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5th Workshop on Fats and Oils as Renewable Feedstock for the Chemical Industry

Deoxygenation of stearic acid in the absence of H₂

The relevance of the anhydride reaction pathway



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FOOD & BIODESIGN
WAGENINGEN UR



Universiteit Utrecht

Smart
Mix

Vegetable oils



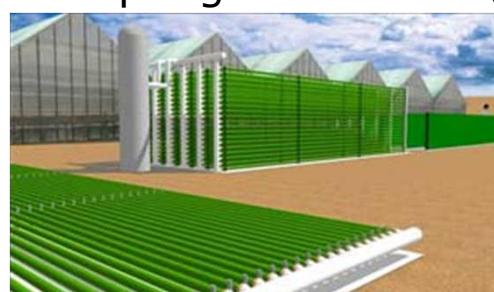
- Wide variety of sources for vegetable oils
 - For instance: Sunflower oil, Soybean oil, Palm oil and Rapeseed oil



→ Land use issues;
food vs. fuel



- Algae oil
 - Possible solution to these problems in future
 - No direct competition with food production
 - Rapid growth rates (10-200 times faster than terrestrial oil crops)^{1,2}



→ AlgaePARC Wageningen UR

¹ Huber et. al., *Chem. Rev.* 2006, 106, 4044-4098

² Christi, *Biotechnol. Adv.* 2007, 25, 294-306

State of the art

1st generation biodiesel



- 1st generation biodiesel: fatty acid methyl esters (FAME)
 - Derived from vegetable oils
 - Produced via transesterification of triglycerides with methanol

- Concerns
 - High purity feedstocks are necessary
 - Engine compatibility issues
 - Lower heat content
 - Poor storage stability



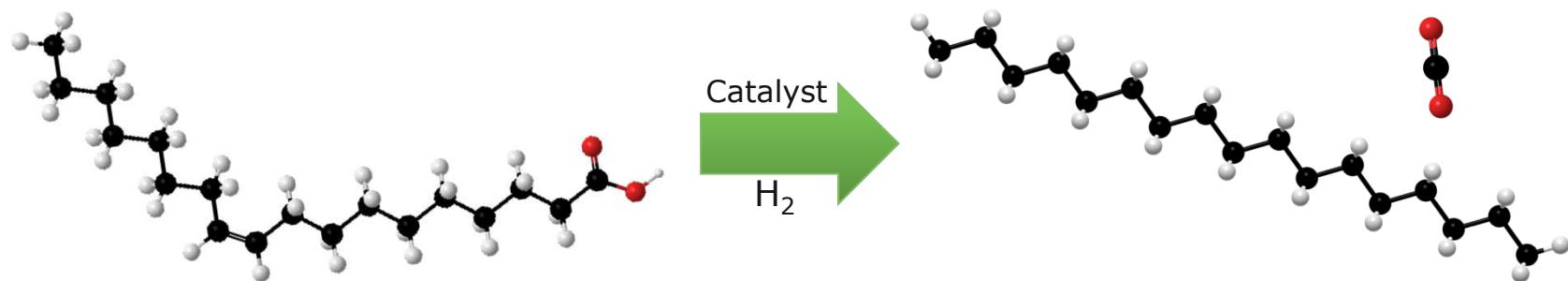
State of the art

2nd generation biodiesel



■ 2nd generation biodiesel

- Derived from vegetable oils or other fatty acid derivatives
- Via catalytic hydrodeoxygenation using hydrogen



■ Advantages

- Low purity feedstocks possible
- Higher fuel quality (heat content and storage stability)
- Fully compatible with existing vehicles and infrastructure

■ Concerns

- Process requires (non-renewable) H₂
 - Reduction of double bond functionalities
 - Hydrodeoxygenation of glycerol to propane,
- Process at elevated P and T (3-10 MPa, 553-618 K)

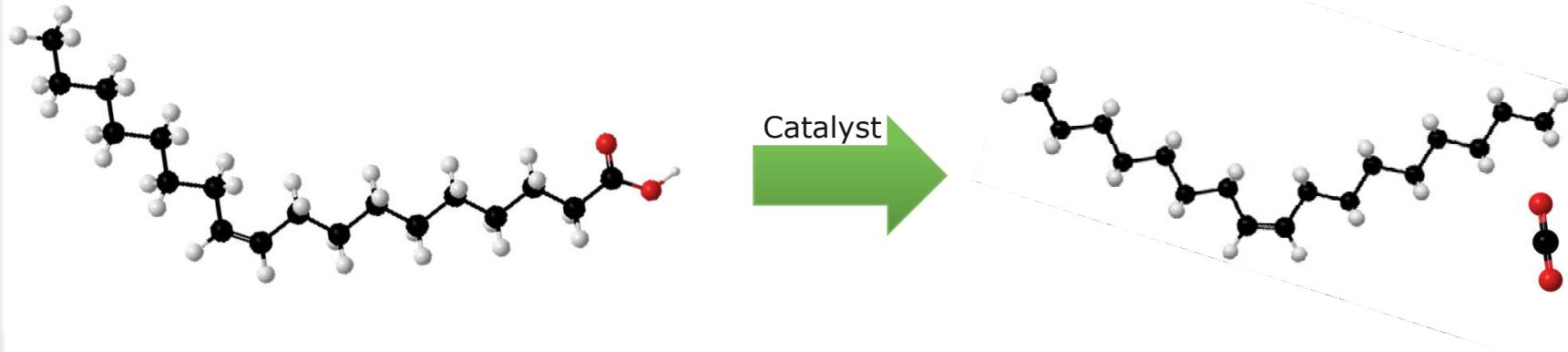
State of the art

Introduction to the project

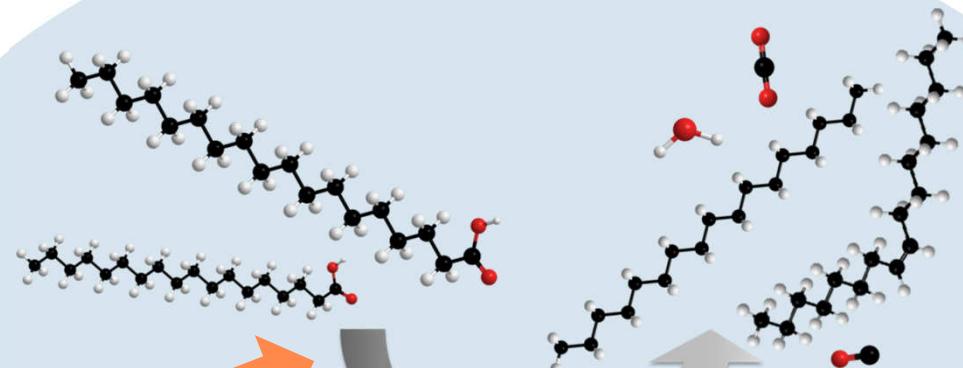


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- A superior process would be the catalytic deoxygenation of fatty acids:
 - At low temperature (< 523 K)
 - With low/no hydrogen consumption
 - Yielding unsaturated hydrocarbons



- Advantages:
 - Excellent low-temperature properties as a fuel
 - Possible applications as chemical building blocks
 - Potential for glycerol valorization



Reaction Pathways
and Intermediates

- Activity & Selectivity
 - Influence of feed conc.
- Deoxygenation reactions
 - Stearic anhydride intermediate

Catalyst:

4.5 wt% Pd/ γ -Al₂O₃ (BASF)

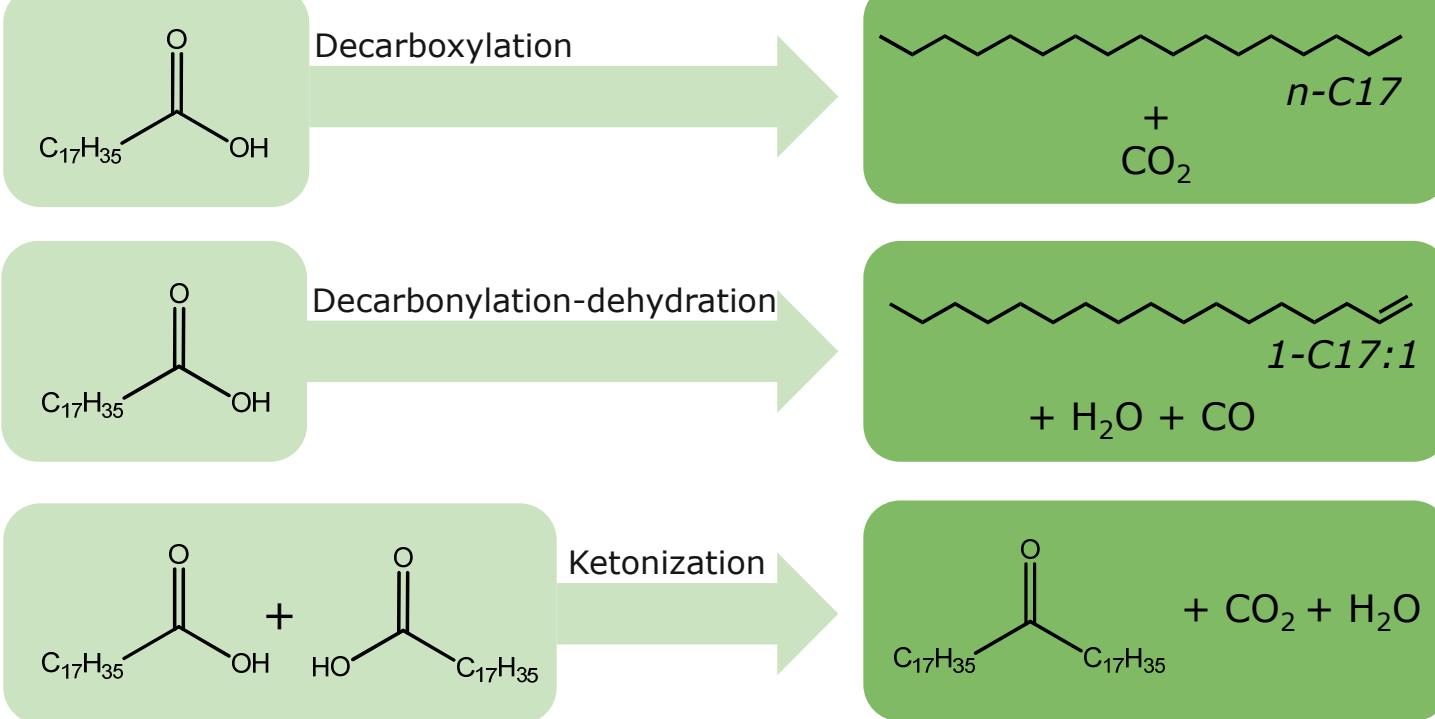
Surface area: 111 m²/g
Av. Particle size: 6.7 nm
Dispersion: 17 %

Deoxygenation reactions

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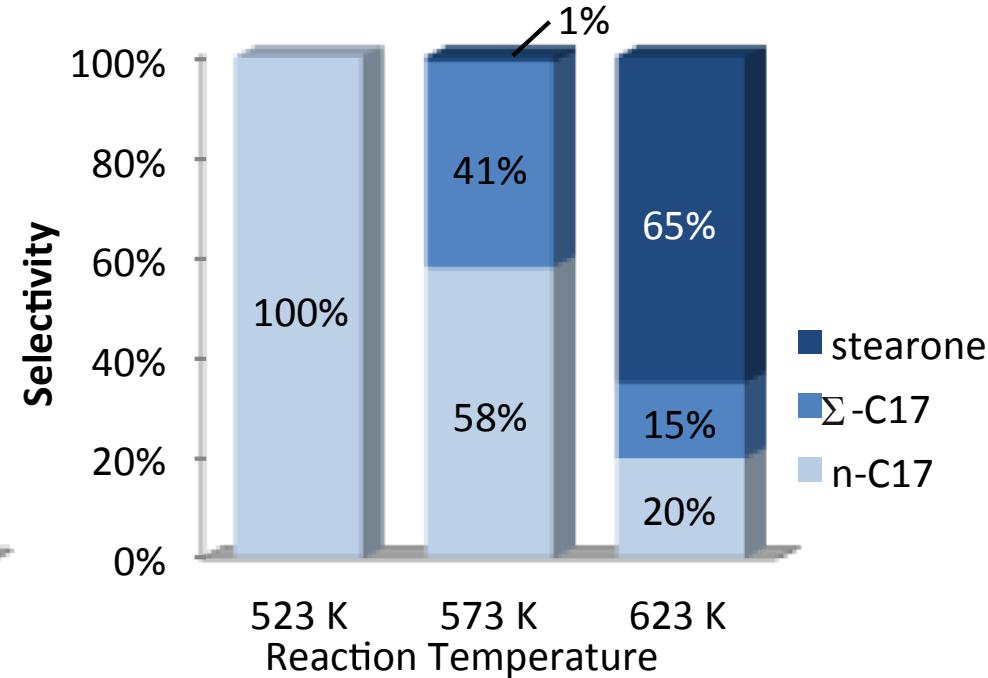
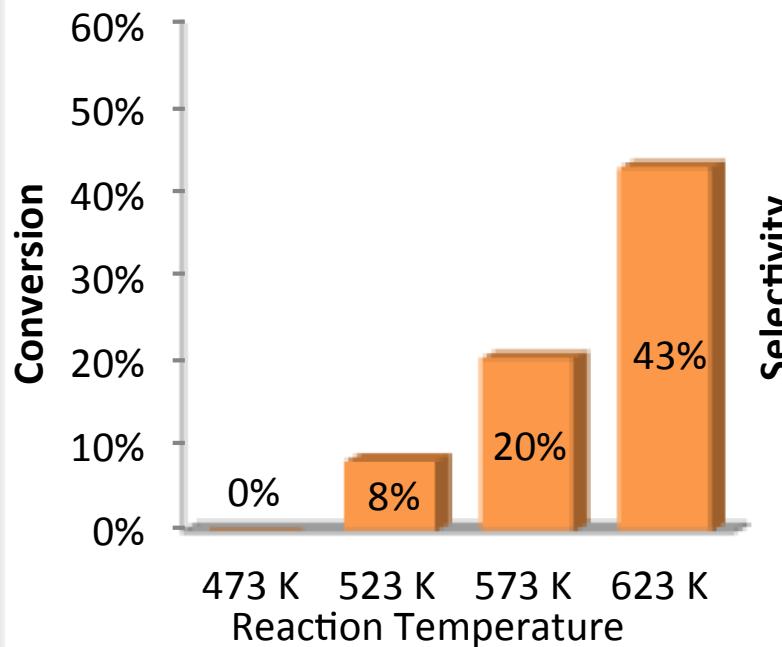


Results

Influence of temperature



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- Lowest deoxygenation temperature at 523 K
 - *Heptadecane formed selectively*

Reaction conditions:

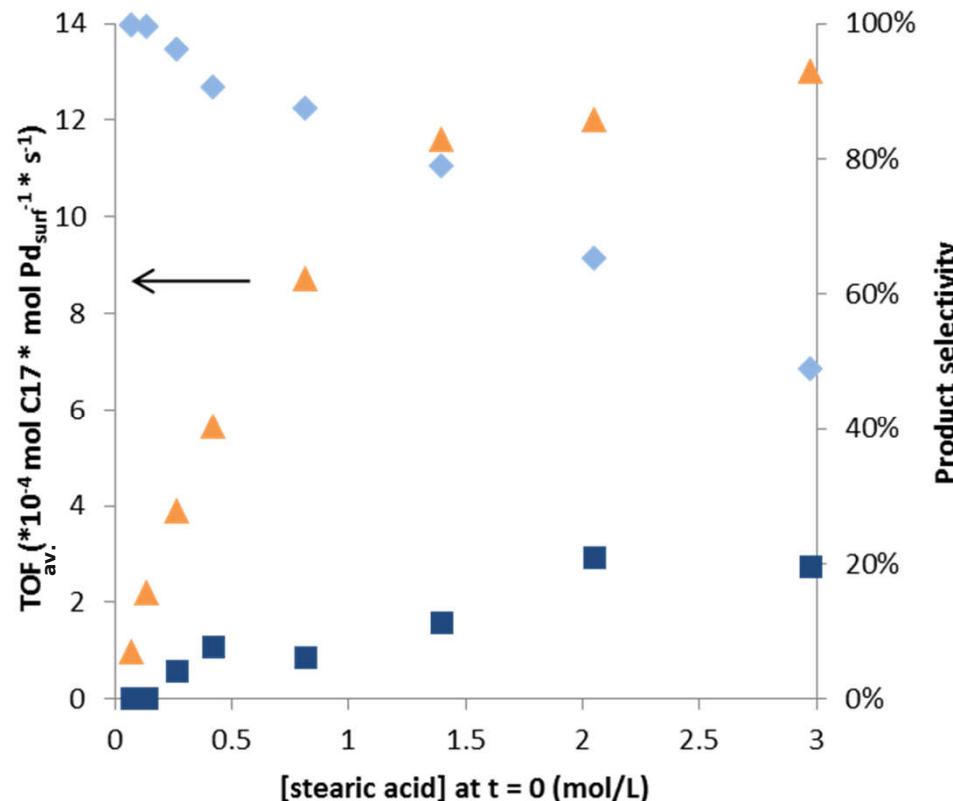
Catalyst: $\text{Pd}/\gamma\text{-Al}_2\text{O}_3$
 Solvent: *dodecane*
 Feed conc.: 0.14 mol L^{-1}
 Reaction time: 6 h
 Pressure: 7 bar N_2

Catalyst Activity & Selectivity



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Influence of stearic acid concentration at 523 K



Reaction conditions:

Catalyst: Pd/ γ -Al₂O₃
 Solvent: dodecane
 Reaction temperature: 523 K
 Reaction time: 24h
 Pressure: 7 bar N₂

- Selective decarboxylation at low (<0.25 mol/L) stearic acid conc.
- >0.25 mol/L: Selectivity to n-C17 decreases
 - Decarbonylation products are formed
 - Ketonization to stearone

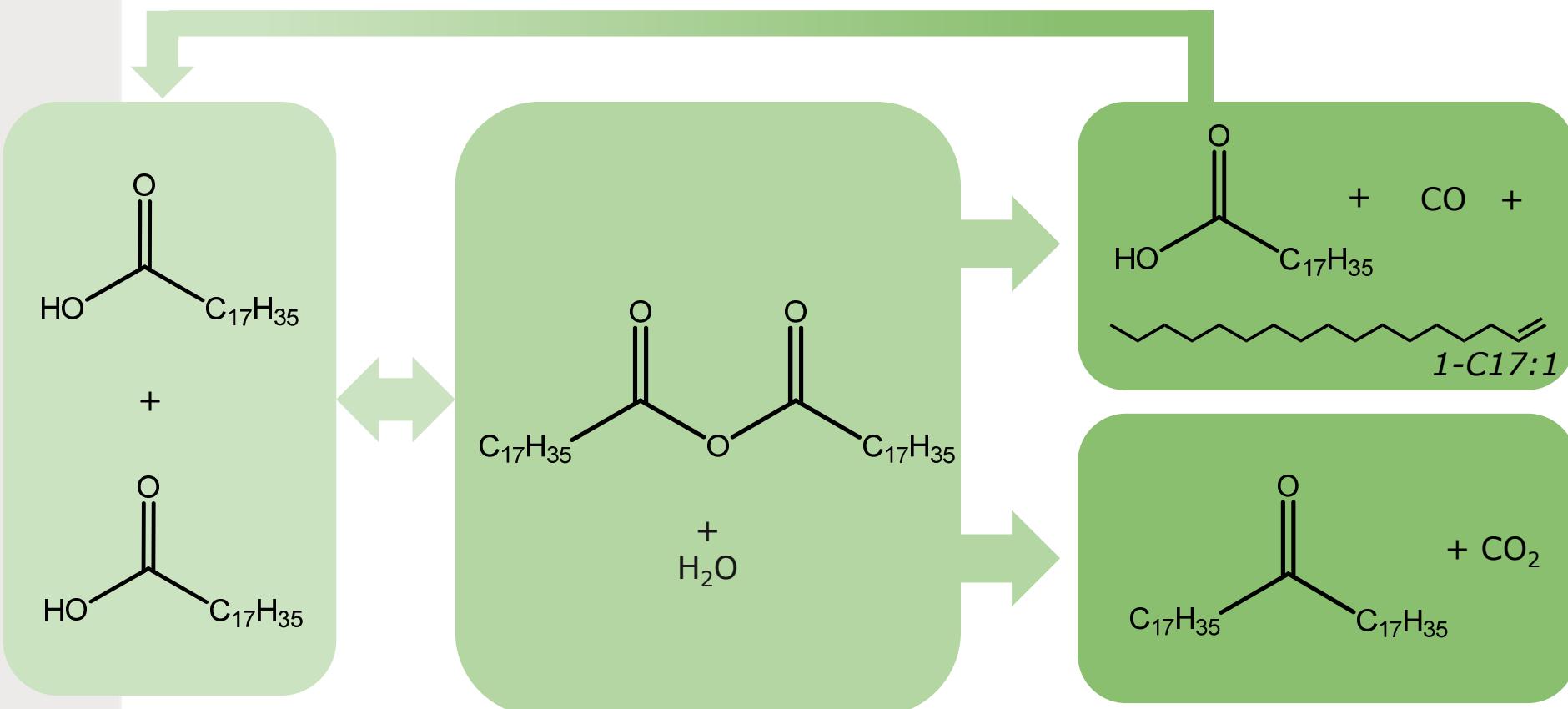
Anhydride intermediate



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Hypothesis

- Possible explanation: Stearic anhydride as intermediate product
- Literature: Stearic anhydride suggested as intermediate product in homogeneous decarbonylation and ketonization reaction of stearic acid^{1,2}



¹ Foglia et. al., *J. Am. Oil Chem. Soc.* 1976, 53, 737-741

² Miller et. al., *J. Org. Chem.* 1993, 58, 18-20

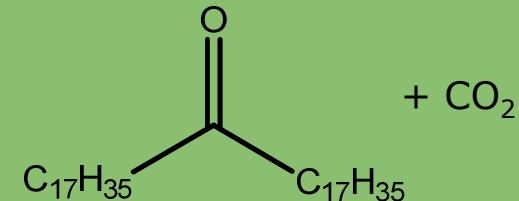
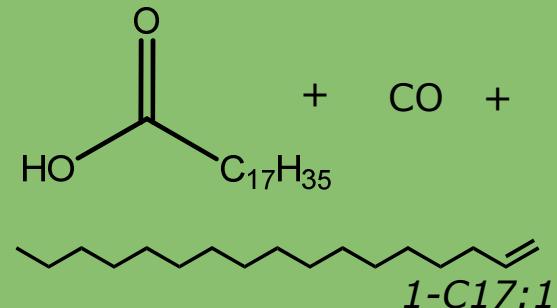
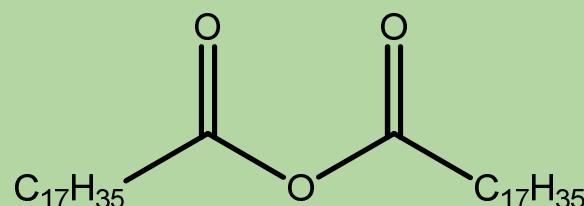
Anhydride intermediate



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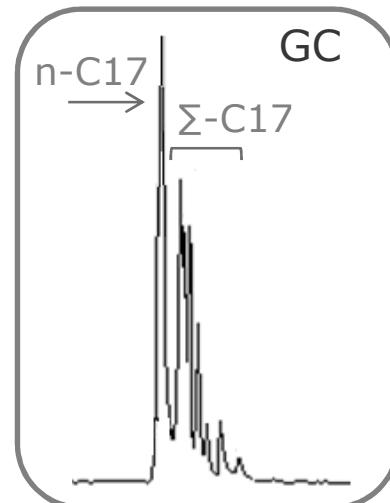
Model reaction

- Reaction with stearic acid anhydride gives 100% conversion to:
 - Stearic acid
 - Heptadecenes (Σ -C17)
 - Heptadecane (n -C17)
 - Stearone (C35)



Reaction conditions:

0.14 mol/L stearic anhydride
523 K, 24h, 7 bar N₂

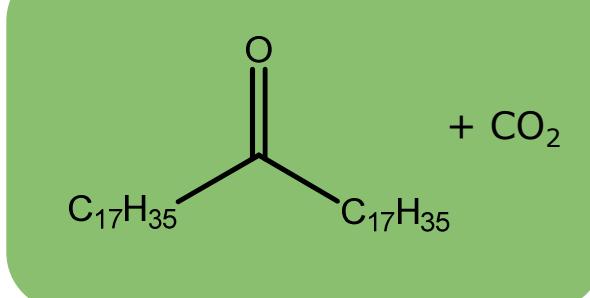
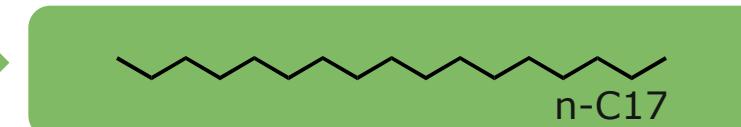
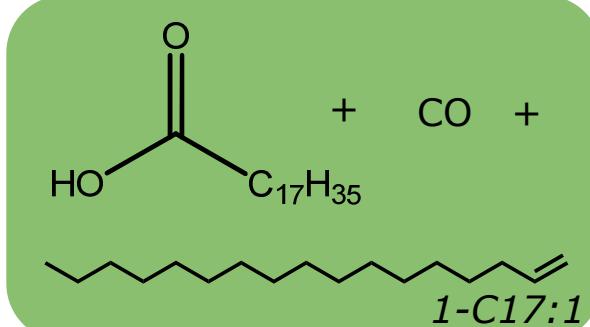


Anhydride intermediate



Model reaction

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Reaction conditions:
0.14 mol/L stearic anhydride
523 K, 24h, 7 bar N₂

Anhydride intermediate

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Overview model reactions



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| Catalyst | Stearic anhydride (g) | Reaction Temp (K) | Reaction time (h) | Conversion (%) | Selectivity (%) | | | | |
|--|-----------------------|-------------------|-------------------|----------------|-----------------|---------------|----|-----|---------|
| | | | | | n-C17 | Σ -C17 | SA | C35 | heavies |
| Pd/ γ -Al ₂ O ₃ | 1.0 | 523 | 5 | 98 | 7 | 42 | 49 | 2 | 0 |
| Pd/ γ -Al ₂ O ₃ | 1.0 | 523 | 24 | 100 | 27 | 25 | 46 | 2 | 0 |
| γ -Al ₂ O ₃ | 1.0 | 523 | 24 | 80 | 0 | 1 | 71 | 28 | 0 |
| none | 1.0 | 523 | 24 | 40 | 0 | 1 | 58 | 26 | 15 |
| Pd/ γ -Al ₂ O ₃ | 10.0 | 523 | 24 | 62 | 14 | 20 | 35 | 12 | 19 |
| Pd/ γ -Al ₂ O ₃ | 1.0 | 473 | 24 | 48 | 4 | 47 | 49 | 0 | 0 |

- Decarbonylation 10 times faster than when starting from stearic acid
 - Anhydride formation from stearic acid rate limiting step
- Pd essential for decarbonylation to HC's.
 - Stearone and other heavies are formed in absence of Palladium
- High anhydride concentration: increase in side product formation
- Stearic anhydride is also converted at 473 K
 - Potential for low temperature decarbonylation of stearic acid?

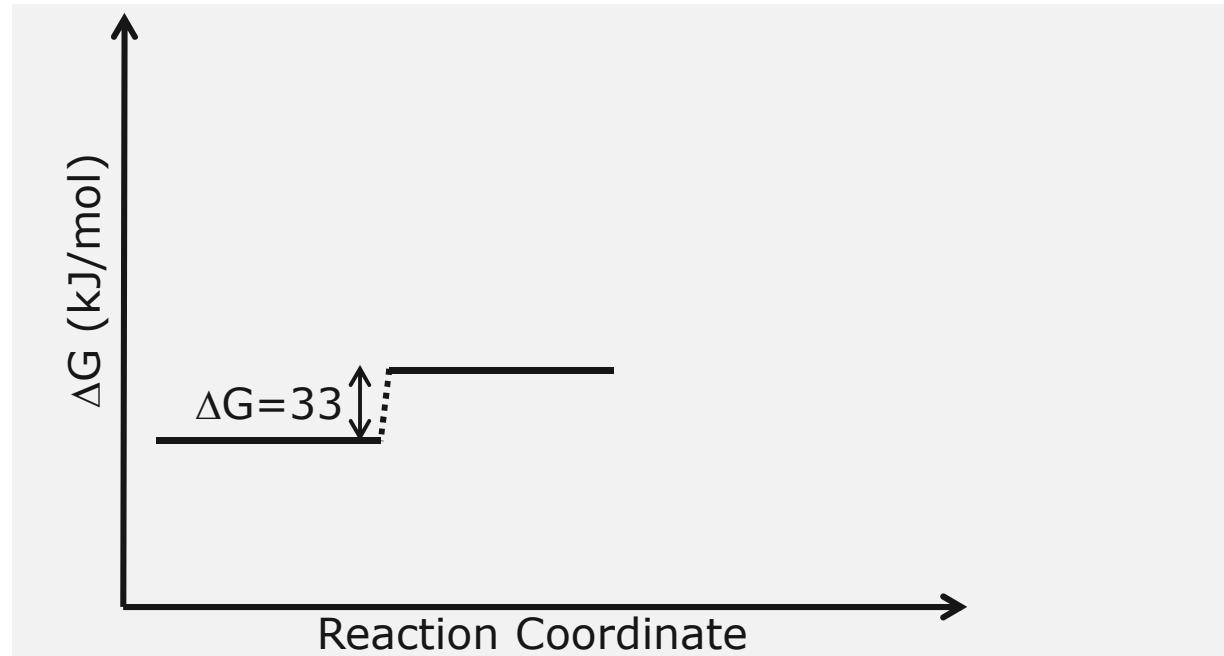
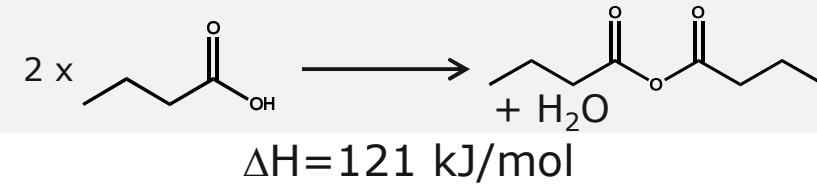
Thermodynamics anhydride formation

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Based on butyric acid at 523 K *



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- Formation of butyric anhydride non-spontaneous at 523 K

*Calculated by HSC

Thermodynamics anhydride conversion

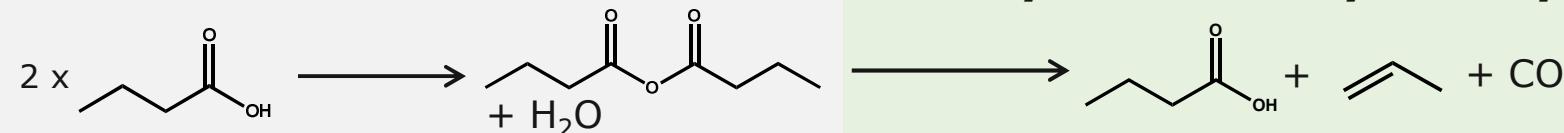
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Based on butyric acid at 523 K *

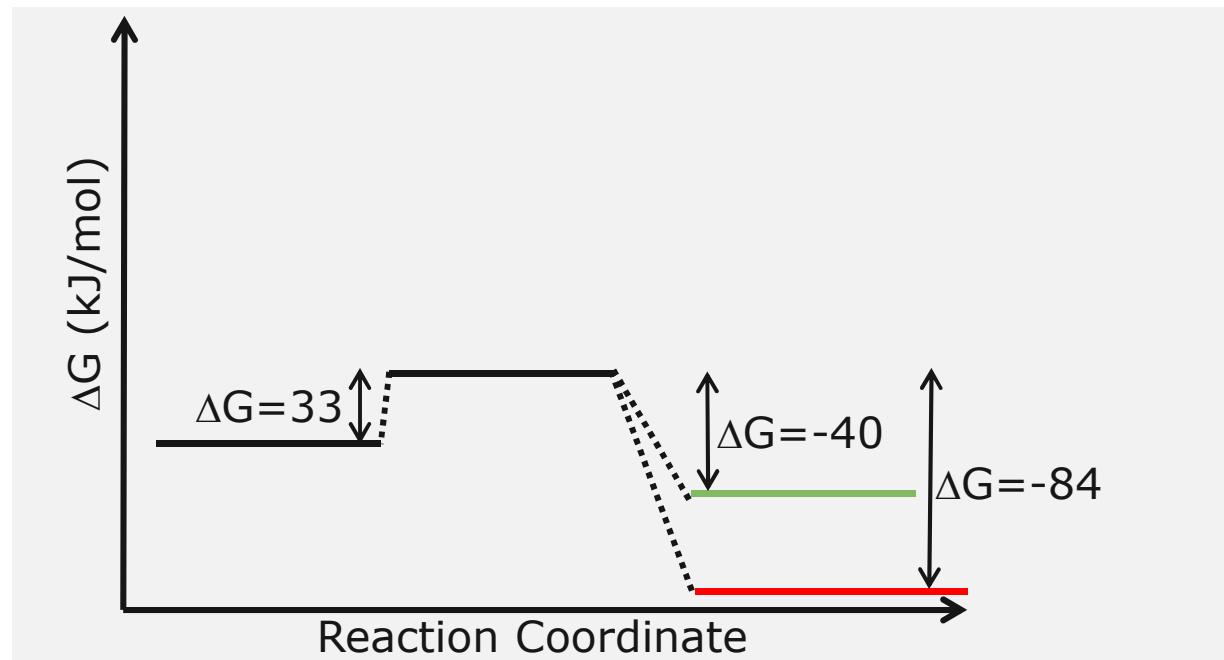
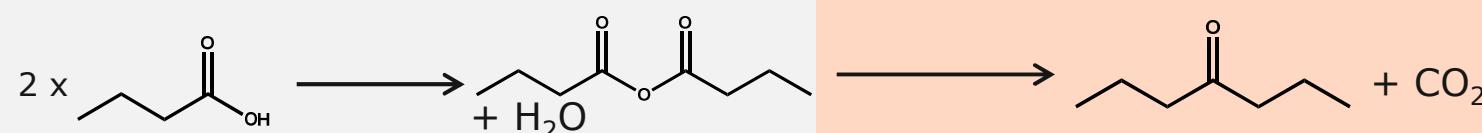


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Decarbonylation of butyric anhydride



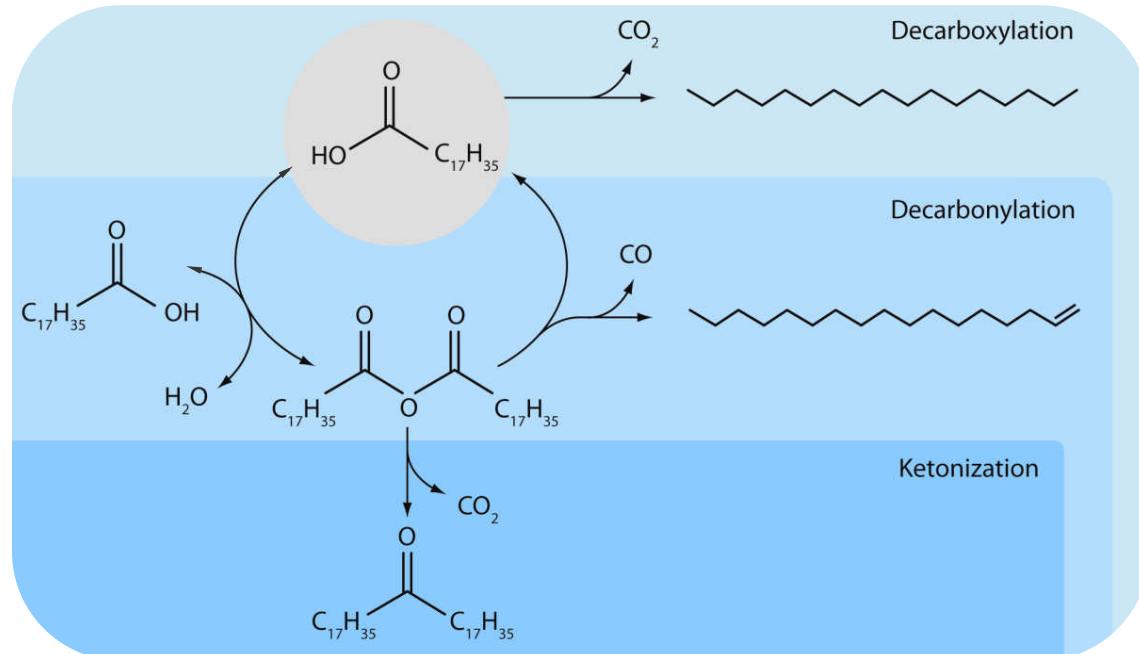
Ketonization of butyric anhydride



- Overall reaction pathway's are thermodynamically feasible

*Calculated by HSC

- There are strong indications for the existence of stearic anhydride as reactive intermediate in the decarbonylation reaction of stearic acid at low temperatures
- Suggested deoxygenation reactions of stearic acid over $\text{Pd}/\text{Al}_2\text{O}_3$ at 523 K:



- Stearic anhydride is selectively converted to 1-heptadecene at 473 K
- Calculations on butyric anhydride show that pathway's are thermodynamically feasible

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