subculture was made after formate was consumed until a stable coculture was obtained. Growth yield was determined by optical density increase and cell number counting with a Burke-Turk counting chamber. Formate and acetate were measured with a HPLC as described elsewhere<sup>26</sup>. Methane and hydrogen were measured by gas chromatograph at the conditions indicated before<sup>21</sup>.

Thermodynamic calculations were after Amend and Shock<sup>25</sup> using the Nernst equation to correct Gibbs energy values for the actual temperature, and the Van't Hoff equation to correct the free energy of formation of reactants and products. The comparative analysis of genome sequences were performed using The Integrated Microbial Genomes (IMG) System<sup>27</sup>, which is available from the US Department of Energy Joint Genome Institute at website of <http://www.jgi.doe.gov>.

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# *Chapter 5*

**Competitive uptake of cobalt and nickel by *Methanosarcina barkeri* and the effect of competitive uptake on growth on methanol**

## Summary

The effect of cobalt and nickel on the corrinoid and F430 content and on growth of *Methanosarcina barkeri* on methanol was studied. The cells were grown in media containing 1 mM sulfide and 200  $\mu$ M EDTA. Thus metal precipitation was kept minimal, enabling direct determination of the cell metal content. Cobalt and nickel limitation was achieved and competition between cobalt and nickel uptake was observed. Uptake efficiency of cobalt was high at low cobalt concentration and decreased when the cobalt concentration in the medium was increased. Corrinoid and F430 content correlated positively with the cell content of the corresponding metal, but incorporation in the corrinoid and F430 was significant less at low cell metal contents, ranging from 35% to 80% for corrinoid and 5% to 15% for F430.

**Keywords:** Nickel, Cobalt, Methanogenesis, Speciation, Bioavailability, competition uptake.

## Introduction

Trace elements, such as cobalt, nickel and iron stimulate anaerobic treatment of different types of wastewater [27,31,35]. Metal availability in wastewater, however, can be severely lowered by precipitation with sulfide [5,17]. On the other hand, metal uptake is also affected antagonistically by other essential metals with similar chemical properties and that are taken up by common transporters. For instance, the uptake of tungsten is antagonistically affected by the presence of molybdenum (or vice versa) in many methanogenic archaea and bacteria [23]. Therefore, for optimal metal dosing, it is important to understand the competition between different metals, as well as the chemical speciation of each individual essential metal.

Anaerobic conversion of methanol containing wastewater is stimulated by the addition of cobalt [2,12,26,28]. Under mesophilic conditions, methanol is mainly degraded by *Methanosarcina*-like methanogens, which convert methanol to methane and CO<sub>2</sub> [11]. The importance of cobalt and nickel for anaerobic treatment is related to the metabolic pathways of anaerobic bacteria and methanogenic archaea [39,41]. Cobalt is present mainly in corrinoid cofactors of methyltransferase that are involved in all kinds of methyl transfer reactions [37,41]. Nickel is present in hydrogenases and carbon monoxide dehydrogenase [15], and in the unique cofactor F430 present in the methyl-CoM reductase that catalyzes the last step of methane formation in methanogens [8,20]. It was estimated that more than 90% of the cell cobalt of *Methanosarcina barkeri* [25] and nearly 70% of the cell nickel of *Methanobacterium thermoautotrophicum* are present in the form of corrinoid and F430, respectively [8]. Both cofactors have similar tetrapyrrole structure and are derived from dihydrosiromhydrochlorin [18,40]. The insertion of cobalt in biosynthesis of corrinoid is carried out by a cobaltochelatase, called CbiX [4]. It is still not clear how nickel is inserted, but it is likely that a similar protein as CbiX plays a role [4]. Cobalt and nickel are taken up by certain transporters: a non-specific low affinity magnesium-transporter and a high-affinity specific transporter [10,15]. There is competition between cobalt and nickel [7,10,24]. All uptake studies only focused on metal uptake or relevant enzyme activities, but not on the growth of microorganisms. The aim of the present study is to quantify cobalt and nickel uptake, and to relate that to the cofactor content and methanogenic activity of *Methanosarcina barkeri*.

## Material and methods

### *Methanogen and Medium composition*

*Methanosarcina barkeri* (DSM 800) was obtained from the Deutsche Sammlung für Mikroorganismen und Zellkulturen (DSMZ, Braunschweig, Germany).

A bicarbonate buffered mineral medium as described elsewhere [36] was used with following modifications: 1) vitamin B<sub>12</sub> was omitted; 2) 5 times more trace element solution was added, which contained no iron, cobalt, nickel and EDTA; 3) Ni(II) and Co(II) were added as chloride salts, EDTA was added to a total concentration of 200 µM as indicated in Table 1; 4) Fe(II) was added as Fe(NH<sub>4</sub>)<sub>2</sub>(SO<sub>4</sub>)<sub>2</sub>·6H<sub>2</sub>O to a final concentration of 50 µM. After preparation and sterilization, the medium was left to equilibrate for at least 24 hours before inoculation. All experiments were carried out in glass serum bottles that were soaked in 4 M HNO<sub>3</sub> and rinsed with de-mineralized water. One-liter bottles containing 300 ml medium and a gas phase of N<sub>2</sub>-CO<sub>2</sub> (170kPa, 80:20, vol/vol) were used. Under these conditions the pH was 7.0 ±0.2.

### *Pure culture studies*

Pure culture studies with *M. barkeri* (DSM 800) were carried out using above described media at the conditions indicated in Table 1. Prior to the experiments, three successive subcultures were made in a medium containing 0.1 µM of both nickel and cobalt and 200 µM EDTA. The inoculum size was 10%. Growth was followed by measuring pressure increase in time using a Chrompack Flow-rate-Pressure meter (Chrompack B.V., the Netherlands). Cumulative methane formation was recalculated based on the stoichiometric reaction of methane formation from methanol ( $4\text{CH}_3\text{OH} \rightarrow 3\text{CH}_4 + \text{CO}_2 + 2\text{H}_2\text{O}$ ). Growth rate was estimated from the methanol degradation curve, since preliminary experiments showed it correlates with the increase of biomass. In the late exponential phase, cells were harvested by centrifugation (32000 g; 20 minutes) and washed with 0.02 M EDTA (pH 7) and centrifuged again. The respective cell pellets were used for determination of dry weight, cofactor content and cell metal content. All experiments and sample analysis were done in four replicates.



### *Cofactor content measurement*

Corrinoid and factor F<sub>430</sub> were analyzed by HPLC according to previous methods [21,38], but with following modifications. An amount of 0.5 g (wet weight) of cell pellet was suspended in phosphate buffer (50 mM, pH 7.5). The cell pellet was re-suspended in acetate buffer (0.5 M, pH 5.0) with 1% KCN. The cofactors were extracted by autoclaving the cell suspension at 121°C for 20 minutes. Cell debris and denatured protein were separated by centrifugation. The cell pellet was resuspended in the same buffer and centrifuged. The resulting supernatants of each sample were pooled and loaded onto C18 reverse phase sep-Pak cartridge (Waters Chromatography, Millipore). The loaded column was washed with distilled water and bound cofactors were eluted by 80% methanol. This fraction was dried by flash evaporation and the residue was dissolved in 1 ml distilled water. HPLC analysis was performed with a Chromosampler C18 column (300 x 3 mm), eluted with a methanol gradient in 0.1% acetate from 20 to 49 % for 20 minutes, 60% for the next 5 minutes and 20% for the last 7 minutes. Corrinoid and factor F<sub>430</sub> were recorded at 540 nm and 430 nm, respectively.

### *Metal content analysis*

Cell and sludge metal contents were determined after microwave digestion (Milestone Ethos E, Monroe, CT, USA) in a mixture of HNO<sub>3</sub> (65%) and HCl (37%) at volume ratio of 1:3 as described by Zandvoort [42]. Digested samples were diluted 10 times before ICP-MS determination. Metal concentrations were determined by Inductively Coupled Plasma Mass Spectrometry (ICP-MS, Perkin Elmer ELAN6000) according to the manufacture's standard procedure.

### *Other analytical methods*

Methanol concentration was measured by gas chromatography using a Chrompack gas chromatograph (Model CP9000) equipped with Sil5 CB column (25 m x 0.32 mm) and flame ionization detector at 300°C. The column temperature was 50°C and the injection port temperature was 250°C. The carrier gas was N<sub>2</sub> saturated with formic acid. For dry weight determination, cells were resuspended after centrifugation in 2 ml H<sub>2</sub>O and transferred to dry aluminum cup of known weight. After drying in a stove at 103°C for 24 hr, the filled cups were left to cool down in an exsiccator and weighted.

## Results

### *Growth of Methanosarcina barkeri*

The effect of cobalt on the growth of a pure culture of *M. barkeri* was studied (Fig.1, Table 1). Growth rate of *M. barkeri* increased with cobalt concentration in the medium up to 0.5  $\mu\text{M}$  (batch 1 to 4), in which nickel and EDTA concentration were kept at 5 and 200  $\mu\text{M}$ , respectively. Fastest growth,  $0.61 \pm 0.02 \text{ day}^{-1}$ , was observed at a cobalt concentration of 0.5  $\mu\text{M}$  (batch 4). A slightly lower growth rate was calculated (batch 5) when cobalt concentration was 5  $\mu\text{M}$ . This suggests that an inhibitory effect of cobalt was higher at a concentration of 5  $\mu\text{M}$ . Growth yield, however, was not affected by the cobalt concentrations in the medium, which was averaged around 4.2 g cell dry weight/mol methanol consumed. The somewhat higher yield in batch 7 can be attributed to metal precipitates, since EDTA was not present.

**Table 1.** Growth rate, growth yield and cell cobalt, cell nickel, corrinoid and F430 content in cells of *M. barkeri* grown in media with varying cobalt, nickel and EDTA concentrations.

Batch	Media ( $\mu\text{M}$ )			Growth rate (/day)	Yield (g DW/mol methanol)	Concentration (nmol/g cell dry weight)			
	$\text{Co}^{2+}$	$\text{Ni}^{2+}$	EDTA			Cell $\text{Co}^{2+}$	Cell $\text{Ni}^{2+}$	Corrinoid	F430
1	0.02	5	200	$0.14 \pm 0.04$	$4.14 \pm 0.09$	$58 \pm 3$	$3759 \pm 238$	$14 \pm 5$	$112 \pm 45$
2	0.05	5	200	$0.26 \pm 0.01$	$4.66 \pm 0.48$	$91 \pm 7$	$4667 \pm 156$	$58 \pm 9$	$174 \pm 15$
3	0.1	5	200	$0.35 \pm 0.06$	$4.26 \pm 0.16$	$124 \pm 5$	$3301 \pm 1.2$	$60 \pm 12$	$194 \pm 9$
4	0.5	5	200	$0.61 \pm 0.02$	$4.05 \pm 0.04$	$473 \pm 27$	$1696 \pm 125$	$403 \pm 43$	$223 \pm 28$
5	5	5	200	$0.56 \pm 0.01$	$3.99 \pm 0.15$	$961 \pm 56$	$701 \pm 32$	$859 \pm 51$	$100 \pm 14$
6	5	0.05	200	$0.28 \pm 0.02$	$4.00 \pm 0.38$	$2082 \pm 100$	$115 \pm 4$	$1998 \pm 135$	$5.4 \pm 0.7$
7	5	5	0	$0.52 \pm 0.01$	$4.84 \pm 0.29$	$4486 \pm 410$	$4496 \pm 452$	$242 \pm 24$	$43 \pm 6$
8	0.1	0.1	200	n.m.	n.m.	n.m.	n.m.	$65 \pm 10$	$18 \pm 2$

n.m.: not measured.

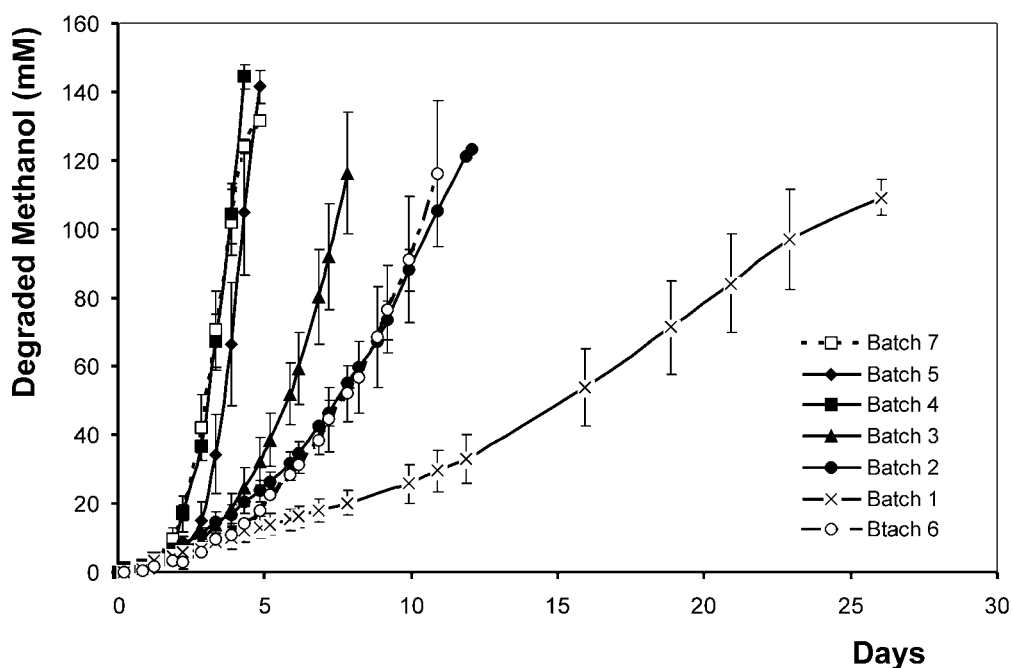
DW: dry weight

Data and standard deviation were from four replicate experiments.

Lowering the nickel concentration from 5  $\mu\text{M}$  to 0.05  $\mu\text{M}$  (Fig. 1 and Table 1) decreased the growth rate by a factor 2 (from  $0.56 \text{ day}^{-1}$  to  $0.28 \text{ day}^{-1}$ ). However, the growth yield was still the same as for the other cultures.

*Cobalt and nickel content in M. barkeri*

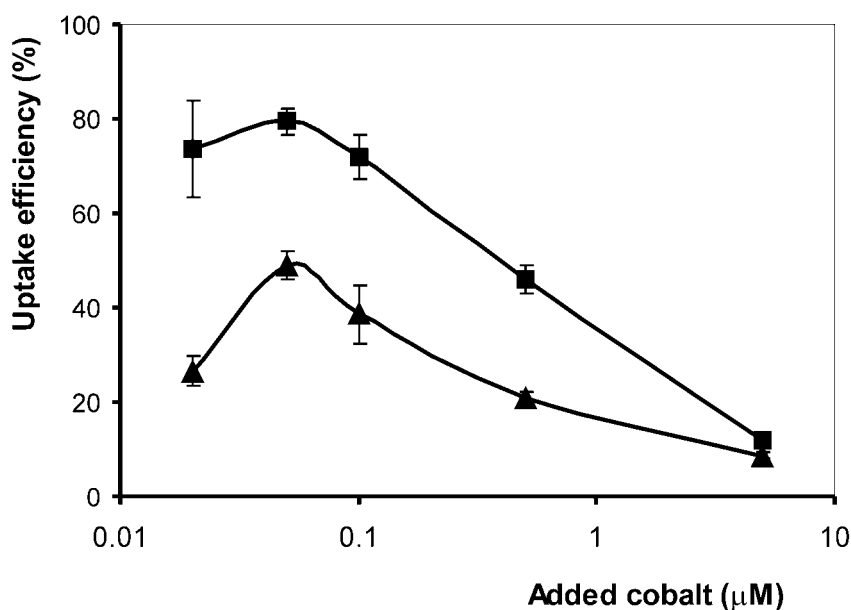
Cobalt and nickel content in the cells of *M. barkeri* grown on methanol were measured to assess the growth-dependent uptake of cobalt (Table 1). Cell cobalt content increased from  $58 \pm 3$  to  $473 \pm 27$  nmol/g cell dry weight when increasing the cobalt concentration from 0.02 to 0.5  $\mu\text{M}$ . A further increase of the cobalt concentration from 0.5  $\mu\text{M}$  to 5  $\mu\text{M}$ , resulted in a doubled cell cobalt content (from  $473 \pm 27$  to  $961 \pm 56$  nmol/g cell dry weight). On the other hand, cell nickel content decreased substantially with the increase of cobalt concentration in the medium with one exception (Batch 2).



**Fig. 1** Methanol degradation by *M. barkeri* in the medium with varying cobalt, nickel and EDTA concentrations. Growth conditions were as stated in Table 1. Data and standard deviation were from four replicate experiments.

Cells of *M. barkeri* grown at a nickel concentration of 0.05  $\mu\text{M}$  and 5  $\mu\text{M}$  cobalt (Batch 6) had a remarkably high cobalt content of  $2082 \pm 100$  nmol /g cell dry weight. This value was twice as that in the cells grown with both 5  $\mu\text{M}$  nickel and cobalt added to the medium. By contrast, cells grown under these conditions had the lowest nickel content, which was only  $115 \pm 4$  nmol /g cell dry weight.

To elucidate the uptake efficiency, the proportion of cobalt or nickel recovered inside cells of *M. barkeri* to the total cobalt or nickel present in the medium was calculated (Fig 2). Almost 80% of the total amount of cobalt was taken up by the cells at cobalt concentrations below 0.05  $\mu\text{M}$ . Upon a further increase of the cobalt in the media, cobalt uptake efficiency



**Fig. 2** Cobalt (■) and nickel (▲) uptake efficiency of *M. barkeri* grown in media with varying cobalt concentrations.

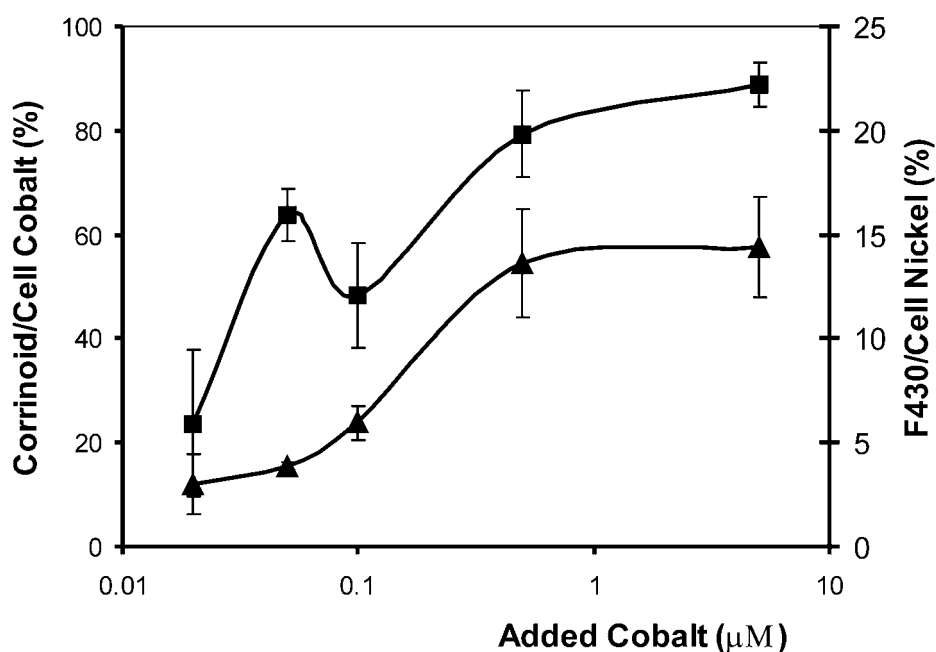
decreased significantly from 80% to 12% (at cobalt concentration of 5  $\mu\text{M}$ ). Nickel uptake efficiency had doubled when the cobalt concentration increased from 0.02 to 0.05  $\mu\text{M}$  in the media. A decreased nickel uptake efficiency was observed with further increased cobalt concentration, although the nickel concentration was kept at 5  $\mu\text{M}$ . When both cobalt and nickel concentrations were at the same concentration of 5  $\mu\text{M}$ , cobalt and nickel uptake efficiencies were similar (12% for cobalt and 8.6% for nickel). Cells grown under nickel limited conditions took up almost all nickel added to the medium (Batch 6). A doubled cobalt uptake efficiency under this condition was also observed in comparison with the medium in which the nickel concentration was 5  $\mu\text{M}$  (24% vs 12%).

*Cell corrinoid and F430 contents in M. barkeri*

The corrinoid content increased with increasing cobalt concentration in the media thus following the pattern of the cell cobalt content. Remarkably, F430 content increased also with the increase of cobalt concentration up to 0.5  $\mu\text{M}$ . However, at a cobalt concentration of 5  $\mu\text{M}$ , F430 content was less than 50% of its maximum measured at 0.5  $\mu\text{M}$  cobalt (Table 1).

The highest corrinoid content,  $1998 \pm 135$  nmol/g cell dry weight, was measured in cells grown in the media with 0.05  $\mu\text{M}$  nickel (batch 6). This value was twice as high as in cells grown with 5  $\mu\text{M}$  nickel and 5  $\mu\text{M}$  cobalt (batch 5,  $859 \pm 51$  nmol/g cell dry weight). F430 content in these cells, however, was more than 18 times lower compared with corresponding cells in batch 5 ( $5.4 \pm 0.7$  vs  $100 \pm 14$  nmol/g cell dry weight).

Fig. 3 depicts the ratio of cell metals (cobalt and nickel) that was present in the form of corrinoid and F430, respectively. It is clear that a relatively higher amount of the cobalt and nickel that was taken up by cells of *M. barkeri* was incorporated into corrinoid and F430,



**Fig. 3** Ratio of corrinoid-cobalt to cell cobalt content (■) and F430-nickel to cell nickel content (▲) in *M. barkeri* grown in media of varying cobalt concentrations.

respectively, when the cobalt concentration increased in the medium. More than 85% of the cobalt was present as corrinoid which may reflect that cobalt is only present in corrinoid in anaerobes [16]. On the other hand, the maximal F430-nickel was 15% of the nickel that had been taken up. This value was observed at 5  $\mu$ M nickel and 5  $\mu$ M cobalt. Nickel is not only present in F430, but also in other enzymes, like hydrogenase and carbon monoxide dehydrogenase [15,16].

## Discussion

*M. barkeri* grew at a similar rate in the presence or the absence of EDTA (Batch 5 and 7). This indicates that such an EDTA concentration is not toxic for this microorganism. The optimal cobalt concentration was around 0.5  $\mu$ M, which is consistent with what was found before [12]. The increased growth rate could be related to an increased free cobalt concentration as was found in another study [19]. This stimulated the uptake of cobalt, which resulted in higher cell cobalt content, higher corrinoid content and faster growth.

A slightly inhibitory effect was observed at cobalt concentration of 5  $\mu$ M, which is far lower than 0.8 mM, which was found to inhibit methanogenesis [2]. In that study, no EDTA was present. Obviously, the presence of EDTA in our study as metal chelating compound increased metal bioavailability, therefore inhibitory cobalt concentration became lower. Metal ligands, such as humic substances, EDTA, NTA and citric acid, have been proven to increase the bio-availability of trace metals, and thus stimulate growth of microorganisms [3,29] and the performance of methanogenic bioreactors [14]. Yeast extract, besides its role as source of vitamins, improves metal availability, likely due to the presence of complexing compounds [13]. Our results of corrinoid and F430 contents in cells grown in the absence of EDTA were around three times lower than those grown in the presence of EDTA, although it had little effect on the growth rate of *M. barkeri* on methanol (Batch 5 vs Batch 7 in Table 1). This result clearly showed that bioavailability of cobalt and nickel is influenced by the presence of EDTA.

Cell cobalt and nickel contents in cells of *M. barkeri* grown in the absence of EDTA likely were overestimated, due to co-sedimentation of cells and metal precipitate (Batch 7,

Table 1). In the presence of EDTA, cobalt and nickel were present in soluble EDTA complexes, thus preventing metal sulfide precipitation that may bias the metal content analysis. Reduction of the sulfide concentration in the medium to 0.3 mM to avoid metal precipitation allowed a better analysis of cell cobalt and nickel contents in methanogenic archaea [30]; 0.17-2  $\mu\text{mol}$  cobalt/g cell dry weight and 1.1-3  $\mu\text{mol}$  nickel/g cell dry weight were determined in different methanogenic species grown on different substrates [30]. Cells of *M. barkeri* grown at similar cobalt and nickel concentrations in the presence of EDTA in our study (Batch 5) had comparable cobalt and nickel contents as found in the above study.

Cells of *M. barkeri* grew slowly at cobalt concentrations below 0.1  $\mu\text{M}$ . They also had profoundly lower cell cobalt and corrinoid contents. Apparently, they were limited by the availability and uptake of cobalt. Little is known about cobalt and nickel transport systems in methanogens. An uptake system for nickel was described in *Methanotherx concilii*, which has an affinity of  $K_m = 91 \mu\text{M}$  and uptake capacity of 23 nmol/min/mg dry weight [1]. *Methanobacterium bryantii* transported nickel against a concentration gradient by a high-affinity system ( $K_m = 3.1 \mu\text{M}$ ) [20]. Magnesium, calcium, or manganese had little influence on nickel uptake in this methanogen; cobalt, however, did compete when its concentration was 10 times higher than nickel [1,20]. The best studied specific cobalt and nickel transporters were in *E. coli* and other microorganisms [10]. One of the transporters, Nik, is an ABC transporter with relative high affinity ( $K_m < 0.1 \mu\text{M}$ ) [6]. Another one, HoxN, is an integral membrane permease with extremely high affinity ( $K_m = 10 \text{ nM}$ ) but a low capacity of 1.5 pmol  $\text{Ni}^{2+}$ /min/mg protein [7]. Both nickel transporters were found to be also involved in cobalt uptake [10]. Specific high affinity cobalt permeases were found in *Rhodococcus rhodochrous* [24] and *Schizosaccharomyces pombe* [9]. Cobalt uptake activity is inhibited by the presence of nickel, although other metals such as manganese, iron and copper had no effect [9,24]. Our findings that cell nickel content decreased with increasing cobalt concentration in the medium and that cell cobalt increased with decreasing nickel concentration in the medium suggest that such competition of uptake of cobalt and nickel also occurs in *M. barkeri*. We speculate that cobalt is transported by a high affinity and low capacity transporter at low cobalt concentration (below 0.1  $\mu\text{M}$ ) and by another lower affinity but higher capacity transporter at high cobalt concentration (above 0.1  $\mu\text{M}$ ). The slower growth rate observed at lower cobalt concentration seemed to be caused by this lower capacity transporter. Since such a transporter has a high affinity, it is still operational at an extremely

low concentration. Therefore, the cobalt uptake efficiency is much higher (up to 80%, Fig.2) at lower cobalt concentrations than at high cobalt concentrations. It is also a reflection of the regulation of transcription of different transporter genes under cobalt limited conditions, in order to fulfill its high cobalt requirement, as was found for the Nik transporter [6]. Uptake efficiency decreased at high cobalt concentration, and the similar values (12% for cobalt and 8.6% for nickel) at 5  $\mu$ M cobalt and nickel might indicate that they share the same transporter(s).

Corrinoid and F430 are important cofactors in methanogens [39]. *M. barkeri* has been studied as a source for Vitamin B12 production using methanol as substrate [25,32-34]. A corrinoid of 8.5 mg/l was produced at 40  $\mu$ M cobalt and 250 mM methanol [34], which is just twice as much as achieved at 5  $\mu$ M cobalt and 200 mM methanol. It is not known yet why *M. barkeri* synthesizes so much corrinoids, but corrinoid content in the cells had a clear relation with growth rates when cobalt is the growth-limiting factor (Table 1). This is in accordance with previous findings that both the methanogenic activity and the corrinoid content increased by the addition of cobalt (8.4  $\mu$ M), resulting in a fast growth rate of 0.6 /day [22]. Therefore, corrinoid and F430 content can be an indicator of metal limitation of bioreactors. It was found that both performance of a lab-scale reactor and the specific methanogenic activity of the sludge from this reactor on methanol increased significantly even after 44 days bioreactor operation on methanol without the addition of both cobalt and nickel [43]. Cofactor content analysis in the sludge samples indicated that the corrinoid and the F430 content increased 8 times and 1.5 times, although the sludge severely loses its cobalt and nickel content [43]. Metal content data showed this sludge had similar cobalt and nickel content [43]. The other sludge used in the same study under same conditions, which showed decrease of methanogenic activity and both cofactor content after 50 days operation on methanol, had much higher (4 times) nickel content than cobalt content. We speculate that competitive uptake of cobalt and nickel could be one of the reasons for the different responses of these two reactors. Therefore, in practice, it is also important to pay attention to the possibility of one metal at high concentration might suppress the uptake of another in optimization of trace metal dosing to bioreactors.



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# *Chapter 6*

## **Effect of tungsten and molybdenum on growth of a syntrophic coculture of *Syntrophobacter fumaroxidans* and *Methanospirillum hungatei***

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## Summary

The trace elements tungsten and molybdenum play an essential role in the growth of anaerobic microorganisms. Depletion of tungsten and/or molybdenum in the media did not affect axenic growth of *Syntrophobacter fumaroxidans* on propionate + fumarate, indicating under these conditions this organism does not have a high tungsten or molybdenum requirement. However, growth of *Methanospirillum hungatei* on either formate or hydrogen and carbon dioxide required tungsten, and molybdenum can replace tungsten to some extent. Growth of the *Syntrophobacter-Methanospirillum* coculture on propionate is significantly affected by the addition of these two metals. Measurement of enzyme levels in cell extracts of syntrophically grown cells indicated that the levels of hydrogenase and formate dehydrogenase activity were correlated with the methane formation rates by the cocultures, which suggests both hydrogen and formate play important role in syntrophic propionate oxidation.

**Keywords:** *Syntrophobacter fumaroxidans*; *Methanospirillum hungatei*; Propionate oxidation; Tungsten; Molybdenum; Syntrophy.

## Introduction

Tungsten (W) and molybdenum (Mo) are essential trace elements for growth of many anaerobic microorganisms (Kletzin and Adams 1996). Several redox-enzymes depend on these metals in obligate anaerobes. Examples of enzymes which contain either W or Mo are: formate dehydrogenase (FDH), which is required for energy conservation and carbon assimilation in anaerobic bacteria and archaea (Ljungdahl and Andreesen 1978; Ferry 1999), formylmethanofuran dehydrogenase (FMDH), which reduces carbon dioxide (CO<sub>2</sub>) and couples the formyl group to methanofuran in methanogens (Hochheimer et al. 1998), a variety of aldehyde oxidizing enzymes and acetylene hydratase (Kletzin and Adams 1996). Since the chemical and catalytic properties of these two metals are very similar, some enzymes contain either Mo or W, and some microorganisms even contain analogues of enzymes containing either W or Mo, depending on the growth conditions (Bertram et al. 1994; Hochheimer et al. 1998; Stewart et al. 2000; Brondino et al. 2004). However, most microorganisms just possess one type of enzyme, in which the W and Mo can not effectively replace each other (Jones and Stadtman 1977; Van Bruggen et al. 1986; Zindel et al. 1988; Afshar et al. 1998), and in some cases, they even have antagonistic effects (Ljungdahl and Andreesen 1978; Zellner and Winter 1987; May et al. 1988). It was hypothesized that mesophilic microorganisms prefer to incorporate Mo into their enzymes, while thermophilic microorganisms prefer W (Kletzin and Adams 1996).

We were interested in the effect of W and Mo on growth of *Syntrophobacter fumaroxidans*. This anaerobic bacterium oxidizes propionate via the methyl-malonyl-CoA pathway and is able to dispose of electrons by either fumarate or sulfate reduction (Plugge et al. 1993; Stams et al. 1993; Harmsen et al. 1998). Without these electron acceptors, *S. fumaroxidans* reduces protons to hydrogen (H<sub>2</sub>) and bicarbonate to formate by means of hydrogenase (H<sub>2</sub>ase) and FDH (Stams and Dong 1995). H<sub>2</sub> and formate formation coupled to propionate oxidation are endergonic under standard conditions. Therefore, the levels of H<sub>2</sub> and/or formate have to be kept low in order to make the conversion energetically feasible (Stams 1994; Schink 1997). Low H<sub>2</sub> and formate levels are created by methanogenic partners that grow on H<sub>2</sub> and CO<sub>2</sub> and/or formate. Interspecies electron transfer in syntrophic propionate oxidizing consortia has been studied, but it is still unclear whether hydrogen or formate is the preferred electron carrier (Stams 1994; Schink 1997; de Bok et al. 2004). *Syntrophobacter* species only oxidize propionate together with methanogens that utilize both

H<sub>2</sub> and formate, such as *Methanospirillum hungatei* and *Methanobacterium formicicum*, not with *Methanobrevibacter* strains that only utilize H<sub>2</sub> (Dong et al. 1994). Therefore, besides H<sub>2</sub>, formate was also considered to play a role in syntrophic propionate oxidation (Thiele and Zeikus 1988; Boone et al. 1989; Stams and Dong 1995). Biochemical evidence was obtained as well (Dong and Stams 1995; de Bok et al. 2002a). Both microorganisms possess H<sub>2</sub>ases and FDHs, of which the expression levels are much higher during syntrophic growth on propionate compared to the pure cultures (de Bok et al. 2002a), and two W-containing FDHs were purified from *S. fumaroxidans* (de Bok et al. 2003). We hypothesized that when interspecies formate-transfer is essential, syntrophic growth of the *Syntrophobacter-Methanospirillum* coculture should be affected by the level of W and/or Mo. In this study we investigated the importance of W and Mo for syntrophic and axenic growth of *S. fumaroxidans* and *M. hungatei*, and determined the FDH and H<sub>2</sub>ase levels in cell extracts.

## Materials and methods

### *Growth conditions*

*Syntrophobacter fumaroxidans* (DSM10017) and *Methanospirillum hungatei* (DSM864) were routinely cultured at 37°C in 120-ml serum flasks with 50 ml of medium and a gas phase of 172 KPa N<sub>2</sub>/CO<sub>2</sub> or H<sub>2</sub>/CO<sub>2</sub> (80:20, vol/vol) as described previously (Stams et al. 1993). W and Mo were added as sodium tungstate and sodium molybdate. Propionate, fumarate and formate (all sodium salts) were added from 1 M sterile stock solutions as indicated in the text. *M. hungatei* cultures were amended with 2 mM of acetate as a carbon source, and these cultures were shaken at 150 rpm to prevent gas diffusion limitation. To minimize metal contamination, glassware was soaked in a 4 M nitric acid solution for three days; butyl rubber stoppers were soaked overnight and washed thoroughly with nano-pure water before use. All solutions and media were prepared with ultra-pure water. All chemicals and vitamins were of the highest grade.

### *Cell separation and fractionation*

The cells were harvested in the late exponential phase by centrifugation under anoxic conditions as described previously (de Bok et al. 2002b). Syntrophically grown cells of *S.*



*fumaroxidans* and *M. hungatei* were separated by Percoll gradient centrifugation as described before (de Bok et al. 2002b). Separated cells were suspended in buffer A (50mM Tris-HCl, pH 8.0, 100  $\mu$ M sodium dithionite). Cell free extract was obtained by sonication and cell debris was removed by centrifugation at  $16,000 \times g$  (de Bok et al. 2002b).

#### *Enzyme activities*

Enzyme activities were routinely measured at 37°C in N<sub>2</sub>-flushed or H<sub>2</sub>-flushed cuvettes containing 1 ml of 50 mM Tris-HCl and closed with butyl-rubber stoppers. Formate and H<sub>2</sub> oxidation rates were recorded at 578 nm as described by others (Boonstra et al. 1975; Odom and Peck 1981), with 1 mM benzyl viologen (BV<sup>+</sup>,  $\epsilon = 8.65 \text{ mM}^{-1} \text{ cm}^{-1}$ ) as electron acceptor. Protein was determined according to Bradford with bovine serum albumin as a standard (Bradford 1976).

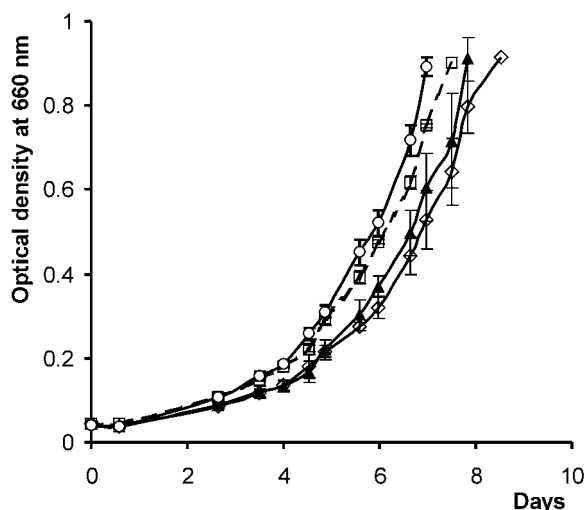
#### *Analytical methods*

Growth was followed by determination of the optical density at 660 nm or by following the methane production. It was assumed that methane formation is linearly correlated to growth. CH<sub>4</sub> and H<sub>2</sub> were determined on a Chrompack 9001 gas chromatograph with a PlotFused silica column (30 m by 0.53 mm) packed with Molsieve 5A (DF=15  $\mu$ m). The temperature of the column, injection port and thermal conductivity detector were 50, 60 and 130°C, respectively. Argon was used as carrier gas (20 ml min<sup>-1</sup>). Metal content of the medium was measured by inductively coupled plasma mass spectrometry (ICP-MS, Elan 6000, Perkin-Elmer).

## **Results and discussion**

#### *Effects of W and Mo on the axenic growth of S. fumaroxidans*

*S. fumaroxidans* is able to ferment fumarate, and it can also couple the oxidation of propionate, H<sub>2</sub> or formate to reduction of fumarate or sulfate (Stams et al. 1993; Harmsen et al. 1998). FDH and H<sub>2</sub>ase are expressed constitutively on all these substrates and substrate combinations (de Bok et al. 2002b). A culture of *S. fumaroxidans* growing on propionate (20 mM) and fumarate (60 mM) was used to study the effects of W and Mo on the axenic growth



**Fig. 1** Axenic growth of *S. fumaroxidans* on propionate (20mM) and fumarate (60mM) after six transfers in medium with W and Mo (▲), W only (○), Mo only (◇) or without W and Mo (□). Data are the mean of duplicate measurements.

of *S. fumaroxidans*. The strain was adapted to each condition by routinely subculturing in fresh medium for six transfers. Growth rates and maximal optical densities were not affected by the absence or presence of W and/or Mo (Table 1, Fig. 1). The average growth rate in each of the different media was around  $0.21 \text{ day}^{-1}$ , which is in the same range as observed previously (Stams et al. 1993). ICP-MS analysis of our basal medium without W and Mo revealed that the residual W and Mo concentrations were below 55 pM and 10 pM, respectively, indicating that chemical contamination as a source of W or Mo in our basal medium was kept to a minimum. Depletion of W to such level, completely inhibited growth of *Pyrobaculum aerophilum* (Afshar et al. 1998). Therefore, our results suggest that *S. fumaroxidans* does not require W and Mo for axenic growth on propionate and fumarate.

*Eubacterium acidaminophilum* (Glanderath 1993). However, unlike these two microorganisms, the FDH level in *S. fumaroxidans* was significantly lower in medium with both W and Mo, as compared to medium with only W. Similar results were obtained for the W- and Mo- containing FDHs in *Desulfovibrio alaskensis* (Brondino et al. 2004) and dimethyl sulfoxide reductase (DMSO) in *Rhodobacter capsulatus* (Stewart et al. 2000). The explanation for this is that although Mo and W can be used by *D. alaskensis* and *R. capsulatus* indiscriminately, there might be a competition for the binding site between the two metals, for which Mo might have a higher affinity, even though its catalytic activity is less efficient than

with W. Therefore, when Mo is not present, W is incorporated in enzymes that prefer Mo, resulting in a higher specific activity. However, the two FDHs from *S. fumaroxidans* that were characterised previously appeared to be W-containing enzymes although both metals were present in the growth medium (de Bok et al. 2003). So if this would be true for the *S. fumaroxidans* FDHs, it would imply that part of the total FDH activity in the cells grown on propionate plus fumarate represents additional FDH(s). Indeed, quantification of the different FDHs in *S. fumaroxidans* suggested that it contains a third FDH (de Bok et al. 2003). In our study, the difference in FDH-level between cells grown in medium without W and Mo and in medium with only Mo was also  $2.5 \text{ U mg}^{-1}$ , which could not be addressed to one of the W-containing-FDHs (de Bok et al. 2003). Therefore, the most likely explanation for our observations is that *S. fumaroxidans* possesses a third constitutively expressed FDH of which the activity increases when Mo is substituted by W. This then would imply that substitution of Mo for W in the two well-studied FDHs does not produce active FDHs. This would be in contrast with the *M. thermoacetica* FDH, which could also incorporate Mo into its active site (Durfor et al. 1983). To confirm our ideas the third FDH of *S. fumaroxidans* would need to be purified from selected media. Although FDH activities in *S. fumaroxidans* strongly depend on either W or Mo, the  $\text{H}_2$ ase levels in *S. fumaroxidans* grown on propionate plus fumarate were not significantly affected by the absence of W and Mo.

#### *Effects of W and Mo on the axenic growth of M. hungatei*

*M. hungatei* utilizes  $\text{H}_2$  and/or formate produced by *S. fumaroxidans* when co-cultured on propionate (Dong et al. 1994). Therefore, the influence of W and Mo on the growth of *M. hungatei* on  $\text{H}_2/\text{CO}_2$  or formate was also assessed to understand the role of these metals in syntrophic propionate oxidation. The composition of the media used to assess the effects of Mo and W on *M. hungatei* was similar as described above for *S. fumaroxidans*, except that acetate (2 mM) was added as extra carbon source. The cultures of *M. hungatei* were adapted to growth on either  $\text{H}_2/\text{CO}_2$  (172 kPa, 80:20, vol/vol) or formate (120 mM) as substrate for at least three subsequent transfers in the corresponding media. Growth was followed by measuring methane ( $\text{CH}_4$ ) formation.

**Table 1** Growth rates and specific formate dehydrogenase (FDH) and hydrogenase (H<sub>2</sub>ase) activities in cell extracts of *S. fumaroxidans* (grown on propionate plus fumarate) and *M. hungatei* (grown on formate or H<sub>2</sub>/CO<sub>2</sub>) after adaptation to growth in media with or without W and/or Mo.

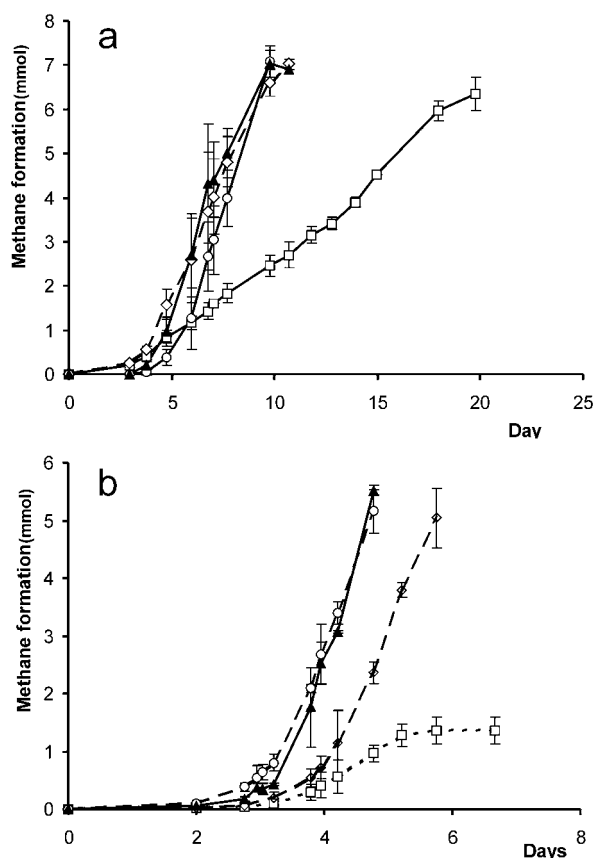
Medium	I	II	III	IV
WO <sub>4</sub> <sup>2-</sup> (μM)	0	0	0.1	0.1
MoO <sub>4</sub> <sup>2-</sup> (μM)	0	0.1	0	0.1
<b><i>S. fumaroxidans</i> (propionate/fumarate)</b>				
FDH (U mg <sup>-1</sup> )	2.5±0.1	5.0±0.5	25.3±0.1.3	14.5±0.4
H <sub>2</sub> ase (U mg <sup>-1</sup> )	15.6±0.4	9.1±0.4	7.4±0.9	17.1±0.1
Growth rate (day <sup>-1</sup> )	0.21±0.03	0.19±0.01	0.22±0.01	0.21±0.02
<b><i>M. hungatei</i> (formate)</b>				
FDH ((U mg <sup>-1</sup> )	0.3±0.1	1.1±0.1	7.3±0.4	4.8±0.8
H <sub>2</sub> ase (U mg <sup>-1</sup> )	14.5±2.1	9.2±1.2	5.6±0.1	2.5±0.1
Growth rate (day <sup>-1</sup> )	0.11±0.02	0.41±0.03	0.33±0.05	0.41±0.01
<b><i>M. hungatei</i> (H<sub>2</sub>/CO<sub>2</sub>)</b>				
FDH (U mg <sup>-1</sup> )	0.006±0.0	3.2±0.1	18±0.4	25±0.5
H <sub>2</sub> ase (U mg <sup>-1</sup> )	0.8±0.1	1.3±0.1	1.7±0.2	1.7±0.2
Growth rate (day <sup>-1</sup> )	0.40±0.16 <sup>a</sup>	0.60±0.07	0.76±0.06	0.87±0.08

<sup>a</sup> Growth ceased after a short exponential phase, from which the growth rate was calculated.

<sup>b</sup> Growth rates are the mean of triplicate measurements and enzyme activities are duplicate measurements.

The importance of W and Mo in methanogenesis has been recognized for a long time. The stimulating effect of both elements was found to be related to either the FDH levels in methanogens growing on formate, such as *M. formicicum* and *Methanococcus vannielii* (Jones and Stadtman 1981; May et al. 1988), or to the FMDH level in methanogens growing on H<sub>2</sub>/CO<sub>2</sub> such as *Methanothermobacter wolfei* and *Methanothermobacter marburgensis* (Bertram et al. 1994; Hochheimer et al. 1998). Growth of *M. formicicum* and *M. vannielii* on H<sub>2</sub>/CO<sub>2</sub> was not affected by Mo or W when H<sub>2</sub>/CO<sub>2</sub> was substrate instead of formate, as FDH is not required for autotrophic growth (Jones and Stadtman 1981; May et al. 1988). Similar to these two methanogens, *M. hungatei* grows on both H<sub>2</sub>/CO<sub>2</sub> and formate. Therefore, one can expect that growth on formate but not on H<sub>2</sub>/CO<sub>2</sub> is influenced by W or Mo. Indeed, presence of either W or Mo stimulated growth of *M. hungatei* on formate (Fig. 2a, Table 1). The highest growth rates (0.41 day<sup>-1</sup>) were observed when Mo was present in the medium (medium II and IV). In the absence of Mo but presence of W the growth rate was slightly lower (0.33

day<sup>-1</sup>). When both W and Mo were absent, the growth rate was only 0.11 day<sup>-1</sup>. The highest FDH-level was detected when only W was present in the medium and it was substantially lower when W was absent, suggesting the presence of W-containing-FDH(s) in *M. hungatei*. Apparently, the growth rate of *M. hungatei* was directly related to the FDH activity, as both FDH level and growth rate increased about 4 times when Mo was added in the medium. But, further increase of FDH level by addition of W did not further increase growth rate,



**Fig. 2** Growth as determined from methane production of *M. hungatei* on formate (a) or on H<sub>2</sub>/CO<sub>2</sub> (b) in the media with W and Mo (▲), W only (○), Mo only (◇) or without W and Mo (□). Data are the mean of triplicate measurements.

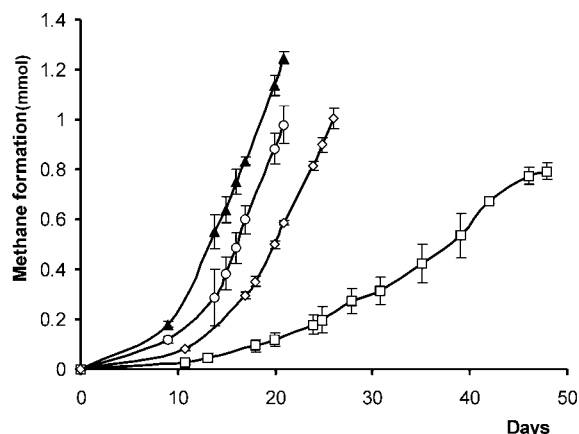
indicating that something other than FDH is limiting. These results are more difficult to interpret since we do not know if the *M. hungatei* FDH(s) contain W and methanogens also contain FMDH that is also Mo or W dependent (Bertram et al. 1994; Kletzin and Adams 1996; Hochheimer et al. 1998). However, all FDHs from mesophilic methanogens studied so far contain Mo. If we assume that also the *M. hungatei* FDH(s) contains Mo, our results suggest that W stimulates the production of Mo-containing-FDH and that W effectively substitutes Mo in *M. hungatei* FDH, resulting in an enzyme with an even higher activity.

However, we do not exclude the possibility that *M. hungatei* possesses a W-containing-FDH, and that perhaps W-containing-FDHs are much more common than we think.

Growth of *M. hungatei* on  $H_2/CO_2$  was also stimulated by W and Mo (Fig. 2b, Table 1). The highest growth rates of *M. hungatei* on  $H_2/CO_2$  ( $0.87$  &  $0.76$  day<sup>-1</sup>) were measured in the cultures grown in the presence of W (Medium III & IV). Growth rates, FDH and  $H_2$ ase levels were substantially lower in the media without W (Medium I & II). When both W and Mo were absent the culture eventually ceased to grow after a short exponential growth phase. The FDH level in these cells was significant almost negligible, which suggests that FDH is also required for growth on  $H_2/CO_2$ . There are some reports that FDH is needed for biosynthesis in some methanogens during growth on  $H_2/CO_2$  (Tanner et al. 1989; White 1997). Interestingly, even *fdh* gene expression was found to be controlled by the presence of  $H_2$  and not by the presence of formate in *Methanococcus maripaludis* (Wood et al. 2003). A stimulating effect of W on methanogens growing on  $H_2/CO_2$  has also been demonstrated for *Methanocorpusculum parvum* and *Methanoplanus endosymbiosus* (Van Bruggen et al. 1986; Zellner and Winter 1987). Clearly this might also be true for *M. hungatei*, as increased FDH levels were observed when it grew on  $H_2/CO_2$ . The effects of W and Mo on growth of *M. hungatei* could be also related to the FMDH-level, as it was speculated by Kletzin and Adams (Kletzin and Adams 1996). Then, the most likely explanation for our results is that *M. hungatei* contains a W-FMDH in which W can be substituted by Mo, or that it contains a W-FMDH as well as a Mo-FMDHs as was found for *M. wolfei* and *M. thermoautotrophicus* (Bertram et al. 1994; Hochheimer et al. 1998).

#### *Effects of W and Mo on co-cultures of S. fumaroxidans and M. hungatei*

To study if W and Mo are required for syntrophic growth on propionate, co-cultures of *S. fumaroxidans* and *M. hungatei* were cultivated on propionate (30mM) in media with or without Mo and W. Cells were successfully separated by percoll gradient centrifugation. The FDH and  $H_2$ ase activities in the cell-free extracts of syntrophically grown *S. fumaroxidans* and *M. hungatei* cells are presented in Table 2. Maximum methane formation rates in these co-cultures were calculated from the methane production curves (Fig. 3).



**Fig. 3** Syntrophic propionate oxidation as determined from methane production by a coculture of *S. fumaroxidans* and *M. hungatei* in the media with W and Mo (▲), W only (○), Mo only (◇) or without W and Mo (□). Data are the mean of triplicate measurements.

**Table 2.** The effects of W and Mo on the CH<sub>4</sub> formation rates and specific formate dehydrogenase (FDH) and hydrogenase (H<sub>2</sub>ase) activities in the cell extracts of *S. fumaroxidans* and *M. hungatei* grown syntrophically on propionate (30 mM). Cells of *S. fumaroxidans* and *M. hungatei* were separated by percoll gradient centrifugation.

Medium	I	II	III	IV
WO <sub>4</sub> <sup>2-</sup> (μM)	0	0	0.1	0.1
MoO <sub>4</sub> <sup>2-</sup> (μM)	0	0.1	0	0.1
<i>S. fumaroxidans</i>				
FDH (U mg <sup>-1</sup> )	5.5±0.4	19.5±1.1	102±3.1	95±0.9
H <sub>2</sub> ase (U mg <sup>-1</sup> )	8.2±0.1	9.5±0.7	9.9±0.6	12.7±1.5
<i>M. hungatei</i>				
FDH (U mg <sup>-1</sup> )	0.02±0.02	2.2±0.3	25.5±1.2	44±2.1
H <sub>2</sub> ase (U mg <sup>-1</sup> )	0.6±0.1	0.8±0.1	1.8±0.2	3.2±0.4
CH <sub>4</sub> formation rate <sup>a</sup> (nmol min <sup>-1</sup> ml <sup>-1</sup> )	0.13±0.02	0.41±0.03	0.57±0.04	0.59±0.02

<sup>a</sup> CH<sub>4</sub> formation rates are the mean of triplicate measurements and enzyme activities are duplicate measurements.

Also in syntrophically grown cells of *S. fumaroxidans* and *M. hungatei* the highest FDH levels were detected when W was present in the medium (medium III and IV). These

specific activities were much higher than those in axenically grown cells of *S. fumaroxidans* and *M. hungatei* on formate, consistent with findings reported previously (de Bok et al. 2002a). In W-depleted media (medium I and II), FDH levels were significantly lower in both organisms (Table 2). The highest methane formation rate,  $0.59 \text{ nmol min}^{-1} \text{ ml}^{-1}$ , was measured in medium with both W and Mo, comparable to the rate measured by Dong and Stams (Dong and Stams 1995). The rate was more or less the same ( $0.57 \text{ nmol min}^{-1} \text{ ml}^{-1}$ ) when Mo was limiting, but it decreased to  $0.41 \text{ nmol min}^{-1} \text{ ml}^{-1}$  in W-depleted medium (medium II). In the medium without W and Mo the methane formation rate was only  $0.13 \text{ nmol min}^{-1} \text{ ml}^{-1}$ , which is at least due to the inhibition of *M. hungatei* by W- and Mo limitation as we demonstrated in our experiments with axenic cultures. The FDH-level in *M. hungatei* under these conditions was  $0.02 \text{ U mg}^{-1}$ , which is almost negligible compared to its level in medium without any limitations, considering that the efficiency of percoll separation with these co-cultures is not 100% (de Bok et al. 2002a), and assuming this activity could be attributed to residual FDH from *S. fumaroxidans* cells in the percoll separated *M. hungatei* cells. Therefore we can state that *S. fumaroxidans* and *M. hungatei* are able to grow syntrophically with  $\text{H}_2$  as the only interspecies electron carrier. Whether the lower rate can be attributed to the absence of interspecies formate transfer alone is not clear, because we do not know how much the *M. hungatei* FMDH is affected by W- and Mo-limitation in the co-cultures, since in this case there is also competition for residual W and Mo between the individual organisms. However, if we assume that W is required for  $\text{CO}_2$ -reduction in *S. fumaroxidans* both for disposal of electrons as hypothesized by de Bok and co-workers (de Bok et al. 2003), and for  $\text{CO}_2$  fixation for biomass synthesis (Plugge et al. 1993), and that the *M. hungatei* FMDH is a Mo-enzyme (or a W-enzyme in which Mo can replace W effectively) the contribution of formate to interspecies electron transfer is perhaps not that high. The  $\text{CH}_4$ -formation rate in medium with Mo was only  $\sim 1/3$  less than compared to the rate in medium containing both metals. Also here we have to be careful with our conclusions, since  $\text{CO}_2$  reductase activity has not been demonstrated for any of the Mo-containing FDHs so far, while most W-containing FDHs did reduce  $\text{CO}_2$  in vitro (de Bok et al. 2003). So if in there is no residual  $\text{CO}_2$ -reductase activity in *S. fumaroxidans* in W-limited medium, apparently interspecies  $\text{H}_2$  transfer prevails in this situation, but it will need further investigation to confirm this. However,  $\text{H}_2$  is assumed to be the preferred electron carrier in dense aggregated biomass whereas formate is more favourable in suspended cultures (Boone et al. 1989; Schmidt and Ahring 1995). Limitation of W and Mo may also affect the aggregation behaviour of organisms that depend on syntrophic relationships, although such effect has never been reported. Floc formation was observed in



syntrophic co-cultures of *S. fumaroxidans* and *M. hungatei* (de Bok et al. 2002a), and in our experiments we noticed that the formation of aggregates was more evident in cultures without W than in cultures with W (results not shown).

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## Chapter 6

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# *Chapter 7*

**Summary and concluding remarks**

Anaerobic treatment of wastewater is a proven technology that has several advantages. The successful operation of an anaerobic wastewater treatment plant depends on well functioning and balanced microbial communities in the sludge of bioreactors, which consists of fermentative bacteria, homoacetogens and methanogens. Trace metals are extremely important for high-rate bioreactors, due to their roles in key enzymes or cofactors of metabolic pathways, e.g., cobalt in corrinoid of methyltransferases of methanogens and homoacetogens, nickel in F430 of methyl-CoM reductase in methanogens and carbon monoxide dehydrogenase in methanogens and homoacetogens, tungsten and molybdenum in formate dehydrogenase of methanogens and homoacetogens. Addition of these metals in the medium or influent of bioreactors showed the stimulation of growth of microorganisms and an enhanced performance of the wastewater treatment system.

However, proper dosing of these metals as nutrient is a great challenge, since dosing of a metal at a high concentration is toxic for growth of microorganisms and dosing of a specific metal may lead to an out-competition of one group of microorganisms by another. For instance, cobalt dosing caused acidification of a bioreactor under mesophilic conditions, when methanol is the main pollutant (4). Therefore, it is important to get a better understanding of the microorganisms in sludge and their requirement of metals as nutrients for certain physiological functions. The objective of part of the research described in this thesis was to understand the microbial aspects of methanogenesis, and the role of metals on the metabolism of methanogenic consortia, in order to apply the obtained knowledge to optimize trace metal dosing in anaerobic bioreactors, using methanol as model substrate and cobalt as model metal nutrient.

#### *Methanol is converted syntrophically under thermophilic conditions*

As mentioned above, acetate accumulation in the effluent is a problem in the treatment of methanolic wastewater under mesophilic conditions, and caused deterioration of the performance of the bioreactor (4). However, in our previous study, no significant acetate accumulation was observed in a lab-scale thermophilic bioreactor treating synthetic methanol-containing wastewater (7). It was demonstrated, by using specific inhibitors and nuclear magnetic resonance spectroscopy, that besides direct conversion of methanol to methane by methylotrophic methanogens, indirect conversion via  $H_2$  by homoacetogens and hydrogenotrophic methanogens plays an important role (7, 8). This is different from methanol

conversion under mesophilic conditions, which is mainly carried out by *Methanosarcina* species (2). Using 16S rRNA based molecular approaches, it was found that *Methanothermobacter*- and *Methanomethylovorans*-related methanogens, and *Moorella*-related homoacetogens are dominant species in this thermophilic sludge (10). Therefore, the first part of this thesis focused on the isolation and characterization of the dominant microorganisms that play a role in the thermophilic conversion of methanol.

In the research described in **Chapter 2**, a novel methanogen, *Methanomethylovorans* (*Mmv*) *thermophila* strain L2FAW, was isolated from this sludge and characterized as the second thermophilic, obligated methylotrophic, fresh water species (fully-characterized so far) after *Methanosarcina* (*Ms*) *thermophila*. *Mmv. thermophila* grows on methanol with a maximal specific growth rate of  $0.05 \text{ hr}^{-1}$ , which is similar to the growth rate of *Ms. thermophila*. The strain was enriched and isolated by using cobalt-containing medium. The growth on methanol is stimulated by the addition of cobalt; the optimal cobalt concentration is 0.5 to 2  $\mu\text{M}$ . Cobalt is important for direct methanol conversion by this methanogen. Unlike *Ms. thermophila*, *Mmv. thermophila* cannot grow on acetate,  $\text{H}_2/\text{CO}_2$ . Therefore, this strain is specialized in methanol conversion in this sludge.

By using a cobalt-deficient medium, a methanol-degrading culture was enriched from the sludge sample, which contained mainly spore-forming bacteria and long-rod shaped  $\text{H}_2$ -consuming methanogens. Methane is the end product in this enrichment culture when cobalt was absent in the medium (**Chapter 3**). The spore-forming bacterium is characterized as a novel homoacetogen, *Moorella hydrogenoformans*. In pure culture this homoacetogenic bacterium grows on methanol with acetate as main final product, and  $\text{H}_2$  and formate as minor end products. In a coculture with the  $\text{H}_2$ -consuming methanogen (characterized as *Methanothermobacter* sp NJ1), it converted methanol partially to methane and partially to acetate. Remarkably, the dominant end product in this coculture seems to be dependent on the presence of cobalt. If cobalt is present, acetate is the main product; otherwise it is methane (Table 3, **Chapter 3**). This is consistent with the findings of our previous research, in which acetate accumulation from methanol by an enrichment culture (from which these two strains were isolated) increases with an increase of the cobalt concentration in the medium (9).

### *Removal of H<sub>2</sub> is important for methanol conversion*

It is known that most intermediates of the anaerobic digestion process, like ethanol, butyrate, propionate, are only converted when the H<sub>2</sub> partial pressure is kept low by H<sub>2</sub>-consuming methanogens (11). The results described in **Chapter 3** showed that methanol can be converted syntrophically by *Moorella hydrogenoformans*, in a similar manner as other homoacetogens (1, 6). *Moorella hydrogenoformans* grown on methanol produced a substantial amount of H<sub>2</sub>, especially when cobalt is absent from the medium, but acetate is the main end-product. However, when a hydrogenotrophic methanogen is present in the culture, methane is the main product, and less than 10% of methanol is converted to acetate. Obviously, the presence of the methanogen, combined with the absence of cobalt, led to a change in the metabolic route of methanol conversion by homoacetogens.

The mechanism of syntrophic methanol conversion is not clear. *Moorella hydrogenoformans* can grow on carbon monoxide with the formation of H<sub>2</sub>, indicating that an energy converting hydrogenase is present in this homoacetogen. This enzyme was found to exist in many microorganisms, like *E. coli*, *Methanosarcina barkeri*, *Pyrococcus furiosus* and carboxydophilic hydrogenogens (3). In *E. coli*, this enzyme complexes with formate dehydrogenase to form a formate hydrogenlyase that catalyses the conversion of formate to H<sub>2</sub> and CO<sub>2</sub>. This conversion is coupled to the translocation of protons (5). In **Chapter 4**, we demonstrated that *Moorella hydrogenoformans* can grow on formate syntrophically with a H<sub>2</sub>-consuming methanogen, *Methanothermobacter* NJ1. It may have a similar gene cluster of formate hydrogenlyase as found in *Moorella thermoacetica*. Based on above results and the finding by Winter and Ljungdahl (12) that a methanol dehydrogenase might be involved in the oxidation of methanol to formaldehyde or formate, we speculate that the release of reducing equivalents as H<sub>2</sub> by this hydrogenase during methanol oxidation might be a possible mechanism of energy conservation. Under normal growth conditions, homoacetogens obtain energy by formation of acetate. Only under certain conditions, like (in our case) limitation of cobalt, and the presence of methanogens, methanol conversion to H<sub>2</sub> and CO<sub>2</sub> becomes the dominant process.

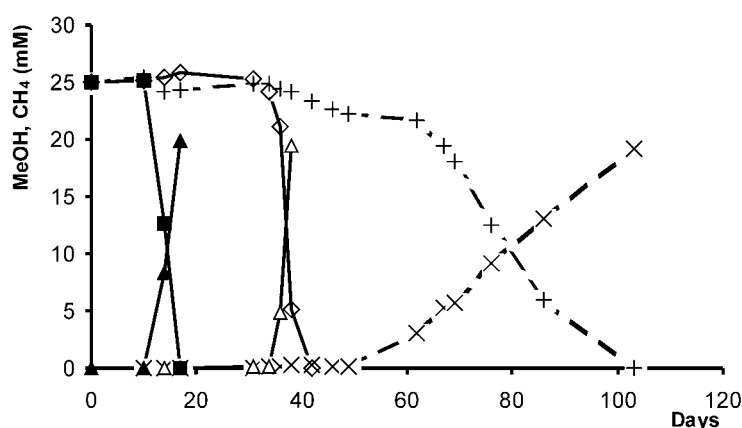
Conversion of methanol to H<sub>2</sub> and CO<sub>2</sub> is thermodynamically unfavorable. Therefore, interspecies electron transfer plays a crucial role in this type of methanol conversion. Electrons are normally transferred as H<sub>2</sub>, but formate transfer was proposed as a possible



mechanism as well (11). The importance of  $H_2$  and formate transfer in syntrophic interaction using propionate oxidation by *Syntrophobacter fumaroxidans* and *Methanospirillum hungatei* as a model was studied in **Chapter 6**. It is found that the methane formation rate from propionate by this coculture correlates with either hydrogenase or formate dehydrogenase activity levels in both microorganisms. The FDH activity in cells of *M. hungatei* grown in molybdenum and tungsten deficient medium is negligible and in *S. fumaroxidans* cells the FDH activity is low. However, methane is still formed by this coculture at relative high rate (20% of that by the coculture grown in non-deficient medium). These results indicated that interspecies  $H_2$  transfer is possible as the only mechanism, but that formate transfer might result in a higher rate of propionate oxidation.

#### *Cobalt can regulate the route of methanol conversion*

Cobalt is essential for the metabolism of methanol, because of its role in corrinoid dependent methyltransferase in the methanogenic and the acetyl-CoA pathways. The importance of cobalt can be seen in the Fig 1. The presence (or amendment) of cobalt resulted a fast methanol degradation and methane formation by a thermophilic enrichment culture. On the other hand, when the culture was grown in the absence of cobalt methanol was still converted to methane after long lag phase and at a much slower rate. Starting from these cultures, *Mvv. thermophila* was isolated from an enrichment culture by using cobalt sufficient



**Fig. 1** The importance of cobalt on the methanol degradation and methane formation by a thermophilic enrichment culture. Symbols: ■: methanol; ▲: methane. Solid lines: culture grown in the presence of 0.5  $\mu$ M cobalt; Dot lines: culture grown in the absence of cobalt in the first 33<sup>rd</sup> days and amended with 0.5  $\mu$ M cobalt at the 33<sup>rd</sup> day; Dashed lines: culture grown in the absence of cobalt.

medium (**Chapter 2**). On the other hand, a syntrophic coculture was enriched by using cobalt deficient medium, from which *M. hydrogenoformans* and *Methanothermobacter* sp. NJ1 were isolated (**Chapter 3**). Optimal cobalt concentration for *M. thermophila* was around 0.5 to 2  $\mu\text{M}$  (**Chapter 2**). At suboptimal conditions, the growth rate of *M. thermophila* is linearly related to the cobalt concentration in the medium (data not show). Although we did not test the optimal cobalt concentration for *M. hydrogenoformans*, its requirement for cobalt in pure culture seems to be high. However, the requirement of cobalt by a coculture of *M. hydrogenoformans* and *Methanothermobacter* sp. NJ1 seems to be low. In fact, addition of cobalt stimulated the formation of acetate (**Chapter 3**, and (9)). The optimal cobalt concentration for syntrophic methanol conversion by an enrichment culture was around 0.1  $\mu\text{M}$ ; at this concentration little acetate accumulated (9). Therefore, cobalt plays a role in the regulation of the pathway of methanol conversion in this coculture: to methanol oxidation to  $\text{H}_2$  and  $\text{CO}_2$  at low cobalt concentration, or to direct methane formation or acetate formation at a high cobalt concentration. This can be used to explain why acetate always accumulates in the effluent of anaerobic bioreactors treating methanolic wastewater upon the addition of cobalt.

#### *Cobalt availability can be affected by nickel*

Mostly, cobalt and nickel share uptake transporters due to their similar chemical properties. However, these metals have different role in the metabolic pathways of methanogenic archaea and homoacetogens. Precipitation of cobalt and nickel by sulfide can severely influence their bioavailability. The effect of cobalt and nickel on the corrinoid and F430 content and on growth of *Methanosarcina barkeri* on methanol was studied in **Chapter 5**. Metal sulfide precipitation was prevented by the addition of EDTA to the media. This enabled the direct determination of the cell metal content. Stimulation of uptake of cobalt and nickel by addition of EDTA was demonstrated by the increase of the corrinoid and F430 content. A direct link of cell cobalt content and corrinoid content with growth rate at sub-optimal cobalt concentration was found. Limitation of nickel on growth on methanol was observed, when cobalt was added in excess. Most interestingly, competitive uptake of cobalt and nickel was demonstrated. This is of importance for the optimization of trace metal dosage for anaerobic treatment process, as was discussed in **Chapter 5**.

### Implications for practice

The results obtained from the research described in this thesis can be applied to optimize metal dosage of anaerobic bioreactors in practice.

- A. It is extremely important to understand the dominant bacterial population of the sludge and the corresponding biodegradation pathways. For example, the requirement of cobalt for the direct methanol conversion is about 10 times higher than that for syntrophic methanol conversion via hydrogen (**Chapter 2, 3, and (9)**). Overdosing of cobalt to stimulate the direct methanol conversion may cause acetate accumulation by homoacetogenic bacteria (**Chapter 3**).
- B. It is also important to maintain balanced consortia in the sludge, especially the H<sub>2</sub>-consuming methanogens, by means of dosing of metals like nickel, tungsten and molybdenum. Maintaining a low H<sub>2</sub> partial pressure is essential for the degradation of intermediates of anaerobic digestion. Syntrophic methanol degradation also needs an efficient removal of H<sub>2</sub> (**Chapter 3, 4 & 5**). Uncoupled H<sub>2</sub> removal and formation may result in an accumulation of acetate.
- C. Due to competitive uptake and antagonistic effect of different metals, e.g. cobalt and nickel (Chapter 5), tungsten and molybdenum (Chapter 6), balanced dosing of all metals required is essential to maintain a high biological activity. Overdosing of a metal may not only cause toxicity of this metal, but also inhibit the uptake of another essential metal.

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# *Samenvatting*

Anaërobe biologische afvalwaterzuivering is een bewezen technologie met belangrijke voordelen. Voor het optimaal functioneren is een anaërobe afvalwaterzuiveringsinstallatie afhankelijk van gebalanceerde microbiële consortia in het reactor slib. Het gaat hierbij om fermentatieve bacteriën, homoacetogenen en methanogenen. Spore-elementen zijn zeer belangrijk voor hoge omzettingssnelheden in bioreactoren, doordat zij deel uitmaken van enzymen en co-factoren met een centrale rol in de metabole afbraak routes. Kobalt is essentieel in het corrinoid van methyl-transferases van methanogenen en homo-acetogenen. Nikkel is essentieel voor de werking van koolmonoxide dehydrogenases en in F430 als co-factor voor methyl-CoM reductase van methanogenen. Wolfraam en molybdeen zijn veel voorkomend in de actieve centra van formiaat dehydrogenases. Toevoeging van deze metalen aan het medium of het influent van bioreactoren zorgt voor een stimulatie van de groei van biomassa en een verhoogde activiteit.

Het toevoegen van de spore-elementen in de juiste dosering is echter een grote uitdaging, doordat hoge concentraties van spore-elementen remmend kunnen werken op de groei van de micro-organismen. Bovendien kan de dosering van een specifiek element tot overheersing van een bepaalde groep van micro-organismen leiden. Kobalt dosering kan bijvoorbeeld leiden tot een verzuring van de bioreactor door vorming van acetaat, zoals beschreven is voor een mesofiele bioreactor met methanol als belangrijkste verontreiniging in het afvalwater (4). Een goed inzicht van de samenstelling van de microbiële populatie van het reactorslib en de spore- elementen behoefte van de micro-organismen is daarom van groot belang. Deel van het hier beschreven onderzoek was gericht op het beter begrijpen van de microbiële achtergrond van methaanvorming uit methanol als substraat en de rol van spore-elementen, in het bijzonder kobalt, met als doel op de methanogene consortia, om tot een betere spore-elementendosering in de praktijk te komen.

#### *Methanol wordt syntroof omgezet onder thermofiele condities*

Zoals genoemd is acetaatvorming een probleem in de behandeling van afvalwater in mesofiele reactoren. Het zorgt voor een afname van de activiteit van de bioreactor (4). Acetaatvorming werd niet waargenomen onder thermofiele condities in lab-schaal reactoren en artificieel methanol bevattend afvalwater (7). Met NMR en het gebruik van specifieke remmers werd aangetoond dat naast de directe omzetting van methanol door methylotrofe methanogenen, methanol vooral ook indirect werd omgezet via  $H_2$  naar methaan door

homoacetogenen en waterstof consumerende methanogenen (7,8). Dit verschilt van de omzetting onder mesofiele condities waar methylotrofe methanogenen van het genus *Methanosarcina* voor de omzetting van methanol zorgen (2). Met behulp van op 16S rRNA gebaseerde moleculaire technieken werd gevonden dat methanogenen uit de genera *Methanothermobacter* en *Methanomethylovorans*, en homoacetogenen uit het genus *Moorella*, dominant aanwezig waren in het thermofiele slib (10). De isolatie en karakterisatie van deze dominante micro-organismen is beschreven in het eerste deel van dit proefschrift.

**Hoofdstuk 2** beschrijft de isolatie en karakterisatie van een tweede bekende thermofiele, obligaat methylotrofe, zoetwater methanogeen, *Methanomethylovorans (Mmv) thermophila* stam L2FAW, na *Methanosarcina (Ms) thermophila*. *Mmv. thermophila* groeit op methanol met een maximale specifieke groeisnelheid van  $0.05 \text{ h}^{-1}$ , hetgeen overeenkomt met de groeisnelheid van *Ms. thermophila*. *Mmv. thermophila* werd geïsoleerd uit een ophopingscultuur waarin kobalt aanwezig was. Een optimale kobaltconcentratie voor groei van  $0.5 - 2.0 \text{ } \mu\text{M}$  werd vastgesteld. Kobalt is belangrijk voor de directe methanol omzetting door deze methylotrofe methanogeen. In tegenstelling tot *Ms. thermophila*, kan *Mmv. thermophila* niet groeien met acetaat of  $\text{H}_2/\text{CO}_2$  als substraat. *Mmv. thermophila* is dus gespecialiseerd in methanol omzetting in het bestudeerde reactor slib.

Wanneer kobalt afwezig was in het medium werd een ophopingscultuur verkregen die methaan vormde uit methanol en voornamelijk bestond uit sporenvormende bacteriën en lange staafvormige  $\text{H}_2$ -consumerende methanogenen (**Hoofdstuk 3**). De sporenvormende bacterie werd geïsoleerd en gekarakteriseerd als een nieuwe homoacetogeen, *Moorella hydrogenoformans*. In reïncultuur vormt deze bacterie voornamelijk acetaat uit methanol, en kleine hoeveelheden formiaat en  $\text{H}_2$ . De  $\text{H}_2$ -consumerende methanogeen werd gekarakteriseerd als een *Methanothermobacter* stam NJ1. De cocultuur van deze methanogeen en de homoacetogeen, vormde deels methaan en deels acetaat met methanol als substraat. De kobaltconcentratie bleek van grote invloed te zijn op de verhouding van gevormd methaan en acetaat. In aanwezigheid van kobalt werd voornamelijk acetaat gevormd, terwijl voornamelijk methaan wordt gevormd als kobalt afwezig is (Tabel 3, **Hoofdstuk 3**). Dit komt overeen met resultaten van eerder onderzoek waarin accumulatie van acetaat correleerde met de kobaltconcentratie in de ophopingscultuur waaruit beide organismen werden geïsoleerd (9).

*Verwijdering van  $H_2$  is van belang voor methanolomzetting.*

Het is bekend dat een lage waterstofspanning essentieel is voor de afbraak van belangrijke intermediären, zoals ethanol, butyraat en propionaat in de anaërobe afbraak. Een lage waterstofspanning wordt bereikt met waterstof-consumerende methanogene archaea (11). De resultaten die zijn beschreven in **Hoofdstuk 3** laten zien dat methanol omgezet kan worden door *Moorella hydrogenoformans*, in syntrofe samenwerking met een methanogeen (1, 6). Met methanol als substraat wordt vooral acetaat gevormd door reïncultures van *Moorella hydrogenoformans*, maar ook een substantieel deel waterstof wordt gevormd, vooral als kobalt wordt weggelaten uit het medium. Als een methanogeen aanwezig is in hetzelfde medium dan wordt voornamelijk methaan gevormd; minder dan 10% van de methanol wordt dan nog omgezet in acetaat. Het is duidelijk dat de aanwezigheid van een methanogeen en de afwezigheid van kobalt in het medium leidt tot een verandering van de metabole route voor methanol omzetting door homoacetogenen.

Het is onduidelijk waar in de syntrofe afbraak van methanol door *Moorella hydrogenoformans* energie, nodig voor groei wordt geconserveerd. Mogelijk speelt een energie conserverende hydrogenase hierin een rol. *Moorella hydrogenoformans* kan  $CO$  met  $H_2O$  omzetten in  $H_2$  en  $CO_2$ , een teken dat een energie conserverende hydrogenase aanwezig is in dit organisme (3). Dit type hydrogenase is aanwezig in meerdere micro-organismen, zoals *Escherichia coli*, *Methanosarcina barkeri*, *Pyrococcus furiosus*, *Rhodospirillum rubrum* en *Carboxydotherrnus hydrogenoformans*, waarin het energie conserveert door middel van de oxidatie van verschillende substraten. In *E. coli* vormt de energie conserverende hydrogenase een enzym complex, bekend als het formiaat-waterstof lyase, met een formiaat dehydrogenase, dat de omzetting van formiaat naar  $H_2$  en  $CO_2$  katalyseert. Energie uit deze omzetting wordt opgeslagen door middel van een gelijktijdige translocatie van protonen over de celmembraan (5). In **Hoofdstuk 4** hebben we laten zien dat *Moorella hydrogenoformans* kan groeien met formiaat als substraat en een waterstof consumerende methanogeen, *Methanothermobacter* NJ1, als syntrofe partner. *Moorella hydrogenoformans* beschikt mogelijk over een zelfde formiaat-waterstof lyase gencluster zoals gevonden in het genoom van *Moorella thermoacetica*. Gebaseerd op dit en op de bevindingen van Winter en Ljungdahl (12) dat zeer waarschijnlijk een methanol dehydrogenase betrokken is bij de omzetting van methanol tot formaldehyde of formiaat, lijkt het waarschijnlijk dat een formiaat-waterstof

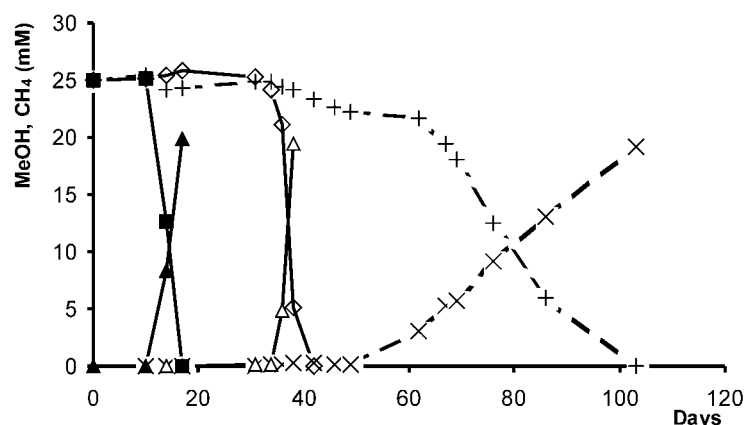


lyase verantwoordelijk is voor de vorming van waterstof en conservering van energie bij de omzetting van methanol door *Moorella hydrogenoformans*. Onder standaard condities halen homoacetogene bacteriën energie uit de vorming van acetaat. Wanneer de beschikbaarheid van kobalt gelimiteerd is en methanogenen aanwezig zijn, wordt de vorming van H<sub>2</sub> en CO<sub>2</sub> door de homoacetogeen een dominant proces.

De omzetting van methanol in H<sub>2</sub> en CO<sub>2</sub> is thermodynamisch ongunstig als de producten ophopen. Daarom is interspecies elektronentransport cruciaal voor deze omzetting. De overdracht vindt vaak plaats via H<sub>2</sub>, maar ook de overdracht via formiaat is voorgesteld als mogelijk mechanisme (11). De syntrofe afbraak van propionaat door *Syntrophobacter fumaroxidans* en *Methanospirillum hungatei* werd bestudeerd als model voor H<sub>2</sub> en formiaat overdracht in **Hoofdstuk 6**. Methaan vorming door deze cocultuur uit propionaat correleerde met hydrogenase- of met formiaat dehydrogenase activiteit van beide organismen. De formiaat dehydrogenase activiteit in cellen van *M. hungatei* die waren gekweekt in medium zonder molybdeen en wolfraam, was verwaarloosbaar en zeer laag in vergelijking met cellen van *S. fumaroxidans*. Deze cocultuur vormde toch methaan met relatief hoge snelheid (20% ten opzichte van een cocultuur met standaard molybdeen en wolfraam). Deze resultaten laten zien dat elektronenoverdracht met H<sub>2</sub> mogelijk is als enige mechanisme, maar dat formiaatoverdracht mogelijk leidt tot een hogere afbraaksnelheid van propionaat.

#### *Kobalt reguleert de route van methanolomzetting*

Kobalt is essentieel voor de afbraak van methanol, omdat het onmisbaar is voor de werking van het corrinoidafhankelijke methyltransferase, dat een belangrijke rol speelt in methanogene en acetogene metabole routes. Het belang van kobalt blijkt uit Figuur 1. Aanwezigheid van kobalt, of latere toevoeging van kobalt aan medium zonder kobalt, resulteert in een snelle afbraak van methanol en de vorming van methaan, door een thermofiele ophopingscultuur. Zonder kobalt vindt ook methanol afbraak en methaanvorming plaats, maar met duidelijk langere lag-fase en met lagere snelheid. Uit de ophopingscultuur met kobalt werd *Mmv. thermophila* geïsoleerd (**Hoofdstuk 2**). Uit dezelfde ophopingscultuur, zonder kobalt, werden *Moorella hydrogenoformans* en *Methanothermobacter* sp. NJ1 geïsoleerd (**Hoofdstuk 3**). De optimale kobaltconcentratie voor *Mmv. thermophila* lag rond de 0.5 – 2.0 µM (**Hoofdstuk 2**). Bij suboptimale kobaltconcentraties is de groeisnelheid van *Mmv. thermophila* lineair daaraan gekoppeld (data niet gegeven). Hoewel de optimale



**Fig. 1** Het effect van kobalt op methanolafbraak (■,+) en methaanvorming (▲,×) door een thermofiele ophopingscultuur. Kobalt was aanwezig in een concentratie van 0.5  $\mu\text{M}$  (dichte symbolen), werd toegevoegd na 33 dagen (open symbolen), of was afwezig (stippel lijn).

kobaltconcentratie voor *Moorella hydrogenoformans* niet is getest, lijkt deze hoog te zijn voor een reïncultuur. Daarentegen is voor een methaanvormende cocultuur van *Moorella hydrogenoformans* met *Methanothermobacter* stam NJ1 de vereiste kobaltconcentratie laag. Sterker nog, toevoeging van kobalt aan de cocultuur verhoogde de acetaatvorming (**Hoofdstuk 3**)(9). De optimale kobaltconcentratie voor syntrofe methanolomzetting tot methaan door de ophopingscultuur lag rond de 0.1  $\mu\text{M}$ ; bij deze concentratie werd weinig acetaat gevormd (9). Hieruit blijkt dat kobalt een belangrijke rol speelt in de regulatie van het mechanisme achter de methanolomzetting door deze ophopingscultuur. Bij lage kobaltconcentraties wordt methanol omgezet tot  $\text{H}_2$  en  $\text{CO}_2$ , waaruit vervolgens methaan gevormd wordt. Bij hoge kobaltconcentraties wordt acetaat gevormd. Dit verklaart waarom na toevoeging van kobalt, acetaat ophoopt in het effluent van anaërobe bioreactoren die methanol bevattend afvalwater verwerken.

*Kobalt beschikbaarheid wordt beïnvloed door nikkel.*

Over het algemeen worden kobalt en nikkel vanwege hun vergelijkbare chemische eigenschappen door dezelfde membraantransporteiwitten opgenomen in de cel. Het neerslaan van nikkel en kobalt als sulfide precipitaten kan hun bio-beschikbaarheid sterk beïnvloeden. Beide elementen hebben elk hun eigen rol in de metabole routes van methanogene archaea en

homoacetogene bacteriën. Het effect van kobalt en nikkel op het corrinoid en F430 gehalte van cellen, en op de groei van *Methanosarcina barkeri* met methanol is bestudeerd in **Hoofdstuk 5**. Door toevoegen van EDTA aan het medium werd het neerslaan van metaalsulfideprecipitaten verhinderd. Daardoor was het mogelijk het metaal gehalte van cellen te bepalen. De stimulerende invloed van EDTA op kobalt en nikkel opname door cellen bleek uit een hogere corrinoid en F430 gehalte. Verder bleek een direct verband te bestaan tussen kobalt en corrinoid gehalte in cellen die gekweekt werden bij suboptimale kobaltconcentraties. Nikkel beschikbaarheid werd limiterend voor groei bij een overmatige kobalt dosering aan het medium. De opname van kobalt en nikkel bleek competitief. Deze waarneming is van belang voor een juiste dosering van spore-elementen aan anaërobe bioreactoren (**Hoofdstuk 5**).

#### *Toepassing in de praktijk*

De bevindingen uit deze studie zijn van belang voor een optimale spore-element dosering aan anaërobe bioreactoren in de praktijk.

- A. Kennis van de dominante bacteriële populatie en afbraakroutes in het reactorslib is zeer belangrijk. Bijvoorbeeld, de kobaltconcentratie nodig voor directe methanolomzetting naar methaan, is een factor 10 hoger dan voor syntrofe methanolomzetting via waterstof (**Hoofdstuk 2, 3**)(9). Een hogere dosering van kobalt om directe methaanvorming te stimuleren kan ook leiden tot acetaatvorming door homoacetogene bacteriën (**Hoofdstuk 3**).
- B. Het is belangrijk om de consortia van methanogenen en homoacetogenen in het reactorslib in balans te houden, en vooral die van de H<sub>2</sub>-consumerende methanogenen, door middel van de dosering van nikkel, wolfram en molybdeen. Het handhaven van een lage waterstofspanning is essentieel voor een volledige afbraak van de intermediären die worden gevormd in de anaërobe afbraak. Een lage waterstofspanning is ook essentieel voor de syntrofe afbraak van methanol (**Hoofdstuk 3, 4, 5**). Een onbalans in de reactorpopulatie kan leiden tot een hogere waterstofspanning en daardoor tot acetaatvorming.

- C. Door competitieve opname tussen, en antagonistische van, de verschillende spore-elementen, b.v. kobalt en nikkel (Hoofdstuk 5) of wolfraam en molybdeen (Hoofdstuk 6), is een uitgebalanceerde dosering van alle spore-elementen noodzakelijk voor een hoge biologische activiteit. De overdosering van een enkel element kan niet alleen de toxiciteit door dit element, maar ook de verhindering van de opname van een ander essentieel element tot gevolg hebben.

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## *Chapter 7*

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