



Deoxygenation of stearic acid in the absence of H_2

The relevance of the anhydride reaction pathway



Stefan Hollak MSc

Co-promotor: Dr. Daan van Es

Promotor: Prof.dr.ir. Krijn de Jong

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FOOD & BIOBASED RESEARCH
WAGENINGEN UR



Universiteit Utrecht

smart
xiw



- Wide variety of sources for vegetable oils
 - For instance: Sunflower oil, Soybean oil, Palm oil and Rapeseed oil



→ Land use issues;
food vs. fuel



- Algae oil
 - Possible solution to these problems in future
 - No direct competition with food production
 - Rapid growth rates (10-200 times faster than terrestrial oil crops)^{1,2}



→ AlgaePARC Wageningen UR

¹ Huber et. al., Chem. Rev. 2006, 106, 4044-4098

² Christi, Biotechnol. Adv. 2007, 25, 294-306

1st generation biodiesel

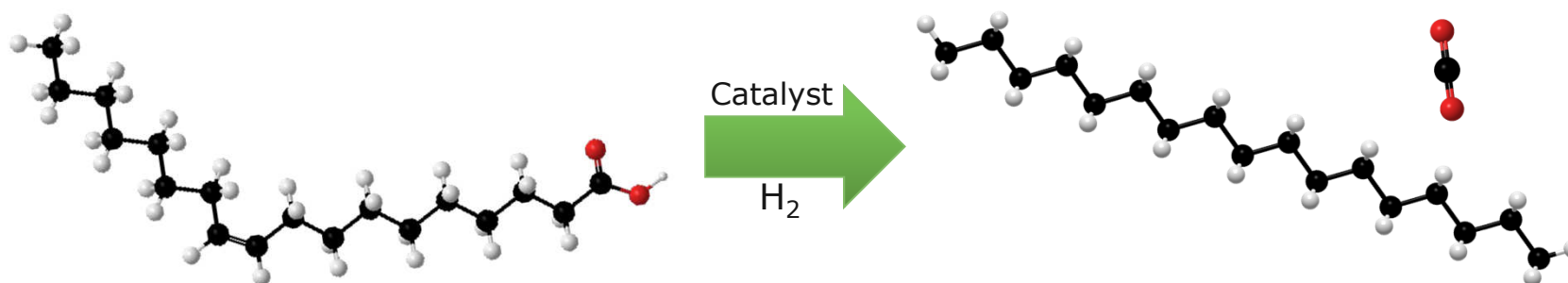
- 1st generation biodiesel: fatty acid methyl esters (FAME)
 - Derived from vegetable oils
 - Produced via transesterification of triglycerides with methanol

- Concerns
 - High purity feedstocks are necessary
 - Engine compatibility issues
 - Lower heat content
 - Poor storage stability



2nd generation biodiesel

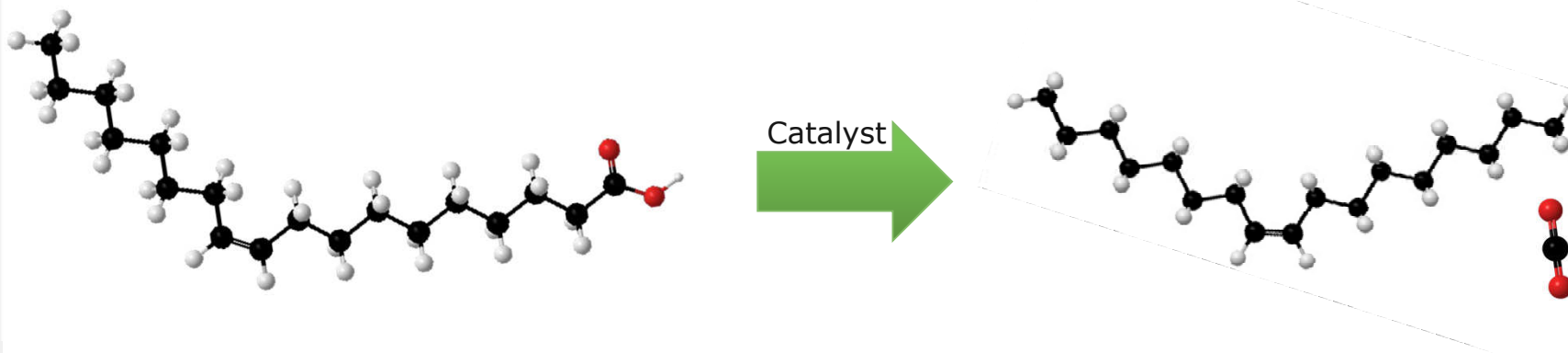
- 2nd generation biodiesel
 - Derived from vegetable oils or other fatty acid derivatives
 - Via catalytic hydrodeoxygenation using hydrogen



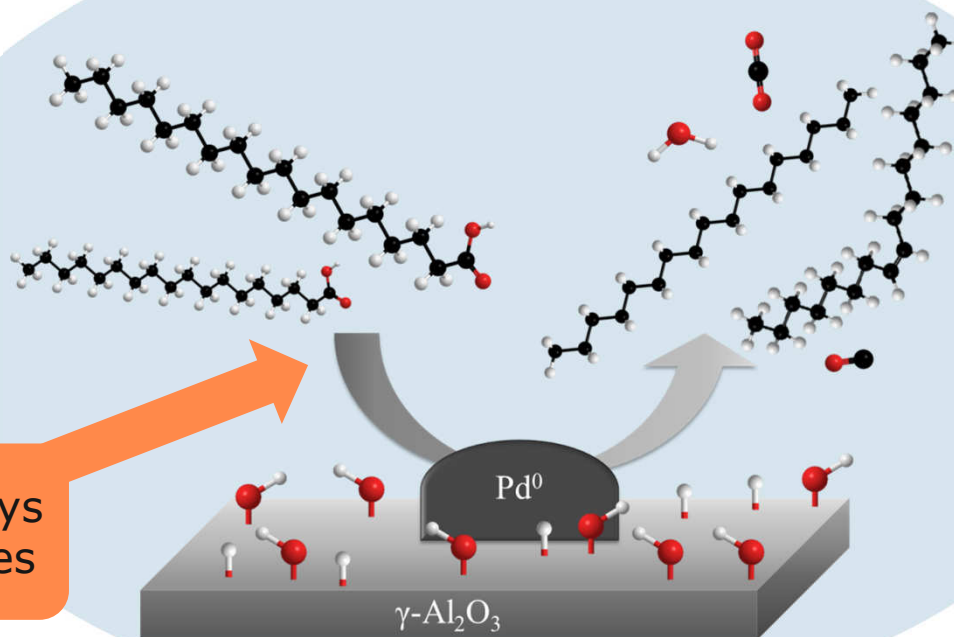
- Advantages
 - Low purity feedstocks possible
 - Higher fuel quality (heat content and storage stability)
 - Fully compatible with existing vehicles and infrastructure
- Concerns
 - Process requires (non-renewable) H₂
 - Reduction of double bond functionalities
 - Hydrodeoxygenation of glycerol to propane,
 - Process at elevated P and T (3-10 MPa, 553-618 K)

Introduction to the project

- A superior process would be the catalytic deoxygenation of fatty acids:
 - At low temperature (< 523 K)
 - With low/no hydrogen consumption
 - Yielding unsaturated hydrocarbons



- Advantages:
 - Excellent low-temperature properties as a fuel
 - Possible applications as chemical building blocks
 - Potential for glycerol valorization



Reaction Pathways and Intermediates

- Activity & Selectivity
 - Influence of feed conc.
- Deoxygenation reactions
 - Stearic anhydride intermediate

Catalyst:

4.5 wt% Pd/ γ -Al₂O₃ (BASF)

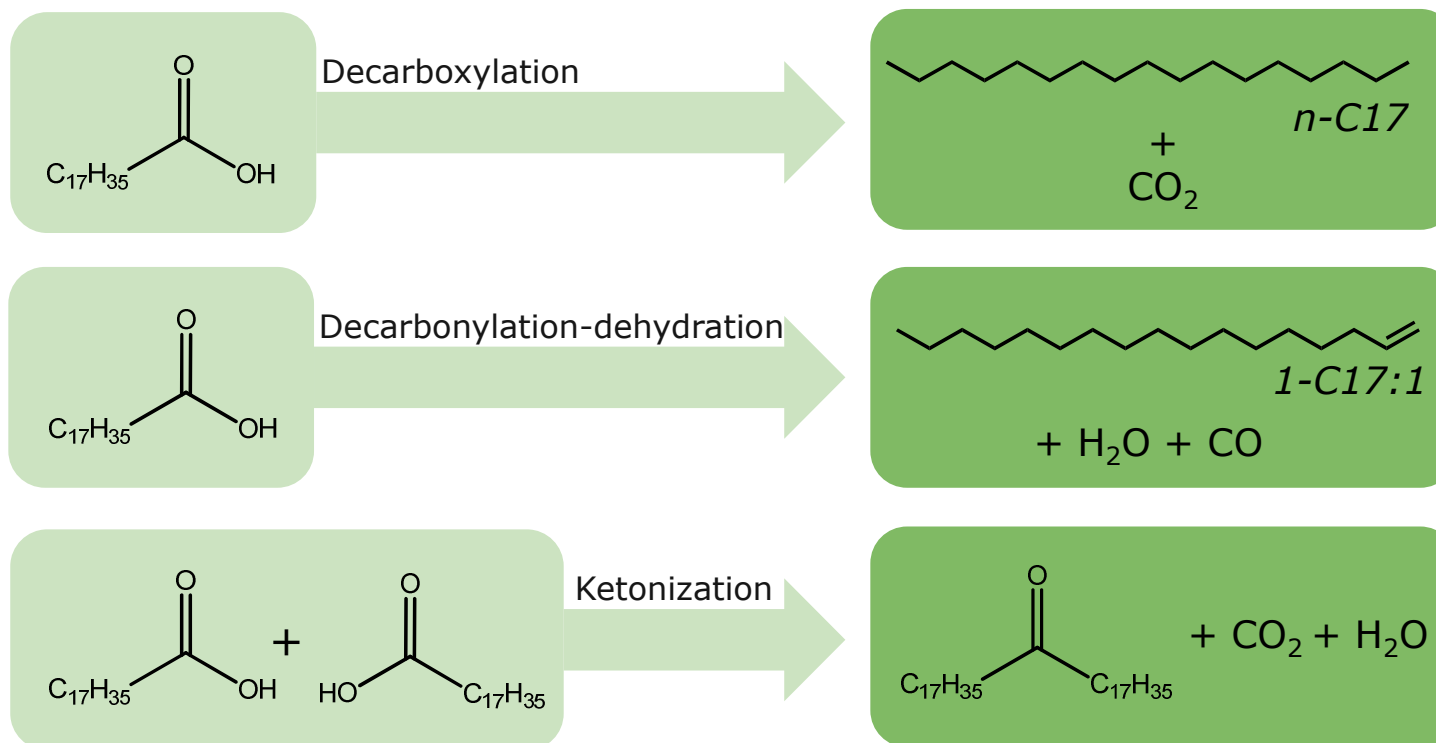
Surface area:	111 m ² /g
Av. Particle size:	6.7 nm
Dispersion:	17 %

Deoxygenation reactions



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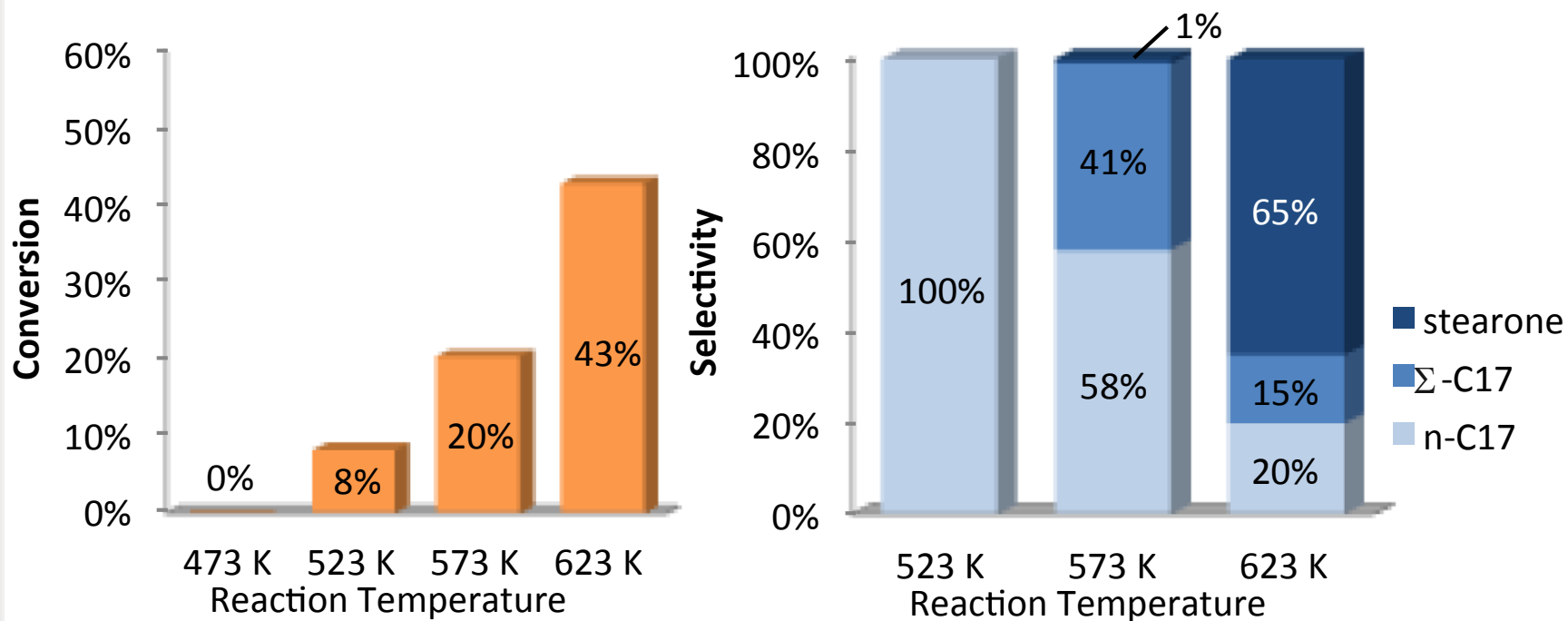


Results

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Influence of temperature



- Lowest deoxygenation temperature at 523 K
 - *Heptadecane formed selectively*

Reaction conditions:

Catalyst: Pd/ γ -Al₂O₃
Solvent: dodecane
Feed conc.: 0.14 mol L⁻¹
Reaction time: 6 h
Pressure: 7 bar N₂

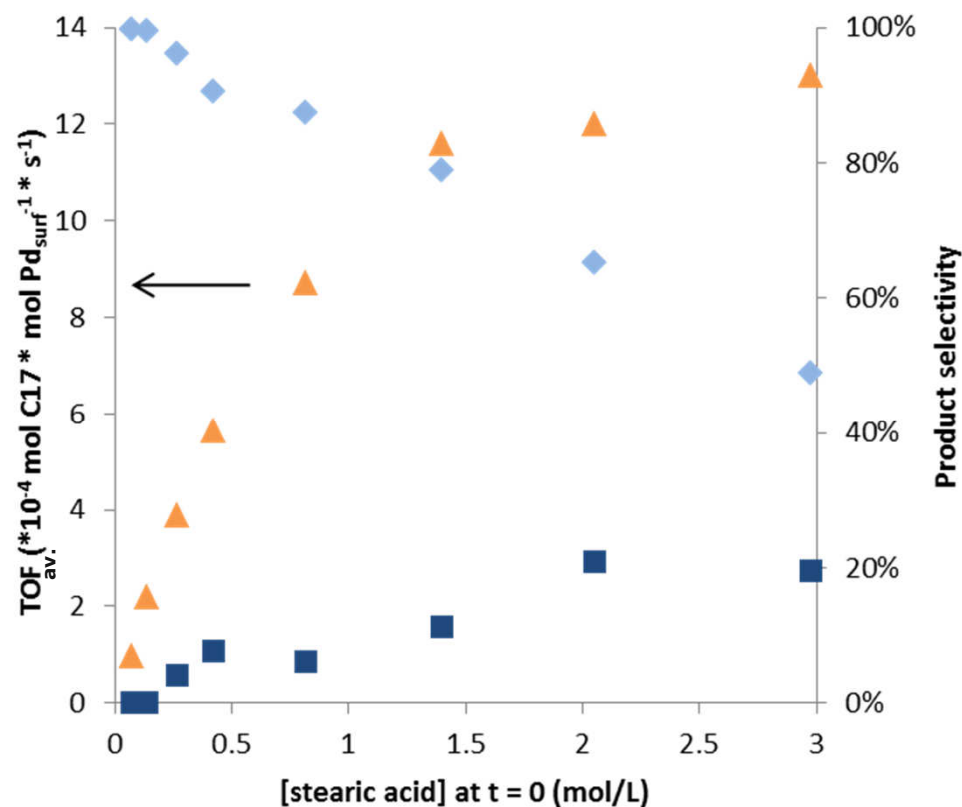
Catalyst Activity & Selectivity

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Influence of stearic acid concentration at 523 K



Reaction conditions:

Catalyst:	Pd/ γ -Al ₂ O ₃
Solvent:	dodecane
Reaction temperature:	523 K
Reaction time:	24h
Pressure:	7 bar N ₂

- Selective decarboxylation at low (<0.25 mol/L) stearic acid conc.
- >0.25 mol/L: Selectivity to n-C17 decreases
 - Decarbonylation products are formed
 - Ketonization to stearone

Anhydride intermediate

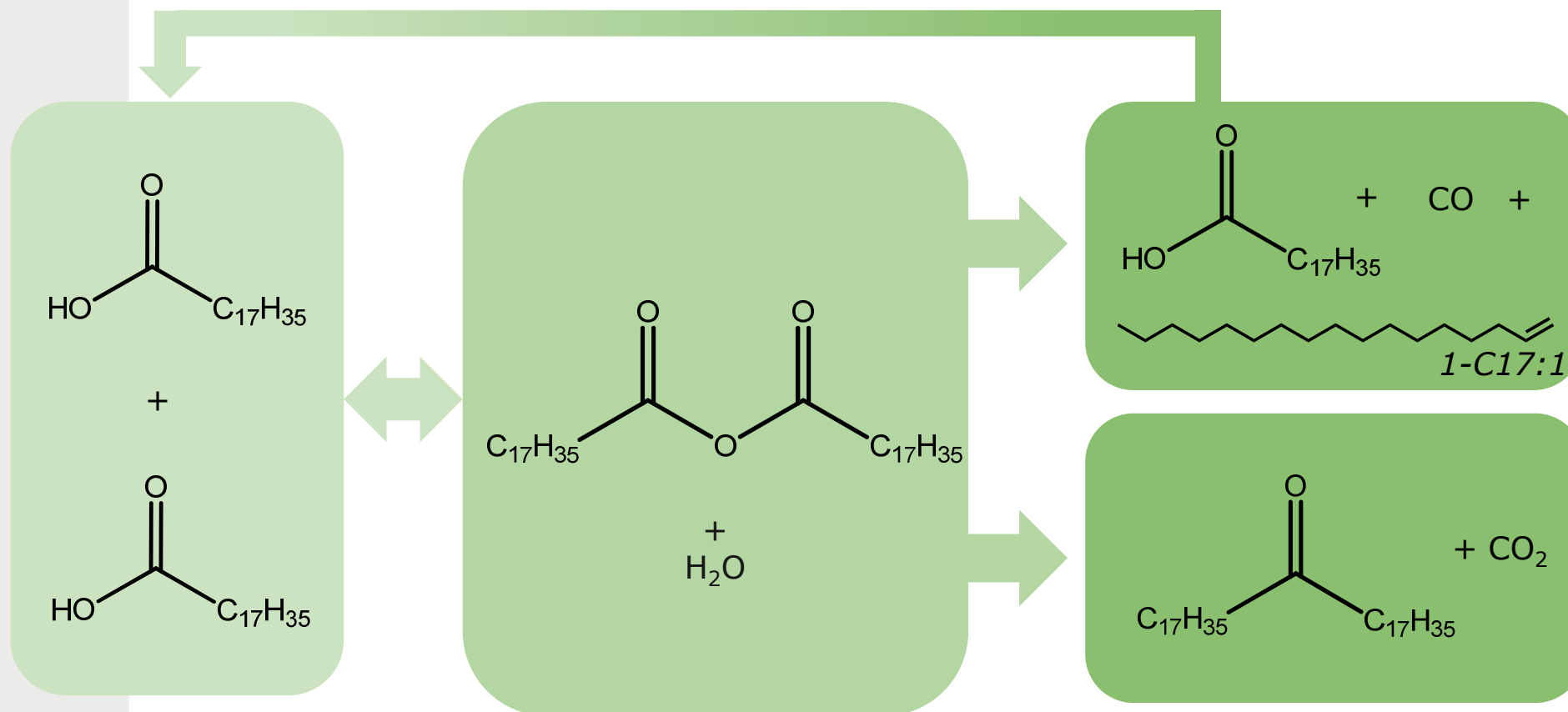
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Hypothesis

- Possible explanation: Stearic anhydride as intermediate product
- Literature: Stearic anhydride suggested as intermediate product in homogeneous decarbonylation and ketonization reaction of stearic acid^{1,2}



¹ Foglia et. al., *J. Am. Oil Chem. Soc.* 1976, 53, 737-741

² Miller et. al., *J. Org. Chem.* 1993, 58, 18-20

Anhydride intermediate

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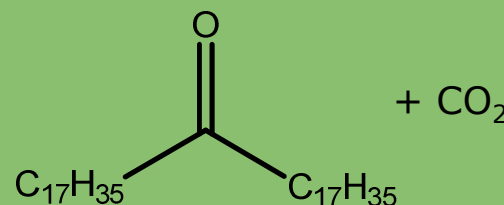
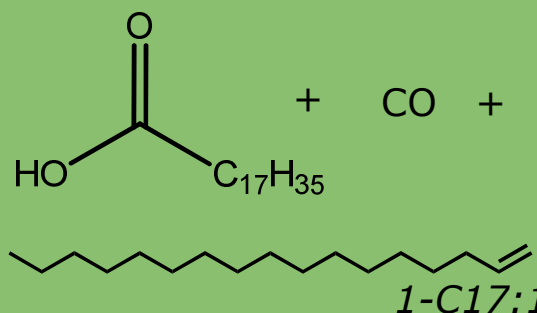
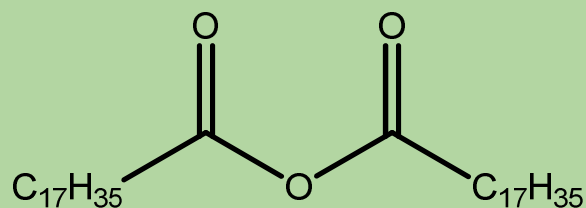
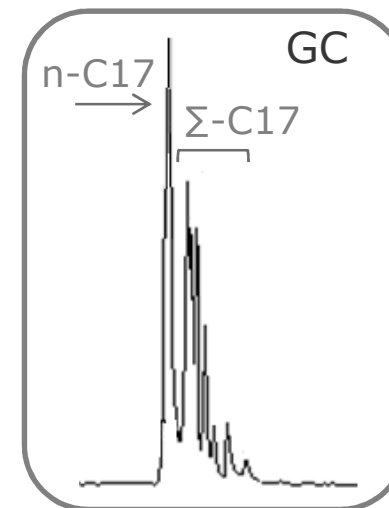


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Model reaction

- Reaction with stearic acid anhydride gives 100% conversion to:

- Stearic acid
- Heptadecenes (Σ -C17)
- Heptadecane (n -C17)
- Stearone (C35)



Reaction conditions:

0.14 mol/L stearic anhydride
523 K, 24h, 7 bar N₂

Anhydride intermediate

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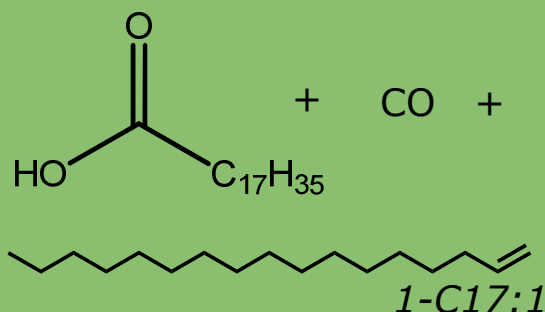
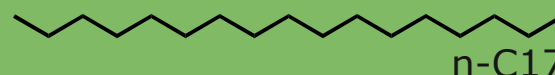


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Model reaction

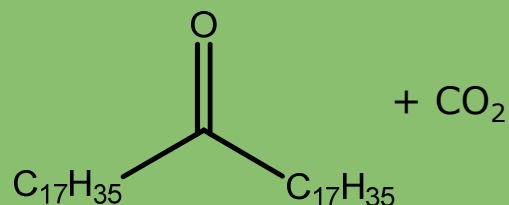
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Transfer hydrogenation

- n-C17
- Σ -C17



Reaction conditions:

0.14 mol/L stearic anhydride
523 K, 24h, 7 bar N₂

Anhydride intermediate

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Overview model reactions

Catalyst	Stearic anhydride (g)	Reaction Temp (K)	Reaction time (h)	Conversion (%)	Selectivity (%)				
					n-C17	Σ-C17	SA	C35	heavies
Pd/γ-Al ₂ O ₃	1.0	523	5	98	7	42	49	2	0
Pd/γ-Al ₂ O ₃	1.0	523	24	100	27	25	46	2	0
γ-Al ₂ O ₃	1.0	523	24	80	0	1	71	28	0
none	1.0	523	24	40	0	1	58	26	15
Pd/γ-Al ₂ O ₃	10.0	523	24	62	14	20	35	12	19
Pd/γ-Al ₂ O ₃	1.0	473	24	48	4	47	49	0	0

- Decarbonylation 10 times faster than when starting from stearic acid
 - Anhydride formation from stearic acid rate limiting step
- Pd essential for decarbonylation to HC's.
 - Stearone and other heavies are formed in absence of Palladium
- High anhydride concentration: increase in side product formation
- Stearic anhydride is also converted at 473 K
 - Potential for low temperature decarbonylation of stearic acid?

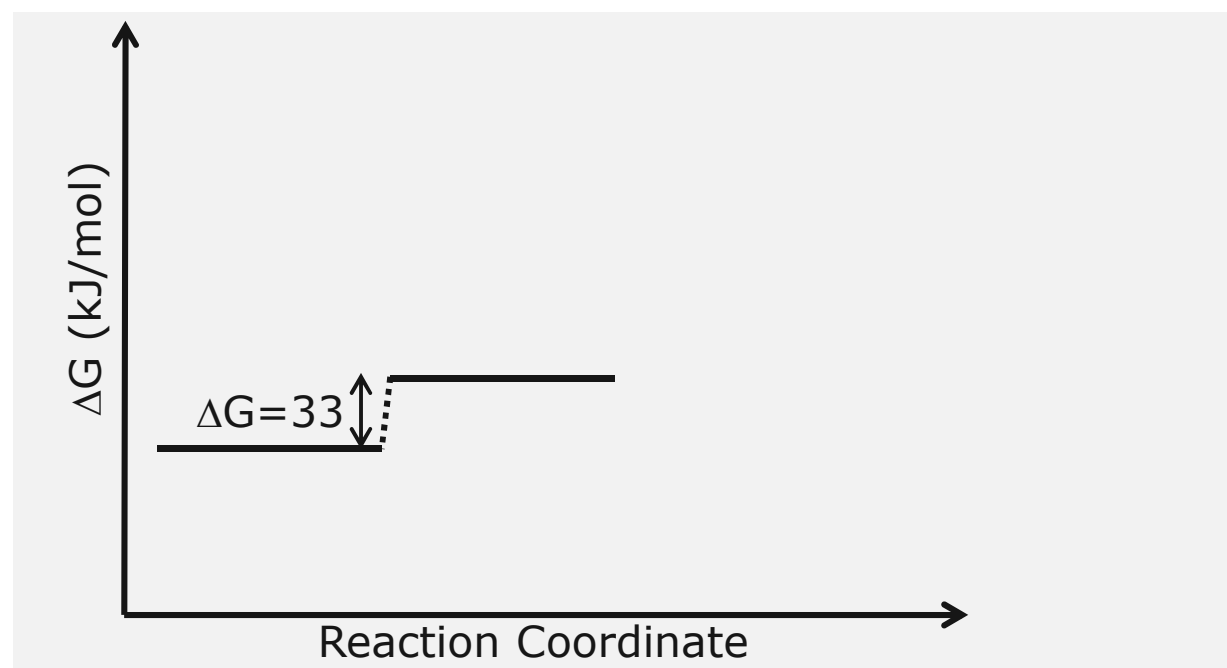
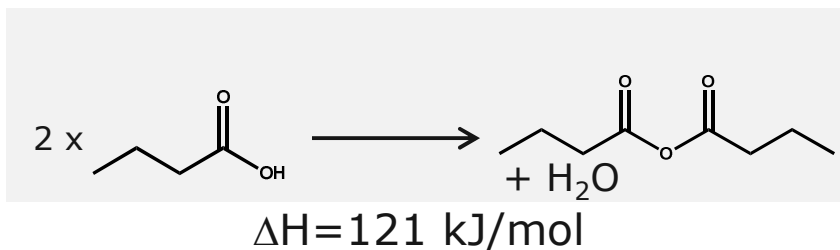
Thermodynamics anhydride formation

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Based on butyric acid at 523 K *



- Formation of butyric anhydride non-spontaneous at 523 K

*Calculated by HSC

Thermodynamics anhydride conversion

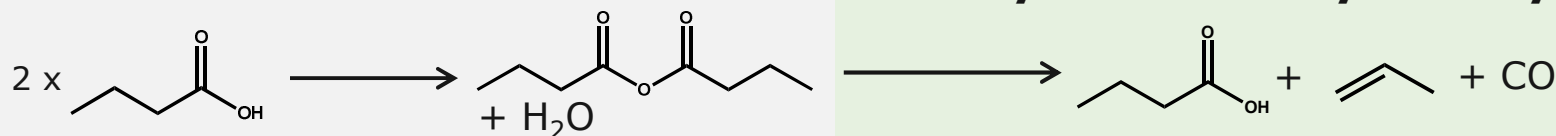
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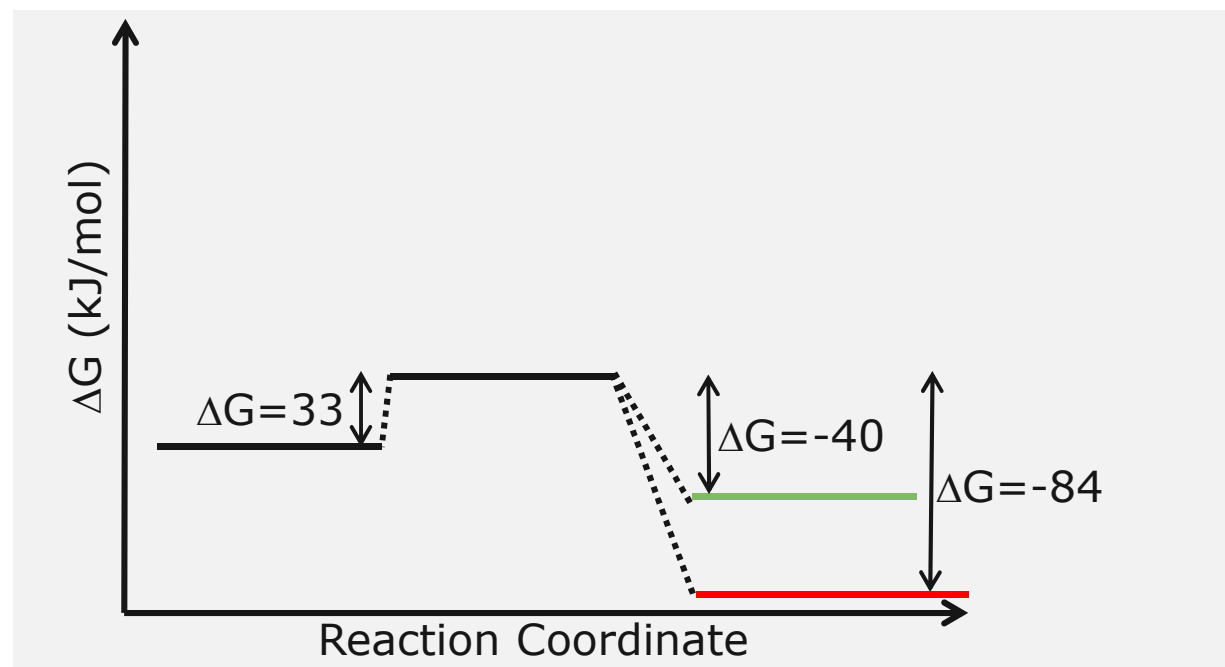
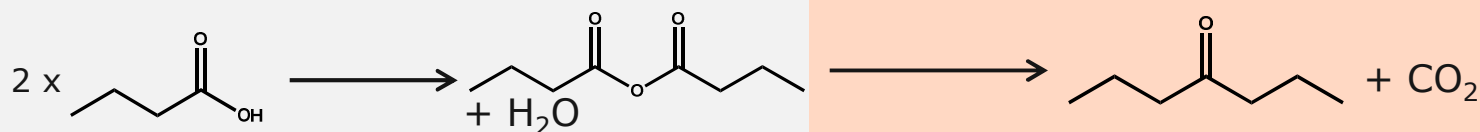
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Based on butyric acid at 523 K *

Decarbonylation of butyric anhydride



Ketonization of butyric anhydride

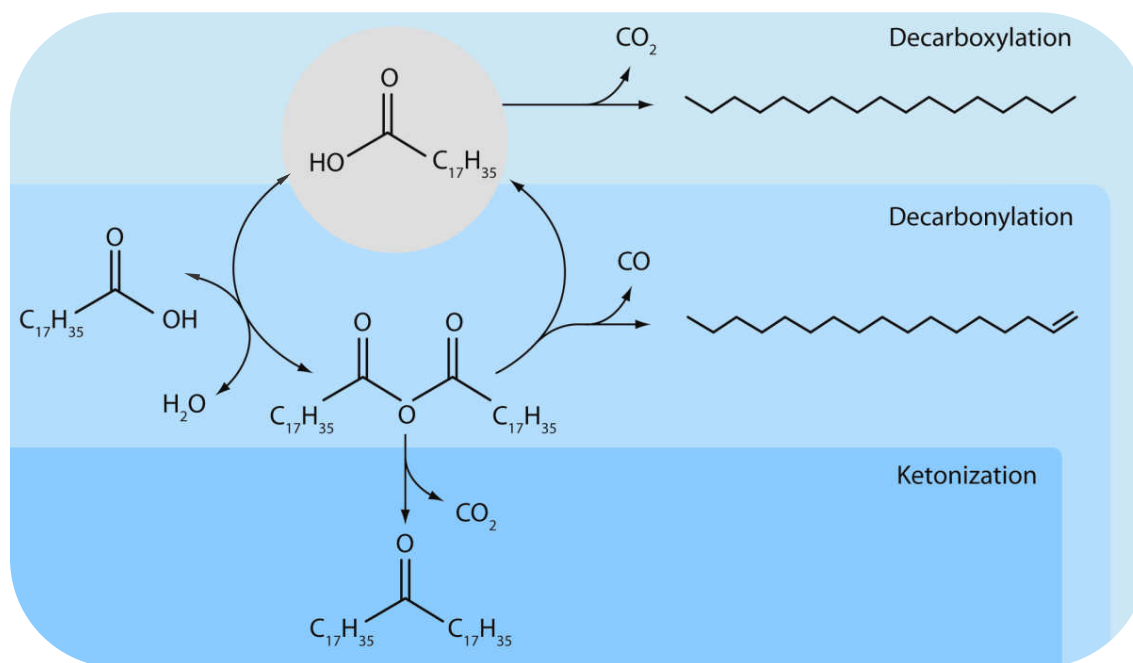


- Overall reaction pathway's are thermodynamically feasible

*Calculated by HSC



- There are strong indications for the existence of stearic anhydride as reactive intermediate in the decarbonylation reaction of stearic acid at low temperatures
- Suggested deoxygenation reactions of stearic acid over Pd/Al₂O₃ at 523 K:



- Stearic anhydride is selectively converted to 1-heptadecene at 473 K
- Calculations on butyric anhydride show that pathway's are thermodynamically feasible



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email: stefan.hollak@wur.nl