

# Temperature response of duckweed growth at the Ecoferm greenhouse

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**Chair group Biobased Chemistry & Technology**

**BSc Thesis Biosystems Engineering**



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8 June 2015



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# ***Temperature response of duckweed growth at the Ecoferm greenhouse***

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## 1 Abstract

In Uddel, the first Ecoferm farm is build. The Ecoferm concept is about reusing manure, ammonia, carbon dioxide and heat from livestock to produce protein rich food, in the form of duckweed. The farms consist of a rose calve stable with a greenhouse on top of it. In the greenhouse there is a basin were the duckweed is cultivated. Via the stable's ventilation, the carbon dioxide and ammonium rich air is blown through a biobed into the greenhouse. In this setup the greenhouse is heated by solar radiation, and via the body heat of the rose calves. The problem however is that in the summer the duckweed at the Ecoferm dies, due to a too high temperature of above 40°C.

This thesis will mainly focus on controlling the temperature of the duckweed at the Ecoferm, in such a way that the duckweed will survive the hot days, optimal control is not considered. This topic is chosen because the dyeing of duckweed is currently the largest problem for the Ecoferm.

In the first chapter, the growth of duckweed, and its associated parameters are discussed. In the second chapter the climate model of the Ecoferm is discussed. This dynamic model is a modified version of the dynamic model made by (van den Top, 2014).

This model, and the literature, lack essential information on the growth/death rate of duckweed at temperatures above 35°C. To be able to model this growth at these temperatures, an experiment is conducted with as goal; determining the death rate of duckweed at temperatures above 35°C. The results and analysis were however not sufficient to construct an accurate dynamic model, but provided enough information to approximate the response at high temperatures.

In the last part of this thesis, the effect of different climate actuators is tested. The conclusion is that with the help of an adiabatic cooler or extra ventilation, the duckweed can survive during the hot summer months. Increasing the total production to 2713.2 kg dry matter per year.

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# 1 Introduction

## 1.1. Background

In the Netherlands there is a large livestock sector. All these animals produce a lot of manure, which can be used to fertilize the land. Due to environmental laws and side effects of fertilization, one can only fertilize the land with a certain amount of manure. Most of the livestock farmers do not have enough land to get rid of all their manure. Therefore these farmers need to transport the manure to arable farmers who can use this for fertilization. Manure consists for only 10% of organic matter and nutrients, so basically they are mainly transporting water.

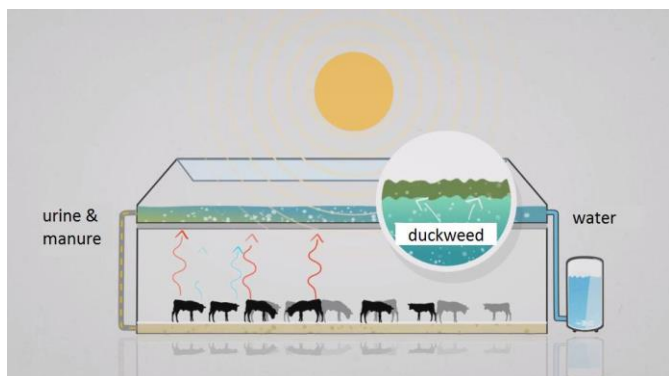
Another problem about this large livestock sector is the demand for (protein rich) feed. To increase the production of the livestock, protein rich food is needed. This protein rich food is provided in the form of soy (Liere et al., 2011). The climate in Europe is not suitable for soy, therefore soy is imported from South America. The production of soybean is intensive and exhausting for the land. Therefore rainforest is felled to create new soybean fields. The current production of protein rich dairy food is unsustainable.

The manure surplus and the protein import are two major problems of the livestock sector. These problems will expand proportionally to the growth of this sector. Especially the dairy sector is expanding fast because soon there will be no milk quota any more.

A sustainable solution for these problems would be to produce protein rich food locally with nutrients from the manure. Innovation Network has developed the Ecoferm concept, which is based on closed cycles. The Ecoferm concept is about reusing manure, ammonia, carbon dioxide and heat from livestock to produce protein rich food, in the form of duckweed and algae. The protein content of duckweed is: 15-40% (Landolt et al., 1987), which is comparable to that of soy: 30-46% (Breene et al., 1988). Due to the high protein content of duckweed, it can be used (partly) as a substitute for soybean. Duckweed can grow in the European climate, on a growth medium made out of urine, water and digestate from a manure digester. This manure/mono-digester also produces biogas for a turbine. In short, the Ecoferm provides a substitute for soybean meal and decreases the manure surplus.

## 1.2. Problem description

In Uddel, the first Ecoferm farm is built. The farms consist of a rose calve stable with a greenhouse on top of it. In the greenhouse there is a basin where the duckweed is cultivated. Via the stable's ventilation, the carbon dioxide and ammonium rich air is blown through a biobed into the greenhouse. In this setup the greenhouse is heated by solar radiation, and via the heat production of the calves.



The amount of produced duckweed is calculated with the model of van den Top (2014). According to this model, the growth of duckweed is inhibited during warm summer days. In reality, there is no



growth at all, the duckweed even dies. The death of the duckweed is probably caused by too high temperatures. According to van den Top (2014), the temperatures in the greenhouse can rise above 40°C, which is lethal to duckweed (Stanley and Madewell, 1976).

### 1.3. Aim

In the current situation, the problem lies in the extreme growth conditions during summer. The goal of this thesis is to:

- Control the climate in the greenhouse so the cultivation of duckweed can continue during summer.
- Construct a model of the growth/death rate of duckweed at high temperatures.

### 1.4. Research questions

To get a better understanding of the growth of duckweed during summer, the following research questions are formulated:

Growth behaviour:

- 1) How does the growth rate of duckweed behave in the Ecoferm greenhouse?
- 2) How does the growth rate of duckweed behave at high temperatures in the greenhouse?

Control/ model:

- 3) Which parameters are important for the climate in the greenhouse?
- 4) Which climate actuator influences the temperature of the duckweed the most?
  - a. White wash
  - b. Solar screen
  - c. Ventilation
  - d. Adiabatic cooler
- 5) Which climate actuators are needed for the duckweed to survive the hot summer months?
- 6) What climate actuators are the most effective to increase the duckweed production year round?

### 1.5. Delimitations

The Ecoferm greenhouse in Uddel contains the following subsystems: *Stable, Manure pit, Calves, Biobed, Greenhouse, Mono-digester, Buffers, and Generator.*

In my thesis, I will try to optimize the temperature in the greenhouse for optimal growth conditions. The effects of nutrients in the growth medium and ammonium and carbon dioxide in the air are not investigated.

The effects of the manure pit on the temperature of the duckweed are not significant, and therefore neglected. The mono-digester and the generator produce a lot of heat, all the heat produced by these subsystems is used in other processes outside the Ecoferm and therefore do not influence the climate in the greenhouse. The gasses coming out of generator are released into the air outside the system, and therefore do not significantly influence the climate in the greenhouse.

In the systems stable, biobed and greenhouse, the effects of ventilation, evaporation, conduction and convection are taken into account. The influence of solar radiation on the temperature in the stable is neglected. In the biobed and the greenhouse, solar radiation is taken into account.

## 1.6. Approach

Insight of the growth behaviour is important to understand the growth model and for optimization of the growth conditions.

Question 1, the growth behaviour of the duckweed in the Ecoferm greenhouse is investigated with a literature study. The most important literature is van den Top (2014).

Question 2, about the growth/death rate of duckweed at high temperatures, Little is known. The current growth models describe growth at temperatures up to 35°C. At the Ecoferm, temperatures can rise up to 42°C. At these high temperatures, duckweed dies, but there is no model describing the death rate. Therefore an experiment is conducted to determine the death rate of duckweed at these temperatures myself.

To answer all the questions about the model of the Ecoferm greenhouse and the control of it, the model itself is needed. The dynamic model will be a modified version of the model of van den Top (2014). This model will be expanded and climate actuators will be integrated in it.

Question 3, the parameters that influence the temperature in the greenhouse the most will be determined using a sensitivity analysis. The outcome of this analysis will be used to validate the model.

Question 4, to determine of the influence of the climate actuators on the greenhouse temperature, a sensitivity analysis will be used.

Question 5, the algorithm of the death rate of duckweed and the climate actuators will be implemented in the dynamic model. The effect of these climate actuators on the growth rate will be tested via simulation.

Question 6, the climate actuator with the largest influence on the temperature doesn't necessarily increase the duckweed growth the most. It is possible for a less sensitive climate actuator to influence the temperature in a better way, for example a solar screen that prevents the duckweed from overheating during the day and keeps the heat inside during the night to increase the growth. To find the climate actuator with the best growth results several simulations will be run.

## 2 Literature

In chapter 2.1 the effects of temperature on the growth rate are discussed. Not only the intrinsic growth rate, but also the influence of temperature on the dry weight and protein content of the duckweed. In chapter 2.2 growth factors except temperature are discussed such as the effect of light, and nutrients in the growth medium. These growth factors will not be investigated, but their influence is essential background information.

### 2.1 Growth as function of temperature

Temperature is among the most important environmental factors that control plant development, growth and yield (Yan and Hunt, 1999). In this chapter, the current and some alternative growth models as function temperature will be discussed. Also the growth/death rate at high temperatures will be discussed. In the end of this chapter other effects than growth as function of temperature will be discussed.

#### 2.1.1 Currently used growth model

To describe the growth of *L.minor*, the growth model of Lasfar et al. (2007) is used. This growth model is also used by van den Top (2014). The growth model is as follows:

Equation 2.1.1-1

$$r_i = \alpha_T * p_1 \left( \frac{T - T_{op}}{T_{op}} \right)^2 * p_2 \frac{T - T_{op}}{T_{op}}$$

Symbol	Meaning	Value	Unit
$r_i$	Intrinsic growth rate	-	$day^{-1}$
$\alpha_T$	Growth constant for other factors	-	$day^{-1}$
$p_1$	Non dimensional constant	0.41	—
$p_2$	Non dimensional constant	0.0025	—
$T$	Temperature growth medium	-	$^{\circ}C$
$T_{op}$	Optimal growth medium temperature	26	$^{\circ}C$

This model is based on the following graph.

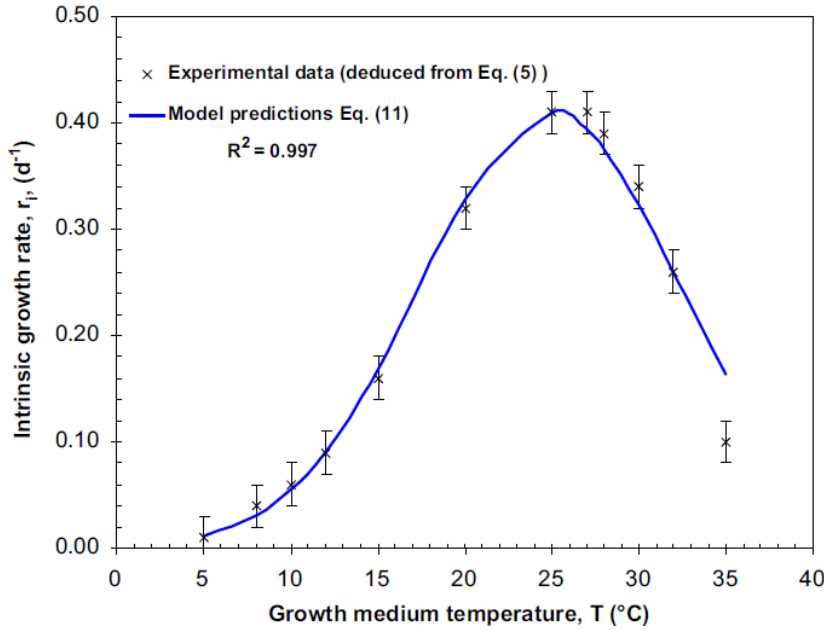


Figure 1 (Lasfar et al., 2007) Intrinsic growth rate as a function of temperature; the bars represent the maximum error.

The aim of the research of Lasfar et al. (2007) was to mathematically express the duckweed (*Lemna minor*) intrinsic growth rate. The intrinsic growth rate is different from the relative growth rate, because it corrects for the mat density. To correct for the mat density, the following formula is used.

Equation 2.1.1-2

$$\frac{dD}{dt} = \frac{D_l - D}{D_l} * r_i * D$$

Where  $D_l$  is the upper limit of the mat density, above this point the growth rate is close to zero.  $D$  is the instant mat density and  $D_0$  the initial mat density. When integrated, this formula gives the mat density as function of time.

Equation 2.1.1-3

$$D = \frac{D_l * D_0}{(D_l - D_0) * e^{-r_i * t} + D_0}$$

At temperatures above 30°C the error of the model is large. In Figure 1, one can see that the calculated curve differs from the measured data at 35°C. In the current model, extrapolation is used to approximate the growth rate of duckweed at these temperatures. Looking at figure 1, one can conclude that extrapolation is not accurate for higher temperatures.

The function is based on measured data. Looking at the graph, the function approximates the measurements accurately, except for higher temperatures. This can be explained by the limitations of a black/grey box model. This model is designed for temperatures from 5°C till 32°C. Above this temperature, the growth kinetics of duckweed change, and therefore the model loses accuracy.

### 2.1.2 Alternative growth models

For L.minor van der Heide et al. (2006) found a similar growth rate curve as Lasfar et al. (2007), as a function of temperature. In this research parameters of three different growth functions were estimated.

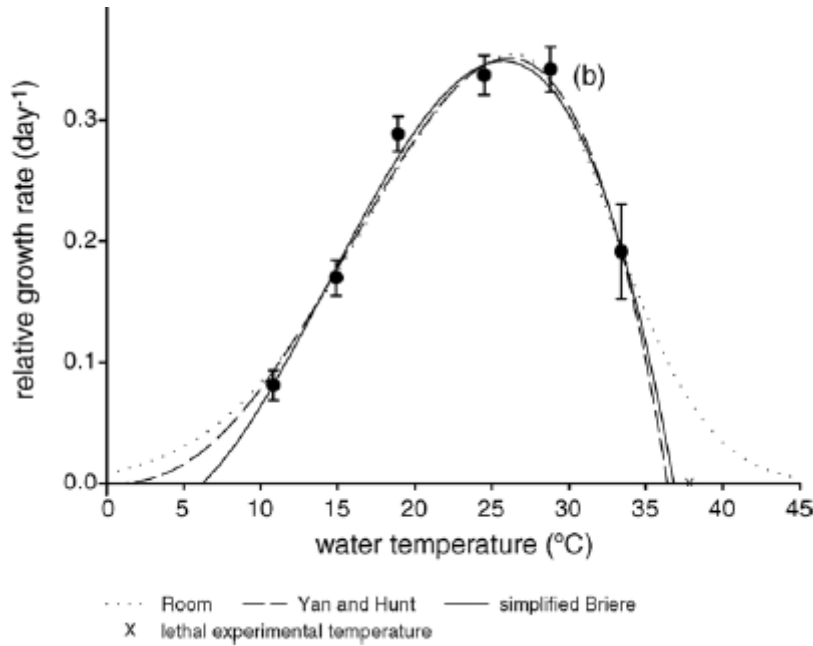


Figure 2 (van der Heide et al., 2006) Relative growth rate as a function of temperature; the bars represent the maximum error.

The relative growth rates at the different temperatures were calculated assuming exponential growth (Equation 2.1.1-2): exponential growth is assumed because the amount of biomass produced depends on the current amount of biomass. In this research, contrary to (Lasfar et al., 2007), the mat density is considered to have no effect on the growth rate of duckweed.

#### Equation 2.1.2-1

$$R = \frac{\ln(B_1) - \ln(B_0)}{\Delta t}$$

Symbol	Meaning	Unit
$R$	Relative growth rate	$day^{-1}$
$B_1$	Biomass at t=end	$kg$
$B_0$	Biomass at t=0	$kg$
$\Delta t$	Time interval between measurements	$day$

Room (1986) composed a mathematical model (Equation 2.1.1-2). In this model, a logarithmic relation between the temperature and the relative growth rate is assumed. The model is a linearized model around the maximum growth rate at the optimal temperature. The model is as follows (Figure 2, the dotted line):

Equation 2.1.2-2 (Room, 1986)

$$R = R_{max}e^x \begin{cases} x = a(T_{opt} - T)^2 \text{ if } T < T_{opt} \\ x = b(T_{opt} - T)^2 \text{ if } T > T_{opt} \end{cases}$$

Symbol	Meaning	Unit
$R$	Relative growth rate	$day^{-1}$
$R_{max}$	Maximum growth rate	$day^{-1}$
$a$	Crop specific growth parameter for temperatures lower than the optimum	—
$b$	Crop specific growth parameter for temperatures higher than the optimum	—
$T_{opt}$	Optimal growth temperature	$^{\circ}C$
$T$	Instant temperature of the duckweed	$^{\circ}C$

A major problem of this model is that it has a horizontal asymptote at  $R = 0$ . It is known that at high temperatures duckweed dies. One can see that, according to this model, the growth rate at 38°C is significant, but van der Heide et al. (2006) himself stated that L.minor dies at this temperature.

Yan and Hunt (1999) designed a model that predicts the growth rate of a plant, dependent on only three parameters, which can be determined experimentally (Figure 2, the striped line) .

Equation 2.1.2-3

$$R(T) = R_{max} * \left( \frac{T_{max} - T}{T_{max} - T_{opt}} \right) * \left( \frac{T}{T_{opt}} \right)^{\frac{T_{opt}}{T_{max} - T_{opt}}}$$

Symbol	Meaning	Unit
$R(T)$	Relative growth rate as function of temperature	$day^{-1}$
$R_{max}$	Maximum growth rate	$day^{-1}$
$T$	Temperature	$^{\circ}C$
$T_{max}$	Maximum temperature for which the duckweed does not die	$^{\circ}C$
$T_{opt}$	Optimal growth temperature for the duckweed	$^{\circ}C$

In this growth model,  $T_{min}$  is assumed to be zero, and therefore omitted from this formula. The model only has three model parameters, therefore theoretically, three measurements would be sufficient for the curve fitting, provided that the treatment temperatures span  $T_{opt}$  (Yan and Hunt, 1999).

### 2.1.3 Death rate of L.minor

Stanley and Madewell (1976) did research for growth and death rate of L.minor at high temperatures. In their research the 50% lethality ( $LD_{50}$ ) and the 50% growth inhibition ( $I_{50}$ ) level were determined for each 2°C interval from 40°C to 60°C.  $LD_{50}$  and  $I_{50}$  were identical, which indicated that acute toxicity was the only cause of inhibition. The temperature interaction followed the curve:

Equation 2.1.3-1

$$T = \begin{cases} 57,0 - 3,894 \log(t) & \text{if } (T < 50^\circ\text{C}) \\ 61,7 - 6,566 \log(t) & \text{if } (T > 50^\circ\text{C}) \end{cases}$$

Symbol	Meaning	Unit
$T$	Duckweed temperature	$^\circ\text{C}$
$t$	Time it takes before 50% of the population is extinct	$s$

This research showed a connection between light exposure and thermal tolerance. Exposure to light during the lethal temperature decreased mortality and increased subsequent growth with longer exposures at temperatures below 50° but had no effect with short exposures at temperatures above 50°C.

### 2.1.4 Growth kinetics

The energy to make essential molecules and growth material comes from photosynthesis. In the process of photosynthesis Rubisco is an enzyme catalysing the reaction to fixate carbon dioxide and energy. Rubisco can catalyse carboxylation, this is the forming of sugar, but Rubisco can also catalyse oxygenation, the burning of sugar (Evert and Eichhorn, 2013) If oxygenation is the dominant process, the plant will burn its fixed carbon and energy. Lemna Minor uses C3 photosynthesis (Landolt et al., 1987) to fixate carbon dioxide and solar energy, it therefore has no method to prevent oxygenation.

Whether carboxylation or oxygenation happens depends on the ratio of carbon dioxide and oxygen in the chloroplast (Farquhar et al., 1980). Duckweed gets most of its carbon dioxide and oxygen from the water it floats on (Filbin and Hough, 1985), therefore the concentrations and solubility of carbon dioxide and oxygen in water are important parameters. Because the solubility of carbon dioxide at room temperature is much higher than that of oxygen, the carboxylation dominates. Carbon dioxide and oxygen are less soluble at higher temperatures, but the solubility of carbon dioxide decreases much faster as function of temperature than that of oxygen (Farquhar et al., 1980). Therefore, at higher temperatures photorespiration increases. A plant cannot die because of photorespiration, but the growth can be strongly inhibited, or even stop (Evert and Eichhorn, 2013). This process explains the growth rate drop at temperatures above 30°C.

### 2.1.5 Dry weight as function of temperature

The dry weight fraction of L.minor is influenced by the temperature; especially at optimal temperatures, the dry weight percentage of L.minor is relatively low. The area per dry weight in L.minor rises from 12.5°C to 27.5°C to the threefold value (Hodgson, 1970).

The growth rate of L.minor is temperature dependent. The growth rate is highest for a temperature of 26°C, however, the dry weight production might be optimal at another temperature. Hodgson (1970) noted that the rate of net assimilation of L.minor only slightly rises from 12.5°C to 17.5°C and falls to  $\frac{2}{3}$  of the maximum value at 27.5°C. The growth rate is higher at 27.5°C, but the assimilation rate is lower.

### 2.1.6 Protein production as function of temperature

The existing model of van den Top (2014) describes the dry weight production of the duckweed at the Ecoferm. This duckweed is supposed to be protein rich dairy food, with a protein content ranging from 15% to 45% of dry weight (Landolt et al., 1987). However, the exact protein content of duckweed is unknown, and not calculated in the existing model. Protein per frond, per root, and per

unit dry weight is greater in plants grown at 23.9°C than at 18.3°C. Average protein content is 1.7-3.1-fold higher in fronds grown at 23.9°C than those grown at 18.3°C (Lehman et al., 1981). These numbers suggest that one can increase the protein production by controlling the temperature. Though this is an interesting topic I will not research it in this thesis.

### **2.1.7 Summary**

In the model of van den Top (2014) the lowest water temperature is round 5°C and the highest temperature round 42°C. At high temperatures (30°C and above) the existing growth model is incomplete. At these temperatures some of the duckweed will die. In the existing model, death is not possible. According to Stanley and Madewell (1976) 50% lethality is reached after 2 hours at 42°C; this temperature is reached at the Ecoferm. According to van der Heide et al. (2006) temperatures of 38°C, are lethal to *L.minor*.

## **2.2 Growth factors except temperature**

The growth of duckweed is dependent on several factors; in this chapter all growth factors except for the temperature will be discussed.

### **2.2.1 Solar radiation**

The measurement of light intensity is not always comparable. In literature, sometimes, light intensity is measured in lux,  $\text{mmol m}^{-2}\text{s}^{-1}$  or  $\text{Wm}^{-2}$ . There is no single conversion factor between lux,  $\text{mmol m}^{-2}\text{s}^{-1}$  and  $\text{Wm}^{-2}$ ; there is a different conversion factor for every wavelength, and it is not possible to make a conversion unless one knows the spectral composition of the light. However, for sunlight, there is an approximate conversion of 0.0079  $\text{Wm}^{-2}$  per lux, 0.22  $\text{Wm}^{-2}$  per  $\text{mmol m}^{-2}\text{s}^{-1}$  and 0.036  $\text{mmol m}^{-2}\text{s}^{-1}$  per lux.

It is difficult to determine the effects of the amount of light on the growth rate of duckweed, there are several factors influencing the photosynthesis rate. Both light intensity (chapter 2.2.1.1) and photoperiod (chapter 2.2.1.2) are important for the growth of duckweed (Peeters et al., 2013). Also there is a minimum threshold to start the photosynthesis and a saturation point for light intensity (Landolt et al., 1987). The minimum threshold, saturation point, and the photosynthesis rate also depend on temperature (Landolt et al., 1987).

#### **2.2.1.1 Light intensity**

Ashby and Oxley (1935) did research on photosynthesis in *L.minor* as function of light intensity and temperature, Figure 3 shows the findings of their research. Ashby and Oxley (1935) did not document the exact light composition used in the experiment, but they tried to approximate sunlight, so the estimation of 0.036  $\text{mmol m}^{-2}\text{s}^{-1}$  per lux ( $16000 \text{ lux} = 5.8 \cdot 10^2 \text{ mmol m}^{-2}\text{s}^{-1}$ ) should be fairly accurate.



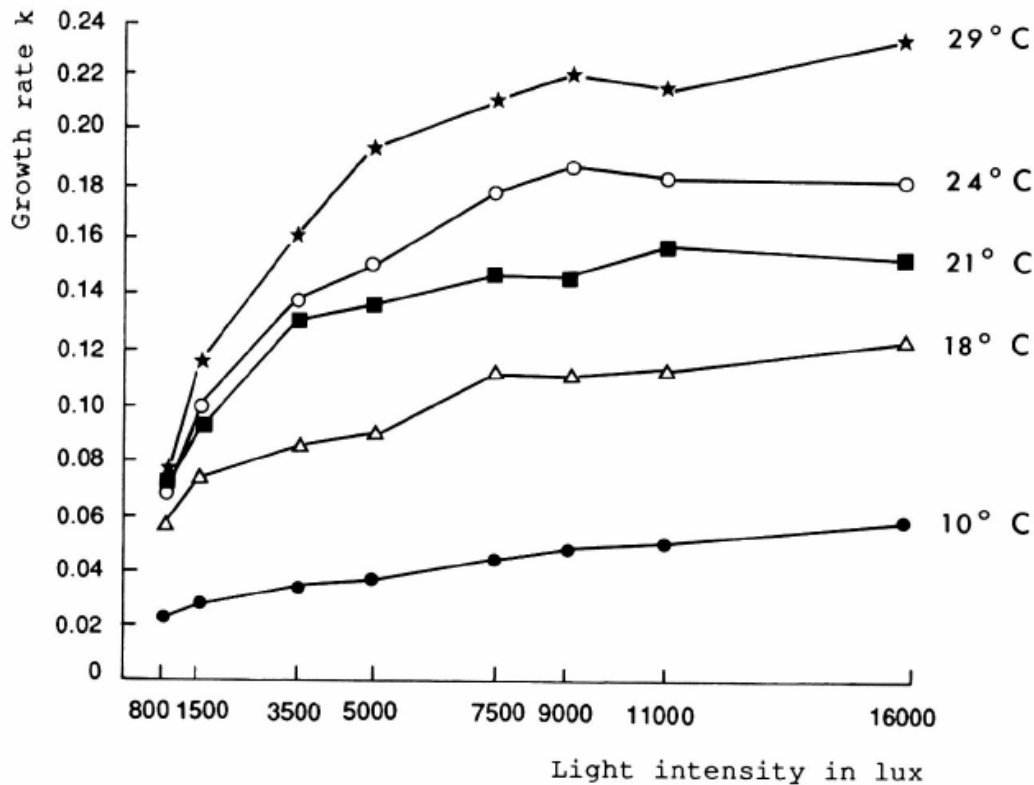


Figure 3 (Ashby and Oxley, 1935) Growth rates of *L. minor* at different light intensities and different temperatures

The effects of light intensity and temperature on photosynthetic oxygen evolution by two week old cultures of Lemna were investigated by Wedge and Burris (1982). Photosynthesis was light-saturated at  $600 \mu\text{E m}^{-2} \text{s}^{-1}$  for all temperatures, except  $30^\circ\text{C}$  where saturation was at  $300 \mu\text{E m}^{-2} \text{s}^{-1}$  (full sunlight was measured as  $1400 \mu\text{E m}^{-2} \text{s}^{-1}$ ). At light intensities higher than  $1200 \mu\text{E m}^{-2} \text{s}^{-1}$  photosynthesis was inhibited. Similar experiments were performed with six week old cultures of Lemna and photosynthesis was again saturated at  $300\text{-}600 \mu\text{E m}^{-2} \text{s}^{-1}$ , but photo inhibition did not occur until at least  $2000 \mu\text{E m}^{-2} \text{s}^{-1}$ . These results suggest that older fronds are more robust.

### 2.2.1.2 Photoperiod

The relation between photoperiod and growth rate is linear at low light intensities; at higher light intensities they approach an optimum asymptotically. The growth rate of Lemnaceae is highest under continuous light ((Ashby, 1929), (Landolt, 1957)). Near light saturation, the increase is no longer linear. One must notice that this research is done on *L. gibba* instead of *L. minor*, both are in the Lemnaceae family of duckweed, but they are a different species. At optimal intensities the optimal photoperiod for *L. minor* is 13 hours (Lasfar et al., 2007).

### 2.2.2 Growth medium and nutrients

The availability of nutrients is crucial for growth, in chapter 2.2.2.1 and 2.2.2.2, the required concentration for nutrients in the growth medium will be discussed. Not only availability of nutrients, but also the acidity (chapter 2.2.2.3) and availability of carbon dioxide (chapter 2.2.2.4) are important factors.

### 2.2.2.1 Nitrogen and phosphorus

The research by Szabó et al. (2005) showed that nitrogen and phosphorus have the largest effect on the growth rate of duckweed, compared to all other components.

In Lasfar et al. (2007), it was found that the L.minor intrinsic growth rate does not depend on the N and P concentrations, as long as they exceed 4.0mg-NL<sup>-1</sup> and 0.74 mg-P L<sup>-1</sup> respectively (Figure 4 and Figure 5).

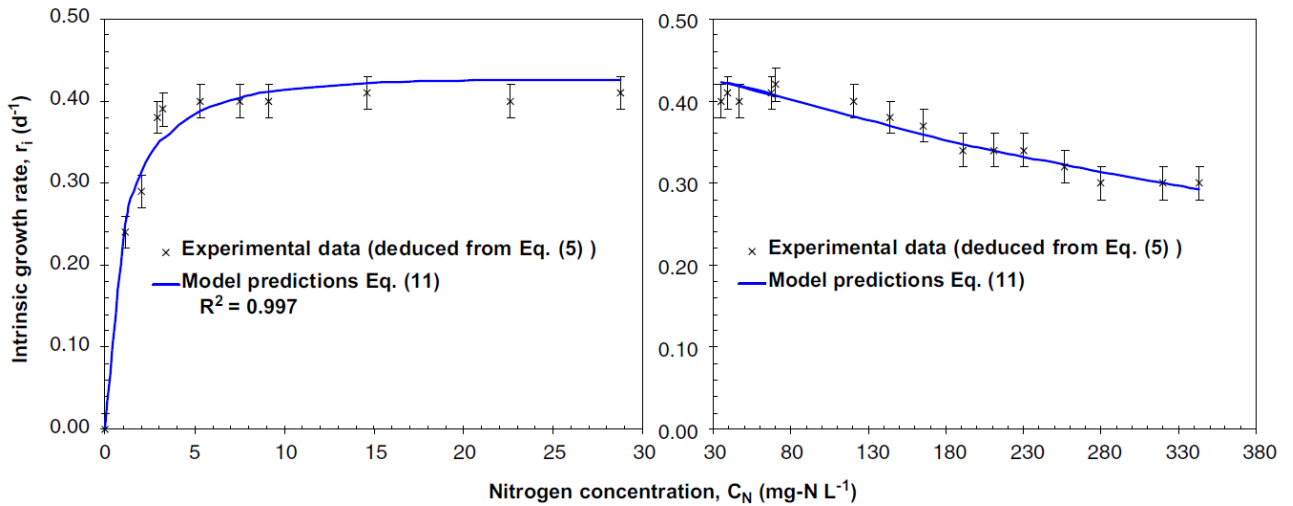


Figure 4 (Lasfar et al., 2007) Intrinsic growth rate as a function of nitrogen concentration.

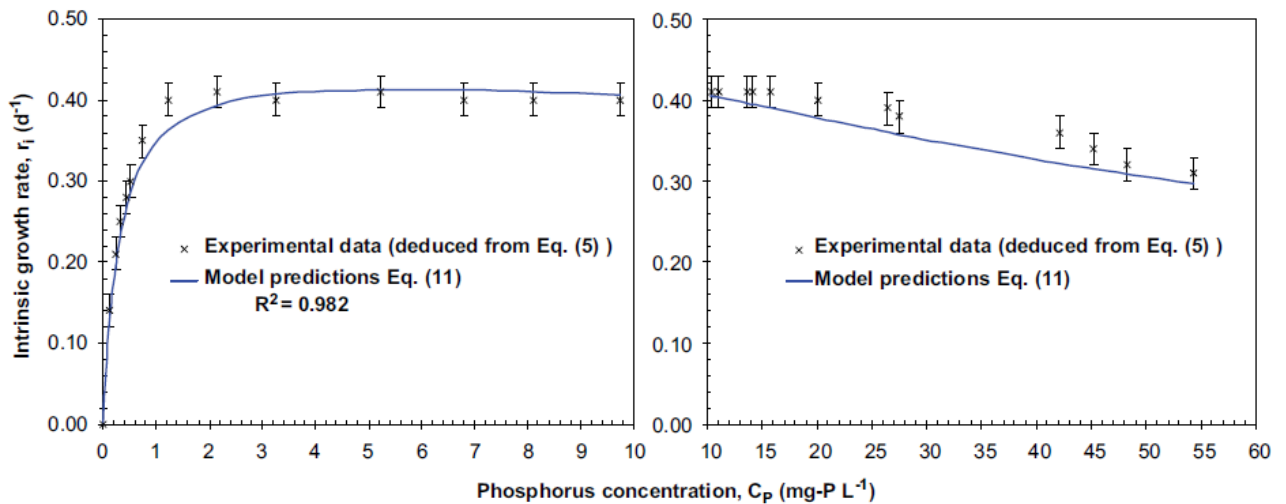


Figure 5 (Lasfar et al., 2007) Intrinsic growth rate as a function of phosphorus concentration.

Duckweed is able to take up nitrogen in the form of nitrate, nitrite, ammonium, urea or amino acids. However, the most important substances are nitrate and ammonium Landolt et al. (1987)

Ammonia is in the breath of the rose calves and is also evaporated from the urine in the stable. This results in an increased ammonia concentration in the air of the stable. This air is ventilated through the biobed into the greenhouse, increasing its ammonia concentration.

#### **2.2.2.2 Other nutrients**

#### **2.2.2.3 Acidity (Currey)**

The effect of the pH on duckweed plants is complex, because the solubility of all nutrients change with different pH values. Exceeding the pH limits causes growth inhibition and finally duckweed mortality. The lower pH limit is due to CO<sub>2</sub> uptake. When the pH of the medium decreases, it is hard to get sufficient CO<sub>2</sub> from the medium (Landolt et al., 1987). The optimal pH is fairly neutral. A pH of 6.2 is optimal according to van den Top (2014) and McLay (1976).

#### **2.2.2.4 Carbon dioxide**

L.minor requires a minimum CO<sub>2</sub> concentration of 65 ppm for autotrophic growth. At 330 ppm CO<sub>2</sub>, a concentration which corresponds to the normal air composition, L.minor has a much higher growth rate. A supply of 9000 ppm CO<sub>2</sub> does not increase the growth rate, but the dry weight of the fronds (Landolt et al., 1987). Duckweed can also take up carbon from the growth medium. Filbin and Hough (1985) found that, most of the carbon uptake of L.minor comes from the growth medium. When there is not enough carbon available in the medium, carbon is taken up directly from the air. This however slows down the growth rate. Higher concentrations of CO<sub>2</sub> in the air increase the rate at which the CO<sub>2</sub> dissolves in water. Therefore an increase in CO<sub>2</sub> concentrations in the greenhouse are important.

#### **2.2.3 Lag period**

Previous studies showed that duckweed needs some time to accumulate to a new growth medium. Alaerts (2000) noticed that there was a slight N and P reduction in the growth medium after switching to a different growth medium, but no growth. This phenomenon indicates that the duckweed accumulated N and P in its cells without increasing its weight during the lag phase, resulting in a higher N and P contents of the duckweed.

The lag period is fairly long for duckweed, according to Landolt et al. (1987): in Lemnaceae the preconditions of cultivation have a much longer lasting effect on the growth rate than in unicellular organisms, since the formation of the new buds takes place many days before their appearance. As a rule, the experimental conditions should be kept constant for at least 4 weeks before beginning the growth rate measurements. Since the appearance of new daughter fronds is enabled by the elongation of the cells, short-time change in the culture conditions (e.g. short fluctuation of temperature, replacement of the nutrient solution) may show up in a short-term change of growth rate.

### **3 Simulation**

In this chapter the simulation model is described, this model is an expansion of the model of (van den Top, 2014). In chapter 3.1 the climate model of the Ecoferm is described, in chapter 3.4 the growth model of duckweed is described and in chapter 3.5 climate actuators to control the growth conditions of the duckweed are described.

#### **3.1 The Ecoferm as it is**

The Ecoferm greenhouse is built on top of a rose calve stable. The stable and the greenhouse have a large contact surface. Also the ventilation from the stable goes into the greenhouse via the biobed, so the interaction between those components therefore is large. These three rooms all have their

own climate behaviour. In this chapter the climate behaviour and the interaction of these compartments will be discussed.

Building properties are important parameters for the model. In this thesis the most important building properties are related to heat transfer between building components and solar Irradiance. The orientation and roof angle influence the solar energy that is available for the duckweed plants. In figure 8, a map of the Ecoferm farm with the orientation and dimensions is given.

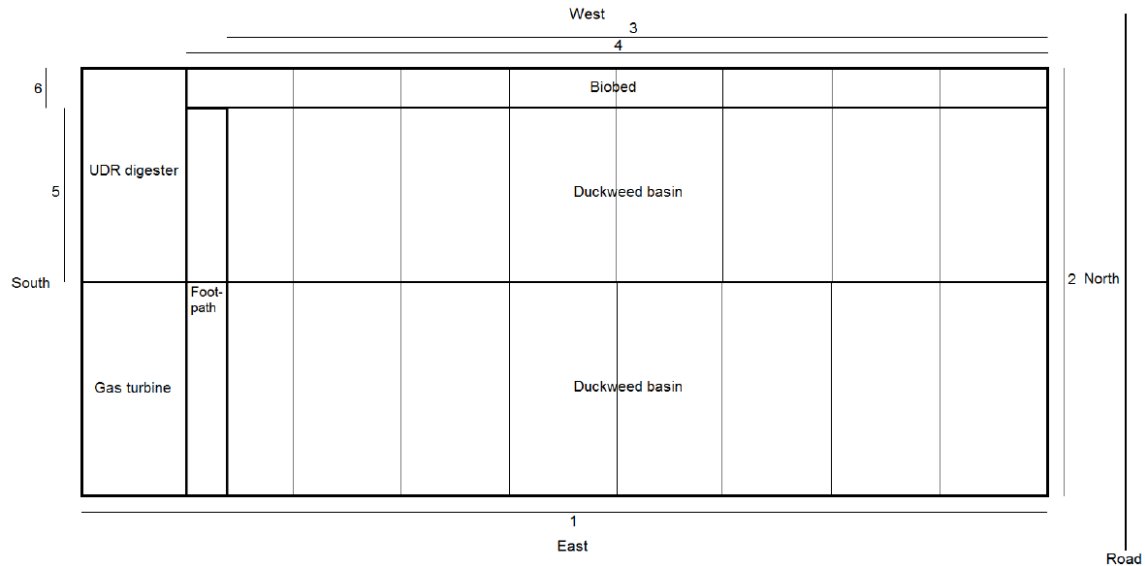


Figure 8 – Map of the ECOFERM farm with the orientation. The thin blocks are the eight departments on the ground floor, the thick blocks are the duckweed basin and biobed(van den Top, 2014). The numbers are lengths and given in table 1.

Number	Length (m)	Orientation	East-West
1	110	Latitude	52.26
2	52	Longitude	5.76
3	95	Roof angle(°)	14.50
4	100	Height first floor (m)	4.25
5	22	Height second floor (m)	3.75
6	4	Height roof (m)	7.00
		Height basin (m)	0.50
		Depth growth medium(m)	0.30

Table 1 – Building properties of ECOFERM: lengths, various heights, orientation and roof angle(Kroes, 2014; van den Top, 2014).

Because the duckweed basin is not symmetric with the building, a roof side specific calculation must be made to determine the correct solar irradiance per square meter. The orientation and specific building properties are important to develop a thermal model of the greenhouse. These building properties are given in table 1.

### 3.2 Integration method

The integration method is important for the accuracy, therefore several methods have been taken into account.

### 3.2.1 Ode45

This is the standard integration method of Matlab. It integrates a function with a variable 4<sup>th</sup>-5<sup>th</sup> order runge kutta method. This Integration method is accurate at the cost of medium computation time. This integration method has problems with Boolean operators in the climate controller.

### 3.2.2 Ode23

This integration method is less accurate than Ode45 because it only uses variable 2<sup>th</sup> and 3<sup>th</sup> order runge kutta this function is also programmed to handle moderately stiff systems, it therefore can handle the Boolean operators of the controller.

### 3.2.3 Euler

Euler is the simplest integration method, does not give any errors and has the fastest computation time. It also has the lowest accuracy of all of them.

### 3.2.4 Euler vs ode23

To determine which integration method is the best for the experiments, a simple test is performed. In this test only twenty days of the summer of the year are simulated. Ode23 took 164s and Euler 75s for the same simulation. The decrease in simulation time is especially useful for analysis of the system such as, sensitivity analysis. The largest difference in temperature between the two simulation methods was 0.04 °C. This difference was not increasing in time. Because the Euler method was more than twice as fast as Ode23 and because the difference in result was irrelevant, the Euler method is used in further simulations.

## 3.3 Climate model

In this chapter the formulas used in the climate model are discussed. In chapter 3.3.1 the main formula about the change in temperature is discussed. Chapter 3.3.3.1 is about interaction of components of the greenhouse due to evaporation and condensation. All the outdoor climate data is coming from (KNMI, 2009), further referred to as selyear.

### 3.3.1 Change in temperature

The temperature is important for the growth of duckweed. In the model the following states represent a temperature:  $T_{stable}$   $T_{biobed}$   $T_{greenhouse}$   $T_{water}$   $T_{roof}$  and  $T_{duckweed}$ . The change in these temperatures is calculated using a differential equation.

Equation 3.3.1-1

$$\frac{dT}{dt} = \frac{Q_{production} + Q_{convection} + Q_{rad} - Q_{latent} + Q_{vent} + Q_{r_{H2O}}}{\rho \cdot cp \cdot V}$$

Variable	Definition	Unit
$\frac{dT}{dt}$	Change in temperature	°C · s <sup>-1</sup>
$Q_{vent}$	Energy flow by ventilation(chapter 3.3.4.1)	W
$Q_{production}$	Energy production of the compartment, currently there is only heat production in the stable(chapter 3.3.5.1)	W
$Q_{convection}$	Energy flow as effect of convection(chapter 3.3.1)	W
$Q_{rad}$	Energy flow due to radiation(chapter 3.3.1)	W
$Q_{latent}$	Energy flow sensible heat to latent heat(chapter	W

	3.3.3.4)	
$\rho$	Density of the material	$\frac{kg}{m^3}$
$cp$	Specific heat capacity of the material	$\frac{J}{kg \cdot K}$
$V$	Volume of the material	$m^3$

### 3.3.1 Radiation

#### 3.3.1.1 Outdoor radiation

Solar radiation has a large influence on the climate in the Ecoferm greenhouse. The effects of solar radiation on the greenhouse tem

The intensity of the radiation in the greenhouse is calculated based in the sun position and measured sunlight intensity. The measured sunlight intensity is from the selyear dataset.

The declination of the sun

Equation 3.3.1-1 (Keller and Costa, 2011)

$$\begin{aligned} \text{declination} = & 0.3963723 - 22.9132845 \cdot \cos(\text{timeDegree}) + 4.0254304 \\ & \cdot \sin(\text{timeDegree}) - 0.387205 \cdot \cos(\text{timeDegree}) + 0.05196728 \cdot \sin(2 \\ & \cdot \text{timeDegree}) - 0.1545267 \cdot \cos(3 \cdot \text{timeDegree}) + 0.08479777 \\ & \cdot \sin(\text{timeDegree}) \end{aligned}$$

Correction for the time difference between the solar time and the mean solar time

Equation 3.3.1-2(Keller and Costa, 2011)

$$\begin{aligned} dt.eot = & 229.2 \cdot (0.000075 + 0.001868 \cdot \cos(\text{timeDegree}) - 0.032077 \cdot \sin(\text{timeDegree}) \\ & - 0.014615 \cdot \cos(2 \cdot \text{timeDegree}) - 0.04089 \cdot \sin(2 \cdot \text{timeDegree})) \end{aligned}$$

Correction for the time difference between the time zone and the local time. The time system we use uses time zones, assuming the time in a zone is the same everywhere. The movement of the sun, however is continues. This causes a difference in solar time and local civil time.

Equation 3.3.1-3(Ooster, 2014)

$$dt.lct = ((\text{longitude}/15) - \text{timezone}) \cdot 60$$

All previously mentioned corrections are combined in the following formula.

Equation 3.3.1-4

$$\text{time.lst} = \text{time.out} + dt.eot + dt.lct$$

Hour angle, angle of the sun, 0 when the sun is perpendicular to the earth surface at the specific location.

Equation 3.3.1-5(Keller and Costa, 2011)

$$ha = (720 - \text{time.lst})/4$$

Elevation, elevation angle of the sun

Equation 3.3.1-6(Keller and Costa, 2011)

$$elevation = asin(cosd(latitude) \cdot cos(ha) \cdot cos(declination) + sin(latitude) \cdot sin(declination))$$

Azimuth Calculate azimuth corner. Azimuth angle from north, moving to the east gives a positive sign

Equation 3.3.1-7(Keller and Costa, 2011)

$$azimuth = acos((sin(latitude) \cdot cos(declination) \cdot cos(ha) - cos(latitude) \cdot sin(declination)) / cos(elevation))$$

It is assumed that when the solar angle is below 0° the sun does not give any radiation. Sets azimuth to 0 when it is night

$$elevation(elevation < 0) = 0$$

$$azimuth(elevation \leq 0) = 0;$$

Makes the azimuth negative after solar noon. After noon, the azimuth decreases.

$$inRange = (time.lst \geq 720);$$

$$azimuth(inRange) = -azimuth(inRange);$$

### 3.3.1.2 Radiation in the greenhouse

The greenhouse is heated by solar radiation. All the objects in the greenhouse also have interaction via radiation. Due to low temperature differences, the objects in the greenhouse do not emit a significant amount of shortwave radiation, therefore only long wave radiation is taken into account.

Equation 3.3.1-8

$$\left. \begin{matrix} Q_{rol} \\ Q_{rdwl} \\ Q_{rwl} \end{matrix} \right\} = A_{roof} \cdot E_{roof} \cdot \sigma \cdot \left\{ \begin{matrix} Esk \\ Edw \\ Ew \end{matrix} \right\} \cdot \left( \left( \left\{ \begin{matrix} T_{sky} \\ T_{duckweed} \\ T_{water} \end{matrix} \right\} + T_k \right)^4 - (T_{roof} + T_k)^4 \right)$$

Variable	Definition	Unit
$Q_{rol}$	Long wave radiation absorption from sky	$W$
$Q_{rdwl}$	Long wave radiation absorption from duckweed	$W$
$Q_{rwl}$	Long wave radiation absorption from water	$W$
$A_{roof}$	Area roof	$m^2$
$E_{roof}$	Emission coefficient for the roof	—
$\sigma$	Stefan Boltzmann constant	$\frac{W}{m^2} \cdot K^4$
$Esk$	Emission coefficient for the sky	—

$E_{dw}$	Emission coefficient for the duckweed	–
$E_w$	Emission coefficient for the water	–
$T_{sky}$	Sky temperature	°C
$T_{duckweed}$	Duckweed temperature	°C
$T_{water}$	Water temperature	°C
$T_k$	Convert factor from degrees Celsius to Kelvin	°C

### 3.3.2 Convection and conduction

In this chapter, heat flow by convection and conduction is discussed. The time constant of the outdoor temperature is very high, it takes roughly 1 hour to change 1.5 °C. The time constant for the walls is much faster which underpins that the walls are in quasi-steady state. Therefore the conductance of the wall can be approximated using a linear model resulting in simpler calculation. The thermal model of a quasi-steady state wall consists of a wall specific constant, together with a convection constant results in the thermal conductance of an element. These different elements can be air, water, duckweed or a construction element like a wall, roof or floor.

Equation 3.3.2-1

$$Q_{panel} = U \cdot A \cdot \Delta T$$

Variable	Definition	Unit
$Q_{panel}$	Heat transfer through the specific panel	$W$
$U$	Thermal conductance of the specific elements	$\frac{W}{m^2 \cdot K}$
$A$	Contact surface area	$m^2$
$\Delta T$	Temperature difference between the elements	°C

### 3.3.3 Humidity ratio and latent heat

Chapter 3.3.3.1 is about the interaction of temperature between several elements caused by means of evaporation and condensation. The rest of the paragraphs are about the behaviour of the humidity and its influence on the compartments. In these chapters a simplified model is used where it is assumed that vapour condensates instantaneous when the relative humidity is above 100%.

#### 3.3.3.1 Heat exchange by means of evaporation and condensation

Heat exchange through evaporation and condensation is only taken into account for in the greenhouse. This type of interaction is relevant for the temperature of the roof, duckweed and the basin. Equation 3.3.3-1 is the main formula calculating the heat exchange between air and a surface via evaporation and condensation. Basically, this formula is the product of the evaporation heat per mass unit and the mass of evaporated water. If the water condensates, the mass of evaporated water is negative. The interaction of heat by means of evaporation and condensation in the stable and the biobed do not significantly influence the temperature in the greenhouse and are therefore not calculated.

Equation 3.3.3-1 (Ooster, 2014)

$$Q_{H_2O} = (Hv_0 - 2.381 \cdot T_{sf}) \cdot \phi_{H_2O}$$

Variable	Definition	Unit
$Q_{H_2O}$	Heat transfer from the greenhouse air to the roof	$W$



	due to condensation on the roof.	
$Hv0$	Evaporation heat at 0°C	$\frac{J}{kg}$
$T_{sf}$	Surface temperature	
$\phi_{H2O}$	Mass flow rate of water vapour from the indoor air to the indoor side of the roof	$\frac{kg}{s}$

The vapour mass flow of duckweed is calculated using Equation 3.3.3-2 this formula is area of the evaporating surface multiplied by the evaporation flux. The evaporation flux is calculated using the mass transfer coefficient multiplied by the saturation concentration difference between the evaporation surface and the air. The mass transfer coefficient is calculated with Equation 3.3.3-3. The saturation concentration is calculated using the function saturation concentration (Equation 3.3.3-5).

Equation 3.3.3-2

$$\phi_{H2O} = A \cdot k \cdot (sc_a - sc_s)$$

Variable	Definition	Unit
$A$	Surface area	
$k$	Mass transfer coefficient	$\frac{m}{s}$
$sc_a$	Saturation concentration of water vapour at air temperature	$\frac{kg}{m^3}$
$sc_s$	Saturation concentration of water vapour at surface temperature	$\frac{kg}{m^3}$

The mass transfer coefficient is a constant which can be calculated when the heat transfer coefficient of the surface material and basic air properties.

Equation 3.3.3-3

$$k = \frac{\alpha_g}{\rho_{air} \cdot cp_{air} \cdot Le^{\frac{2}{3}}}$$

Variable	Definition	Unit
$\alpha_g$	Heat transfer coefficient from air to surface	$\frac{W}{m^2 \cdot K}$
$Le$	Lewis number	–

### 3.3.3.2 Relative humidity and humidity ratio

The humidity ratio of the outdoor air is coming from (KNMI, 2009), this This is the relative humidity in percentage of the saturation concentration. To solve mass flows, the mass of vapour must be known, therefore the relative humidity is recalculated to the humidity ratio in kg vapour per kg air.

Equation 3.3.3-4

$$X = rh \cdot Xs$$

Variable	Definition	Unit
$X$	Humidity ratio	$\frac{kg \text{ vapour}}{kg \text{ air}}$

$rh$	Relative humidity as percentage of the saturation concentration	–
$X_s$	Humidity ratio at saturation concentration	$\frac{kg\ vapour}{kg\ air}$

The humidity ratio at saturation concentration is influenced by temperature and atmospheric pressure. This formula is used so often that we call this function saturation concentration. This contains the following bilinear model:

Equation 3.3.3-5 (Ooster, 2014)

$$X_s = \frac{0.622 \cdot p_{s_s}}{p_{atmair} - p_{s_s}} \begin{cases} p_{s_s} = 610.5 \cdot 10^{\frac{9.5 \cdot T}{265.5 + T}} \text{ if } (T < 0) \\ p_{s_s} = 610.5 \cdot 10^{\frac{7.5 \cdot T}{273.3 + T}} \text{ if } (T > 0) \end{cases}$$

Variable	Definition	Unit
$p_{s_s}$	Saturation vapour pressure according to the Magnus equation	$kPa$
$p_{atmair}$	Air pressure	$kPa$
$T$	Air temperature	$^{\circ}C$

### 3.3.3.3 Change in humidity ratio

In the compartments stable, biobed and greenhouse, there is air and thus a humidity ratio. The differential equation describing the change in humidity ratio is discussed here. We assume that the compartments have a homogeneous concentration. The differential equation is the following:

Equation 3.3.3-6

$$\frac{dX}{dt} = \frac{vap_p + vap_{in} - vap_{out}}{air_{mass}}$$

Variable	Definition	Unit
$\frac{dX}{dt}$	Change in humidity ratio of the compartment	$\frac{kg\ vapour}{kg\ air} \cdot s^{-1}$
$vap_p$	Vapour production in the compartment	$kg \cdot s^{-1}$
$vap_{in}$	Mass flow of vapour coming in the compartment	$kg \cdot s^{-1}$
$vap_{out}$	Mass flow of vapour going out the compartment	$kg \cdot s^{-1}$
$air_{mass}$	Total mass of dry air in the compartment	$kg$

Rewriting this formula to the variables in the model we get the following formula.

Equation 3.3.3-7

$$\frac{dX}{dt} = \frac{vap_p}{\rho_{air}} + \frac{(X_{in} - X_{out}) \cdot \phi_{fans}}{V}$$

Variable	Definition	Unit
$\rho_{air}$	Air density	$kg \cdot m^{-3}$
$X_{in}$	Humidity ratio of the ventilation flow coming into the compartment	$\frac{kg\ vapour}{kg\ air}$
$X_{out}$	Humidity ratio of the ventilation flow coming out of the compartment, this is the ventilation flow of the compartment itself	$\frac{kg\ vapour}{kg\ air}$

$\phi_{fans}$	Ventilation flow	$m^3 \cdot s^{-1}$
$V$	Volume of the air in the compartment	$m^3$

When the relative humidity is above 100%, it is assumed that the excessive vapour condensates instantaneous. The condense flow is calculated using the Equation 3.3.3-8. The function max is used so the condense flow cannot be negative, otherwise the air would always be saturated. Negative condense flow represents evaporation. The effect of condensation on the energy balance is calculated in chapter 3.3.3.4 Latent heat exchange.

Equation 3.3.3-8

$$\frac{dX_{condens}}{dt} = \frac{\max((X - X_s), 0)}{t_i}$$

Variable	Definition	Unit
$\frac{dX_{condens}}{dt}$	Change in humidity ratio due to condensation	$\frac{kg \text{ vapour}}{kg \text{ air}} \cdot s^{-1}$
$X$	Humidity ratio of the air in the compartment	$\frac{kg \text{ vapour}}{kg \text{ air}}$
$X_s$	Humidity ratio at saturation in the compartment	$\frac{kg \text{ vapour}}{kg \text{ air}}$
$t_i$	Integration time interval	s

### 3.3.3.4 Latent heat exchange

When water is evaporated, sensible heat is transferred to latent heat. Latent heat is the heat energy stored in water vapour. This heat is released in the form of sensible heat when water condensates. In Equation 3.3.3-9 the change in the latent heat due to change in humidity ratio and temperature is calculated. This energy flow is used to calculate the change in temperature in Equation 3.3.1-1.

Equation 3.3.3-9

$$Q_{latent} = \frac{dX}{dt} \cdot \rho_{air} \cdot V \cdot (Hv_0 + cp_{vap} \cdot T)$$

Variable	Definition	Unit
$Q_{latent}$	Change in latent heat	W
$\frac{dX}{dt}$	Change in humidity ratio	$\frac{kg \text{ vapour}}{kg \text{ air}} \cdot s^{-1}$
$\rho_{air}$	Air density	$\frac{kg}{m^3}$
$V$	Volume of air	$m^3$
$Hv_0$	Evaporation heat of water at zero degrees Celsius	$\frac{J}{kg}$
$cp_{vap}$	Heat capacity of vapour	$\frac{J}{kg} \cdot K^{-1}$
$T$	Temperature of the compartment	$^{\circ}C$

## 3.3.4 Ventilation

In the model, the ventilation flow is controlled using a simple controller. This controller calculates the required ventilation based on three variables: evaporated water, carbon dioxide production and the

temperature of the stable. In the chapter 3.5 Climate actuators, the possibilities of an extra ventilator are discussed.

### 3.3.4.1 Heat exchange by ventilation

In the compartments stable, biobed and greenhouse, heat exchange by ventilation takes place. This heat transfer is sensible, as well as latent heat. This heat exchange is calculated using a simple mass balance.

Equation 3.3.4-1

$$\Delta Q_{vent} = Q_{in} - Q_{out}$$

Variable	Definition	Unit
$\Delta Q_{vent}$	Change in heat due to ventilation	$W$
$Q_{in}$	Energy flow coming in the compartment both sensible and latent heat	$W$
$Q_{out}$	Energy flow going out the compartment both sensible and latent heat	$W$

These energy flows consist of sensible, as well as latent heat. The sensible heat flow is the following:

Equation 3.3.4-2

$$Q_{vent_{sens}} = \phi_{air_m} \cdot \Delta T \cdot cp_{air}$$

Variable	Definition	Unit
$Q_{vent_{sens}}$	Sensible heat flow by ventilation	$W$
$\phi_{air_m}$	Ventilation mass flow	$\frac{kg}{s}$
$\Delta T$	Temperature difference between compartments	$^{\circ}C$
$cp_{air}$	Heat capacity of air	$\frac{J}{kg} \cdot K^{-1}$

Equation 3.3.4-3

$$Q_{vent_{lat}} = \phi_{air_m} \cdot \Delta X \cdot (\Delta T \cdot cp_{vap} + Hv0)$$

Variable	Definition	Unit
$Q_{vent_{lat}}$	Latent heat flow by ventilation	$W$
$\phi_{air_m}$	Ventilation mass flow	$\frac{kg}{s}$
$\Delta X$	Difference in relative humidity between compartments	–
$\Delta T$	Temperature difference between compartments	$^{\circ}C$
$cp_{vap}$	Heat capacity of vapour	$\frac{J}{kg} \cdot K^{-1}$
$Hv0$	Evaporation heat of water at zero degrees Celsius	$\frac{J}{kg}$

Combining these formulas gives:

Equation 3.3.4-4

$$\Delta Q_{vent} = \phi_{air_m} \cdot (\Delta T \cdot (cp_{air} + \Delta X) \cdot cp_{vap}) + \Delta X \cdot Hv0$$

### 3.3.4.2 Ventilation control

First the required ventilation for three conditions, the humidity, carbon dioxide concentration and the temperature are calculated separately. Only the highest ventilation requirement will be used in further calculations, therefore the function max is used. Because the ventilation flow cannot exceed the max ventilation capacity, the function minimum is used to select the max ventilation capacity as ventilation flow when the required flow is higher.

Equation 3.3.4-5

$$\phi_{fans} = \min(\max(\phi_{H2O}, \phi_{CO2}, \phi_{temp}), max_{ventilation})$$

Variable	Definition	Unit
$\phi_{fans}$	Current ventilation flow	$m^3 \cdot s^{-1}$

#### 3.3.4.2.1 $\phi_{H2O}$ Ventilation for water vapour

The required ventilation flow for water vapour is the required ventilation to remove all vapour. If the value of  $\phi_{H2O}$  is negative, it represents a negative ventilation flow, which is impossible. Therefore it is filtered out later in the ventilation controller. If the required ventilation flow for vapour is larger than the max ventilation capacity, it will be limited to the maximum possible. The vapour that is not ventilated is stored in a mass balance.

Equation 3.3.4-6 (Ooster, 2014)

$$\phi_{H2O} = \frac{H2O_{calves}}{(x_{out} - x_{stable}) \cdot \rho_{air}}$$

Variable	Definition	Unit
$\phi_{H2O}$	Required ventilation flow to get rid of all evaporated vapour	$m^3 \cdot s^{-1}$
$H2O_{calves}$	Evaporated water by the calves	$kg \cdot s^{-1}$
$x_{out}$	Outdoor humidity ratio	$\frac{kg \text{ vapour}}{kg \text{ air}}$
$x_{stable}$	Humidity ratio in the stable	$\frac{kg \text{ vapour}}{kg \text{ air}}$
$\rho_{air}$	Air density	$\frac{kg}{m^3}$

#### 3.3.4.2.2 $\phi_{CO2}$ Ventilation for carbon dioxide

For the simplified controller, it is assumed that all produced carbon dioxide must be ventilated out of the stable. In a real ventilation controller, ventilation is also based on carbon dioxide concentration as indicator for air quality (Ooster, 2014).

Equation 3.3.4-7 (Ooster, 2014)

$$CO2_{calves} = \frac{Q_{calves} \cdot con \cdot P_{atmair} \cdot M_{CO2}}{t_h \cdot R \cdot (T_{stable} + T_K)}$$

Variable	Definition	Unit
$CO2_{calves}$	Carbon dioxide production by calves Equation 3.3.4-8	$kg \cdot s^{-1}$
$Q_{calves}$	Heat production calves, Equation 3.3.5-1	$W$

$con$	Constant CO2 production in relation to $Q_{calves}$	$h \cdot W^{-1}$
$P_{atmair}$	Air pressure from selyear	$kPa$
$M_{CO2}$	Molecular mass CO2	$kg \cdot kmol^{-1}$
$t_h$	Seconds in an hour	$s$
$R$	Molecular gas constant	$J \cdot kmol^{-1} \cdot K$
$T_K$	Conversion factor from degrees Celsius to kelvin	$^{\circ}C$

Equation 3.3.4-8 (Ooster, 2014)

$$\phi_{CO2} = \frac{CO2_{calves} \cdot 1 \cdot 10^6}{\left(\frac{M_{CO2}}{M_{da}}\right) \cdot (C_{CO2_{ut}} - C_{CO2_{out}}) \cdot \rho_{air}}$$

Variable	Definition	Unit
$\phi_{CO2}$	Required ventilation flow to get rid of all produced carbon dioxide	$m^3 \cdot s^{-1}$
$M_{da}$	Molecular mass dry air	$Kg \cdot kmol^{-1}$
$C_{CO2_{ut}}$	Upper threshold internal CO2 concentration	$ppm$
$C_{CO2_{out}}$	Outdoor CO2 concentration	$ppm$
$\rho_{air}$	Air density	$\frac{kg}{m^3}$

### 3.3.4.2.3 $\phi_{temp}$ Ventilation for temperature

The ventilation requirement for temperature is not sophisticated, it is assumed that temperatures above 30°C are undesirable for the calves. Ventilation requirement is therefore controlled with a simple if statement.

Equation 3.3.4-9

$$\phi_{temp} = \begin{cases} max_{ventilation}, & \text{if } (T_{stable} > 30) \\ 0, & \text{if } (T_{stable} < 30) \end{cases}$$

Variable	Definition	Unit
$\phi_{temp}$	Required ventilation flow to keep the stable temperature below 30°C	$m^3 \cdot s^{-1}$
$max_{ventilation}$	Maximum ventilation capacity of the ventilators in the stable	$m^3 \cdot s^{-1}$
$T_{stable}$	Air temperature in the stable	$^{\circ}C$

## 3.3.5 Stable

The stable has four types of heat transfer: convection and conduction, and sensible to latent heat and ventilation. For the behaviour of these subjects, see chapter 3.3.2, 3.3.3 and 3.3.4. Besides these general heat transfers, in the stable, there is also heat (chapter 3.3.5.1) and vapour (chapter 3.3.5.2) production by the calves. The produced carbon dioxide of the calves is discussed at chapter 3.3.4.2.2, because it is only used to determine the required ventilation flow.

### 3.3.5.1 Heat production

In the stable 1600 rose calves live, who produce heat. The formula below describes the produced amount of heat, where  $cft$  is a correction factor for the ambient temperature of the calves.

Equation 3.3.5-1 (Ooster, 2014)

$$Q_{calves} = (71.5 \cdot (m_{calve} + 150)^{0.5} - 880) \cdot n_{calves} \cdot cft$$

Variable	Definition	Unit
$Q_{calves}$	Total heat production of all the calves	$W$
$m_{calve}$	Mass of a single calve	$kg$
$n_{calves}$	Number of calves	–

Equation 3.3.5-2 (Ooster, 2014)

The floors of the stable are wet. When calves lie on these floors, heat will be transferred to the water on these floors, resulting in latent heat. To correct for this phenomena, a correction factor for the sensible heat is calculated.

$$cft = 4e^{-5} \cdot (T_{ref} - T_{stable})^3 + 1$$

Variable	Definition	Unit
$cft$	Correction factor for heat production of the rose calves as effect of the ambient temperature	–
$T_{stable}$	Ambient temperature of the calves(stable temperature)	$^{\circ}C$
$T_{ref}$	Reference temperature for the formula (20 $^{\circ}C$ )	$^{\circ}C$

### 3.3.5.2 Vapour production

Besides heat, calves also produce vapour. The amount of produced vapour is calculated based on the latent heat production. The latent heat production is calculated via the sensible heat production.

Equation 3.3.5-3 (Ooster, 2014)

$$Q_{calves_s} = Q_{calves} \cdot cfw \cdot (0.8 - 1.85 \cdot 10^{-7} \cdot (T_{stable} + 10)^4)$$

Equation 3.3.5-4

$$Q_{calves_l} = Q_{calves} - Q_{calves_s}$$

Variable	Definition	Unit
$Q_{calves_s}$	Sensible heat production of the total calve population	$W$
$cfw$	Correction factor wet floors	–
$Q_{calves_l}$	Latent heat production calves	$W$

The latent heat production is used to calculate the amount of evaporated water by the calves.

Equation 3.3.5-5

$$H2O_{calves} = \frac{Q_{calves_l}}{Hvo - 2381 \cdot T_{dbody}}$$

Variable	Definition	Unit
$H2O_{calves}$	Evaporated water by the calves	$kg \cdot s^{-1}$
$Hvo$	Evaporation heat at zero degrees Celsius	$J \cdot kg^{-1}$
$T_{dbody}$	Deep body temperature of the calves	$^{\circ}C$

### 3.3.6 Biobed

The biobed has four types of heat transfer, ventilation, conduction, radiation and sensible to latent heat. The ventilation also affects the amount of vapour inside the biobed. Besides heat transfers, there is also a lot of evaporation by the biobed. For calculation regarding the heat transfers and the vapour transfer see chapter....

#### 3.3.6.1 Vapour production and condensation

It is assumed that the humidity ratio in the biobed is at least 100% of the saturation concentration. In practice, air leaving the biobed is fully saturated (Haaring, 2014) In this model, it is assumed that water is instantaneous evaporated when the ventilation air from the stable enters the biobed. The following formula calculates the mass accumulation of water vapour in the ventilated air. When the humidity ratio in the stable is higher than the humidity ratio in the biobed condensation takes place which is represented by a negative value.

Equation 3.3.6-1

$$vent_{bi_{evap}} = \frac{(X_{bi_s} - X_{stable}) \cdot \phi_{fans} \cdot \rho_{air}}{t_i}$$

Variable	Definition	Unit
$vent_{bi_{evap}}$	Evaporated water in the ventilation air coming into the biobed, when water is compensated, this value is negative	$kg \cdot s^{-1}$
$X_{bi_s}$	Humidity ratio of saturation of the air in the biobed	$\frac{kg \text{ vapour}}{kg \text{ air}}$
$X_{stable}$	Humidity ratio of the air in the stable	$\frac{kg \text{ vapour}}{kg \text{ air}}$
$\phi_{fans}$	Current ventilation flow	$m^3 \cdot s^{-1}$
$\rho_{air}$	Air density	$\frac{kg}{m^3}$
$t_i$	Integration time interval	$s$

In the biobed, evaporation also takes place. The change in humidity ratio in the biobed is calculated using the following formula.

Equation 3.3.6-2

$$\frac{dx_{bi}}{dt} = \frac{x_{bi_s} - x_{bi}}{60}$$

Variable	Definition	Unit
$\frac{dx_{bi}}{dt}$	Change in humidity ratio in the air in the biobed due to evaporation and condensation	$s^{-1}$
$X_{bi}$	Humidity ratio in the biobed	$\frac{kg \text{ vapour}}{kg \text{ air}}$

### 3.3.7 Greenhouse

The greenhouse has three types of heat transfer, ventilation, conduction and sensible to latent heat due to evaporation. The greenhouse itself doesn't heat up directly by radiation. The radiation is absorbed by the roof, the water in the basin and the duckweed. For further explanations see chapter **Error! Reference source not found.** The ventilation also affects the amount of vapour inside the reenhouse. For further explanation about the evaporation by the water and the duckweed inside the



greenhouse see chapter 3.3.3.2. For calculation regarding the heat and vapour transfers see paragraph 3.3.3.1.

### 3.3.8 Water in basin

The water in the basin has three types of heat transfer, conduction, radiation and sensible to latent heat due to evaporation.

### 3.3.9 Duckweed

The duckweed in the basin has three types of heat transfer, conduction, radiation and sensible to latent heat due to evaporation.

### 3.3.10 Roof

The roof has three types of heat transfer, conduction, radiation and sensible to latent heat due to condensation.

## 3.4 Growth model of duckweed

The specific growth rate is calculated based on the maximum growth rate (in this formula called  $\alpha$ ) multiplied by a correction factor as function of the variance of the growth parameters.

Equation 3.3.10-1

$$r_i = \alpha \cdot f(x, u, p)$$

Where  $f(x, u, p)$  is the product of a function vector, which functions depend on the states (e.g. mat density and nutrient concentration), inputs and parameters of the system.

This formula is a simplified non-linearized system around an (optimal) point. The exact growth kinetics of duckweed are unknown, therefore black/grey box modelling is used to find a growth function.

## 3.5 Climate actuators

Greenhouse heating caused by global radiation is desirable during cold months, but not during hot months because results in high air temperatures in greenhouse interior space and thus reduction of crop production.

### 3.5.1 Whitewash

Whitewash is some sort of paint, which when applied to the greenhouse windows reduces the radiation transmission of the glass panes. Whitewash needs to be painted on the greenhouse when the solar heat load is so large that plants are damaged due to a high light intensity, or when the temperature in the greenhouse comes above critical values. One major problem of whitewash is that it's not flexible. Once whitewash is applied to the greenhouse, it will constantly provide shading until removed. This means that during periods of low light intensity, e.g. on a cloudy day, early in the morning and at dawn, the shade effect also is applied. The result can be less optimal light levels and decrease in productivity.

The costs associated with using shade compound are primarily the labour to apply and remove the shading compound, as the actual material is not expensive, though the labour costs will be incurred each year shade is applied (Currey, 2013).

(Mashonjowa et al., 2010) showed a decrease in the transmission coefficient of around 20% when whitewash was applied. When whitewash was applied smaller variation of indoor light intensity were measured than without whitewash. When whitewash was applied, the radiation in the greenhouse was almost entirely diffuse and therefore less sensitive to the presence of obstacles. So whitewash does not only influence the amount of light inside the greenhouse, but also influences the diffuse fraction. Increasing the incident fraction of diffuse irradiance, is known to enhance the radiation use efficiency and reduce the problem of leaf scorch common on sunny summer days.(Mashonjowa et al., 2010)

An special category of whitewash is near infrared radiation (Lowry et al.)- reflecting whitewash. NIR is less absorbed by the duckweed. NIR is not necessary needed for photosynthesis or plant growth, but this radiation still contributes to the solar heat load. Too much PAR light is not a problem for most plants, for the majority of plants cultivated in greenhouses, a high PAR and a low NIR transmission (in the summer) is therefore the optimal situation(Kempkes, 2012).

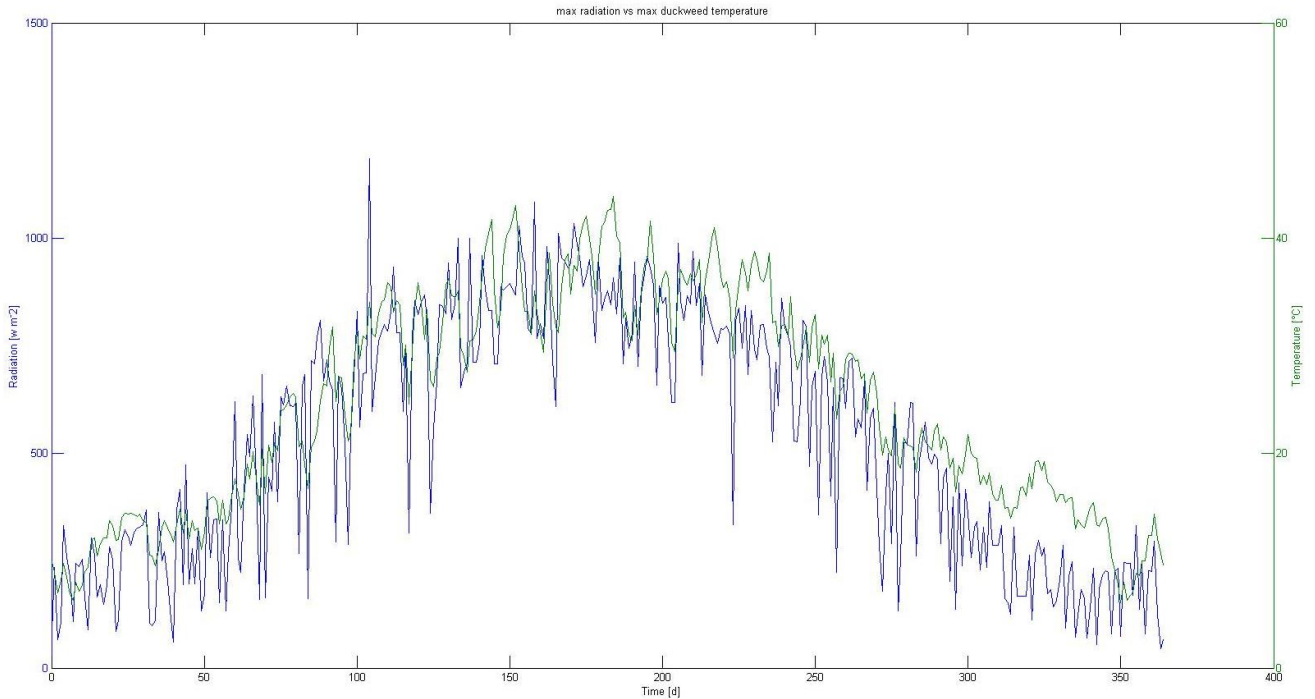
### 3.5.2 Indoor thermal screen

An indoor thermal screen is used to reflect (solar) radiation to decrease the heat load of the greenhouse. Additionally, one of the biggest benefits of shade curtains is that they can also double as an energy curtain when drawn at night to minimize the radiant heat loss and/or the volume of air to be heated



Figure 1 (Agricolas, 2015) half closed Indoor thermal screen

The duckweed temperature and the radiation energy are highly correlated. In the graph below one can see that with high radiation (blue line) the duckweed temperature is also high (green line).



Equation 3.5.2-1 thermal behaviour of the indoor thermal screen (Vanthoor et al., 2011)

$$\begin{aligned}
 Cap_{ThScr} \cdot T_{ThScr} &= H_{AirThScr} + L_{AirThScr} + R_{CanThScr} + R_{FlrThScr} + R_{PipeThScr} - H_{ThScrTop} \\
 &\quad - R_{ThScrCov,in} - R_{ThScrSky}
 \end{aligned}$$

Variable	Definition	Unit
$Cap_{ThScr}$	Heat capacity of the thermal screen	$J \cdot K^{-1}$
$T_{ThScr}$	Temperature of the thermal screen	$^{\circ}C$
$H_{AirThScr}$	Heat exchange between the thermal screen and the air	$W$
$L_{AirThScr}$	Latent heat flux caused by condensation on the thermal screen	$W$
$R_{CanThScr}$	Far infrared heat exchange between the canopy and the thermal screen	$W$
$R_{FlrThScr}$	Far infrared heat exchange between the floor and the thermal screen	$W$
$R_{PipeThScr}$	Far infrared fluxes between the thermal screen and the heating pipes	$W$
$H_{ThScrTop}$	Heat exchange between the thermal screen and the top compartment air	$W$
$R_{ThScrCov,in}$	Far infrared fluxes between the thermal screen and the internal cover layer	$W$
$R_{ThScrSky}$	Far infrared fluxes between the thermal screen and the sky	$W$

The air temperature of the compartment above the thermal screen  $T_{Top}$ , in this study denoted as the ‘top compartment’, is described by:

Equation 3.5.2-2

$$Cap_{Top} \cdot T_{Top} = H_{ThScrTop} - H_{TopCov,in} - H_{TopOut}$$

Variable	Definition	Unit
$Cap_{Top}$	Heat capacity of the air above the thermal screen	$J \cdot K^{-1}$
$T_{Top}$	Temperature of the air above the thermal screen	$^{\circ}C$
$H_{TopCov,in}$	Heat exchange between the top compartment air and the internal cover layer	$W$
$H_{TopOut}$	Heat exchange between the top compartment and the outside air	$W$

The thermal heat conductivity of the greenhouse cover is a greenhouse design parameter which can induce a significant temperature gradient across the cover due to its high insulation capacity. Therefore it is not acceptable to assume a constant temperature in the thermal screen, to compensate for this, both the internal cover temperature and external cover temperature have been modelled. Assuming that the heat capacity of the internal and external cover layer each constitute 10% of the heat capacity of the total cover construction, and assuming that conduction of energy is the only energy transport between the internal and the external cover. The internal and external cover temperature are described with the following formulas:

Equation 3.5.2-3

$$Cap_{Cov,in} \cdot T_{Cov,in} = H_{TopCov,in} + L_{TopCov,in} + R_{CanCov,in} + R_{FlrCov,in} + R_{ThScrCov,in} - H_{Cov,inCov,e}$$

Equation 3.5.2-4

$$Cap_{Cov,e} \cdot T_{Cov,e} = R_{GlobSunCov} + H_{Cov,inCov,e} - H_{Cov,eOut} - R_{Cov,eSky}$$

Variable	Definition	Unit
$Cap_{Cov,in}$	Heat capacities of the internal cover layer	$J \cdot K^{-1}$
$Cap_{Cov,e}$	Heat capacities of the external cover layer	$J \cdot K^{-1}$
$L_{TopCov,in}$	Latent heat flow caused by condensation on the greenhouse cover	$W$
$H_{Cov,inCov,e}$	Heat flow between the internal and external cover layer	$W$
$R_{GlobSunCov}$	Absorbed global solar radiation by the cover	$W$
$H_{Cov,eOut}$	Sensible heat flow from the external cover layer to the outside air	$W$
$R_{Cov,eSky}$	FIR exchange between the top cover layer and the sky	$W$

### 3.5.3 Outdoor sunscreen

Another type of sunscreen is an outdoor sunscreen. This sunscreen is positioned above the rooftop. Shade curtains are placed on the outside of a greenhouse are more effective at reducing temperatures inside a greenhouse because radiant energy from the sun is absorbed or reflected by the curtain outside, before it enters the greenhouse (Currey, 2013). However, the functional life of shade curtain placed outdoors is reduced due to exposure to the elements like snow.



Figure 2 (Hortidaily, 2015) Outdoor sunscreen

The model of an outdoor sun screen can be approximated by assuming there is a shade over the greenhouse and considering that there is no (or only FIR) interaction between the screen and the greenhouse.

### 3.5.4 Adiabatic cooling

Adiabatic cooling is evaporating water to transfer sensible to latent heat, resulting in a reduction in the greenhouse temperature. There are two types of adiabatic cooling in greenhouses. One type simply sprays water droplets throughout the entire greenhouse, resulting in evaporation, reducing temperature. The other type uses a porous wall and forced ventilation. In the porous wall, the water evaporates, reducing the temperature and the cool air is blown into the greenhouse. Both methods are commonly used in greenhouses. The sprayer is the cheapest of both methods, in terms of initial investment and energy use.

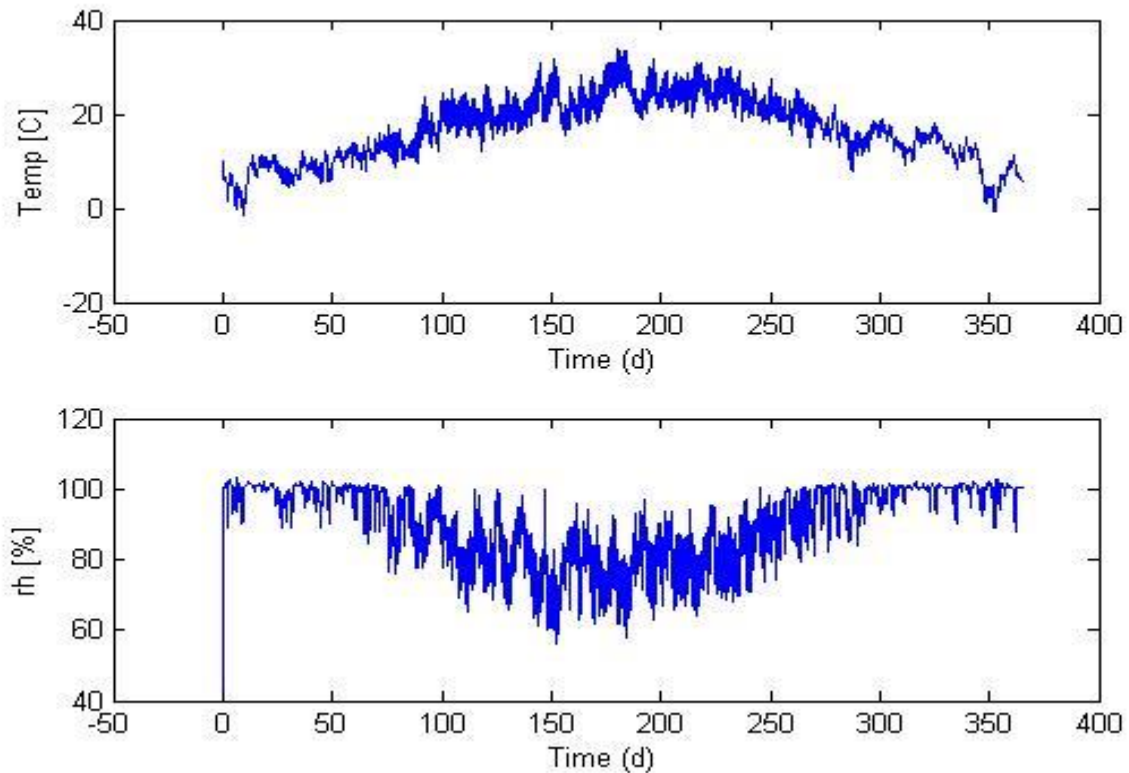


Figure 3 (FineArtAmerica, 2015) Adiabatic cooling sprayer



Figure 4 (Vegtech, 2015) adiabatic cooling porous wall

The porous wall is not literally used in this thesis, but the biobed had the same effect. In this thesis only the adiabatic cooling sprayer is tested as climate actuator. One might think, the air leaving the biobed is fully saturated, so no more adiabatic cooling can take place. This however is not true, the air coming from the biobed heats up in the greenhouse while maintaining the same absolute humidity. The relative humidity therefore lowers to up to and RH of 60% on hot days, as can be seen in the graph below. These days need cooling the most.



**Figure 5 Greenhouse temperature and greenhouse humidity**

For testing this method, a few assumptions need to be made.

It is assumed that this method for cooling does not have any shade effects. On hot days that this system should be active, the light intensity is far beyond the light saturation point of  $75 \frac{W}{m^2}$ , so minor shades from the droplets do not influence the growth rate.

The second assumption is that high humidity, and vapour droplets are no problem for duckweed. The humidity no problem for duckweed because it grows in water and is used to wet situation. The duckweed will not suffocate from water droplets because leaf surface is hydrophobic, resulting in water droplets sliding of the crop.

## 4 Materials and methods

The four most important parameters describing the growth of a plant as function of temperature are: the maximum growth rate and the maximum, minimum and optimal growth temperature (Yan and Hunt, 1999). Yet, the exact maximum temperature is still unknown. The behaviour of the duckweed

above this temperature is also unknown. Stanley and Madewell (1976) observed that in general, fronds killed by heat treatment became bleached after three days.

#### 4.1 Test setup

The test setup must meet several requirements:

- Growth of duckweed must be measured.
  - o The growth curve can be non linear.
- Temperature of the duckweed must be measured.
- Growth medium must not be a limiting factor.
- Radiation must not be a limiting factor.
- Temperature of the duckweed must be constant.
- Temperature gradient in the thermostatic bath must be low and at different containers must be equal.
- Switching between extreme and optimal temperature must be fast.
- Control and measurements must work autonomous and continue during the night.

In the design process, the requirements are taken into account.

#### 4.2 Components

In the pictures below an overview of the test setup is given



Figure 6 Thermostatic bath with samples

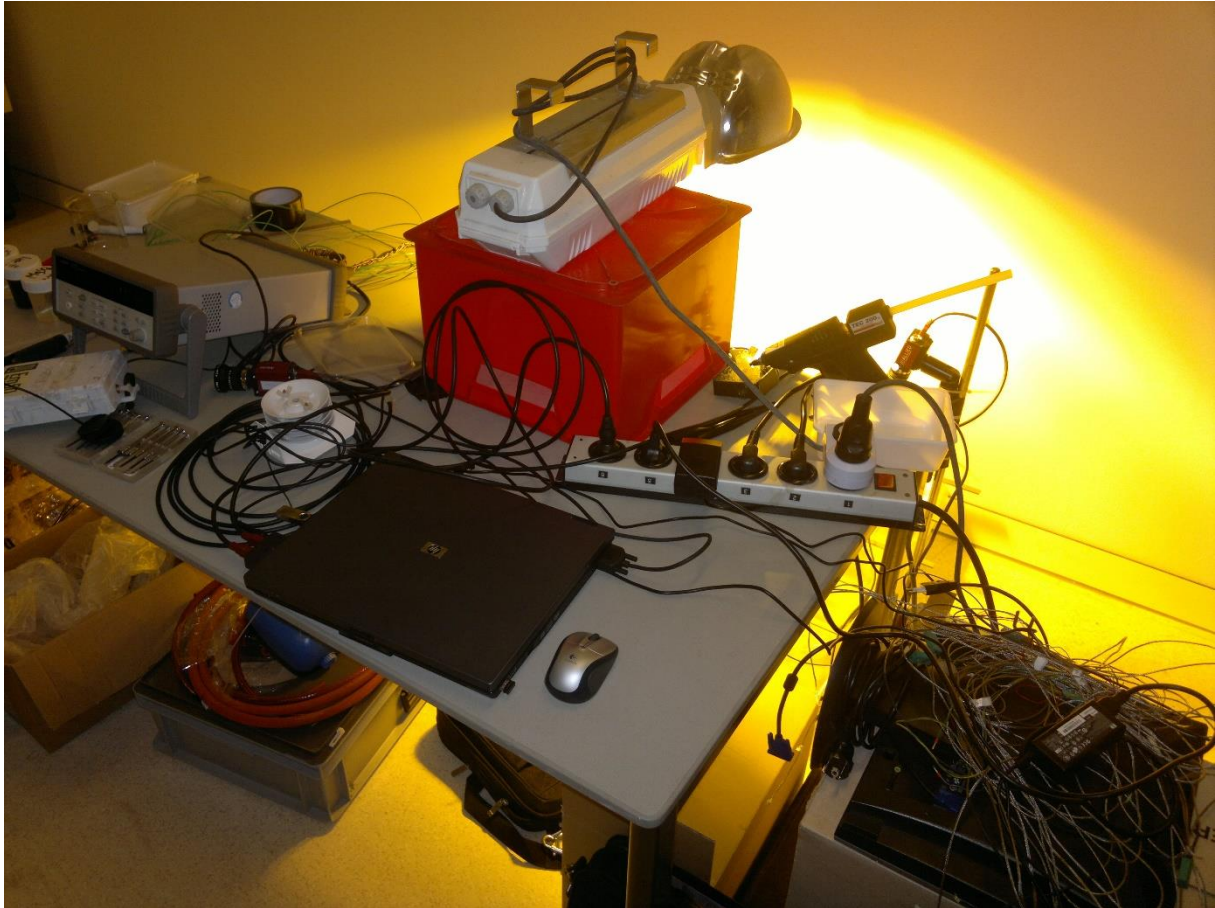


Figure 7 data logger and par lamp

#### 4.2.1 Thermostatic bath

The thermostatic bath is filled with water from the right temperature. In this thermostatic bath the sample tubes will be hung. There will not be any direct contact between the thermostatic bath water and the water inside the sample tubes. The thermostatic bath is 110 centimetres long, 60 centimetres wide and 20 centimetres high. The water level in the thermostatic bath is 15 centimetres high. Water lost by evaporation is manually refilled every day.

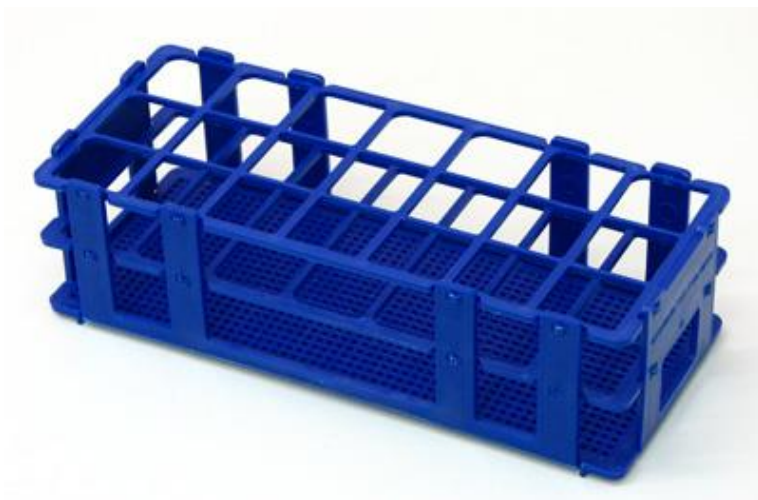


Figure 8 Tube holder from [www.labconusa.com](http://www.labconusa.com)



#### 4.2.2 Heater



Figure 9 Fisher Scientific Polystat 37 from [www.mmsidz.com](http://www.mmsidz.com)

To control the temperature in the thermostatic bath, the Fisher Scientific Polystat 37 is used. This device has an integrated feedback controller with a temperature stability is  $\pm 0.02^{\circ}\text{C}$  and the absolute temperature calibration of  $\pm 3^{\circ}\text{C}$ . Because of the high absolute temperature difference the set point of the Polystat 37 may differ from the desired temperature. Therefore the temperature of the duckweed is measured with thermocouples (chapter 4.2.7) and the set point is adjusted according to these measurements. The heater has a power of 2.0 kW. The device has a working range of  $20\text{-}200^{\circ}\text{C}$ , the minimum working temperature is dependent on the ambient temperature, because no external cooler is attached. Temperature selection is performed digitally and can be selected at a resolution of  $0.1^{\circ}\text{C}$

The circulation pump has a flow rate of 15l/min and is divided into two channels. One channel pumps water directly from the heater to the thermostatic bath. The other channel pumps water via a tube to the farthest corner from the heater of the container. This way the water in the container is steered and it is assumed the thermostatic bath has a perfect homogeneous temperature.

#### 4.2.3 Growth container

As growth container, first square containers of a dimension of 18 cm long, 12 cm width and 7 centimetres high were used. During the experiment it was found that it is difficult to keep the population in these containers clean. After 3 days of testing an algae population started to develop in these containers.



Figure 10 50ml growth container from [www.ecx.images-amazon.com](http://www.ecx.images-amazon.com)

#### 4.2.4 Par lamp

Duckweed needs PAR light to grow. In the first experiment a 1200 W halogen lamp was used. This lamp produced enough PAR, but it was found that it produced too much heat and its lifetime was too short to conduct one experiment. Because of these complications we searched for another lamp, this was an MASTER Green Power CG T 600W Mogul 1SL with an HS 2000 Armature. This light setup is commonly used in greenhouses. This lamp has a high emittance of PAR light and a low emittance of Infra-red radiation. This is essential, because infra-red radiation is not needed for photosynthesis but influences the temperature of the duckweed and thus the experiment. The lamp itself produces 80 W of direct heat, this is not influencing the duckweed. The lamp has an average lifetime of 32000 hours which is more than enough to conduct an experiment without a failing lamp. It has an ignition time of ten seconds to start emitting light and thereafter needs five minutes before it has the right temperature to emit the right light composition. These five minutes the light composition is not optimal, but on a photo period of sixteen hours, this can be neglected.

This light is switched on at 6:00 and switched off at 22:00, giving a photo period of 16 hours. This is not lethal to duckweed (chapter 2.2.1.2). These start and end times are chosen because from the sunrise to sunset, the duckweed might get enough solar energy to start growing. Because all the experiments need the same conditions, the light is switched on. When the light is on, the PAR intensity is around 600  $\mu\text{mol/s}$ . This is above the saturation point for photosynthesis for duckweed, but not lethal (2.2.1.1). Above this light intensity a little less or more light does not influence the growth rate.

Light Technical Characteristics	
Colour Code	220 [CCT of 2000K]
Colour Temperature	2000 K

Photosynthetic Photon Flux PPF	1100 $\mu\text{mol/s}$
Energy Used	600 W
Ignition Time	10 (max) s
Run-up time 90%	5 (max) min
Re-ignition Time [min]	1 (max) min
Energy Efficiency Label (EEL)	A++
Mercury (Hg) Content	30.0 mg
Energy consumption kWh/1000h	680 kWh



Figure 11 MASTER Green Power CG T 600W Mogul 1SL from [www.hortilux.nl](http://www.hortilux.nl)



Figure 12 HS200 armature with MASTER Green Power CG T 600W Mogul 1SL from [www.hortilux.nl](http://www.hortilux.nl)

#### 4.2.5 Growth medium

Duckweed needs more than water and light to survive. In the growth medium essential nutrients are solved. The concentration of these nutrients must not be a limiting factor.

For the estimation of nutrient concentration, we assume a growth rate that is only possible in theory. If one can produce a growth medium no limiting for this high growth rate, one is sure it is not limiting the growth in a real situation. For this reason a growth rate of 100kg dry weight of duckweed per hectare per day is assumed. The growth rate is recalculated to surface of the duckweed container. Concentrations of nutrients in *Lemna minor* are found in Landolt et al. (1987). In this same book, the limiting concentration of nutrients in a growth medium are found. The experiment lasts seven days. The volume of growth medium is 20 ml. The surface pf the duckweed is  $\pi * 1.5^2 = 7.1\text{cm}^2$ .

Equation 4.2.5-1

$$\begin{aligned} \text{TotalNutrientConsumption} \\ = \text{ProductionArea} \cdot \text{ProductionPerArea} \\ \cdot \text{ConcentrationOfTheNutrientInsideTheDuckweed} \cdot \text{DaysOfExperiment} \end{aligned}$$

Equation 4.2.5-2

$$\begin{aligned} \text{RequiredNutrients} \\ = \text{TotalNutrientConsumption} + \text{VolumeOfContainer} \\ \cdot \text{MinimumConcentration} \end{aligned}$$

With the method described above the following amount of nutrients is calculated.

Composition stock solution per litre	Required nutrient	Concentration in stock solution[g/l]	Required volume of stock solution[ml]	Consumed by the duckweed after one week [mg]	Minimum concentration after a week[mg/l]
2 gram MnSO4.H2O (169.02 gr/mole)	Mn	0.649627	0.437053	0.08874	0.001
2.7 gram H3Bo3 (61.83 gr/mole)	B	0.471616		Trace amount	Trace amount
0.5 gram ZnSO4.5H2O (287.54 gr/mole)	Zn	0.113723		0.04488	0.005
78 mg CuSO4.5H2O (249.68 gr/mole)	Cu	0.019837		0.00867	0.005
126 mg Na2MoO4.2H2O (241.9 gr/mole)	Mo	0.049952		Trace amount	Trace amount
Fe	Fe	1.116	0.354	0.39525	0.05
KH2PO4	K	35.33652	0.182	6.375	3.28
	P	28.01616		5.100	2.55
Ca(NO3)2.4H2O	Ca	2.547649	1.250	3.1875	1.87
	N	1.778907		21.93	8.42
MgSO4.7H2O	Mg	5.572037	0.320	1.785	0.30

Table 1 nutrient concentration growth medium

### 4.2.6 Camera

The camera used in this experiment is the ATV Marlin F-145C2 from National Instruments. The reason to choose this camera is:

- It has a good colour depth (12 bits).
- Resolution high enough to distinguish single duckweed fronds.
- It is fully supported by the LabVIEW software, making calibration easy.



Figure 13 ATV Marlin F-145C2 from [www.bilder3.eazyauction.de](http://www.bilder3.eazyauction.de)

Technical Specifications Marlin F-145C2	
Max Frame Rate	10 Hz
Spectrum	Visible Light
Colour depth	12 bits
Connection	IEEE 1394 (fire wire)
Resolution	1392x1040 pixels

Table 2 Technical Specifications Marlin F-145C2

#### 4.2.6.1 Lenses

For the lenses, a Pentax C60402 is a C-mount lens is used. This lens designed for 1/2-inch CCD industrial cameras. The lens has a fast f/1.6 aperture for good low-light images. The lens covers more than 86°. This is a manual iris lens with fixed focus. The iris can be closed down to f/16 to control brighter lighting conditions which is needed to take photos when the PAR lamp is on. The wide view of the lens make it possible for the camera to stand close to the setup and still picture everything. A major consequence of this is that it creates a large barrel distortion, but here can be calibrated for (paragraph 4.2.6.3).

Mount	C-Mount
Image Format	1/2 CCD
Focal Length	4.2 mm
Aperture	f/1.6 to Closed
Iris Type	Manual
Focus Type	Fixed
Horizontal View Angle	86.77°

#### 4.2.6.2 Calibration

There are two types of calibration spectral and spatial calibration.

Spectral calibration is calibrating the intensity of the pixels. The camera used in this experiment is already calibrated for the linearity of the sensor, value. The relationships between the different colour pixels is also dependent on the environment. During the measurements specific light conditions are present. The measurements happen indoors and an artificial light source present. These factors influence the light composition. But luckily, here fore can be calibrated. This is done by letting the camera look at an grey field. When looking at a grey field, a paper with RGB code (122,122,122), the histograms of the three different colours should all be the same. Because the

sensor shows linear behaviour, the sensor value can be multiplied by a constant to make the histograms match. This calibration is done with the help of the LabVIEW software. In this software package one can simply slide three sliders representing these constants. It is assumed that during the measurements the light conditions were constant.

Spatial calibration is calibrating the camera its pixel size. When taking a picture, not all pixels represent the same real world size. This deformation is dependent on the lens and lens settings (Figure 6). This spatial calibration is needed when using a camera to measure area. A calibration grid, a paper with black dots evenly distributed over the paper, is printed. The camera is mounted in its experimental condition and the calibration grid is placed on the place where the duckweed would be. The spatial calibration is also done with the help of the LabVIEW software. When LabVIEW is given the picture of the calibration grid, and the real world distance between the dots, it will calibrate camera automatically.

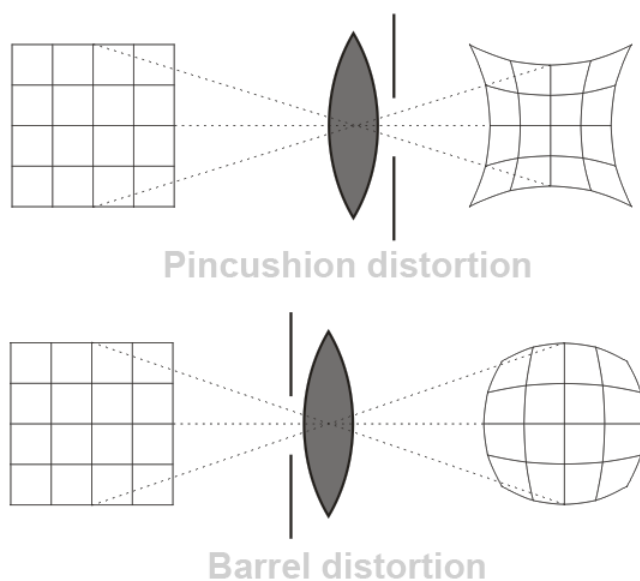


Figure 6 On the left is the camera sensor, on the right the real world area covered by one pixel. From [www.allphotolenses.com](http://www.allphotolenses.com)

#### 4.2.7 Temperature sensor

For the temperature measurements a type K(chromel - alumel) thermocouple is used. This thermocouple has a sensitivity of approximately  $41 \mu\text{V}/^\circ\text{C}$  and a range of  $-200^\circ\text{C} - 1350^\circ\text{C}$ . The sensor is linear at temperatures to  $185^\circ\text{C}$ . For this experiment the temperature of the surface of every container is measured with this K-type thermocouple. How the measurements of the produced voltage are done can be found in the next paragraph. PAR sensor

#### 4.2.8 PAR sensor

The PAR- intensity (Photo synthetically Active Radiation) is an important growth factor. In this experiment, the Apogee Instruments QSO-S PAR Photon Flux Sensor is used to measure the PAR-intensity. The PAR-sensor only measures wavelengths of (400-700) has a range of 0 to  $5,000 \mu\text{mol m}^2\text{s}^{-1}$  with an output of 0 – 1000 mV.

Before these sensors can be used for the experiments, first the characteristics of the sensors must be known to do reliable measurements. This work is done by(Saglibene, 2013), where the following characteristics are examined:

- Linearity of the sensors
- Offset of the sensors
- Difference between the ports of the data logger
- Drift of the sensors on long time measurements

It is found that the sensors give a linear output in the range of  $20 \mu V$  -  $1000 mV$ . The sensors do not have an offset. The ports of the sensor do not influence the measured value. The sensors that are used during the experiments are not affected by drift.

In (Saglibene, 2013)correction factors for the sensors are determined to calibrate the individual sensors. These corrections are very small and not significant for the experiment of my thesis, therefore, the standard Equation 4.2.8-1 provided by the manufacturer, to convert  $mV$  to  $\mu mol m^2 s^{-1}$  is used.

Equation 4.2.8-1

$$\mu mol m^2 s^{-1} = \left( \frac{1500}{4096} \right) \cdot 5.0 \text{ measured value in } mV$$

Figure Figure 14 Apogee Instruments QSO-S PAR Photon Flux Sensor from [www.decagon.com](http://www.decagon.com) shows a photo of the used sensor.



Figure 14 Apogee Instruments QSO-S PAR Photon Flux Sensor from [www.decagon.com](http://www.decagon.com)

#### 4.2.8 Data logger

As data logger the Agilent 34970A with 34901A 20-Channel Armature Multiplexer DMM is used. This device is used to log the data of the thermocouples and the par sensors.

The measurements are done inside a laboratory. In a laboratory, a lot of noise is generated by the power-line. Rejecting Power-Line Noise Voltages Normal mode noise rejection is achieved when the internal DMM measures the average of the input by “integrating” it over a fixed period. If you set the integration time to a whole number of power line cycles (PLCs) of the spurious input, these errors (and their harmonics) will average out to approximately zero.

An important feature of a multiplexer used as a DMM input channel is that only one channel is connected at a time. For example, using a multiplexer module and the internal DMM, you could configure a voltage measurement on channel 1 and a temperature measurement on channel 2. The

instrument first closes the channel 1 relay, makes the voltage measurement, and then opens the relay before moving on to channel 2 (called break-before-make switching)(Agilent). Therefore one data logger can be used to measure different channels and sensor types.

#### 4.2.8.1 Temperature measurement

The temperature is measured using thermocouples. A problem with thermocouples is that connecting them to the data logger creates another thermocouple at the connection. The type of thermocouple is known, so if one knows the temperature of the connection, a correction can be calculated. To do this, the DMM has a Built-in thermocouple reference junction, which measures the temperature of the connections with the data logger. To make sure the reference sensor and the connections are at the same temperature, an isothermal block is used to make the connections. An isothermal block is an electrical insulator, but a good heat conductor. An example for thermocouple type J(in the experiment a k type is used) is given in figure Figure 7.

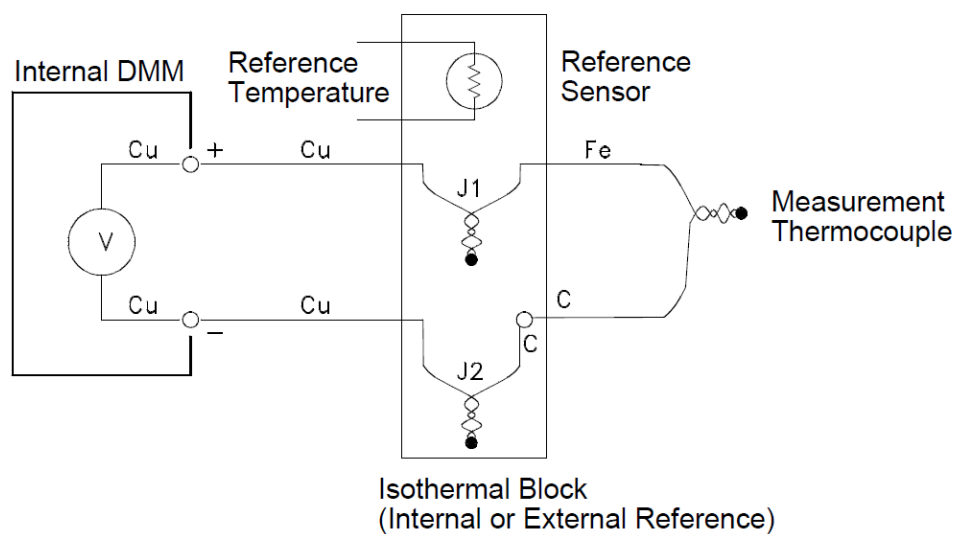


Figure 7 Built-in thermocouple reference junction (Agilent)

The calculations to convert the measured voltage and the reference temperature to the measured temperature are all performed by pre-programmed software in the Agilent 34970A.

For the temperature measurement, a K-type thermocouple is used. With the measurement technique described above the absolute measurement error should be  $\pm 1^\circ\text{C}$  with a temperature coefficient of  $0.03^\circ\text{C}$ .

#### 4.2.8.2 PAR measurement

The par sensor channel is read with a direct current auto scale measurement. The measured voltage is later converted to the measured par light with the help of Microsoft excel. The conversion formula is Equation 4.2.8-1.

#### 4.2.9 Data collecting

The PAR-sensors and the thermocouples were both connected to a Agilent 34970A() data logger. Via RS232 connection, this data logger was connected to a 32 bit PC running Microsoft Windows 7. Controlling and saving of data from the data logger was done by a standalone National Instruments LabVIEW 2010, version 10.0f2 32 bit, script written by Ing. Kees van Asselt(Wageningen University). I



have modified that script to also log pictures as data. The data files were logged to a text file and later imported in Microsoft Office Excel 2010 for further processing. The user logged in on the computer would automatically be logged of by Wageningen UR software, after several hours of inactivity. To prevent this from happening, the program Move Mouse version 3.2.0 from <https://movemouse.codeplex.com/> was used. This program moves the mouse every 30 seconds so the computer will sense activity. This way the data collection can continue day and night.

### 4.3 Methods

First, the duckweed will be grown at optimal conditions, the duckweed can accumulate to the growth medium. When the accumulation is done, the duckweed sample containers will be placed in the hot water container. Because of the small volume of the duckweed samples and the relatively large area of the containers, the time constant is low and the temperature reaches the steady state quickly. After the exposure to the high temperature, the duckweed containers will be placed back to optimal conditions. At optimal growth conditions, the duckweed will be monitored for one week. For the temperature response of the system and the temperature maintenance see chapter 5.1.

To get an idea of the lethal times of exposure at a given temperature, an estimation is made. This estimation is done by extrapolating formula 2.1.3-1. Herby it is assumed that LD50 (50 % of the population dies) is good enough for analysis. To move the samples from high to low temperature, a human is needed. I could only enter the laboratory between 7:00 and 22:00 on Monday to Friday and between 9:00 and 17:00 during the weekend. Besides that, I also had my own agenda. The result of these complications were the following exposure times.

Temperature (°C)	35.6	37.3	39.1	40.9
Expected time of LD 50 (hours)	86	32	11	4
Sample time 1 (hours)	0	0	0	0
Sample time 2 (hours)	23.75	4	2	2
Sample time 3 (hours)	44.5	7.5	4	3
Sample time 4 (hours)	48	20.5	6	4
Sample time 5 (hours)	62	24	8	5
Sample time 6 (hours)	65	27.5	10	6
Sample time 7 (hours)	70	31	12	7

**Table 3 Times of exposure to high temperature**

Based on the existing model, the control population and these measurements, the death rate can be determined. It is close to impossible to determine the death rate directly, because when the duckweed dies, the death fronds will remain shortly in the healthy population and on the outside look healthy as well. The photosynthetic activity can be measured using very expensive special cameras. During my research I didn't have access to this kind of cameras. Another method to determine the activity of duckweed is measuring the respiration rate. During my research, I also didn't have access to this device. The dry mass of duckweed can be weight. This method does not distinguish dead fronds from living fronds, it just measures biomass. Dead duckweeds fronds will turn bleached after three days.

To distinguish living from dead fronds, a camera with digital image processing software is used. The camera takes a picture twice a day and the vision software calculates the area of living duckweed. The area of duckweed is, in this method, a measurement for the amount of duckweed. It is assumed

that dry biomass is directly correlated to the area of duckweed. This in reality is not true, because the dry weight of duckweed is heavily correlated with the temperature. This effect is neglected because the duckweed is, after exposure to the extreme conditions, placed back at optimal conditions. Letting the duckweed restore its nutrient concentrations to concentration at optimal temperatures.

In this experiment area is considered a measurement for biomass, therefore the duckweed must have enough space to expand without overgrowing itself.

With the method described above, the death duckweed fronds have time to change colour and sink to the bottom of the growth medium. Also the damage effect on the surviving fronds will be measured this way.

The duckweed will be grown four weeks prior to the experiment on the growth medium. This growth medium will be refreshed when needed, this doesn't give any long term effects. This way the fronds are also older, therefore they are more adapted to the situation (see chapter 2.2.3 and 2.2.1). In the Ecoferm, the duckweed frond will also be older, and thus more adapted to the situation.

### 4.3.1 Temperature growth model

On the measured results the four types of growth models will be tested. A linear model, a bilinear model, a multi-linear and an exponential model will be tested. A more detail description can be found in the following paragraphs.

#### 4.3.1.1 Linear model

Within the range of 12-22°C the growth rate of *L.minor* is a linear function of the temperature. In this range, the growth rate is related to the temperatures above a specified minimum temperature. In this range, the growing-degree-days method can be used to determine the growth (Yan and Hunt, 1999). The basic equation for growing-degrees-days is:

Equation 4.3.1-1

$$GDD = x - T_{base} \begin{cases} x = \frac{T_{max} + T_{min}}{2} \\ OR \\ x = T_{average} \end{cases}$$

Symbol	Meaning	Unit
$GDD$	Amount of growing-degree-days	°C
$T_{base}$	Minimum temperature for the growth rate to be a linear function of temperature	°C
$T_{uppTresh}$	Maximum temperature for the growth rate to be a linear function of temperature	°C
$T_{max}$	Maximum temperature of the day	°C
$T_{min}$	Minimum temperature of the day	°C
$T_{average}$	Average temperature of the day	°C

Where  $T_{max}$  and  $T_{min}$  are daily maximum and minimum air temperature.  $\frac{T_{max}+T_{min}}{2}$  is an approximation of the average temperature of that day.  $T_{base}$  is the base temperature, the lowest temperature for the growth process to take place. The crop production is the integral of the linearized growth function as function of T(GDD).

Equation 4.3.1-2

$$P = f(T \rightarrow GDD)$$

#### 4.3.1.2 Bilinear model

The linear model is only accurate in the linear part of the growth function. The linear model fails to account for the fact that temperatures above the optimal temperature ( $T_{opt}$ ) inhibit the growth rate. The bilinear model does account for growth inhibition for temperatures above  $T_{opt}$ . This is done with use of a second linear equation for temperatures above  $T_{opt}$ .

Equation 4.3.1-3

$$\begin{cases} r = a_1 + b_1T & \text{if}(T < T_{opt}) \\ r = a_2 + b_2T & \text{if}(T > T_{opt}) \end{cases}$$

This bilinear approach still is not accurate for all temperatures. Around the optimal temperature, the growth rate is not a linear function of temperature as can be seen in figure 1 and 2. Also the growth rate around the minimum and maximum temperature is not accurate.

#### 4.3.1.3 Multi-linear model

A multi-linear model is a composed of three or more linear functions. With the use of more linear functions, the growth rate can be accurately approximated at all the temperatures, as long as one can (experimentally) determine the parameters required for each linear function. A huge disadvantage of the multi-linear model is the amount of required data to compose the model. Another problem is the calibration, the large amount of required parameters renders the approach subject to calibration errors(Yan and Hunt, 1999).

#### 4.3.1.4 Exponential and polynomial model

There are reasons to believe that temperature response of a given process should be a smooth curve((Yan and Hunt, 1999), rather than a rigid combination of linear equations, which introduce abrupt changes. Exponential and polynomials give smooth functions which with the right parameters should be able to predict the growth rate more accurately. A disadvantage of the exponential growth function is that it does not simulate the response to high temperatures, because it does not allow for a reduced growth rate for temperatures above the optimum.

## 5 Experimental results

### 5.1 Temperature in the test setup

The temperature response of the reaction tubes is fast enough for the experiment. In the graph below a temperature response of a growth container from 36°C to the optimal temperature of approximately 26 degrees is shown. One can see that within 10 minutes the desired temperature of approximately 26°C is reached.

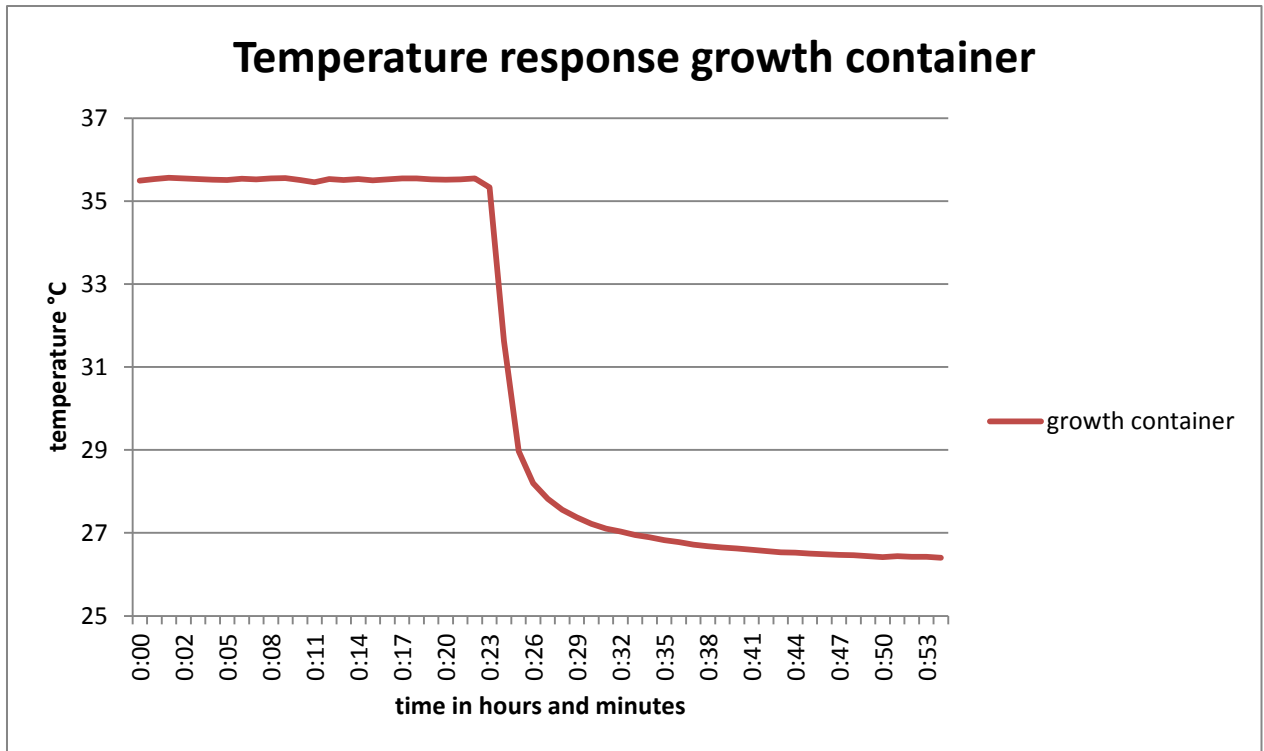


Figure 8 temperature response of a growth container

As said before, the thermostatic bath should maintain a stable temperature, and this should also be the case for the growth containers. In the graph below one can see that the temperature in the thermostatic bath differs only  $\pm 0.2$  °C and the temperature of the reaction tubes only are up to 0.8°C lower and differ maximum 0.2°C from their average.

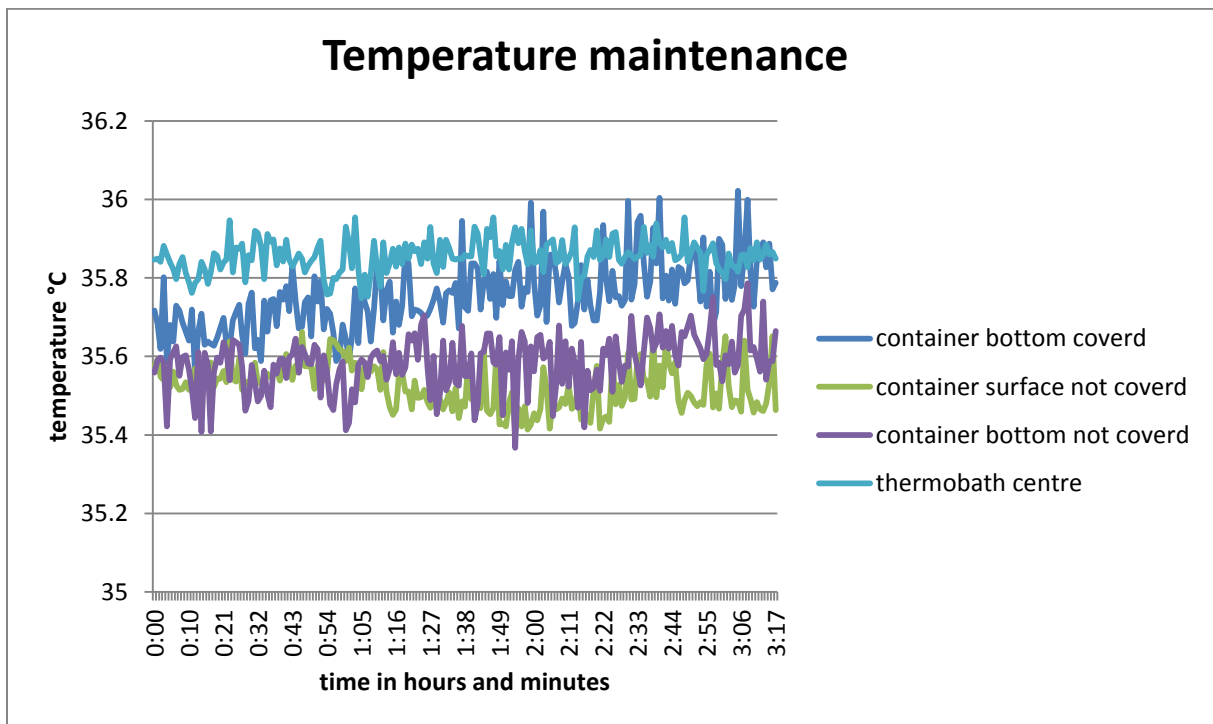


Figure 9 temperature maintenance

## 5.1 Temperature growth curve

In the conducted experiment the growth rate of duckweed as function of temperature and time of exposal was tested. The amount of measured duckweed, in the form of area of healthy duckweed in pixels, can be found in appendix 10.2. Analysis as described in chapter 4.3 is described has failed. Interpreting the data was more difficult than expected and I was running out of time.

To analyse the production of duckweed at the Ecoferm when the duckweed is able to die, and to test the climate actuators mentioned in chapter 3.5 a model describing the behaviour of duckweed at these temperatures is needed. To continue my research, a few assumptions are made based on intuitive interpretation of the data in appendix 10.2.

It can noticed that with an exposure temperature of 40.9°C the duckweed dies, even with an exposure time of two hours. This will be approximated in the model by assuming that with a temperature of 40.9°C the duckweed instantly dies and the duckweed population needs to be restored from an external input. This will be simulated by setting the mat density to 10% of the desired situation.

At the temperatures of 35.6°C and higher, one can see that the amount of duckweed decreases, but restores after a while. This will be approximated by setting the growth rate of the duckweed to zero when a temperature of 35.6°C or higher is present.

## 5.2 Duckweed climate

In this chapter the results of the simulation of the climate actuators is presented. The associated graphs can be found in appendix 10.3.

### 5.2.1 Duckweed without climate control

Has a total dry weight production of 1991.8 kg/year. During the period from day 140 till 220 the duckweed is only harvested once, because during this period the temperature of 40.6°C is reached several times.

### 5.2.2 Extra ventilation

The maximum ventilation is increased to 150 m<sup>3</sup>/s instead of 98.3m<sup>3</sup>/s. Also a simple controller is applied, when the temperature rises above 26°C the ventilator will blow full power. This resulted in a production of 2774.6 kg dry matter per year.

### 5.2.3 Adiabatic cooling

The adiabatic cooler was set to start cooling when the duckweed temperature rises above 26°C. The adiabatic cooler has a max capacity to evaporate 0.01 gram vapour for every kg of dry air present. With these setting a total yield of 2713.2 kg dry matter per year could be achieved. When looking at Figuur 26 Duckweed temperature in the appendix, one can see that the temperature does not rise above 40°C, this means the duckweed doesn't die. This is also confirmed by the mat density (Figure.

### 5.2.4 Whitewash

The tested whitewash has a reflectance of 50%. Her fore, only 50% of the solar energy can be used for heating the greenhouse. A consequence is that the duckweed also gets less sunlight. With the whitewash a total production of 2171.4 kg dry matter will be produced in one year.

### 5.2.5 Thermal screen

The mathematical model of the thermal screen is difficult and I was running out of time, so this is not tested.

## 6 Discussion

### 6.1 Experiment

In general the test setup worked, the time constant of the duckweed temperature was fast enough for assuming an instant temperature transition. The temperature control was stable. The growth medium was not exhausted during the experiment and the light intensity was sufficient. Still the results were not useful for construction for a dynamic model of the duckweed death rate at high temperatures.

Measuring when a duckweed frond is dead is difficult, because with simple sensors it is impossible to directly measure if a frond has died. There are sensors able to directly measure the photosynthetic activity of a plant. These sensors are very expensive and were not available.

The camera was able to distinguish dead and living crops after the frond had four days time to turn white. If the area of duckweed is representative for amount of biomass in the duckweed population is not tested.

Modelling the death rate of duckweed, using the growth of the area of living duckweed and comparing it to a control group, didn't work in the setup mentioned in chapter 4.1. One of the reasons was the available area in the growth containers. During the experiment, the duckweed in the control containers was growing too much that it needed more space than available in the container. Because of this duckweed frond started growing over each other, making it impossible to measure using a RGB camera. Therefore the growth rate of the control group as not correct.

When the initial amount of duckweed will be lowered, the possibility of a too small population becomes present. Therefore larger growing containers are recommended, with a small initial amount of duckweed.

### 6.2 Model

#### 6.2.1 Whitewash

The assumption made for the climate actuators are rough assumptions. The whitewash does decrease the transmittance of the roof, and increase its reflection, but also increases its radiation absorption and insulation. Increasing the indoor temperature of the greenhouse.

### 6.2.2 Adiabatic cooling

In the model it is assumed that the vapour is instantly evaporated and the RH can reach up to 100%. In reality, when the RH is close to 100% the evaporation rate will decrease. Resulting in a reduced amount of evaporated water, and thus a reduced cooling effect.

### 6.2.1 Ventilation

The ventilator capacity of the stable were already very high. Increasing them will bring other problems. Currently the ventilation has to blow the air through a biobed, when the ventilation is increased, the biobed will work as a resistance, making it harder to move this amount of air.

Adding extra ventilators costs money, and use of them cost energy. These costs might be higher than the profit in the form of duckweed.

Another problem is, the ventilator cannot cool the air cooler than the outdoor air. Therefore, extra ventilation cannot prevent the growth inhibition on a hot summer day were the adiabatic cooler can.

## 7 Conclusion

### 7.1 Determining the death rate at high temperatures

Duckweed cannot survive temperatures higher than 40.9°C, when it reaches these temperatures, it will die. At the temperatures of 35.6°C and higher, duckweed dies, but restores after a couple of days at a decent temperature.

### 7.2 Climate actuators

The adiabatic cooling has the same production as the extra ventilation, but because the adiabatic cooler is not dependant on the outdoor temperature and therefore more reliable. The adiabatic cooler is also cheaper and therefore more profitable.

### 7.3 Research questions

The answers to the research questions mentioned in chapter 1.4 are answered throughout this thesis, but I would like to end with a quick summary.

- 1) How does the growth rate of duckweed behave in the Ecoferm greenhouse?  
The duckweed grows the best with a temperature of 26°C. At temperatures of 40.9°C and higher the duckweed instantly dies. The nutrient concentration in the greenhouse can be held close to optimal and therefore will not influence the growth rate. The photo
- 2) How does the growth rate of duckweed behave at high temperatures in the greenhouse?  
Composing a model of the death rate of duckweed as function of temperature failed. By looking at the results, it is assumed that at temperatures above 35.6°C, there is no growth rate. By temperatures above 40.9°C

Control/ model:

- 3) Which parameters are important for the climate in the greenhouse?  
The evaporation rate shows the greatest influence on the temperature in the greenhouse.

- 4) Which climate actuator influences the temperature of the duckweed the most?  
The adiabatic cooler has enough cooling power to let the duckweed survive the hot summer months. And increase the production.
- 5) Which climate actuators are needed for the duckweed to survive the hot summer months?  
Both extra ventilation and the adiabatic cooler can do this.
- 6) What climate actuators are the most effective to increase the duckweed production year round?  
The adiabatic cooler and the extra ventilation both yield the same amount of duckweed. But the adiabatic cooler is able to cool, even when it is really hot outside. Also the adiabatic cooler is cheaper and therefore more financially effective.

## 8 Recommendations

Try to reanalyse the data from the experiment to determine the growth death rate of duckweed at high temperatures. If this is not possible, do the experiment with larger growth containers and more space for the duckweed to grow.

The controller used for controlling the greenhouse climate is a very simple one. Optimal control can be applied to increase further production. However, one must note that duckweed is only cow food. An advanced control system and the climate actuators might not be financially profitable. In the controller a cost function should also be taken into account.

In the literature research of it was shown that heat tolerance of *L.minor* can be enhanced by addition of calcium nitrate to the growth medium. No concrete results were published. But addition of calcium nitrate to the growth medium in the Ecoferm greenhouse could help increase the productivity. Further research about this topic is needed.

In Farquhar et al. (1980) it is mentioned that an increase in CO<sub>2</sub> concentration in the air might increase the thermal tolerance of duckweed. Duckweed has the C<sub>3</sub> type of photosynthesis, when a higher concentration of CO<sub>2</sub> is present, the optimal temperature of this crop increases. This method can also be used to increase the productivity of the Ecoferm, especially at hot days.



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# 10 Appendices

## 10.1 Camera calibration

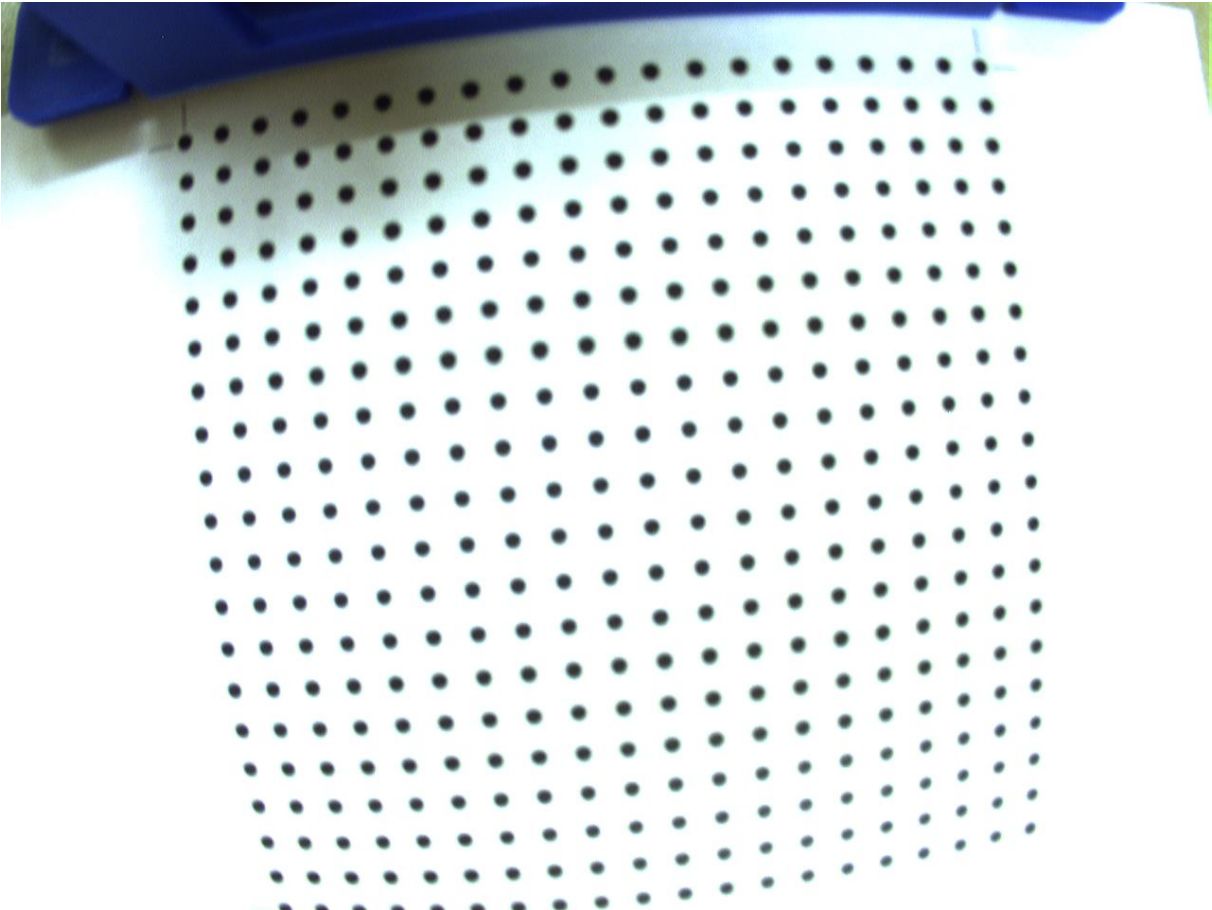


Figure 15 calibration grid

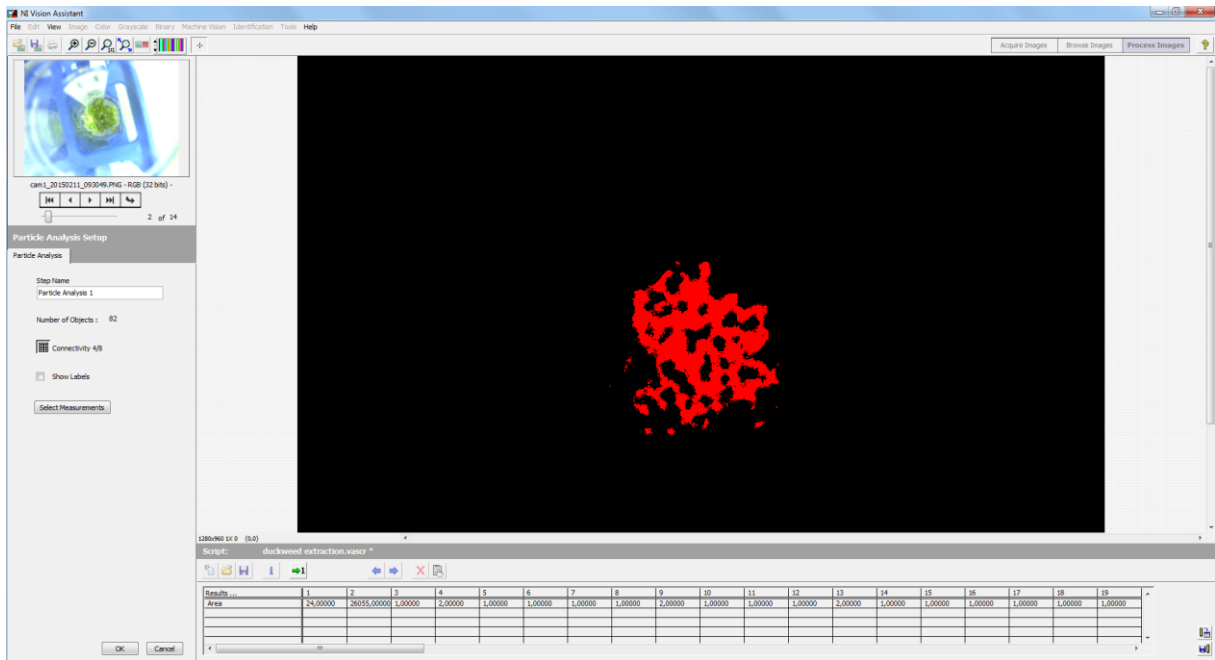
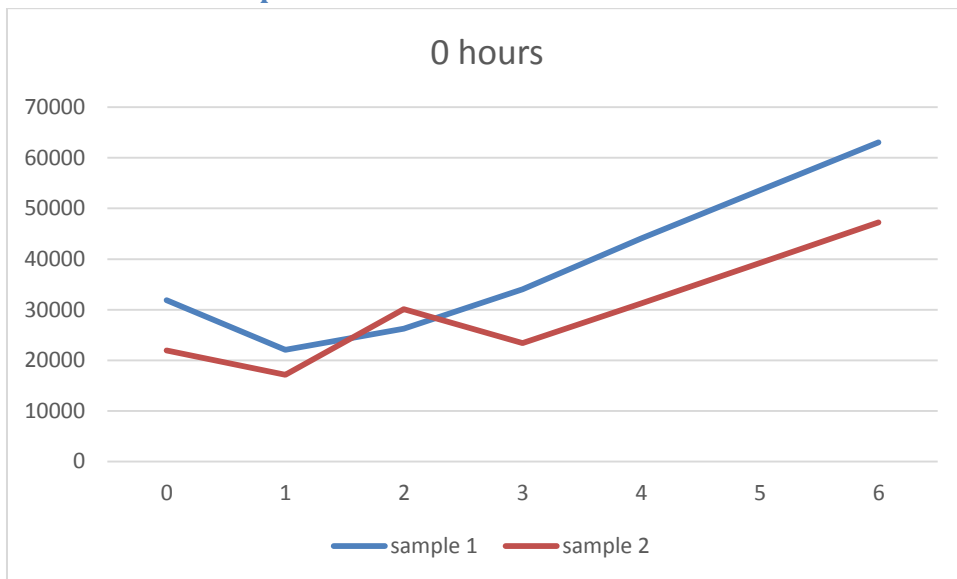
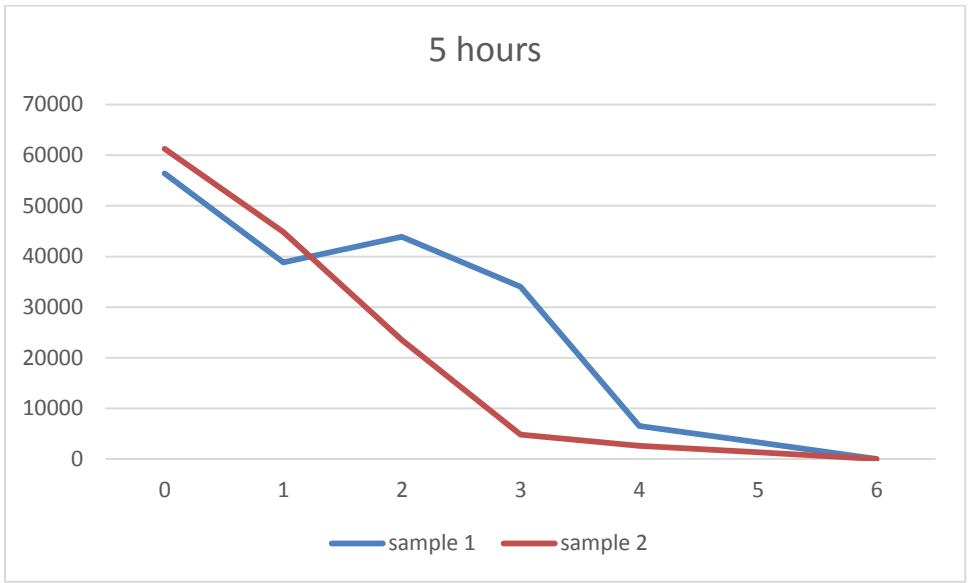
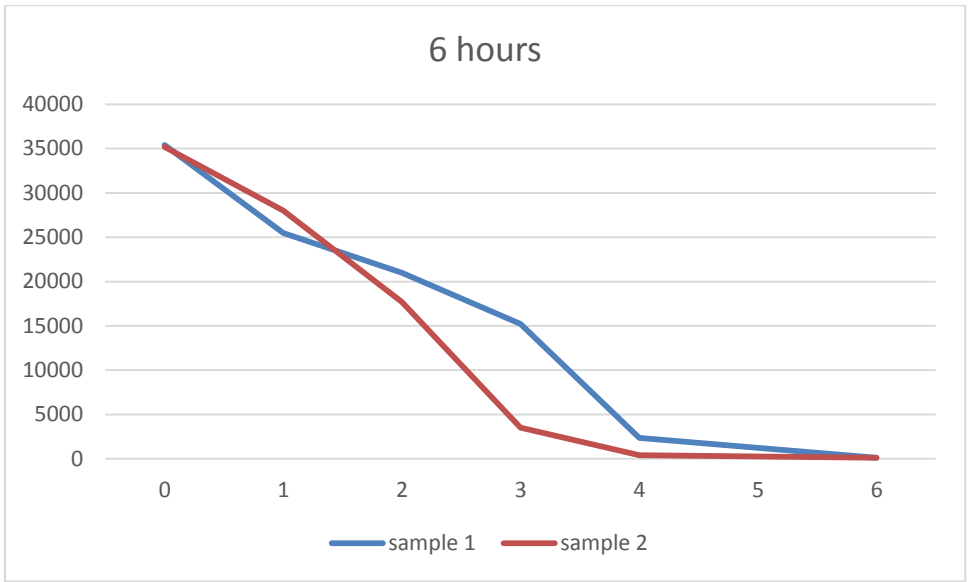
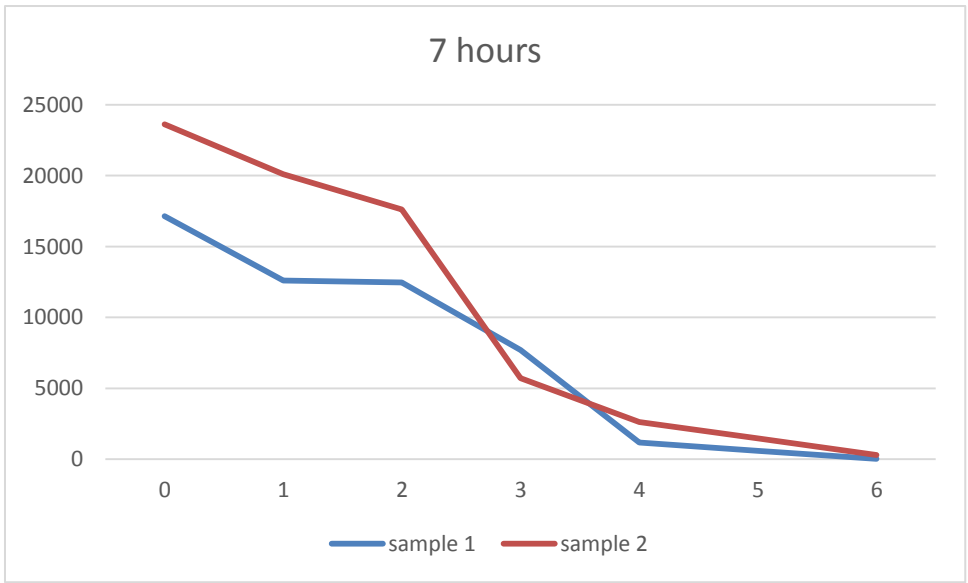


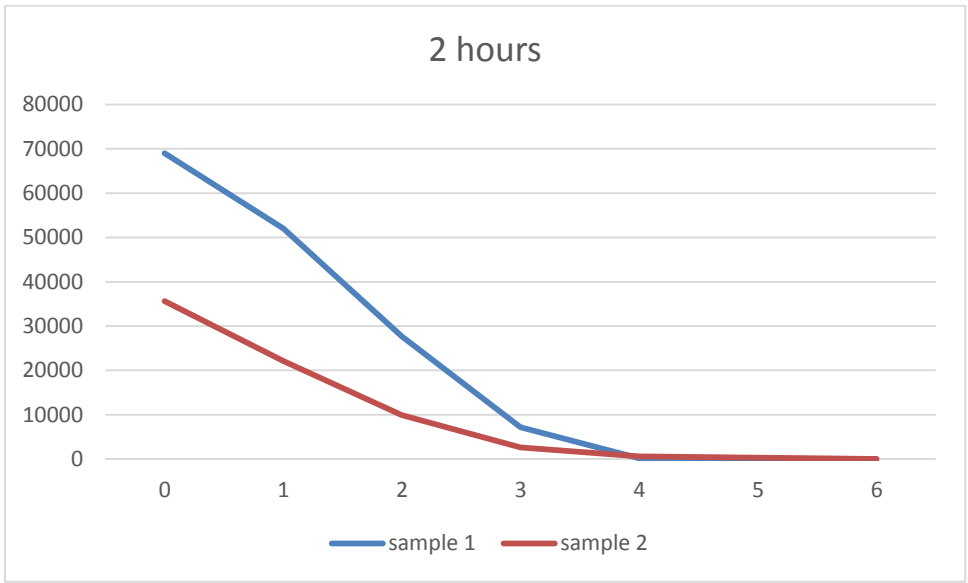
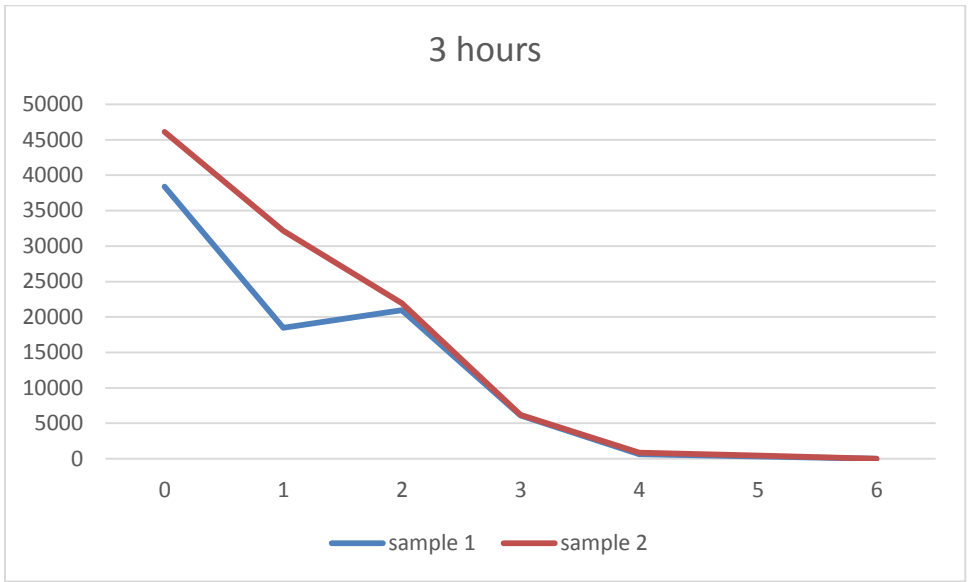
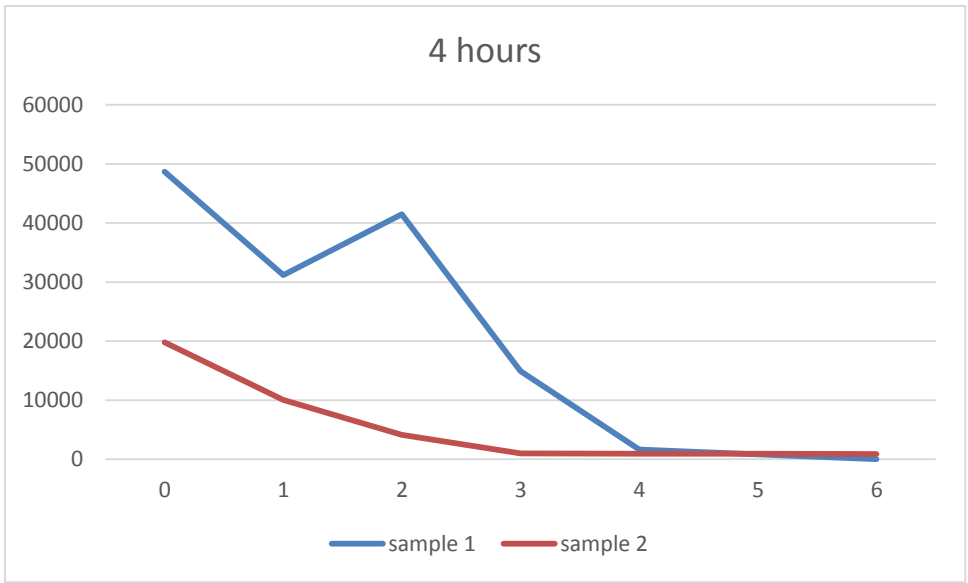
Figure 16 Area measurement

## 10.2 Death rate temperature

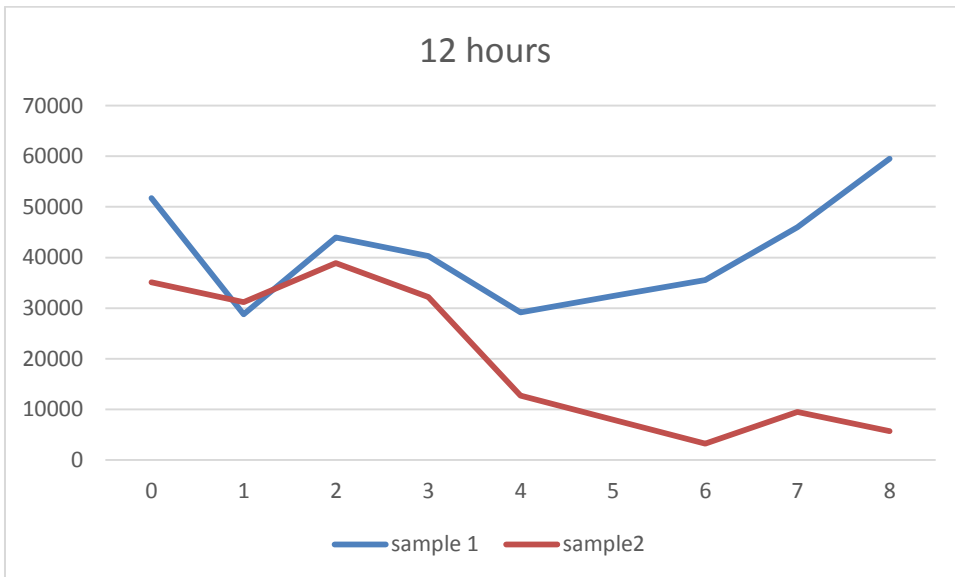
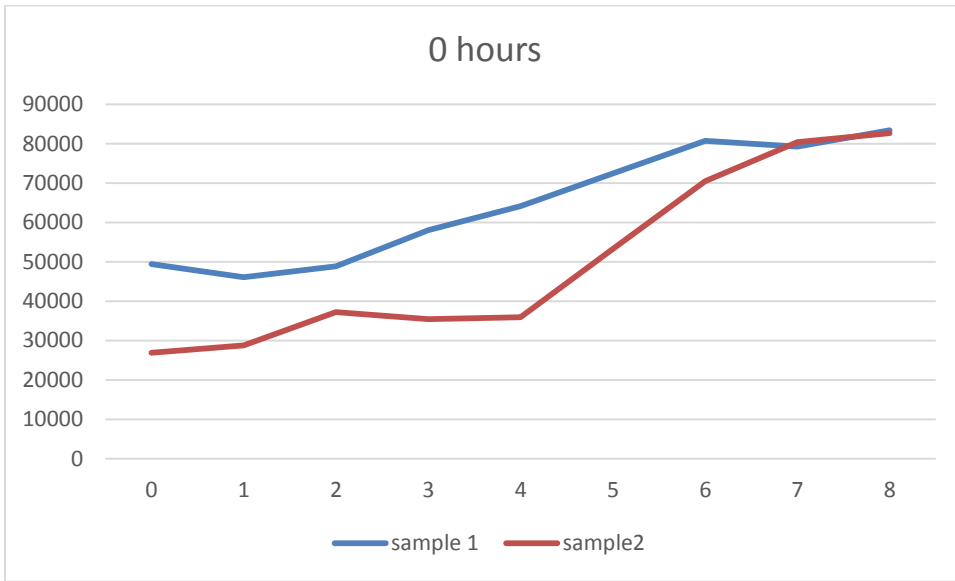
### 10.2.1 Temperature of 40.9°C



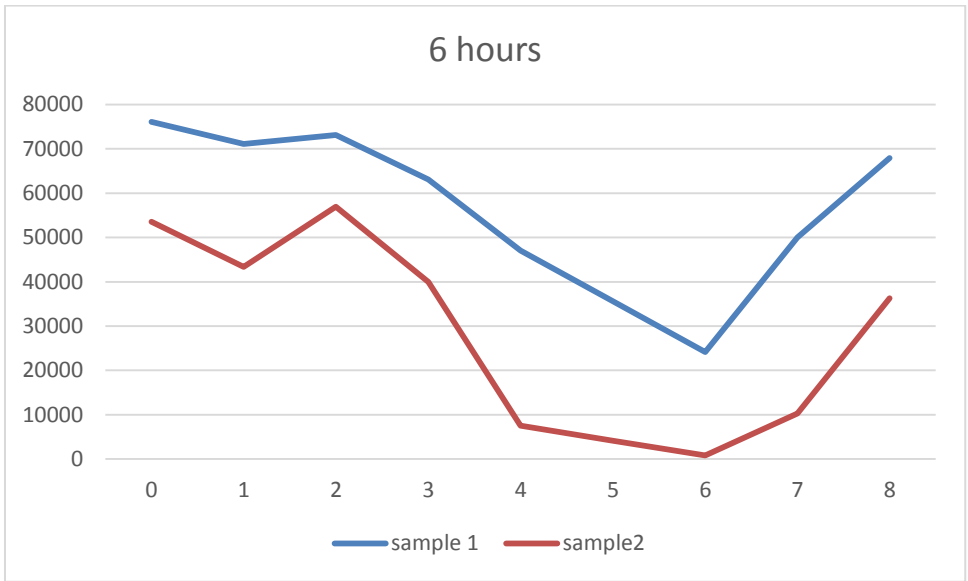
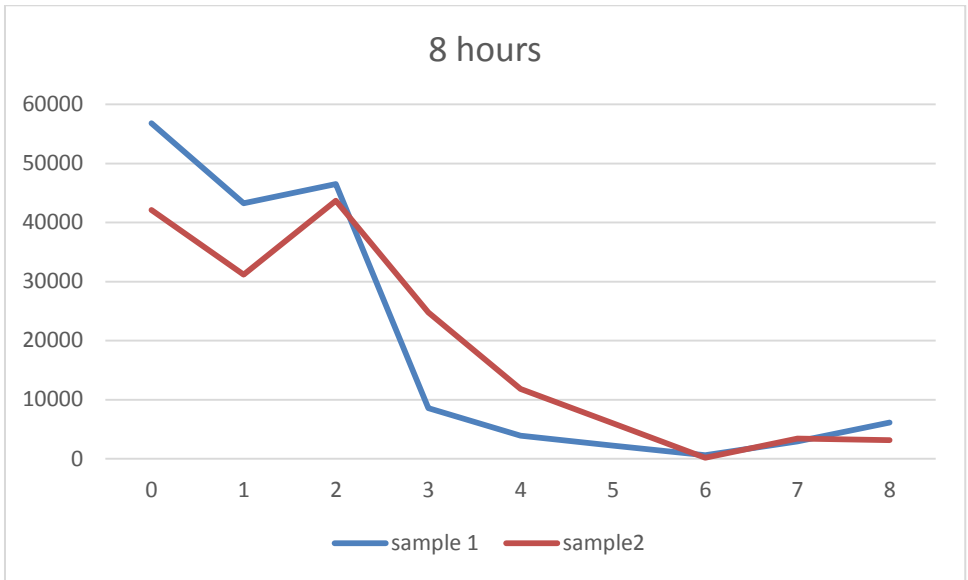
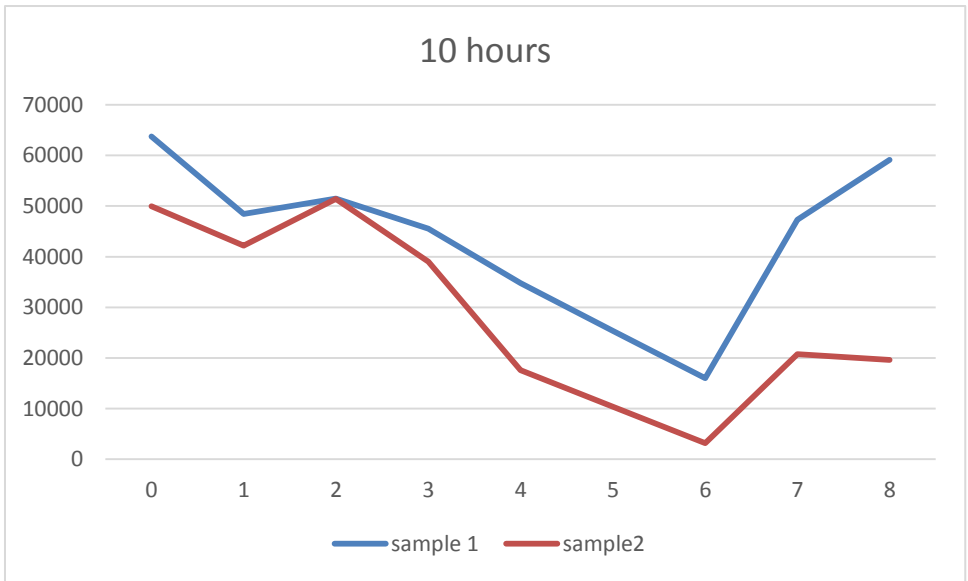


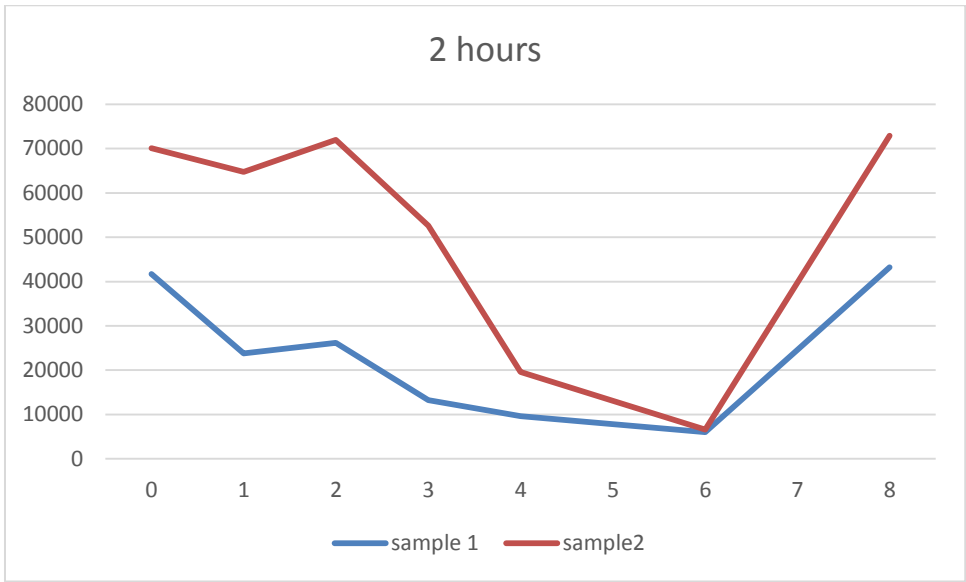
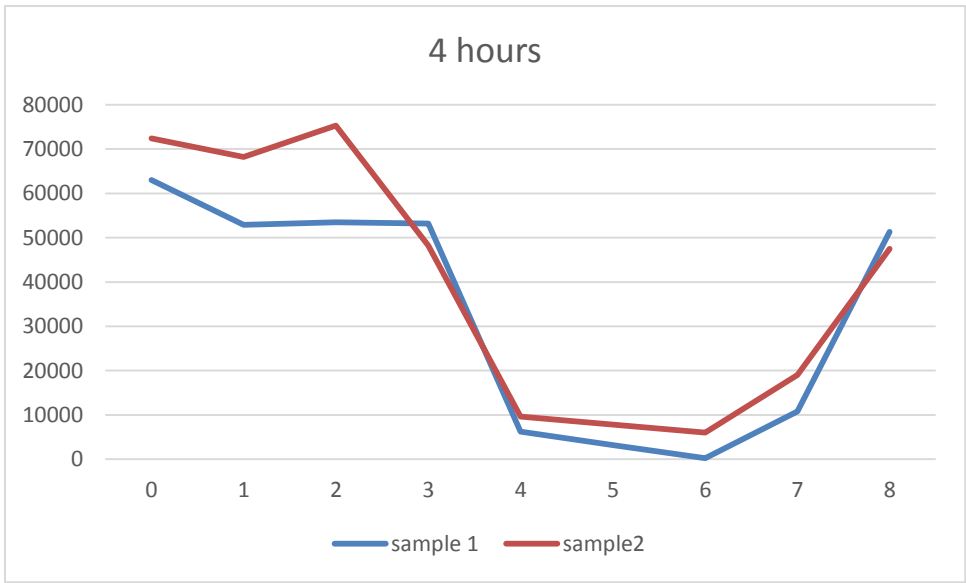


### 10.2.2 Temperature 39.1°C

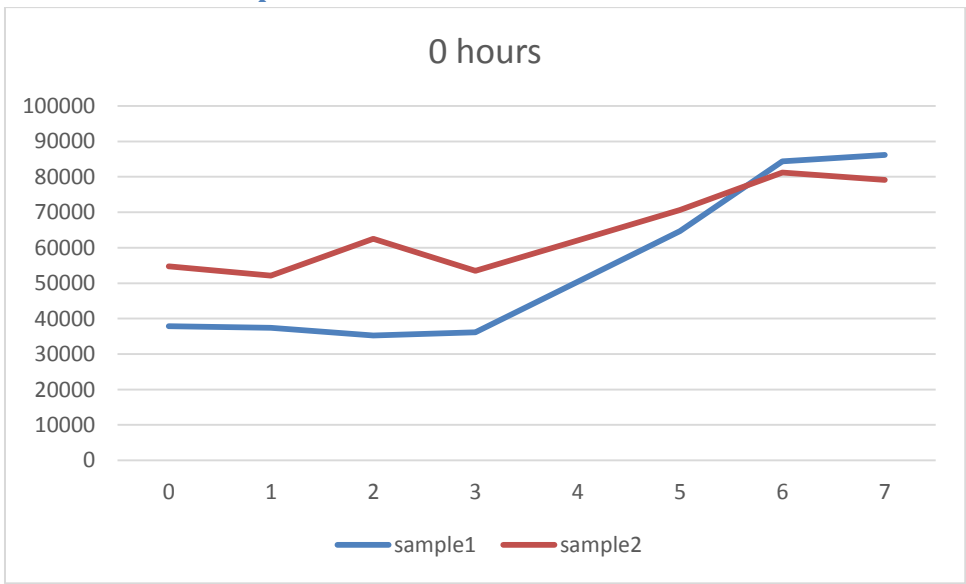


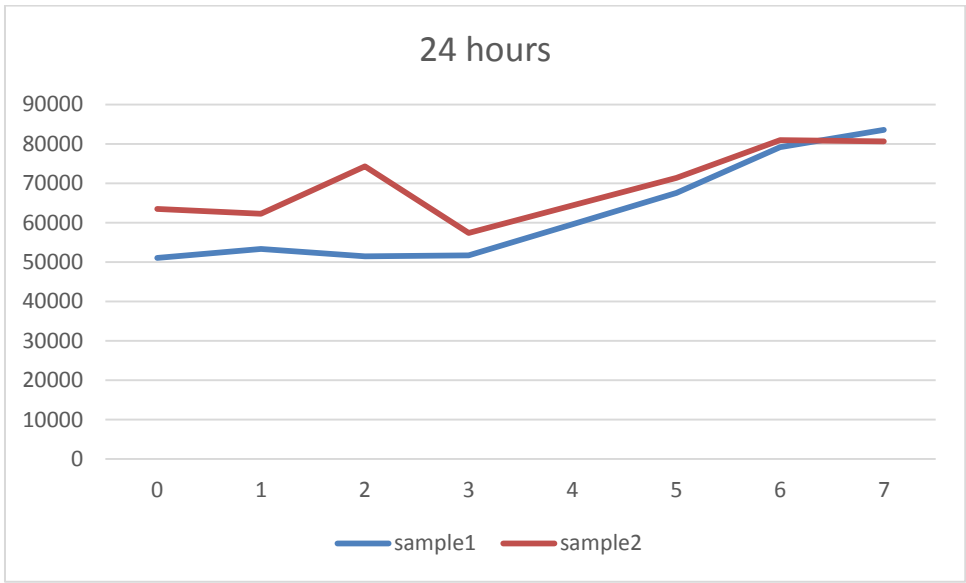
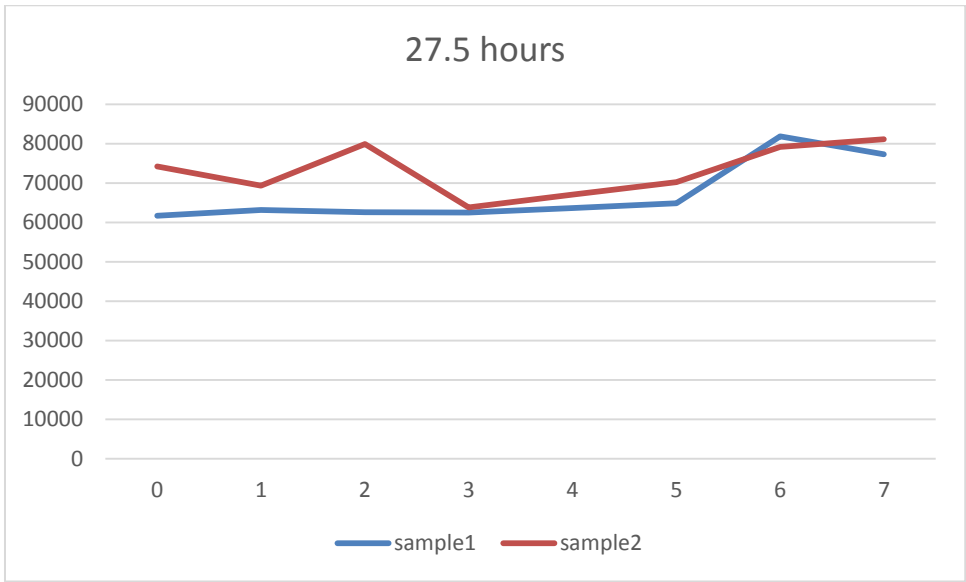
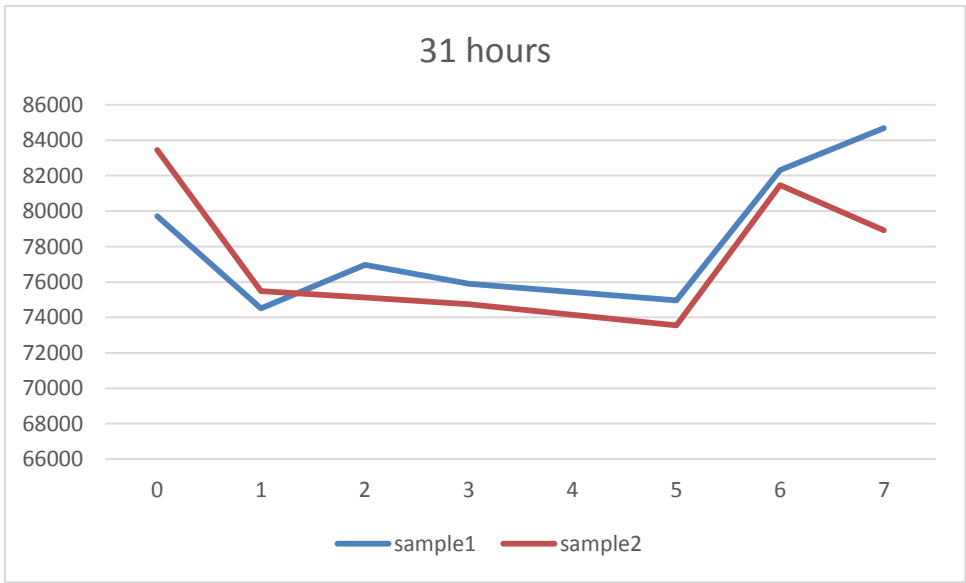


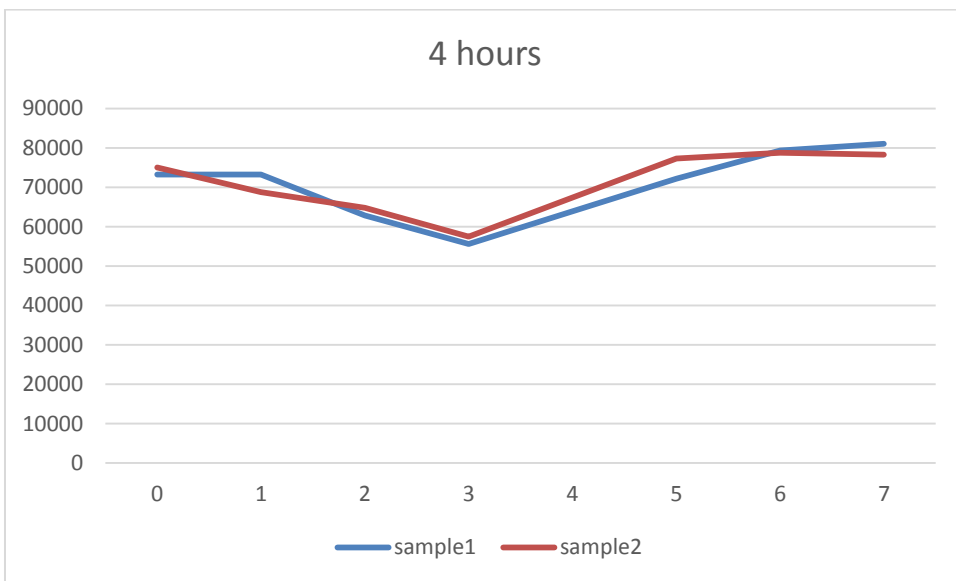
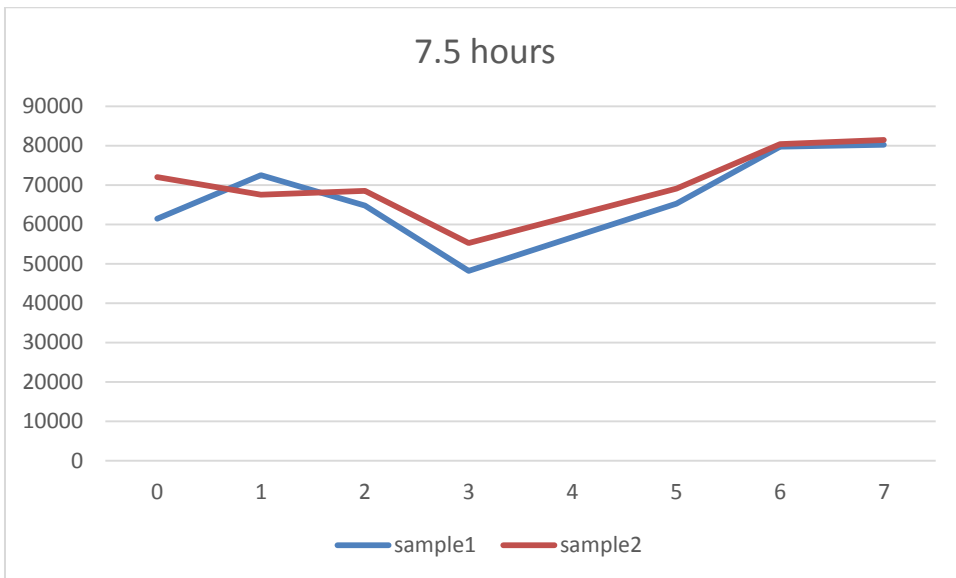
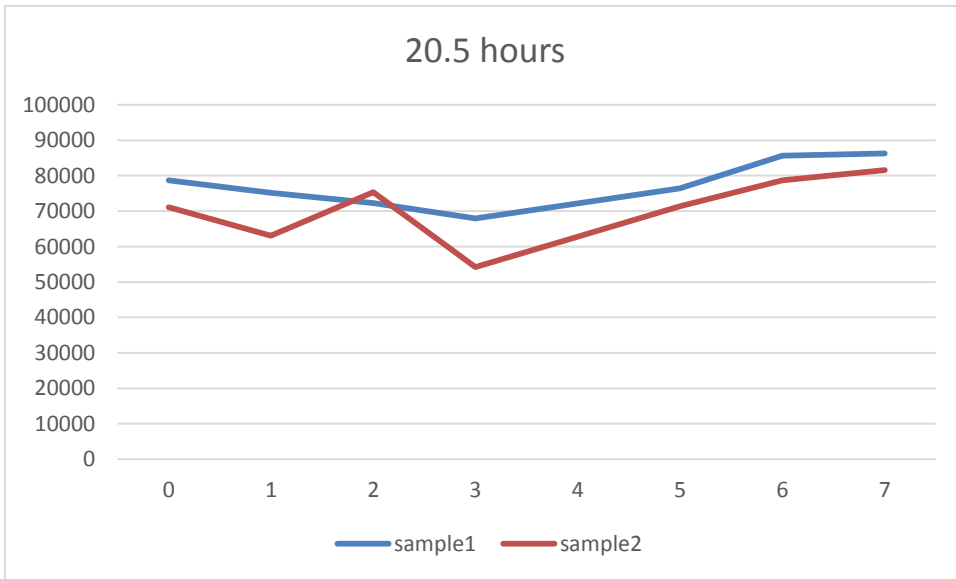




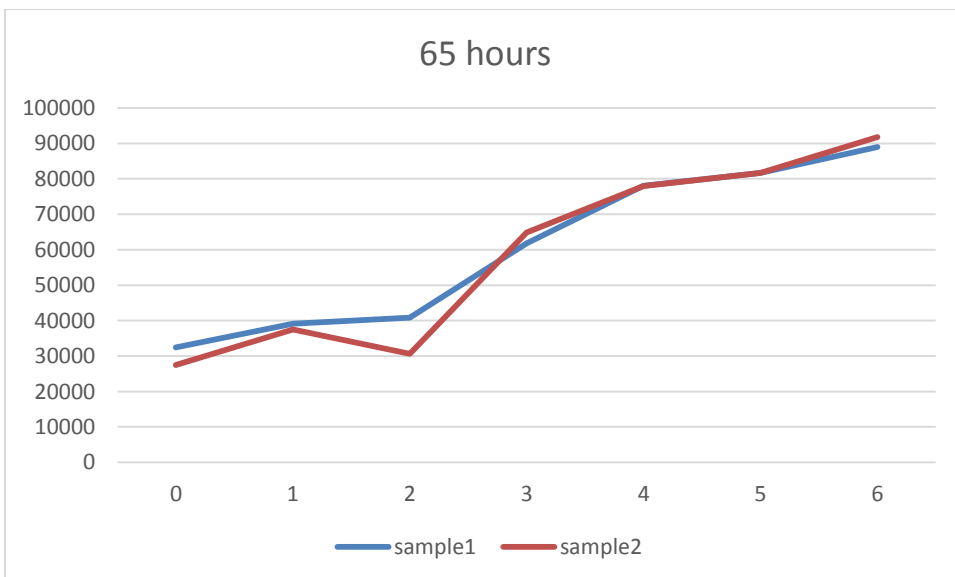
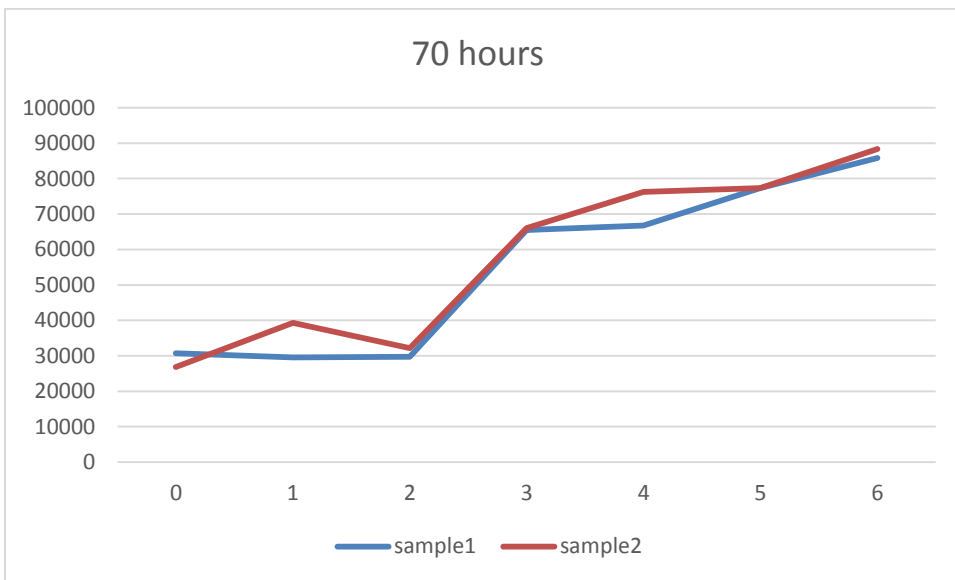
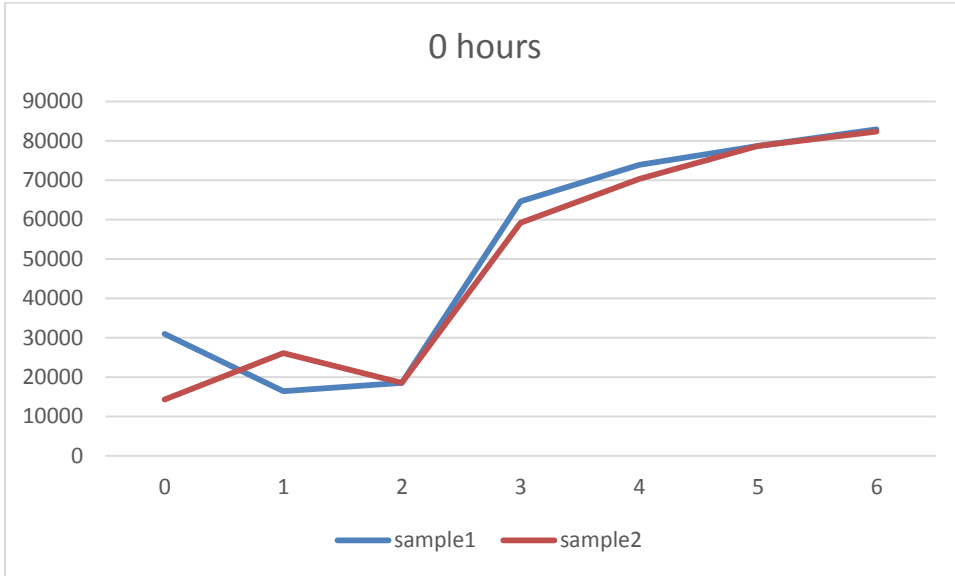
### 10.2.3 Temperature 37.3°C

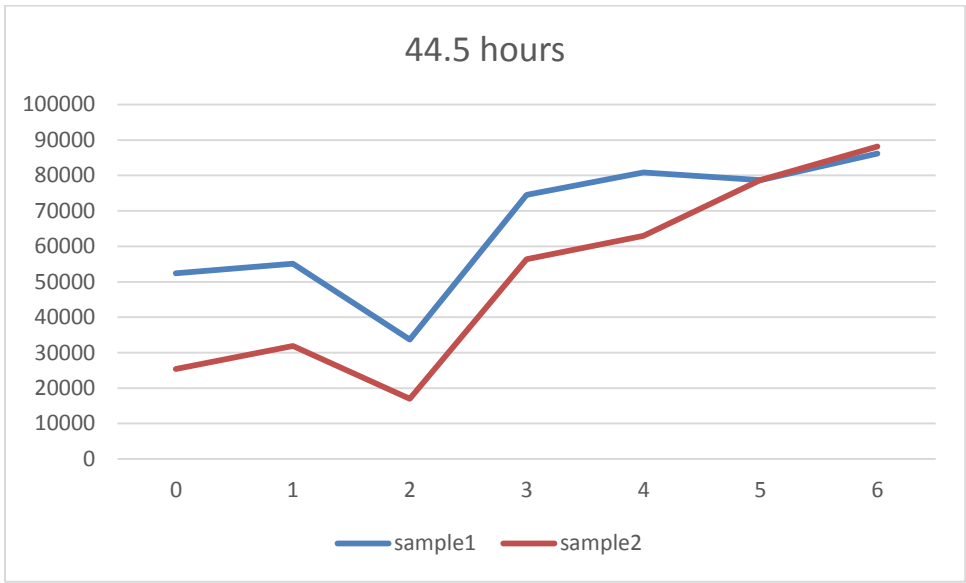
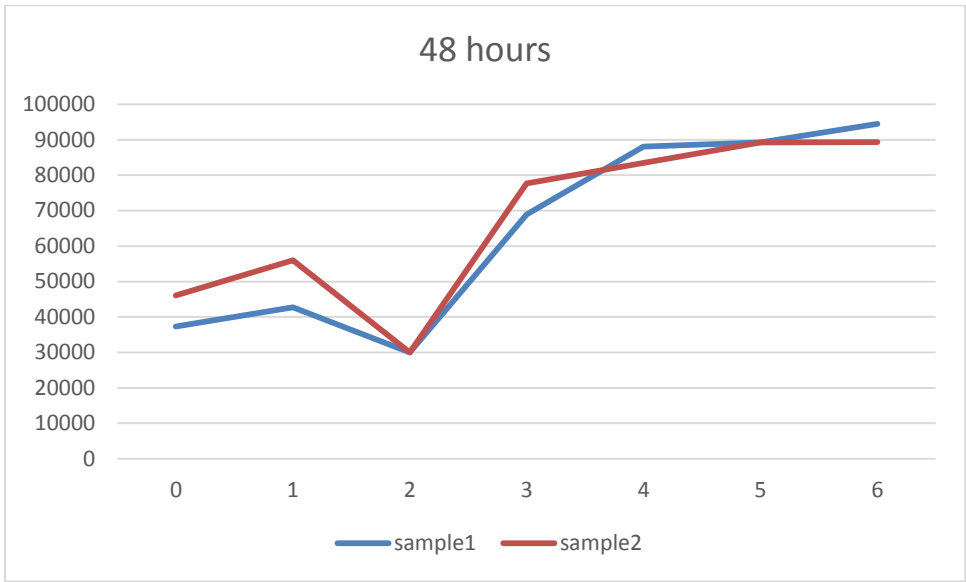
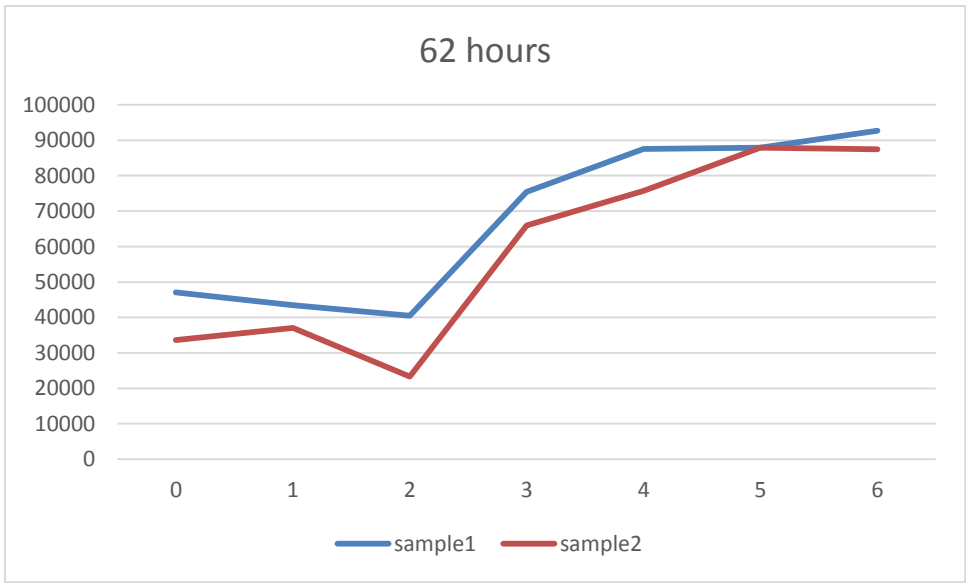


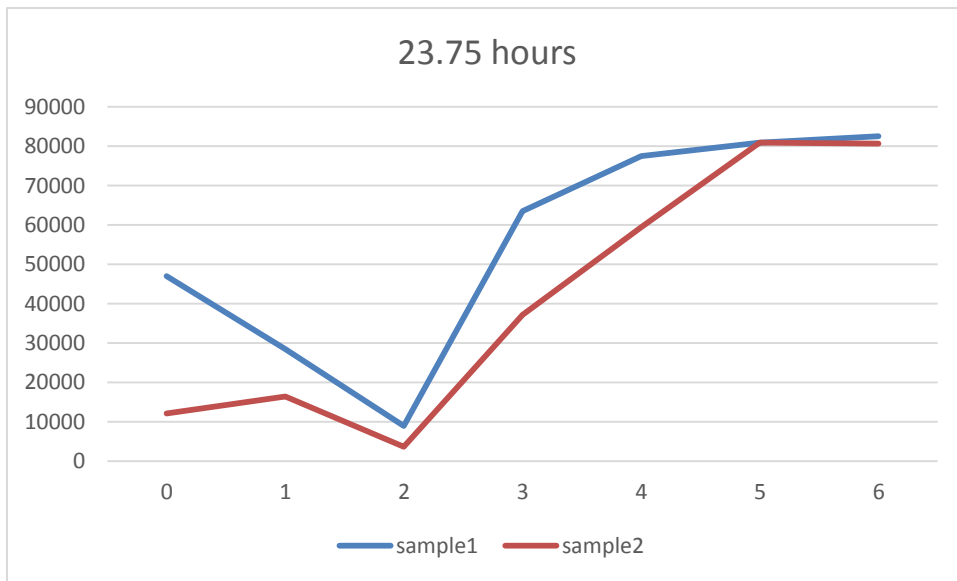




### 10.2.4 Temperature 35.6°C







### 10.3 Climate model

#### 10.3.1 No climate control

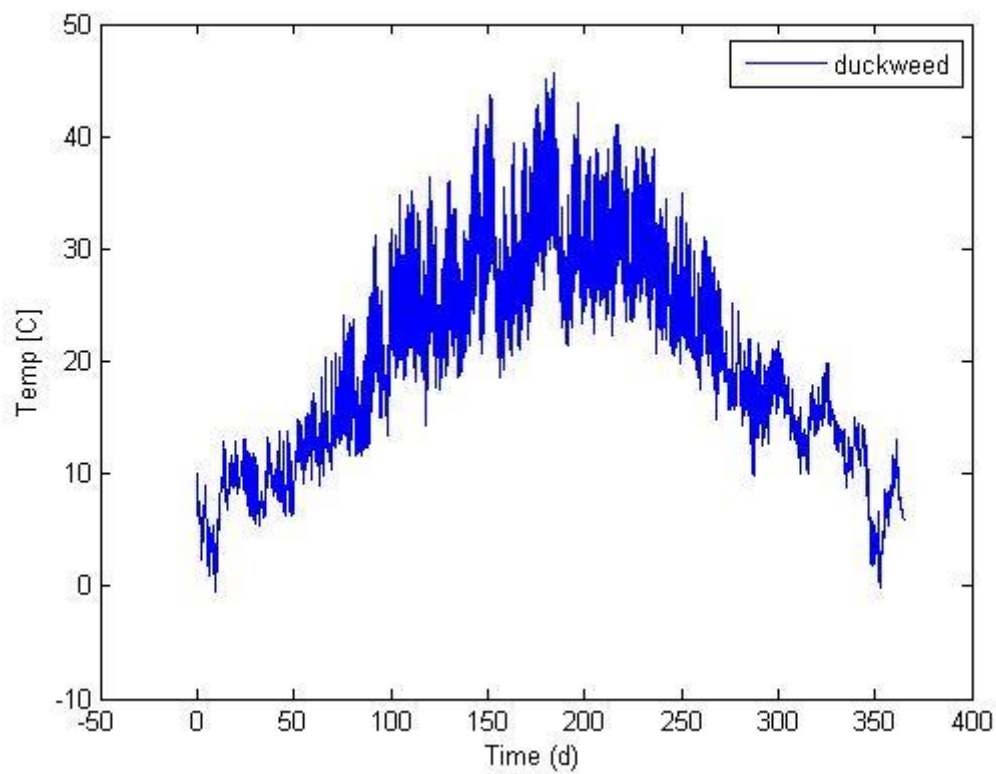


Figure 17 Duckweed temperature

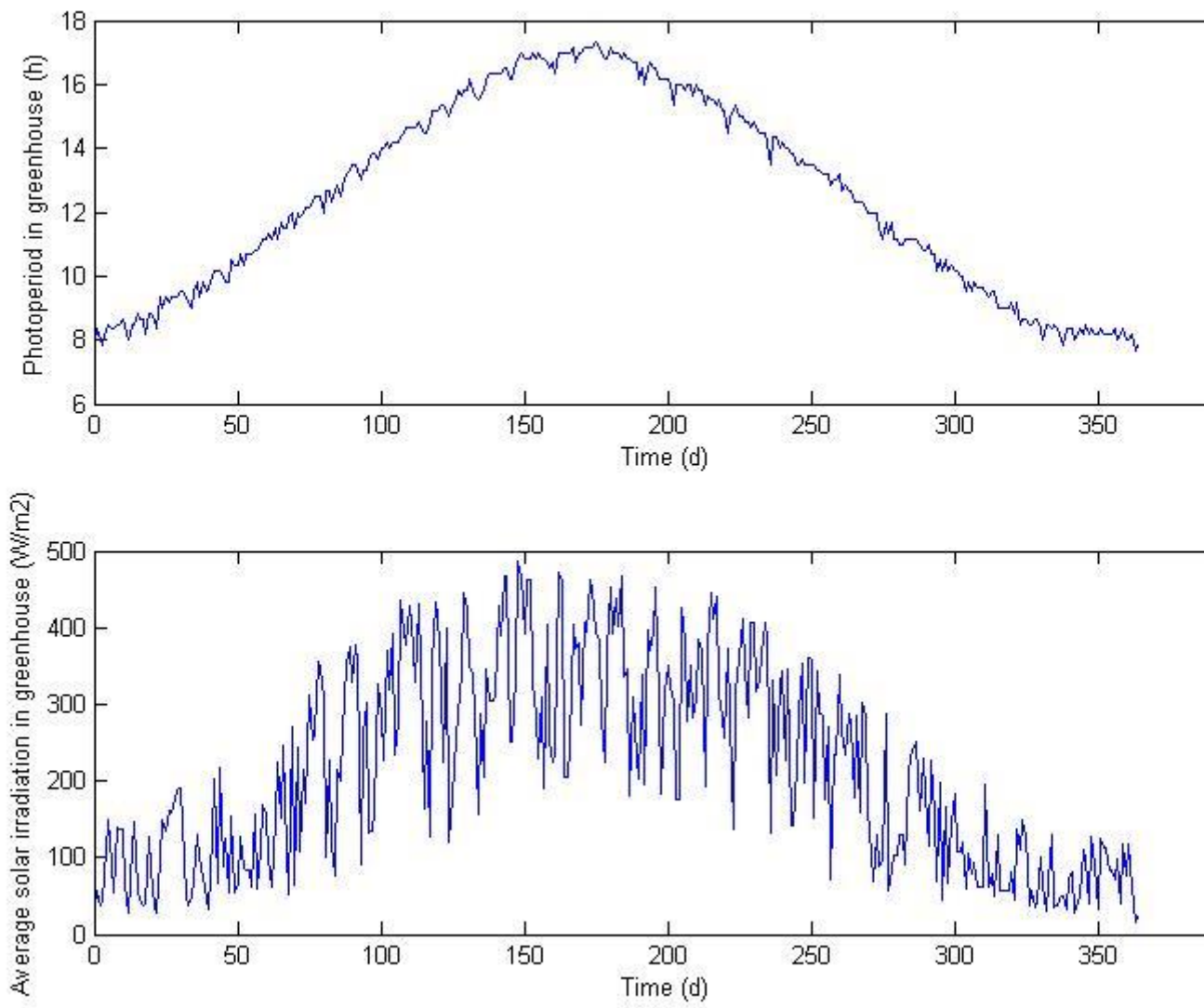


Figure 18 Solar radiation



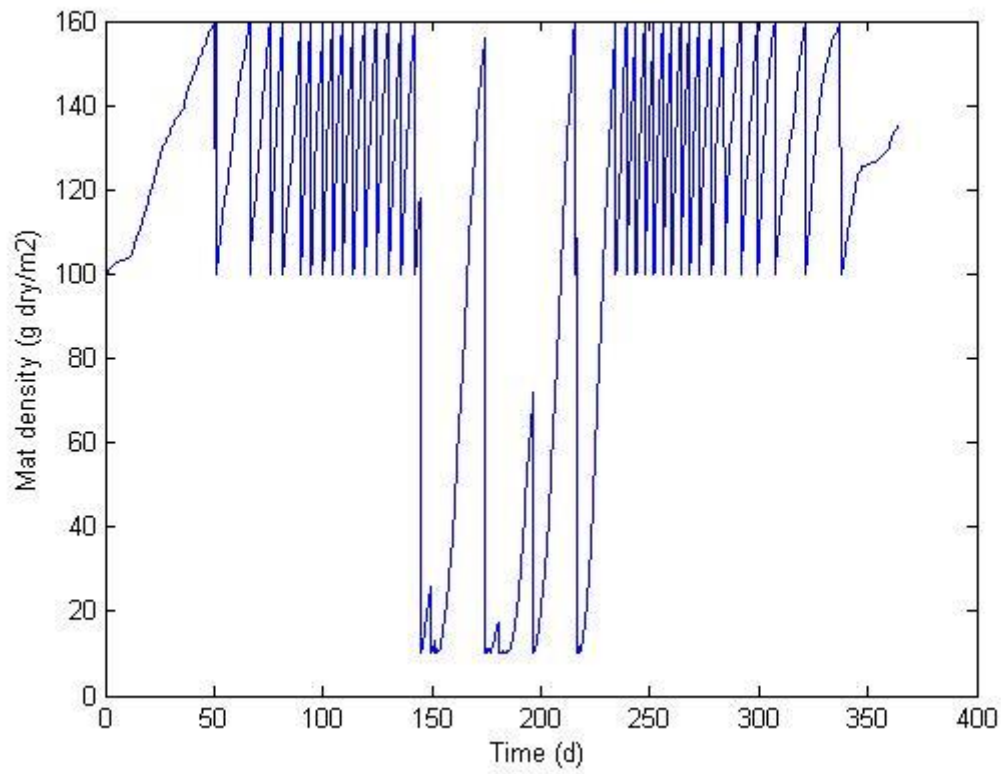


Figure 19 Mat density

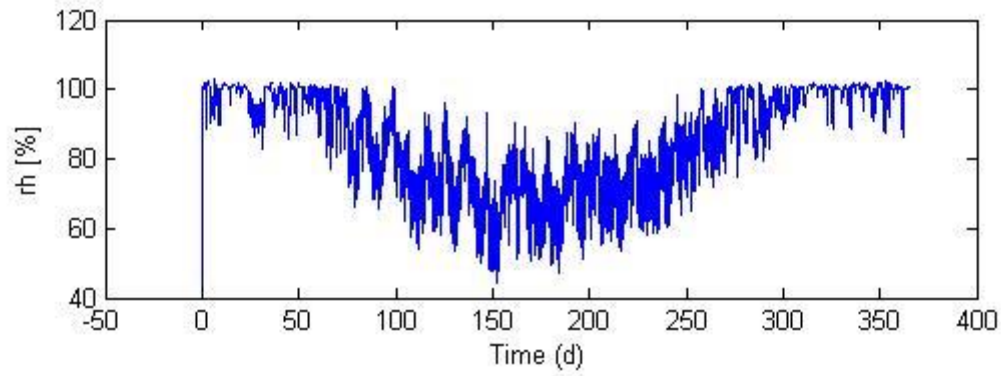


Figure 20 relative humidity

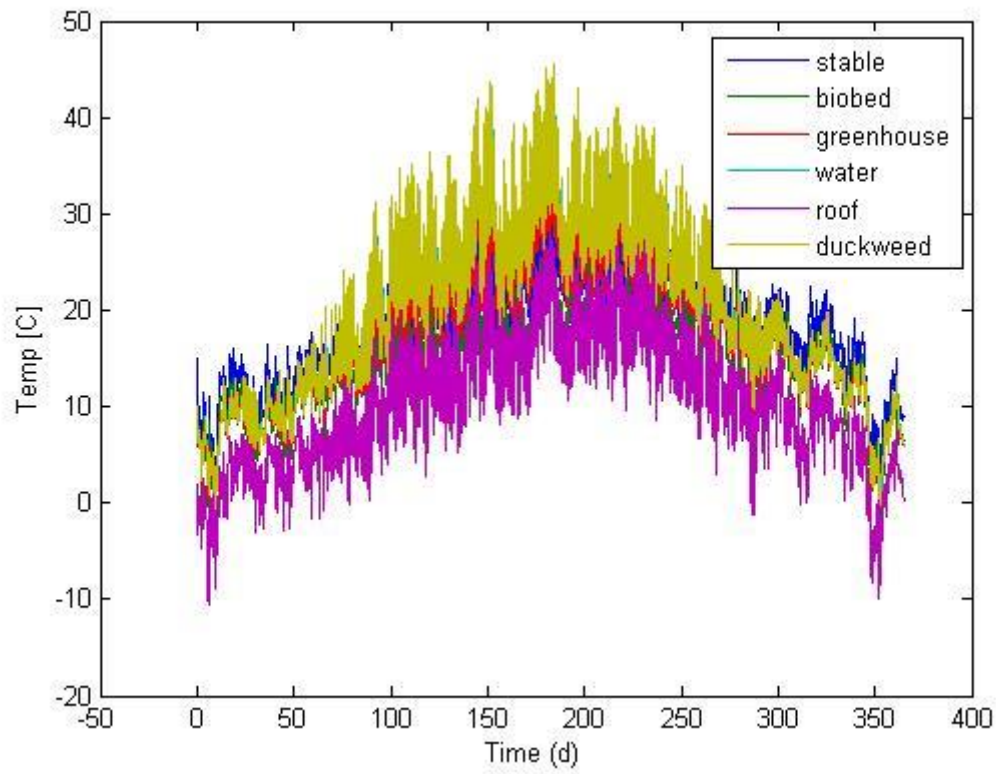


Figure 21 all temperatures

### 10.3.1 Whitewash

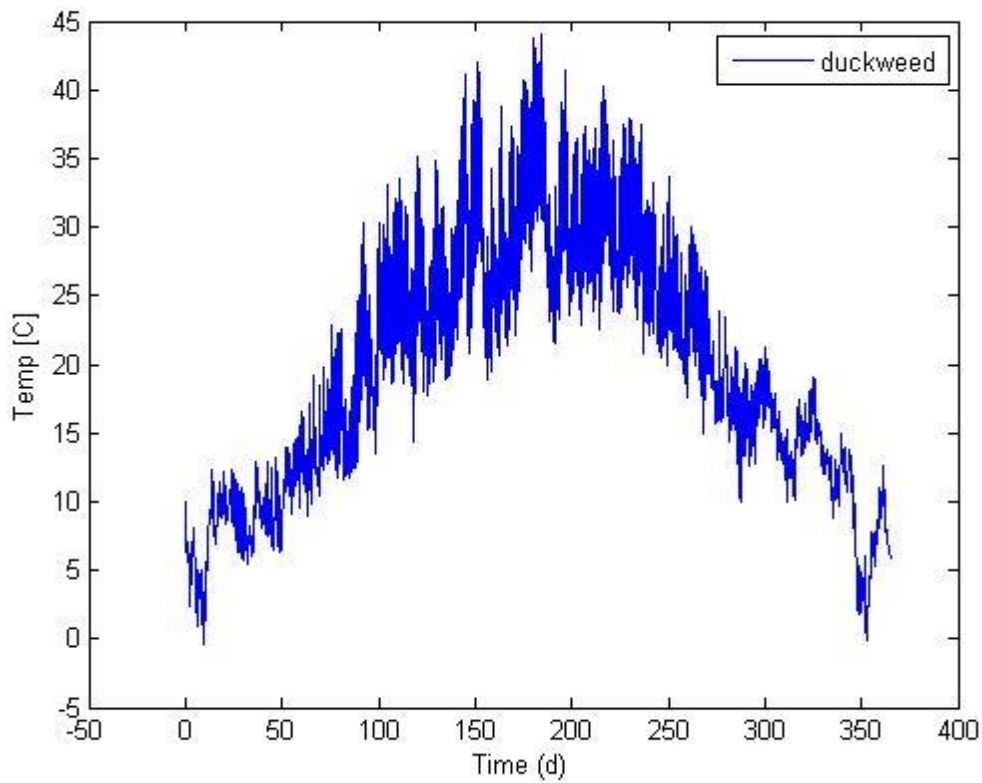


Figure 22 DUCKweed temperature

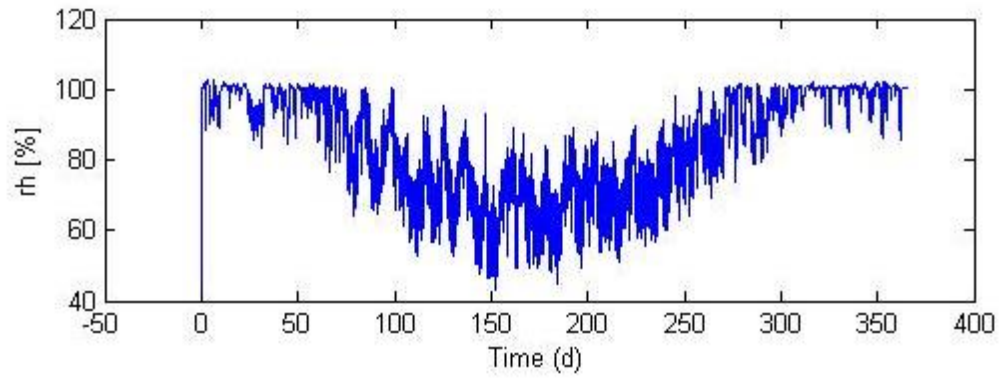


Figure 23 relative humidity greenhouse

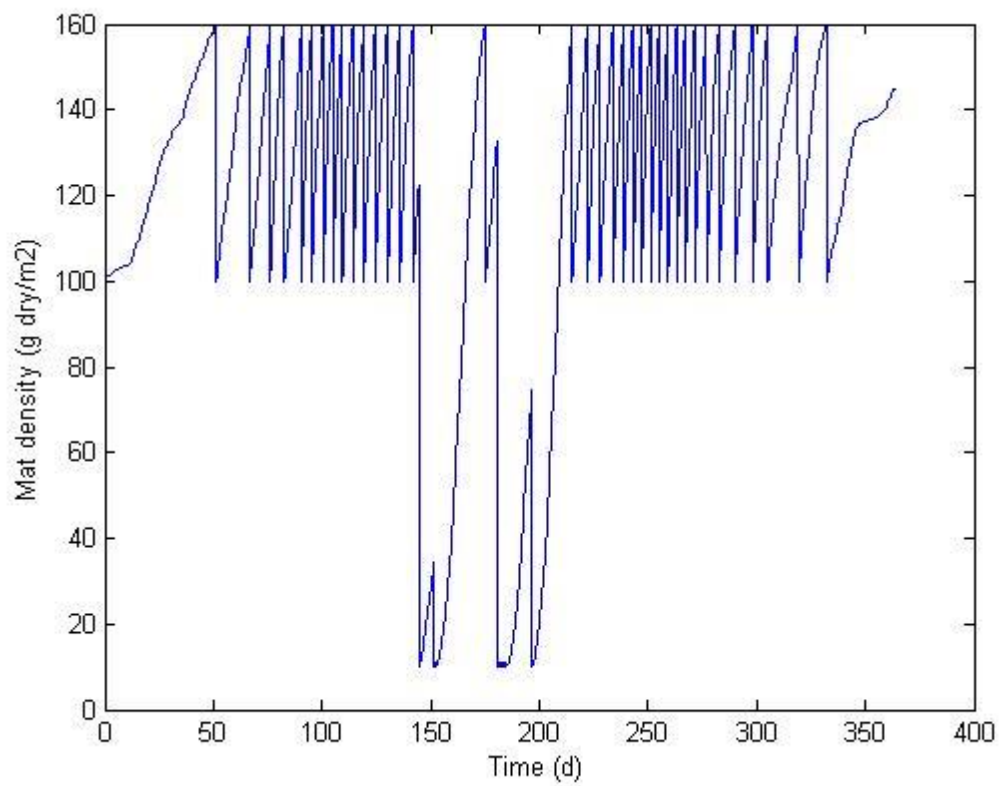
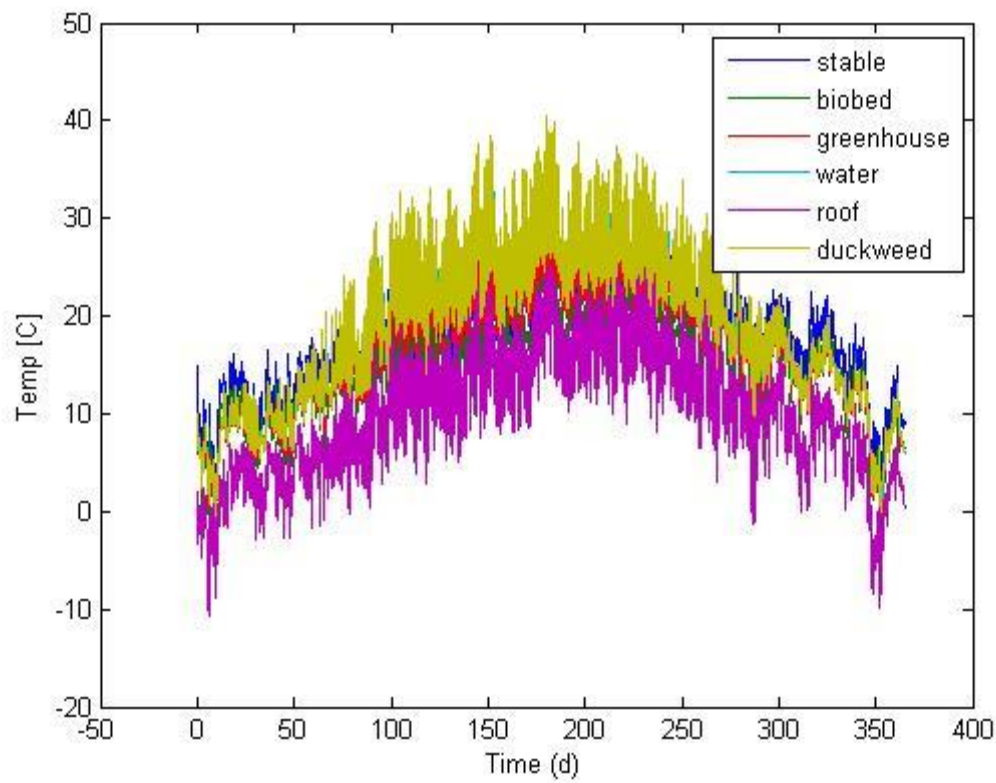
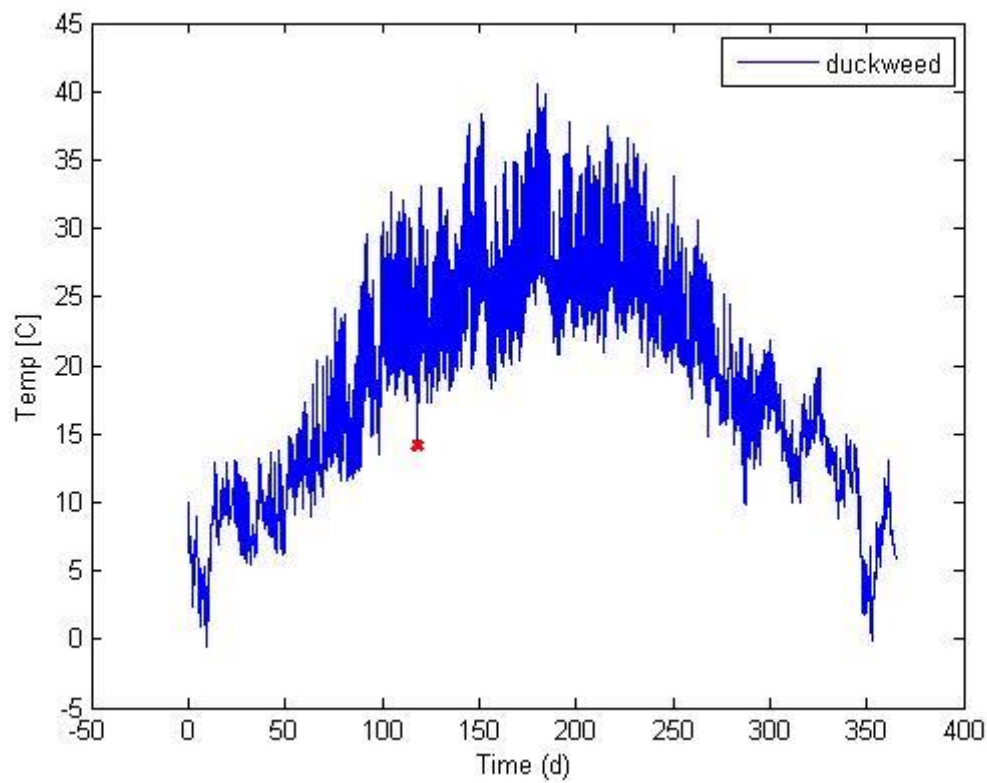


Figure 24 mat density

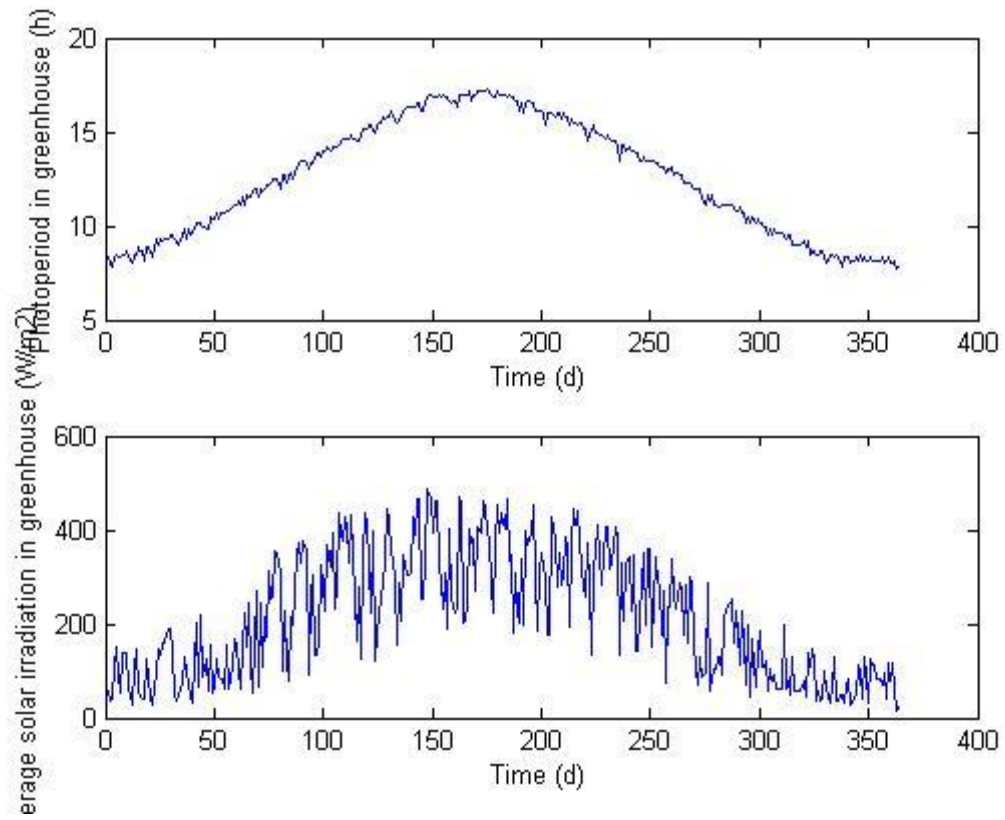
### 10.3.1 Adiabatic cooler



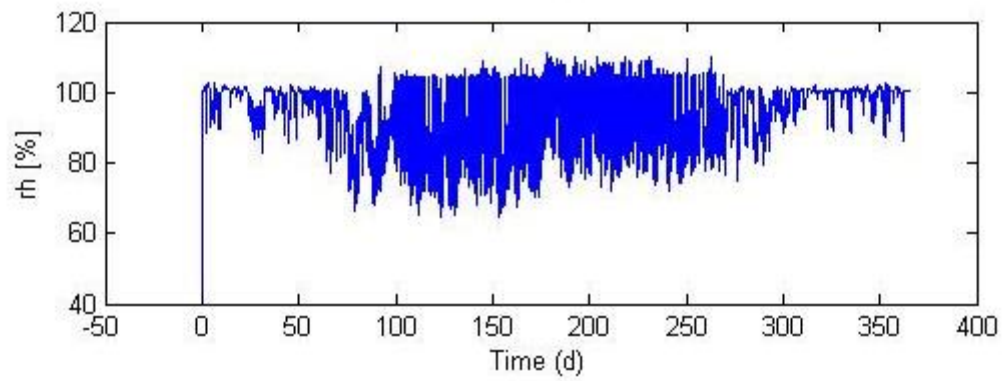
Figuur 25 AI temperaturs



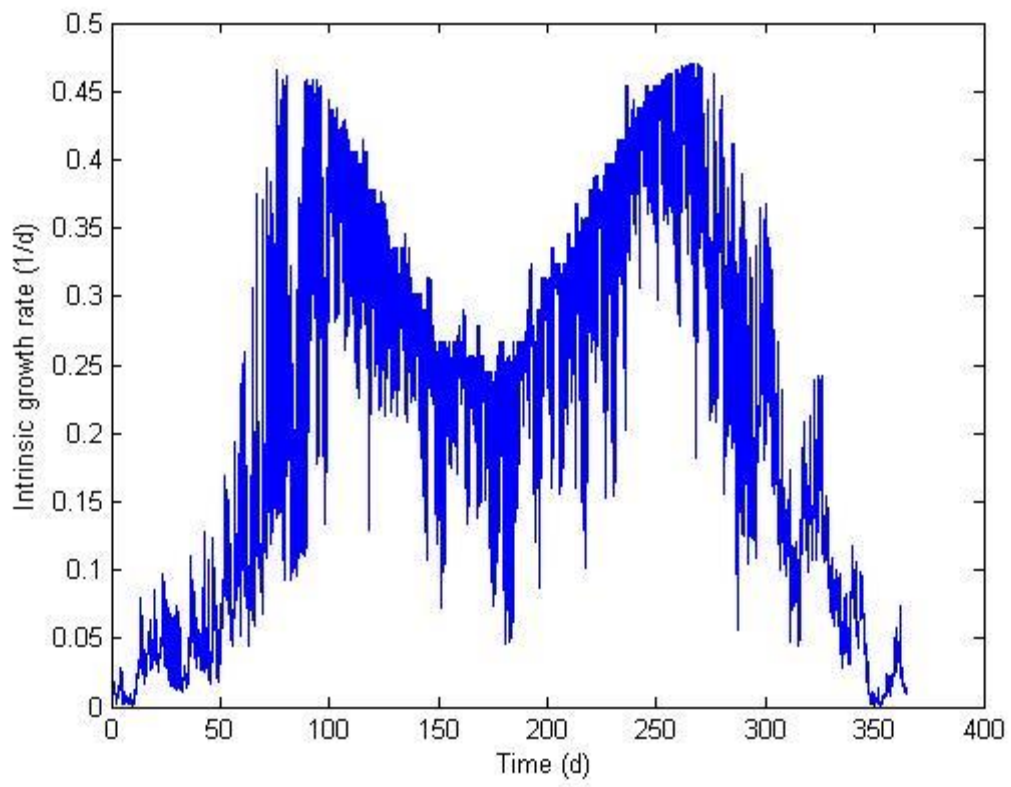
Figuur 26 Duckweed temperature



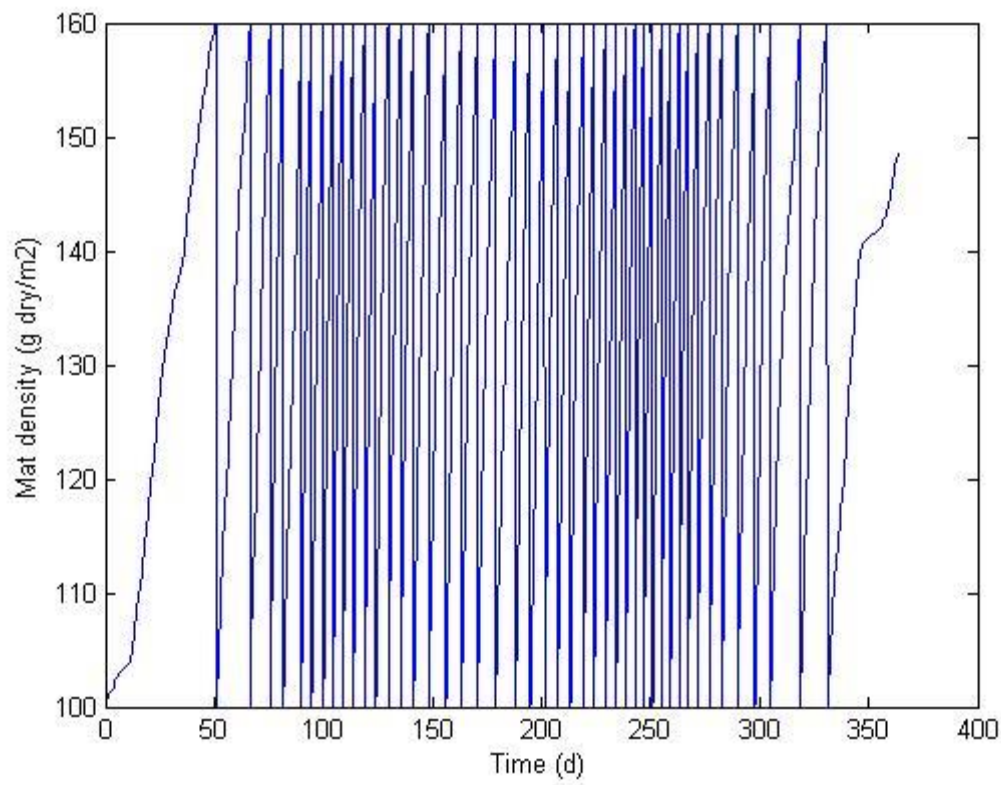
Figuur 27 Solar radiation



Figuur 28 relative humidity

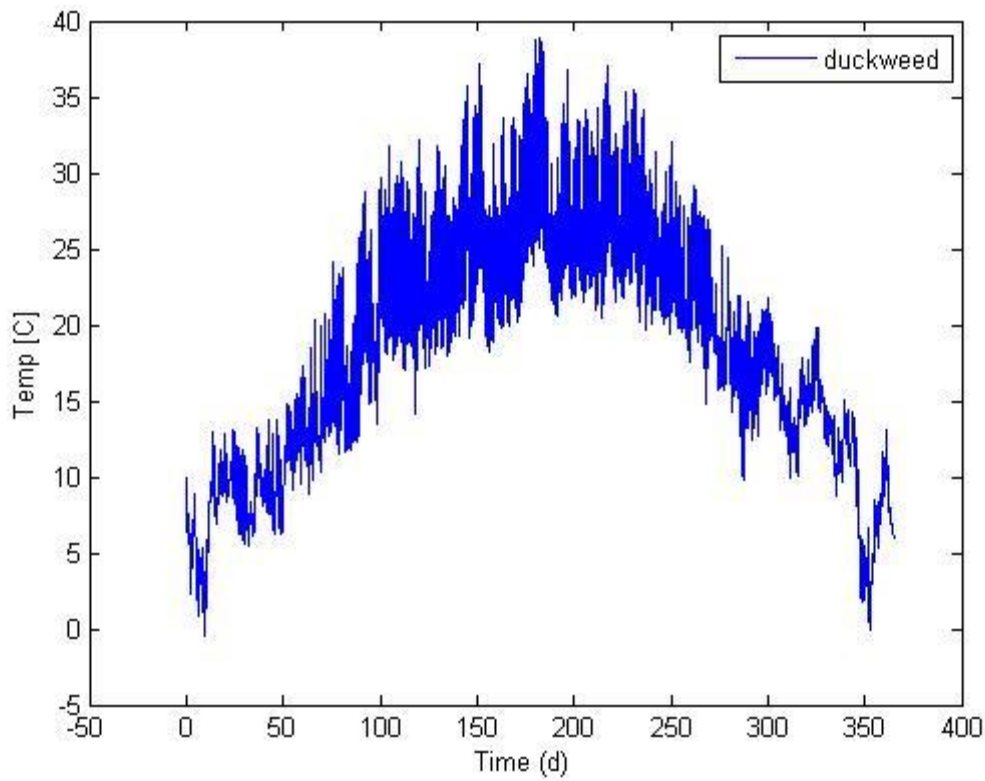


Figuur 29 intrinsic growth rate

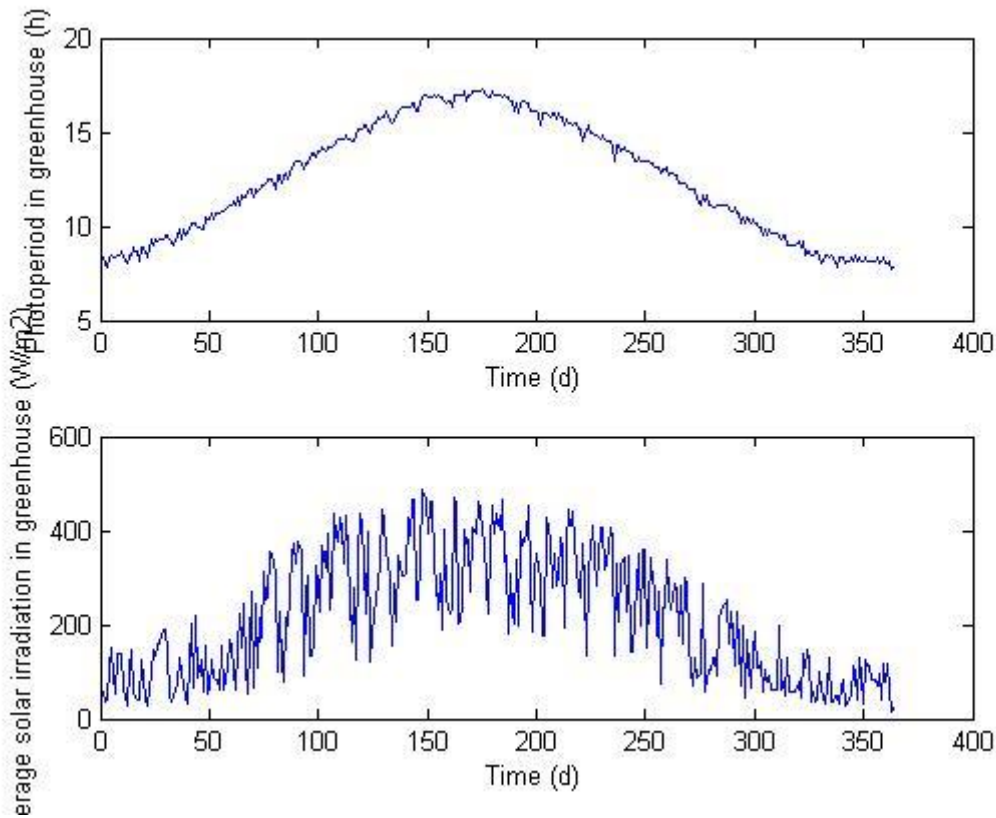


Figuur 30 Mat density

### 10.3.1 Ventilation

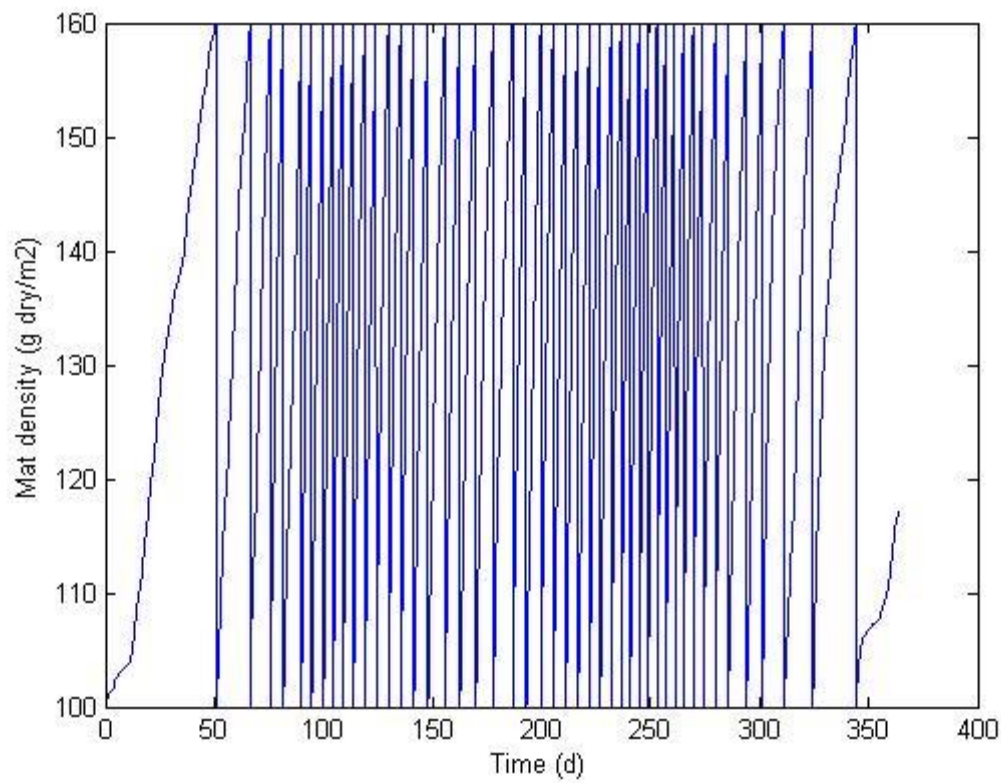


Figuur 31 Duckweed temperaturre

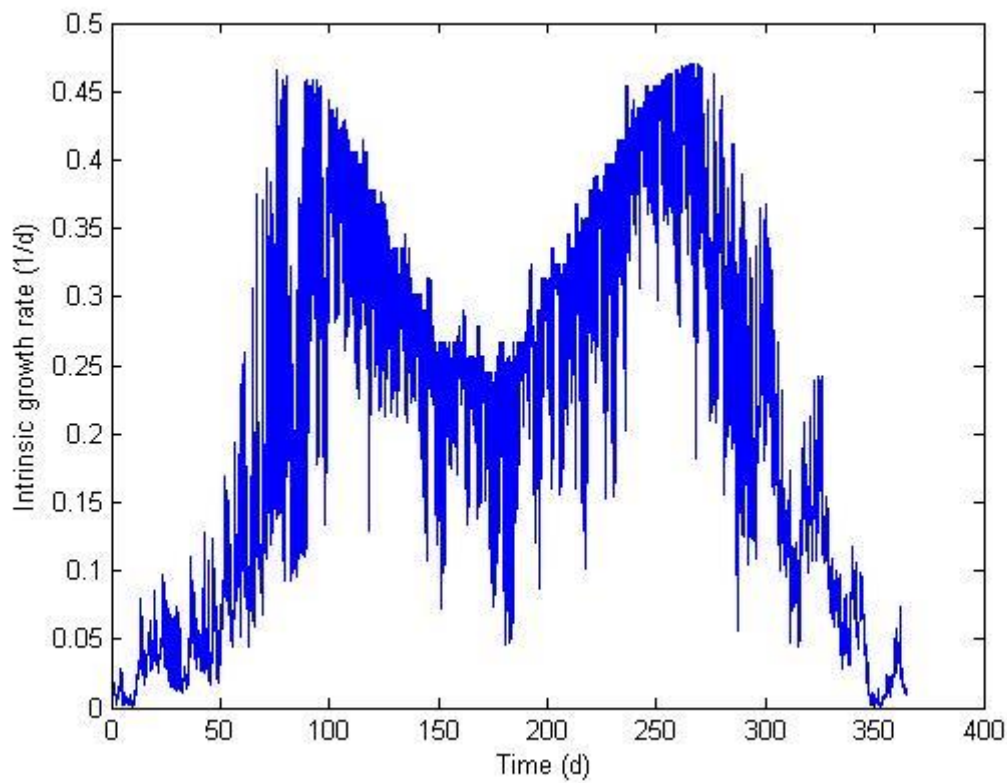


Figuur 32 Solar radiation

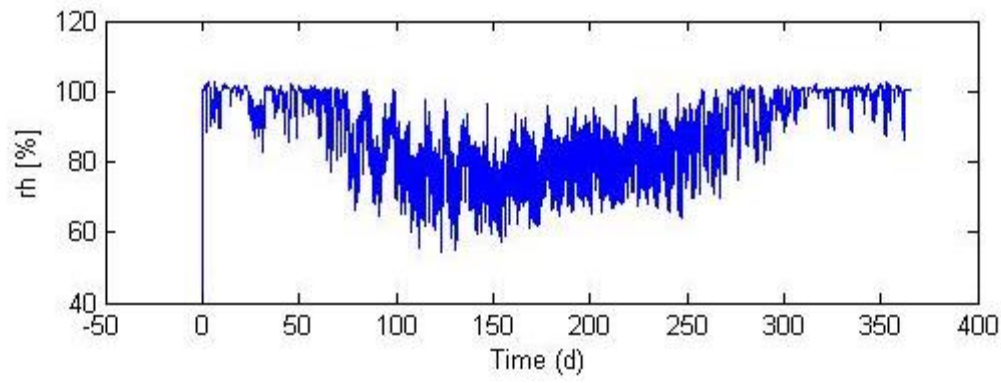




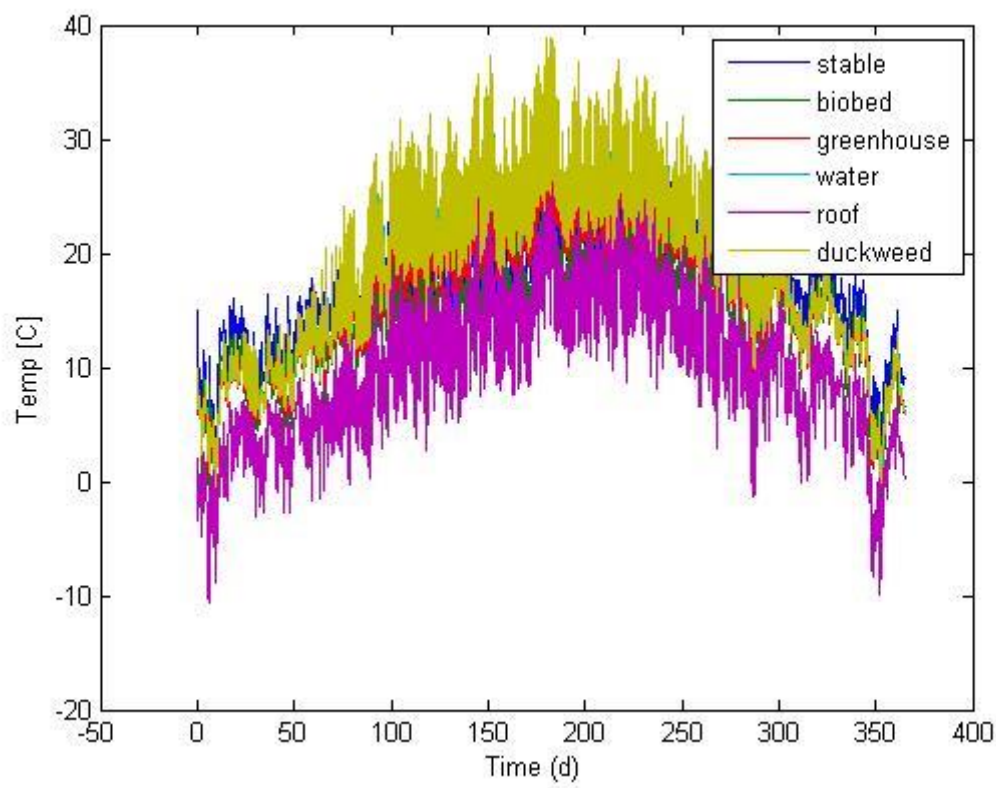
Figuur 33 mat density



Figuur 34 intrinsic growth rate



Figuur 35 relative humidity



Figuur 36 all temperatures