# AlgaePARC

Translating research into applications

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## From a craft to an industrial process...

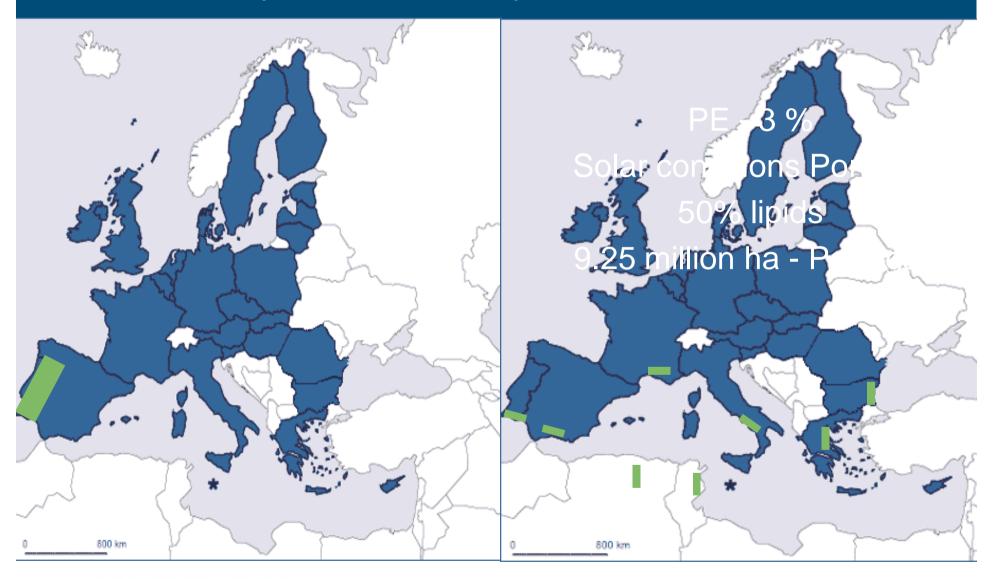
- Current worldwide microalgal manufacturing infrastructure
  ~5000 tons of dry algal biomass
- High value products such as carotenoids and w-3 fatty acids used for food and feed ingredients.
- Total market volume is €1.25 billion (average market price of €250/kg dry biomass)
- World production of palm oil is nearly 40 million tons, with a market value of ~0.50 €/kg

Scale up

**Production costs** 



### Transport Fuels in Europe - 0.4 billion m3





Wijffels R.H., Barbosa M.J. (2010) An outlook on microalgal biofuels. *Science* 329: 796-799

### **Production costs**

- At 1 ha scale today: 10 €/kg
- At 100 ha scale today: 4 €/kg
- What will be possible: 0.40 €/kg



### How?

- Increasing photosynthetic efficiency
- Integrate processes (free nutrients)
- Decreasing mixing

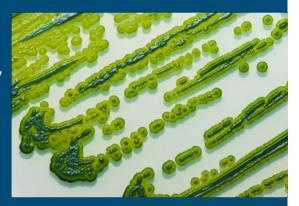


Choosing locations with higher irradiations

Scale-up

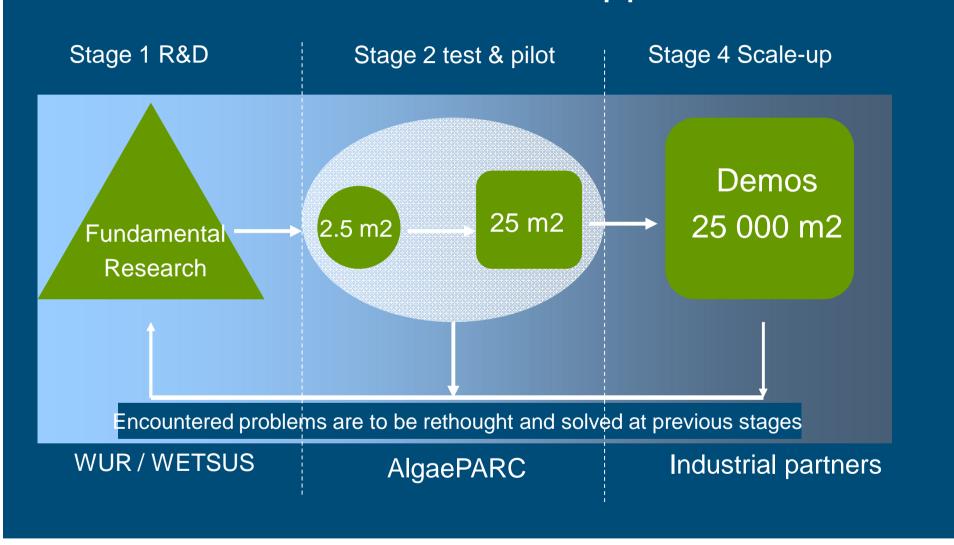
**Production costs** 

Energy requirement





## Translate research towards applications





## AlgaePARC

an international, open and independent centre for applied research on microalgae

The ultimate objective of AlgaePARC is to develop technology for sustainable production of feedstock for fuel, chemicals, food and feed

R&D at AlgaePARC is aimed to fill the gap between fundamental research on algae and full-scale algae production facilities

Production costs

Scale-up

Energy requirement



#### Production costs:

Increasing Photosynthetic Efficiency – what margin do we have?

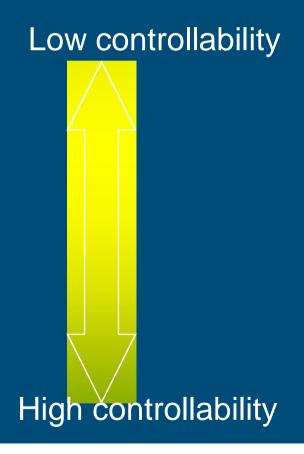
PE 9.0 % reflection on PBR 8.6 % night biomass loss 7.8 % maintenance What's left ?... 7.4% Light saturation? ca 50% reduction in Nutrient limitations? CO<sub>2</sub> production cost Inhibition? O<sub>2</sub>, light Practice?... 3 - 4%



## What's determining photosynthetic efficiency outdoors?

#### Measured / controlled parameters

- Light intensity
- Temperature
- O<sub>2</sub> partial pressure
- CO<sub>2</sub> partial pressure
- Gas flow rate / Liquid velocity
- Dilution rate
- pH
- Nutrients





## Production costs: Photosynthetic Efficiency

At lab scale a photosynthetic efficiency of 6% seems to be within reach

Cuaresma et al., 2010

What about

- Pilot scale 10 100 m<sup>2</sup>
- Extended time > 1 yr

## Scale-up

#### Information for design of full-scale plants

- Representative productivities
- Photobioreactor design
- Performance of different systems
- Operation strategies
- Plant layout



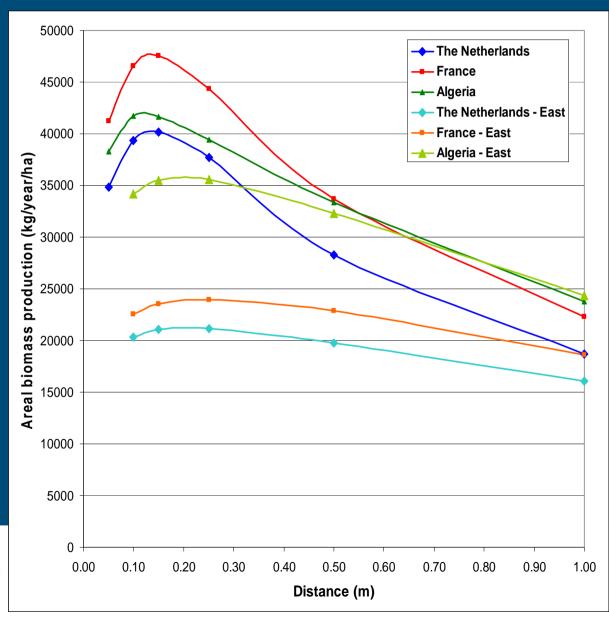
## Scale-up

### Layout

e.g Effect panel distance and orientation

Sleg**e**rs et al, submitted





## **Energy requirements**

- Gassing
  - Supply CO<sub>2</sub>
  - Remove O<sub>2</sub>
- Mixing
  - Prevent sedimentation
  - Distribute nutrients and light
- Harvesting



- Enhance transfer rates

Process control to exploit external conditions





## Time Plan and R&D Activities

Literature Research

Screening experiments

Feedstocks

Comparison Photobioreactors

New reactor concepts and process optimization

Test business cases



2013

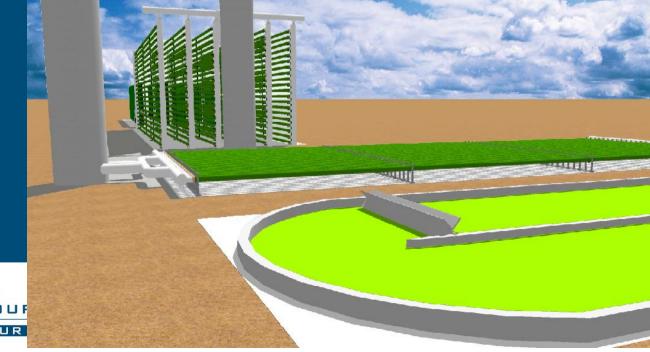
2014

2015

2016

## 24 m<sup>2</sup> systems

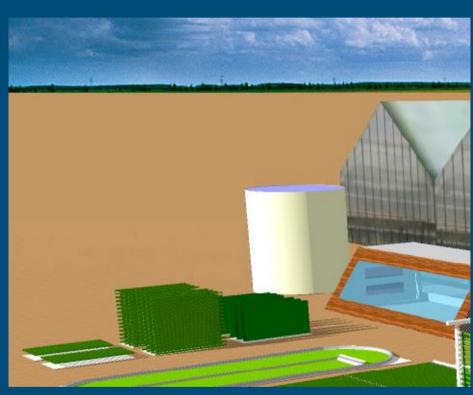
- Long time performance (1 year)
- 4 systems running in parallel
- Problems: solve in lab
- Representative productivities for full scale
- Information for design of full scale plants (layout, distance between tubes or plates, light path, orientation)





## 2.4 m<sup>2</sup> systems

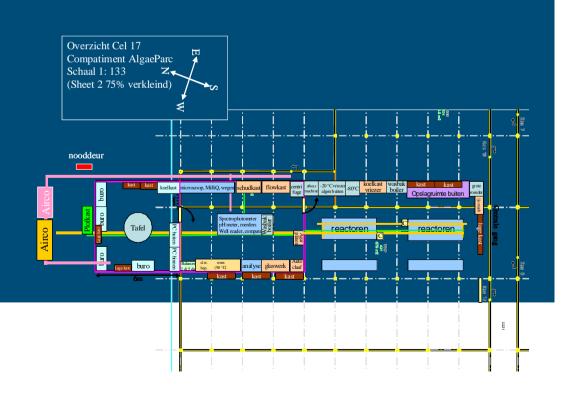
- Phase between lab and pilot
- Test things where you are not sure of
- Different strains
- Different feed stocks
- Adaptations in design
- New systems
- If successful
  - To 25 m<sup>2</sup> scale
- If not successful
  - More experiments
  - Reject



### ...and a Lab

- Storage of strains
- Medium optimisation
- Initial test of feedstocks
- Screening
- Analytics
- Support for outdoors

mL ->m3 in situ





## Cultivations systems (24 m<sup>2</sup>)

#### Open pond

- Reference

#### Horizontal tubes

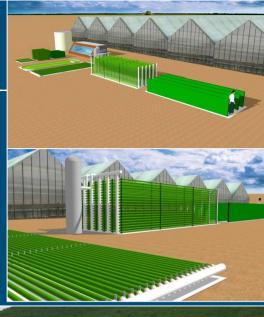
- high light intensity
- oxygen accumulation

#### Vertical stacked hor. tubes

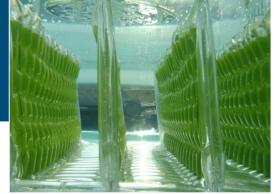
- light dilution
- oxygen accumulation

#### Vertical plastic films (ProviApt)

- light dilution
- no oxygen accumulation









## Screening Experiments

- Axenic strains
- Storage of strains (cryopreserved or freeze dried)
- Strain selection on growth rate, lipid content and extractability (well plate experiments).
- Optimisation of cultivations conditions (temperature, pH, macronutrients)
- Testing promising strains in experimental units outdoors (2.5 m² photobioreactors)

- Strains with high biomass and oil productivities
- Database with strains, growth rates and lipid content



#### **Feedstocks**

- Comparison industrial grade nutrients vs. analytical grade nutrients
- Selection of the most promising waste streams as feedstocks
- Determination of growth rate and lipid content of microalgae grown on selected waste streams\waste gas (different sources of CO<sub>2</sub>, N and P)
- Extension of database from literature research

- Selection of best strains for different feedstock combinations
- Algae uptake capacity of nutrients from different waste streams



## Comparison of Photobioreactors

- Areal and volumetric biomass and lipid productivity
- Energy balance
- Nutrient requirements
- Carbon dioxide consumption and oxygen production
- Operational costs
- Cleanability
- Culture stability (assessment of infections and algae population)
- Robustness of the system

- -Long time performance
- Biomass and lipid productivity
- -Metabolic performance under different conditions
  - -Determination of culture stability
- Information for improvement of operation strategies

### New reactor concepts and process optimization

- Test new concepts and variations on reactor design / layout
- Optimize photobioreactors geometrically
- Develop operation strategies
  - Dilution rate /harvesting time
  - Media recycling
  - Heating/cooling vs. operation costs and energy requirements
- Optimise productivity and decrease energy requirements by dynamic process control to exploit external conditions:
  - adjusting biomass concentration, circulation velocity or gas flow rate

- Fast assessment of performance of new concepts and variations
  - Development of operational strategies
  - Optimization of lipid and biomass productivity

#### Test Business cases

- Reorganisation of initial systems and performance of new runs with different waste streams
- Translation of data from pilot plant photobioreactor to industrial scale. The following parameters will be evaluated: productivity, costs, energy, and technical feasibility

- Proof of concept of different business cases
- Knowledge of the costs, energy requirements and technical feasibility based on experimental data (that can be used in the design of demonstration plants)



## Financial structure AlgaePARC 7 M€

- AlgaePARC facility:
  - Ministry of Agriculture
    - Province of Gelderland
    - Wageningen UR + industry
- AlgaePARC research program (2011-2015):
  - Part of Towards Biosolar Cells
    - in cash contribution companies
    - in cash matching TBSC
- Ambition to become international independent center of applied algae research
  - Additional projects photobioreactor technology, processes and biorefinery
  - Contract research



## Time Plan

- Indoors facilities, December, 2010
- Outdoor reactors + facilities, March 2010
- Grand Opening Mid May 2011

WAGENINGEN UR





# www.algae.wur.nl www.AlgaePARC.com



