

# SimpleTreat.i Sensitivity Analysis

A.C. Sneekes, J.T. van der Wal

Report C058/09



Institute for Marine Resources and Ecosystem Studies

Wageningen **IMARES**

Client: StatoilHydro Research Centre  
Forskningssenter Rotvoll  
Arkitekt Ebbels vei 10  
Rannheim N-7035, Norway

Publication Date: 16-06-2009

- Wageningen **IMARES** conducts research providing knowledge necessary for the protection, harvest and usage of marine and coastal areas.
- Wageningen **IMARES** is a knowledge and research partner for governmental authorities, private industry and social organisations for which marine habitat and resources are of interest.
- Wageningen **IMARES** provides strategic and applied ecological investigation related to ecological and economic developments.

© 2009 Wageningen **IMARES**

Wageningen IMARES is registered in the Dutch trade record  
Amsterdam nr. 34135929,  
BTW nr. NL 811383696B04.

The Management of IMARES is not responsible for resulting damage, as well as for damage resulting from the application of results or research obtained by IMARES, its clients or any claims related to the application of information found within its research. This report has been made on the request of the client and is wholly the client's property. This report may not be reproduced and/or published partially or in its entirety without the express written consent of the client.

A\_4\_3\_2-V6.2

# Contents

Summary .....	4
1 Introduction.....	5
2 Data specifications .....	6
3 SimpleTreat.i 3.3.....	7
4 Base case calculations.....	9
4.1 WWTP Mongstad.....	9
4.2 WWTP Melkøya .....	12
4.3 WWTP Kollsnes .....	15
4.4 Distribution of compounds .....	18
5 Influence of parameters on the model .....	22
5.1 Compound related .....	22
5.2 Climate .....	24
5.3 Sewage.....	26
5.4 Biodegradation .....	30
5.5 Extra: size of the primary settler .....	32
6 Conclusions and recommendations .....	33
7 Quality Assurance .....	34
References .....	35
Justification.....	36
Annex A: Listing of sensitivity analysis results .....	
Annex B: SimpleTreat.i (v. 3.3, 15 May 09), Using the Batch-tab.....	

# Summary

The topic of this report is a sensitivity analysis of the SimpleTreat.i model. SimpleTreat.i (Van der Wal 2008) is a slightly modified version of the SimpleTreat model for evaluating municipal waste water treatment plants (WWTPs). The original SimpleTreat model is described in Struijs (1996). The modifications are intended to make SimpleTreat.i more easily applicable in an industrial setting. Both the initial modifications and the sensitivity analyses have been performed under contracts from StatoilHydro.

The sensitivity analyses was done by systematically changing an input parameter from its initial value by adding or subtracting five percent. A clear deviation in the model results from the expected five percent change would indicate a hit. A lower than expected change in the result would indicate a parameter to which the model is insensitive, a higher than expected change would indicate a parameter to which the model is highly sensitive.

The sensitivity analyses included calculations based on six compounds and three existing waste water treatment plants run by StatoilHydro. The required input data for the base cases was supplied by StatoilHydro.

The following parameters were varied:

- 1) Compound related parameters
  - molecular weight,
  - $K_{ow}$ ,
  - vapour pressure,
  - solubility and the
  - Henry constant (H);
- 2) Climate parameters
  - Air temperature,
  - Water temperature,
  - Wind speed;
- 3) Sewage related parameters
  - total daily sewage inflow,
  - concentration of compound inflow,
  - concentration of suspended solids of the raw sewage,
  - sludge loading rate (dropped from the final analysis) and
  - type of aeration;
- 4) Biodegradation parameters
  - Biodegradation speed
  - Temperature dependence.

Final results from the sensitivity analysis show that SimpleTreat.i is not sensitive to changes in the input parameters. All changes in input values were closely matches by the resulting changes in the model outcome. No parameters are identified as being more important to know precisely than others with respect to model sensitivity.

Considering the aspect of uncertainty a recommendation is made to distinguish between types of parameters that can be reliably be determined and those that are perceived as more challenging to establish a reliable estimate for. Examples of this second group are biodegradation parameters and vapour pressure. Based on this distinction more effort spent on decreasing uncertainty surrounding these parameters will improve the confidence that can be put on the results of the model.

# 1 Introduction

In a recent project for StatoilHydro changes were made to the existing SimpleTreat-model. These changes are intended to make the model more easily applicable in an industrial setting. The original model, developed at the RIVM (Struijs, 1996) was meant for modeling a waste water treatment plant (WWTP) in a municipal setting. The changes made to SimpleTreat were made on the basis of version 3.1 of the spreadsheet model and resulted in a model named SimpleTreat.i. The changes made in SimpleTreat.i are documented in Van der Wal, 2008.

StatoilHydro wishes to use this model to study the efficiency of existing WWTP's at their facilities with respect to known compounds used at that site and present in the waste water. They may also choose to use SimpleTreat.i to ascertain whether addition of a WWTP to an existing site or inclusion of a WWTP in a new development is advisable. All these options fit well with StatoilHydro's goal of achieving Zero Harmful Discharge (StatoilHydro, 2008).

The SimpleTreat model is a well-accepted model for municipal WWTP's and is part of the EUSES 2.0 (European Union System for the Evaluation of Substances), which is a decision-support system for the evaluation of the risks of substances to man and the environment (EC, 2004).

SimpleTreat.i is intended for use in more industrial conditions. Therefore, StatoilHydro asked Wageningen IMARES to perform a sensitivity analysis of the model. With the sensitivity analysis knowledge is gained for StatoilHydro on the applicability of the SimpleTreat.i model for their specific purposes and which inputs need to be accurately known. This will in turn help them in putting the model to good use and allows them to make sound decisions on e.g. requirements for a measurement program or the implementation of a WWTP at some studied location.

## 2 Data specifications

StatoilHydro delivered information on three industrial WWTP's (Mongstad, Melkøya and Kollsness) and in total six compounds (benzene, naphthalene, phenol, mercury, polyoxyethylene oleyl amine and monoethyleneglycol). Not all required data for the characterization of the chemicals were provided. When possible, supplementary data were extracted from literature sources. For the remaining parameters, default values were used. The WWTP's of Mongstad and Melkøya consist of two parallel placed bioreactors and separators. Calculations are performed for one stream and additional calculations are performed for determining the influence of the WWTP's dimensions.

Values below the detection limit as provided by StatoilHydro were inserted in the model at 50% of the detection limit. Zero values were included as zero values (e.g. inflow mercury for Mongstad).

The influence of a primary sedimentation unit in a WWTP was determined by adding a small sedimentation system (depth of 1 meter) in the 9-box.

In addition to the changes made by Van der Wal (2008), an adaptation of the model was needed. Van der Wal describes a relation between the input of solids in the raw sewage with the sewage flow and the concentration of the suspended solids in the raw sewage and uses this relation to calculate the default values. Using data from an industrial WWTP in combination with a default value other than the sewage flow, results in a false output. Therefore, the relationship described by Van der Wal was used in the calculations and implemented in the model.

While analyzing the sensitivity of the model, some errors and unclear functions were discovered and fixed resulting in a new version of the model: SimpleTreat.i 3.2. In May 2009 a work session was held at StatoilHydro in Stavanger to discuss the findings of the sensitivity analysis and to find the best method of implementing the model in the on-going work at StatoilHydro of implementing an EIF-Onshore. The EIF-Onshore assesses the environmental impact of an onshore installation on the (marine or aquatic) environment. As a method of modelling the of a (biological) WWTP SimpleTreat.i is expected to become part of the EIF-Onshore system. During this session a further improvement of the SimpleTreat.i was noticed. These changes are the topic of the next section.

### 3 SimpleTreat.i 3.3

The original SimpleTreat-model (Struis, 1996) is intended for use with municipal waste water treatment plants. It is often used to assess the efficiency of such a WWTP while it is still in the planning phase. The use of preset Sludge Loading Rate (SLR-) settings that are known to work well in reality results in a municipal WWTP automatically sized to have a size (volume) that is fitting for the population it will serve and the per capita amount of sewage generated. Also many municipal WWTP have been designed and are operating at SLRs closely matching the values available from table 1 on the Input-tabl of the model.

Versions 3.1 and 3.2 also operated by calculating the WWTP efficiency based on these preset SLRs. It was however noticed from the results that the exact values of a given WWTP were not reproduced by the model.

The relationship between the SLR, the HRT (PS), SRT and HRT were therefore investigated, based on the available data from Table 1. A perfect mathematical relationship based on a power function was found to exist between the SLR and the other three parameters: the Hydraulic Retention Time of the Primary Settler (HRT (PS)), the Sludge Retention time (SRT) and the Hydraulic Retention Time (HRT). These relationships are presented in Figure 1.

*Table 1 Sludge loading rate (SLR) related to hydraulic retention time, (HRT) and sludge retention time (SRT). HRT with primary sedimentation (PS) and without; PS has no influence on SRT.*

SLR ( $\text{kg}_{\text{BOD}} \cdot \text{kg}_{\text{dwt}}^{-1} \cdot \text{d}^{-1}$ )	HRT (PS) (hr)	HRT (hr)	SRT (d)	nitrification (-)
0.04 (low)	25.9	40.5	37.0	yes
0.06 (low)	17.3	27	24.1	yes
0.1 (low)	10.4	16.2	14.1	yes
0.15 (medium)	6.9	10.8	9.2	yes
0.2 (medium)	5.2	8.1	6.8	no
0.3 (high)	3.5	5.4	4.5	no
0.6 high)	1.7	2.7	2.2	no

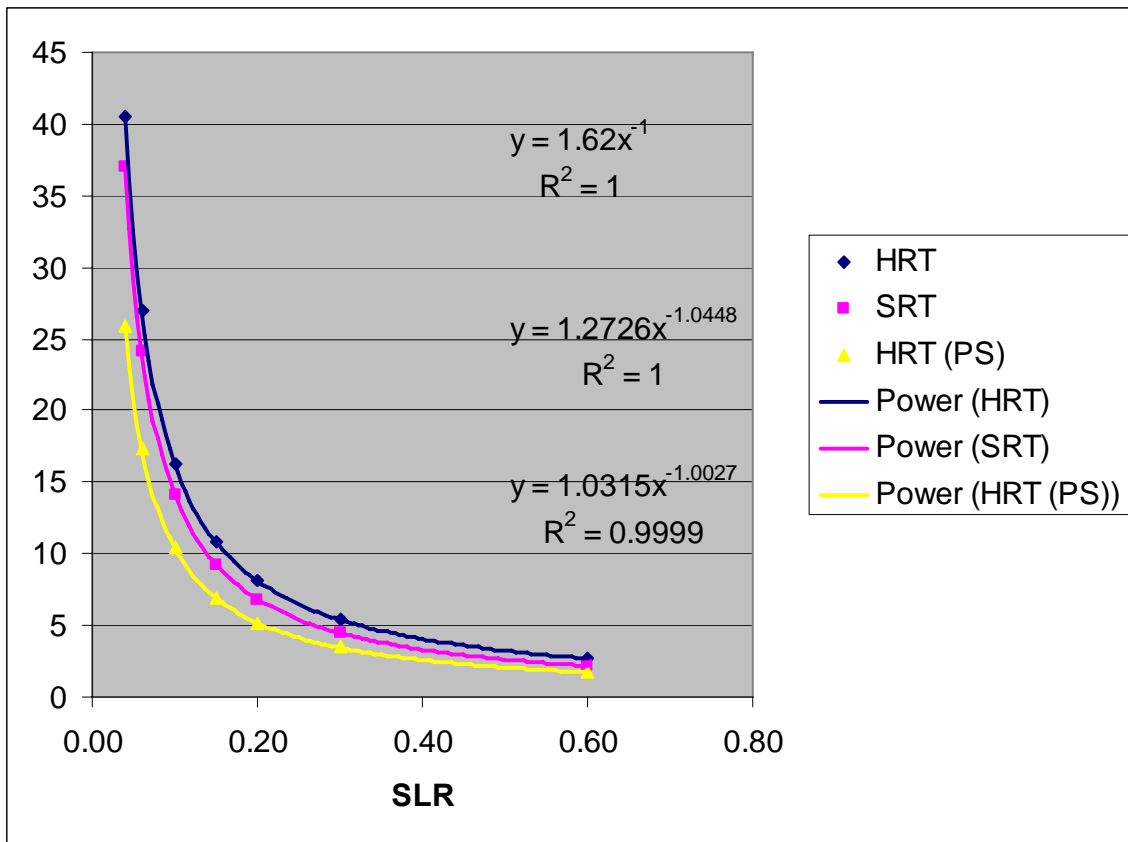


Figure 1 Mathematical relations between Sludge loading rate (SLR) and hydraulic retention times (HRT, HTR (PS)) and sludge retention time (SRT).

In version 3.3 SimpleTreat.i was changed to take one more input value on the Input-tab: Volume aerator (6-box). Using this the HRT of the 6-box WWTP can be calculated. This is the ratio of 'Sewage Flow daily total' / Volume aerator (6-box) \* 24. The final multiplication is a conversion factor from days (for the Sewage Flow) to hours (for the HRT).

The relationship between SLR and HRT ( $HRT = 1.62 / SLR$ ) can now be inverted and the exact SLR for a specific 6-box WWTP is known. From this point on version 3.3 of the model does its calculations as always.

As a result of this change SimpleTreat.i 3.3 is even more easily applicable in an industrial setting. Especially when assessing an existing WWTPs with known volumes of sewage flow and basins. Results are also expected to more closely resemble the actual performance of the WWTP. Version 3.2 may be easier to use when performing an assessment for a planned WWTP and pre-selecting an applicable SLR from table 1 (on the Input-tab).



## 4 Base case calculations

### 4.1 WWTP Mongstad

The WWTP Mongstad is located in the South West part of Norway (coordinates: 60°48' 48N, 05°02'02E). The plant consists of two parallel placed separate bioreactors and separators. Each stream operates with a daily flow of 2,065,000 litres, containing 50 mg/L of suspended solids. The bioreactor is continuously aerated from the bottom.

For the gas plant Mongstad, information was provided of five compounds: Benzene, Naphthalene, Phenol, Mercury (as HgCl<sub>2</sub>) and Polyoxyethylene oleyl amine. Results of the reference calculations for 6-box are shown in Table 2.

Zero inflow concentration was given for mercury and therefore results on distribution and elimination may not be realistic. The calculated measured concentrations of mercury in sludge and effluent show presence of the metal, even though there is no metal in the inflow. This is the result of how the model is intended to operate, when a zero concentration is input, this value is overridden with a 0.5 mg/l default value.

For polyoxyethylene oleyl amine, some of the physical-chemical data was lacking including molecular weight and octanol-water distributions (Kow). The default value of 100 for molecular weight would be an underestimation for this polymer, but exact values are difficult to determine as the repeating oxyethylene groups typically range from 4 to 180 (<http://chemicalland21.com/specialtychem/perchem/ETHOXYLATED%20OLEYL%20AMINE.htm>).

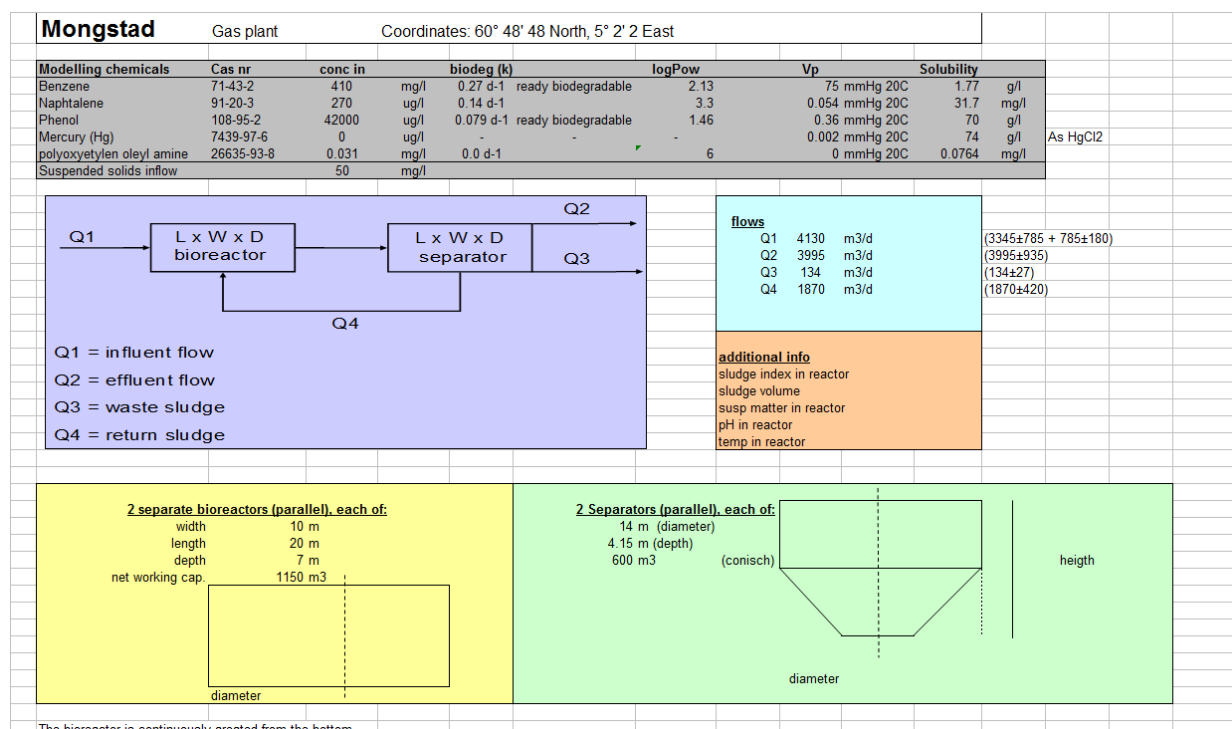


Figure 2 Data as provided on the Mongstad WWTP

The Sludge Loading Rate for the Mongstad WWTP calculated from the input values using the relationship from Section 3 is 0.121 kg BOD/ (kg DWT.d).

For evaluating the environmental performance of the Mongstad WWTP the numbers are presented in Table 2. The distribution of the compounds across the environmental compartments (shown as Summary of distribution in

Table 2) is presented a pie charts in Figure 3. The most important outcome is probably the total effluent concentration as this is the most relevant to compare with environmental quality objectives or other concentrations set either by law or in e.g. an environmental license.

Table 2 View of the 6-box output for WWTP Mongstad (B= Benzene, N = Naphthalene, Ph = Phenol, M = Mercury, Poe = Polyoxyethylene oleyl amine)

		<b>B</b>	<b>N</b>	<b>Ph</b>	<b>M</b> (as HgCl <sub>2</sub> )	<b>Poe</b>
[c] inflow	(mg/L)	410	270	42000	0 (def.=0.5)	0.031
<b>Elimination in the aerator (%)</b>						
stripping		48.3	10.6	100.0	0.0	0.0
biodegradation		6.7	6.2	0.0	0.0	0.0
Total		55.0	16.8	100.0	0.0	0.0
<b>Elimination in the solids liquid separator (%)</b>						
volatilization		6.2	8.0	0.0	0.0	0.0
via surplus sludge		0.2	2.8	0.0	0.0	2.0
Total		6.4	10.8	0.0	0.0	2.0
Total elimination from waste water (%)		61.4	27.6	100.0	0.0	2.0
Total emission via effluent (%)		38.6	72.4	0.0	100.0	98.0
% dissolved		71.9	0.0	100.0	97.6	97.6
% associated		0.5	0.0	0.0	0.4	0.4
Balance		100.0	100.0	100.0	100.0	100.0
<b>Summary of distribution (%)</b>						
to air		54.5	18.6	100.0	0.0	0.0
to water		38.6	72.4	0.0	100.0	98.0
via surplus sludge		0.2	2.8	0.0	0.0	2.0
degraded		6.7	6.2	0.0	0.0	0.0
Total		100.0	100.0	100.0	100.0	100.0
<b>Concentrations</b>						
in air	(g/m <sup>3</sup> )	0.01	2.3*10 <sup>-03</sup>	1.9	2.0*10 <sup>-10</sup>	1.2*10 <sup>-11</sup>
in surplus sludge	(mg/kg)	4518.7	46100.2	32.3	0.6	3.8
in effluent (total)	(mg/L)	158.3	195.4	5.0*10 <sup>-03</sup>	0.5	0.03
dissolved	(mg/L)	158.2	194.1	4.0*10 <sup>-03</sup>	0.5	0.03
associated	(mg/L)	0.1	1.4	9.7 0 <sup>-04</sup>	1.8*10 <sup>-05</sup>	1.1*10 <sup>-04</sup>
in solids effluent	(mg/kg)	4518.7	46100.2	32.3	0.6	3.8

In a WWTP configured like Mongstad with a relatively high SLR, the sewage spends not a lot of time in the plant, this can be seen by the differences between the compounds regarding where and when and by which process they are removed from the water column. A compound with a high volatility like Phenol is completely removed by stripping in the aerator. Less volatile compounds such as Benzene and Naphthalene remain in the system longer and are partially biodegraded. Some of these compounds also escape to the air by volatilization from the settling basin. Other compounds such as not susceptible to volatilization and/or biodegradation and as a result most or all leaves the WWTP with the effluent.

In comparison with the other WWTP in this Sensitiity Analysis operating with lower SLRs biodegradation and volatilization are less important in Mongstad than they are in Melkøya or Kolsnes.

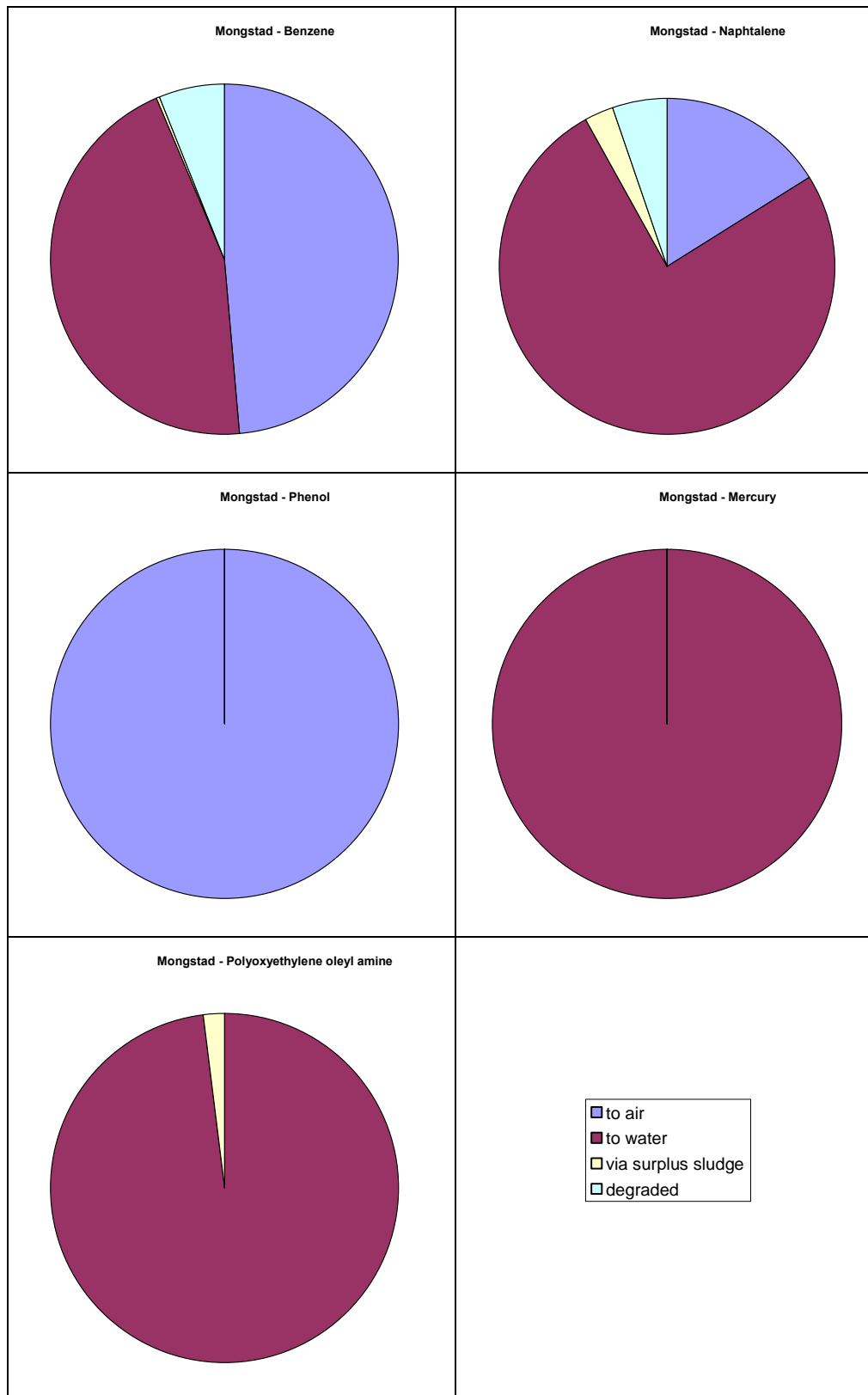


Figure 3 Mongstad environmental fate for all five compounds (6-box)

## 4.2 WWTP Melkøya

The WWTP Melkøya is located in the Northern part of Norway (coordinates: 70°41'20N, 23°36'25E). The plant consists of two parallel placed separate bioreactors and separators. Each stream operates with a daily flow of 84,000 litres, containing very low levels of suspended solids ( $\ll 1$  mg/L). The bioreactor is continuously aerated from the bottom.

For the gas plant Melkøya, information was provided of five compounds: Benzene, Naphtalene, Phenol, Mercury (as  $\text{HgCl}_2$ ) and Monoethyleneglycol. Results of the reference calculations for 6-box are shown in Table 3.

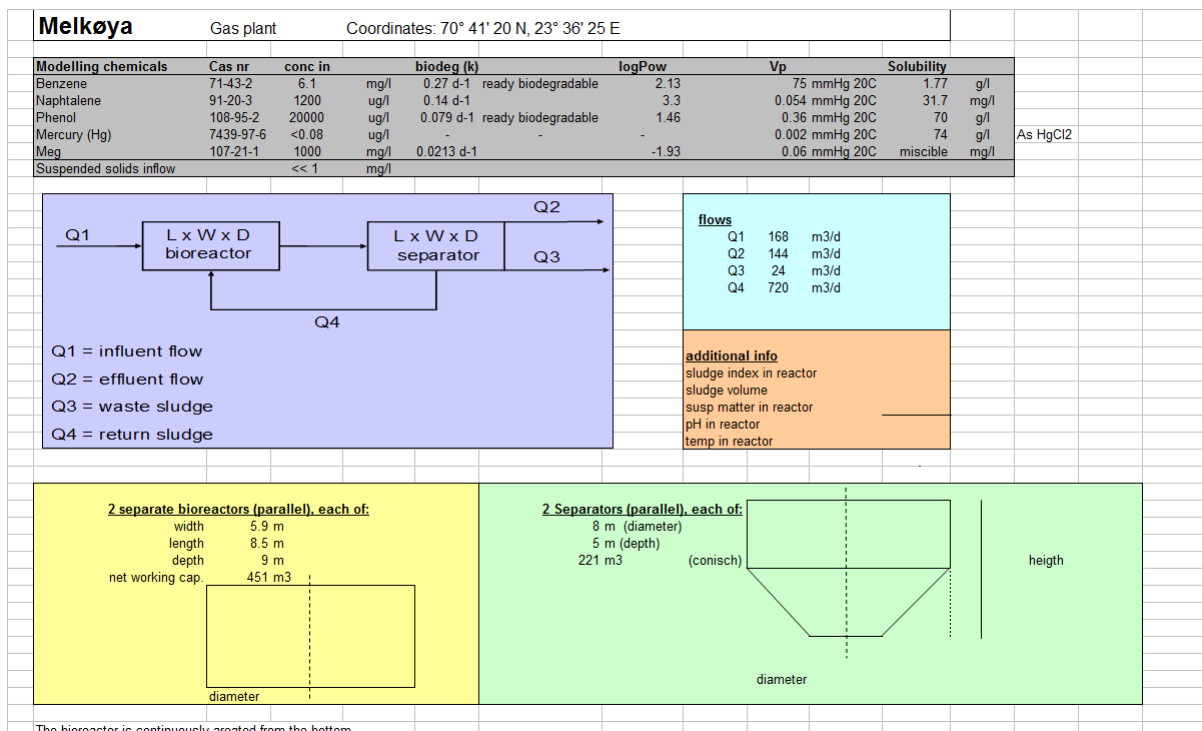


Figure 4 Data as provided on the Melkøya WWTP

The Sludge Loading Rate for the Melkøya WWTP calculated from the input values using the relationship from Section 3 is 0.013 kg BOD/ (kg DWT.d).

For evaluating the environmental performance of the Melkøya WWTP the numbers are presented in Table 3. The distribution of the compounds across the environmental compartments (shown as Summary of distribution in Table 4) is presented a pie charts in Figure 5. The most important outcome is probably the total effluent concentration as this is the most relevant to compare with environmental quality objectives or other concentrations set either by law or in e.g. an environmental license.

Table 3 View of the 6-box output for WWTP Melkøya (B= Benzene, N = Naphthalene, Ph = Phenol, M = Mercury, Meg = Monoethyleneglycol)

		<b>B</b>	<b>N</b>	<b>Ph</b>	<b>M<sup>a</sup></b> <b>(as HgCl<sub>2</sub>)</b>	<b>Meg</b>
[c] inflow	(mg/L)	6.1	1.2	20	4*10 <sup>-5</sup>	1000
Elimination in the aerator (%)						
stripping		46.1	33.7	100.0	0.0	0.0
biodegradation		31.7	26.6	0.0	0.0	10.3
total		77.8	60.4	100.0	0.0	10.3
Elimination in the solids liquid separator (%)						
volatilization		12.1	17.5	0.0	0.0	0.0
via surplus sludge		0.1	1.0	0.0	0.0	0.0
total		12.2	18.5	0.0	0.0	0.0
Total elimination from waste water (%)		90.0	78.8	100.0	0.0	10.3
Total emission via effluent (%)		10.0	21.2	0.0	100.0	89.7
% dissolved		10.0	21.0	0.0	100.0	89.7
% associated		0.0	0.2	0.0	0.0	0.0
balance		100.0	100.0	100.0	100.0	100.0
Summary of distribution (%)						
to air		58.2	51.2	100.0	0.0	0.1
to water		10.0	21.2	0.0	100.0	89.7
via surplus sludge		0.1	1.0	0.0	0.0	0.0
degraded		31.7	26.6	0.0	0.0	10.3
total		100.0	100.0	100.0	100.0	100.0
Concentrations						
in air	(g/m <sup>3</sup> )	1.2*10 <sup>-05</sup>	2.1*10 <sup>-06</sup>	6.7*10 <sup>-05</sup>	9.0*10 <sup>-15</sup>	2.0*10 <sup>-06</sup>
in surplus sludge	(mg/kg)	28.6	82.3	1.2*10 <sup>-05</sup>	4.9*10 <sup>-05</sup>	33.1
in effluent (total)	(mg/L)	0.6	0.3	7.8*10 <sup>-09</sup>	4.0*10 <sup>-05</sup>	896.8
dissolved	(mg/L)	0.6	0.3	7.4*10 <sup>-09</sup>	4.0*10 <sup>-05</sup>	896.8
associated	(mg/L)	0.001	0.002	3.7*10 <sup>-10</sup>	1.5*10 <sup>-09</sup>	0.001
in solids effluent	(mg/kg)	28.6	82.3	1.2*10 <sup>-05</sup>	4.9*10 <sup>-05</sup>	33.1

<sup>a</sup> concentration inflow on bases of 50% detection limit

In a WWTP configured like Melkøya with a low SLR, the sewage spends a considerable amount of time in the plant, as a result compounds such as Benzene and Naphthalene which are not very volatile are in the system long enough for both volatilization and biodegradation to play a significant part in their removal from the water column. A volatile compound like Phenol is completely removed by stripping to the air in the aerator, even in a WWTP like Mongstad operating at a higher SLR and with shorter times spent within the system. Other compounds such as not susceptible to volatilization and/or biodegradation and as a result most or all leaves the WWTP with the effluent.

In comparison with the other WWTP in this Sensitiity Analysis operating with lower SLRs biodegradation and volatilization are more important in Melkøya than they are in Mongstad or Kolsness.

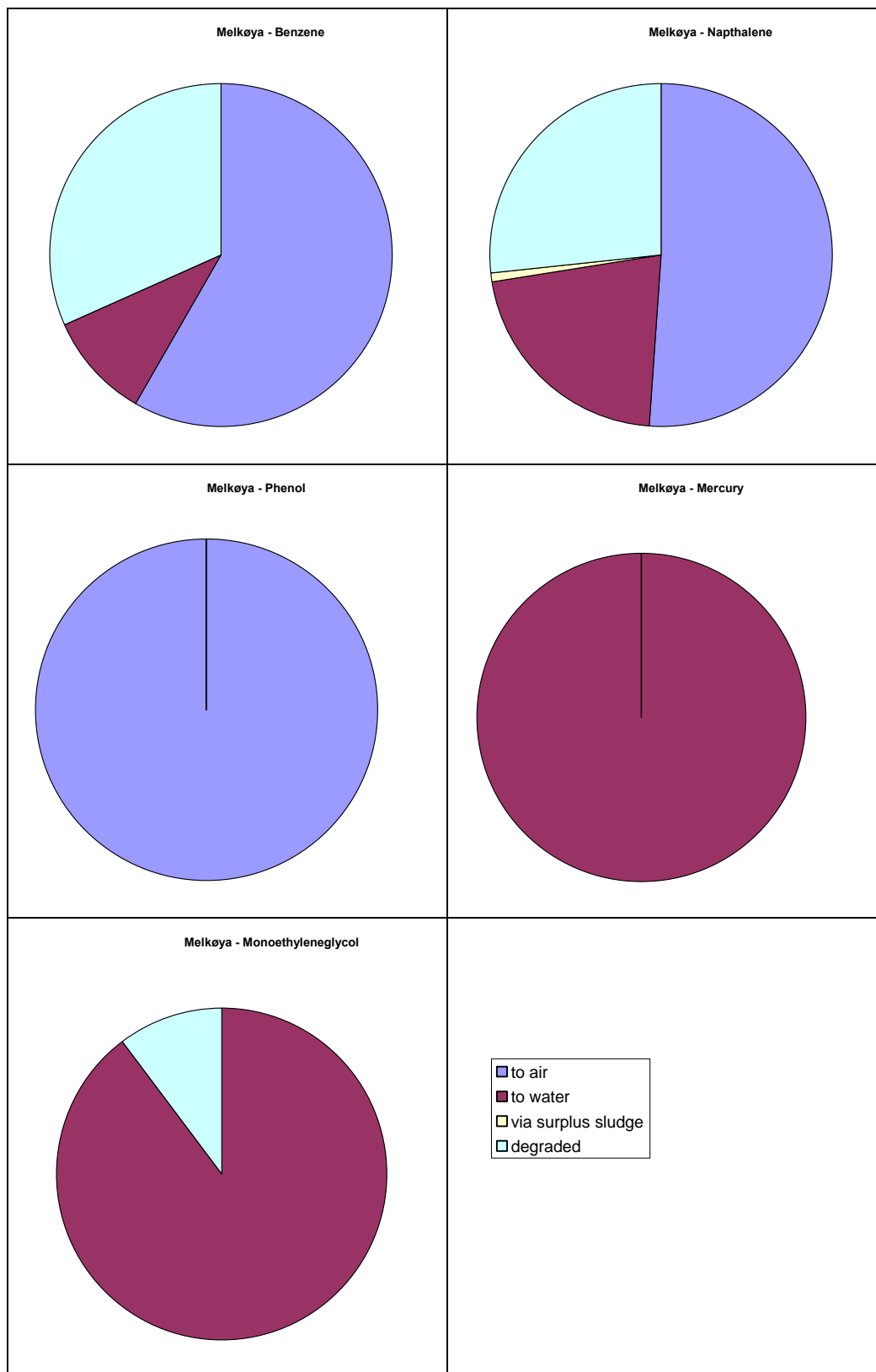


Figure 5 Melkøya environmental fate for all five compounds (6-box)

### 4.3 WWTP Kollsnes

The WWTP Kollsnes is located in the Southern part of Norway (coordinates: 58°54'06N, 05°34'58E). The plant consists of a separate bioreactor and separator. The stream operates with a daily flow of 1,200,000 litres, containing very low levels of suspended solids (<<1 mg/L). The bioreactor is continuously aerated from the bottom.

For the gas plant Kollsnes, information was provided of five compounds: Benzene, Naphthalene, Phenol, Mercury (as HgCl<sub>2</sub>) and Monoethyleneglycol. Results of the reference calculations for 6-box are shown in Table 4.

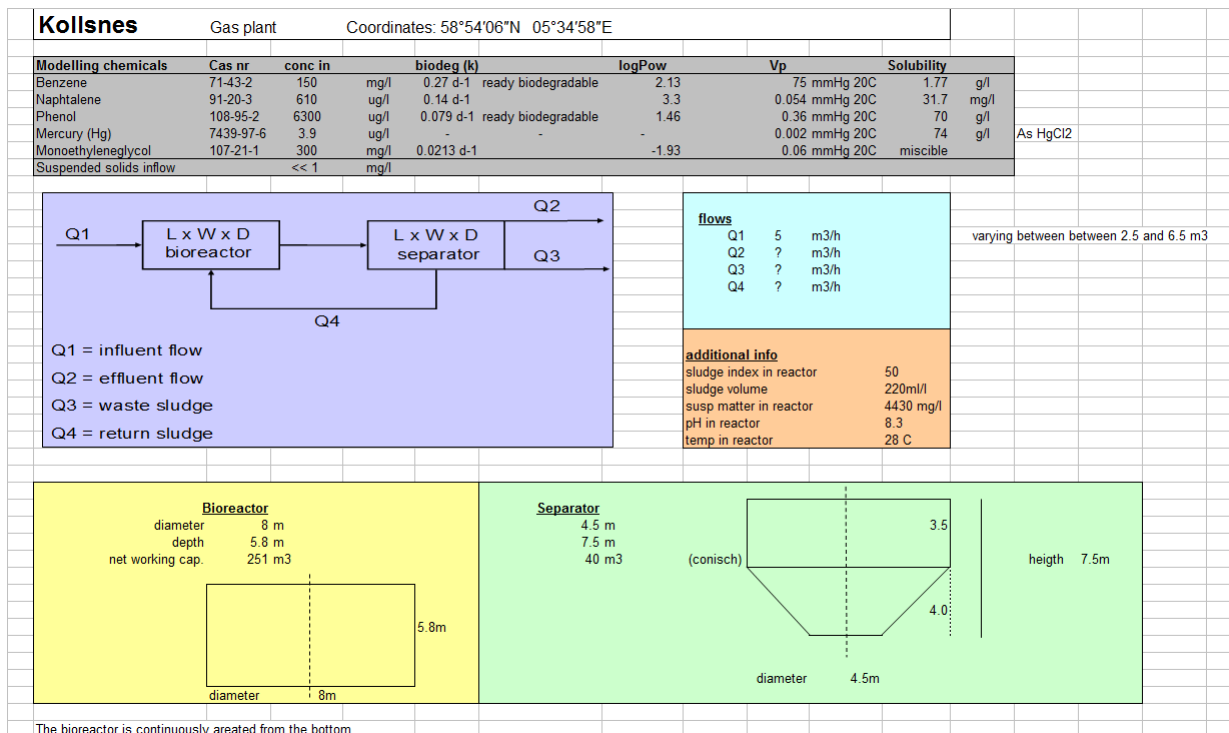


Figure 6 Data as provided on the Kollsnes WWTP

The Sludge Loading Rate for the Kollsnes WWTP calculated from the input values using the relationship from Section 3 is 0.032 kg BOD/ (kg DWT.d).

For evaluating the environmental performance of the Kollsnes WWTP the numbers are presented in Table 4. The distribution of the compounds across the environmental compartments (shown as Summary of distribution in Table 4) is presented as pie charts in Figure 7. The most important outcome is probably the total effluent concentration as this is the most relevant to compare with environmental quality objectives or other concentrations set either by law or in e.g. an environmental license.

Table 4 View of the 6-box output for WWTP Kollsnes (B= Benzene, N = Naphthalene, Ph = Phenol, M = Mercury, Meg = Monoethyleneglycol)

		<b>B</b>	<b>N</b>	<b>Ph</b>	<b>M</b> (as HgCl <sub>2</sub> )	<b>Meg</b>
[c] inflow	(mg/L)	150	0.61	6.3	3.9*10 <sup>-3</sup>	300
<b>Elimination in the aerator (%)</b>						
stripping		54.2	30.3	100.0	0.0	0.0
biodegradation		16.5	15.3	0.0	0.0	4.3
total		70.7	45.6	100.0	0.0	4.3
<b>Elimination in the solids liquid separator (%)</b>						
volatilization		2.7	3.4	0.0	0.0	0.0
via surplus sludge		0.1	1.7	0.0	0.0	0.0
total		2.8	5.1	0.0	0.0	0.0
Total elimination from waste water (%)		73.5	50.8	100.0	0.0	4.3
Total emission via effluent (%)		26.5	49.2	0.0	100.0	95.7
% dissolved		26.5	48.9	0.0	100.0	95.7
% associated		0.0	0.3	0.0	0.0	0.0
balance		100.0	100.0	100.0	100.0	100.0
<b>Summary of distribution (%)</b>						
to air		56.9	33.8	100.0	0.0	0.0
to water		26.5	49.2	0.0	100.0	95.7
via surplus sludge		0.1	1.7	0.0	0.0	0.0
degraded		16.5	15.3	0.0	0.0	4.3
total		100.0	100.0	100.0	100.0	100.0
<b>Concentrations</b>						
in air	(g/m <sup>3</sup> )	5.7*10 <sup>-04</sup>	1.4*10 <sup>-06</sup>	4.2*10 <sup>-05</sup>	6.3*10 <sup>-13</sup>	4.7*10 <sup>-07</sup>
in surplus sludge	(mg/kg)	1078.9	68.4	1.3*10 <sup>-05</sup>	0.005	10.6
in effluent (total)	(mg/L)	39.8	0.3	2.4*10 <sup>-09</sup>	0.004	287.1
dissolved	(mg/L)	39.7	0.3	2.0*10 <sup>-09</sup>	0.004	287.1
associated	(mg/L)	0.0	0.002	3.9*10 <sup>-10</sup>	1.4*10 <sup>-07</sup>	3.2*10 <sup>-04</sup>
in solids effluent	(mg/kg)	1078.9	68.4	1.3*10 <sup>-05</sup>	0.005	10.6

In a WWTP configured like Kollsnes with a low SLR, though clearly higher than Melkøya, the sewage spends a considerable amount of time in the plant. The distribution over the environmental compartments and efficiency of this plant are intermediate between the other two (Mongstad and Melkøya).



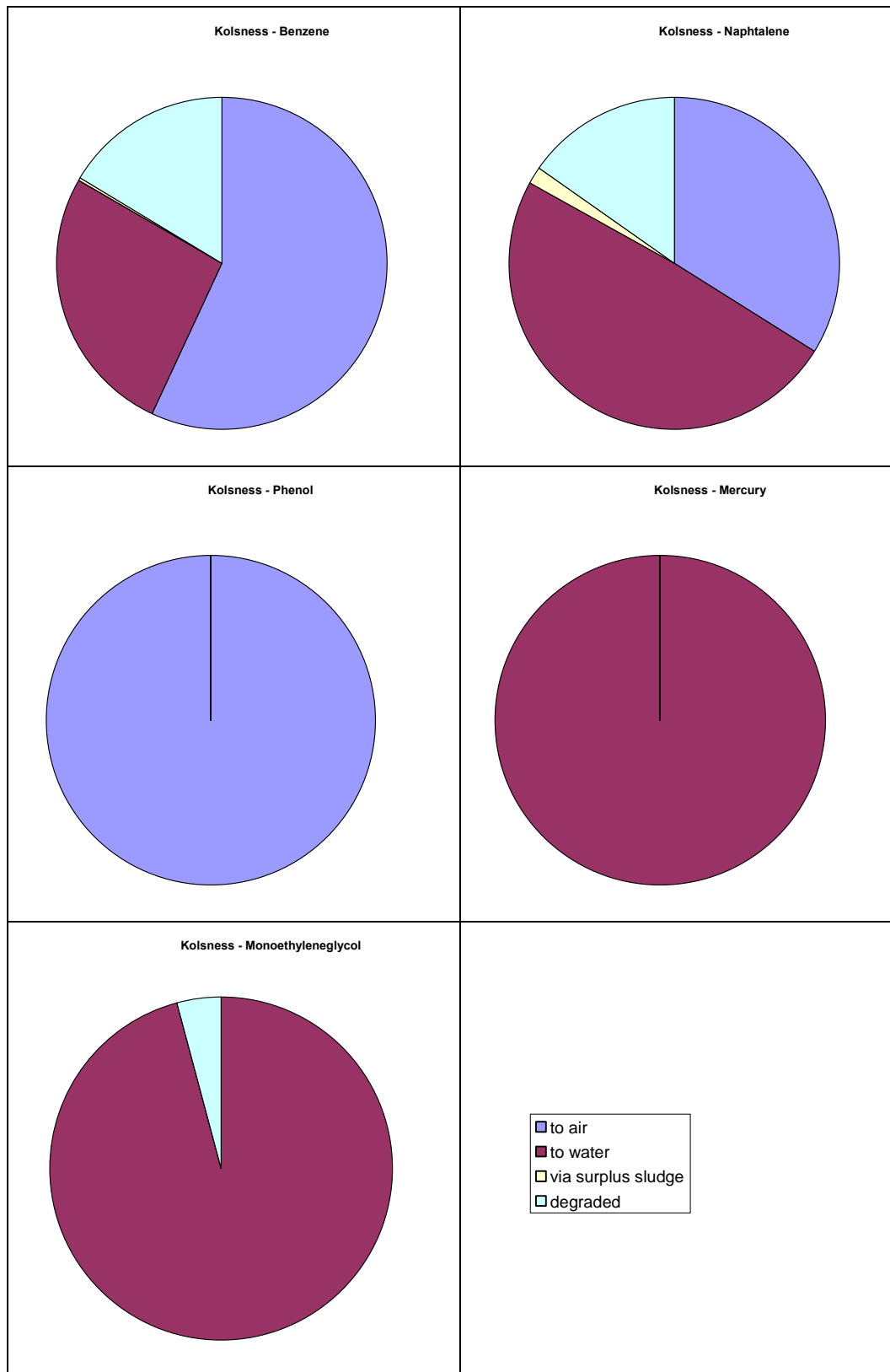


Figure 7 Kolsnes environmental fate for all five compounds (6-box)

#### 4.4 Distribution of compounds

For the three WWTP's, the calculated distribution and removal efficiencies for all compounds relate logically to each other. For the distribution this can best be seen by comparing the graphs of all compounds as given in Figure 3, Figure 5 and Figure 7

The size of the WWTP and the input flow of the compound determine the amount of benzene and naphthalene in the air or water, as well as the amount degraded. From the Mongstad WWTP 38% of benzene resp. 72% of naphthalene entering the WWTP is released with the effluent. For the Melkøya WWTP this improves to only 10% of benzene and 21% for Naphtalene. The major contribution to this improvement comes from increased biodegradation taking place.

Phenol will be entirely present in the air after treatment in the WWTP's. For all three WWTP's, phenol was 100% eliminated from the wastewater by stripping. Adding a primary sedimentation did not influence the amount of elimination, but only the location of elimination. Circa 17% of phenol was eliminated by volatilization in the sedimentation system using a sedimentation system with a depth of 1 m.

All mercury (as  $HgCl_2$ ) and most of the monoethyleneglycol (90-95% in water and 5-10% biodegraded) and polyoxyethylene oleyl amine (98% in water, 2% via surplus sludge) will be present in the water after treatment in WWTP's.

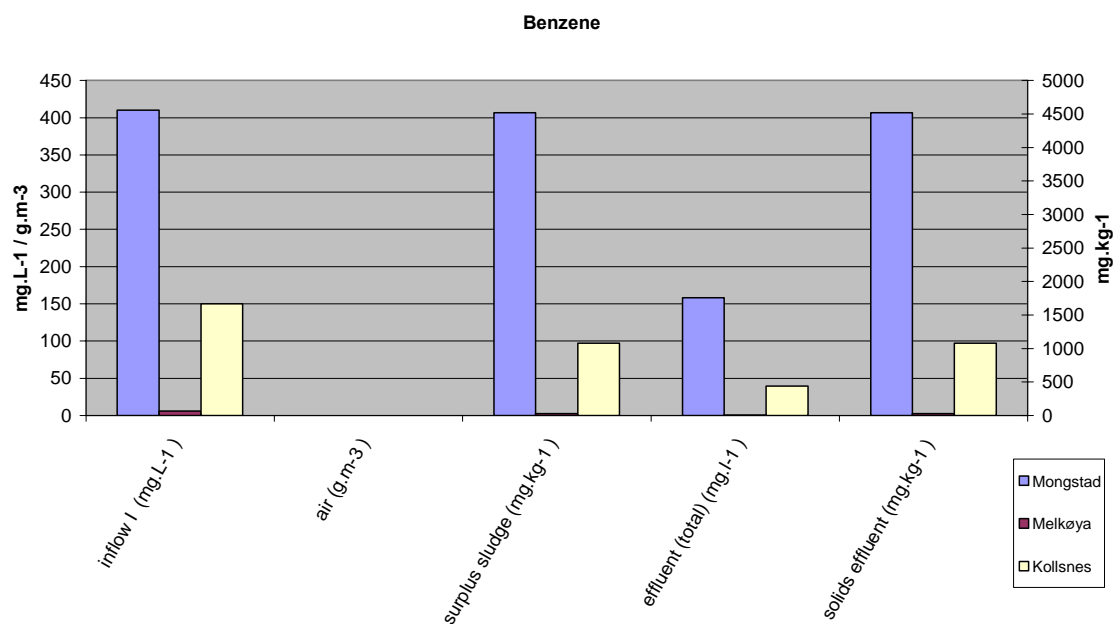


Figure 8 Comparison of benzene concentrations between the three WWTPs (6-box)

Concentrations of benzene as calculated for each of the three WWTPs are shown in Figure 8. Concentrations in water (mg/l) and air ( $g/m^3$ ) relate to the left axis, concentrations in sludge and solids effluent (mg/kg) relate to the right axis. Benzene concentrations at Mongstad are highest, lowest in Melkøya and intermediate in Kolsnes.

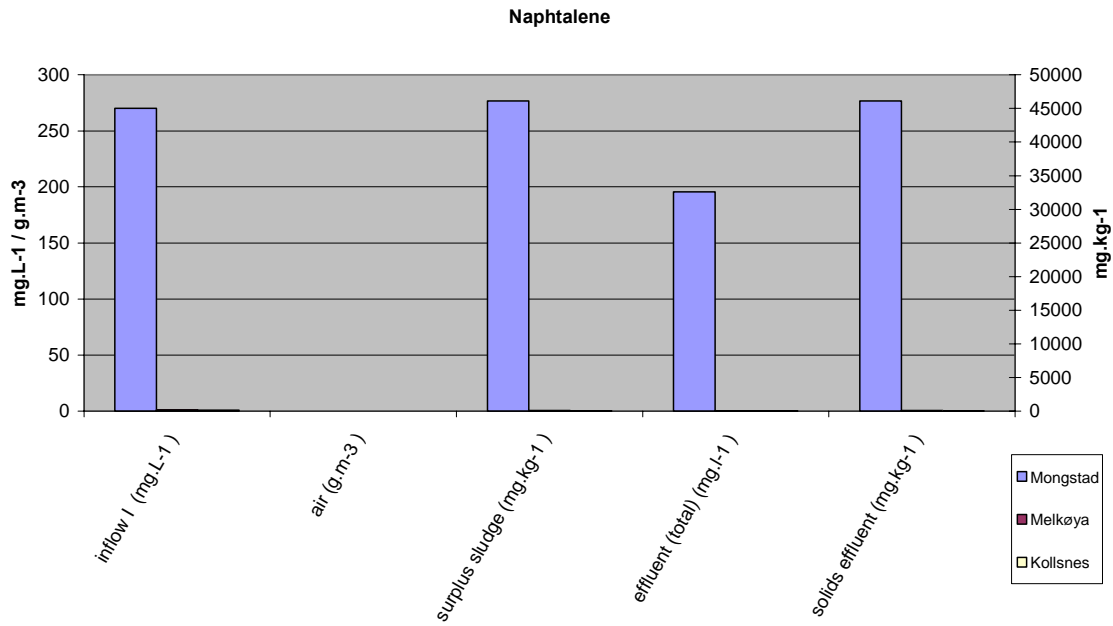


Figure 9 Comparison of naphtalene concentrations between the three WWTPs (6-box)

As can be seen in Figure 9 Naphtalene concentrations are much higher at the Mongstand location than at the other locations.

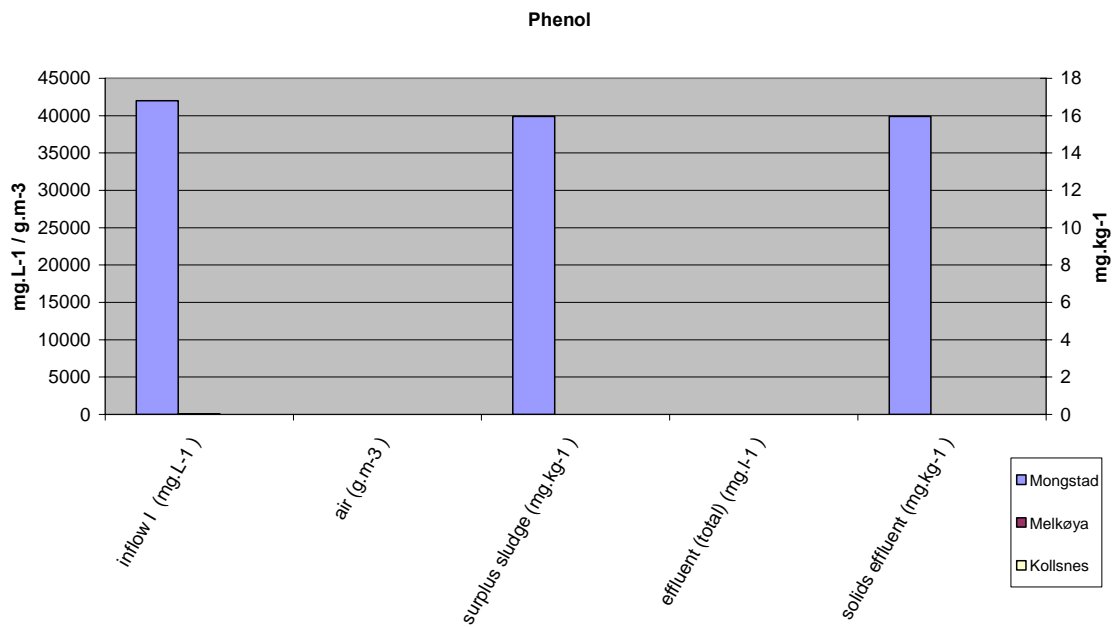


Figure 10 Comparison of phenol concentrations between the three WWTPs (6-box)

Also for Phenol (Figure 10) concentrations are much higher at Mongstand than elsewhere.

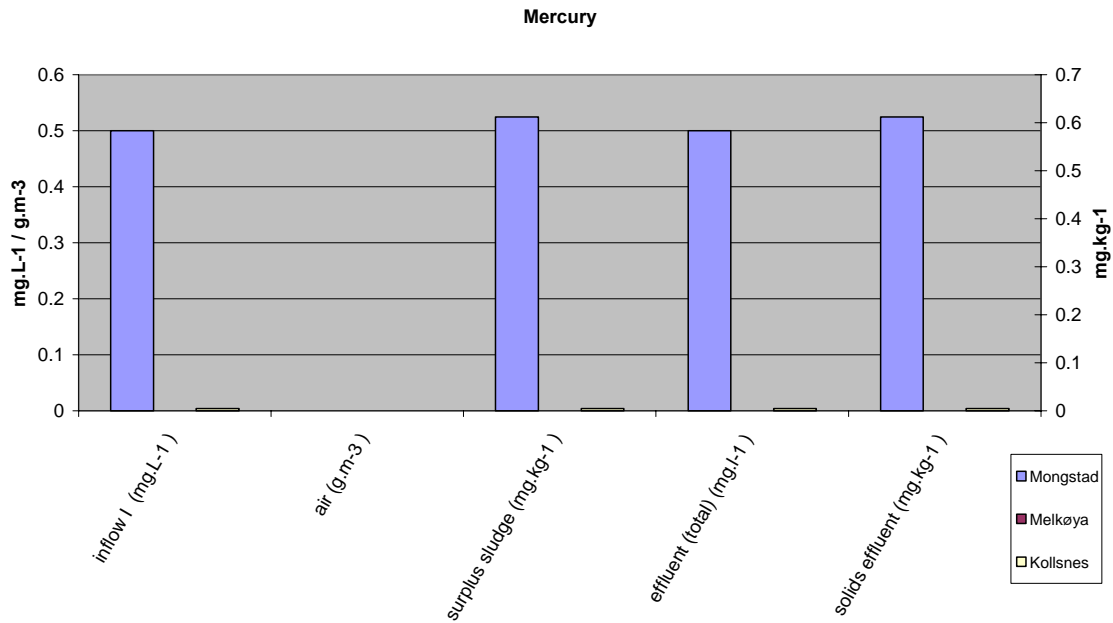


Figure 11 Comparison of mercury concentrations between the three WWTPs (6-box)

A situation apparently repeated for Mercury (Figure 11). This is however deceptive. The 0.5 ml/l inflow concentration for Mercury is generated by the model (by design) when confronted with a 0 (zero) input value.

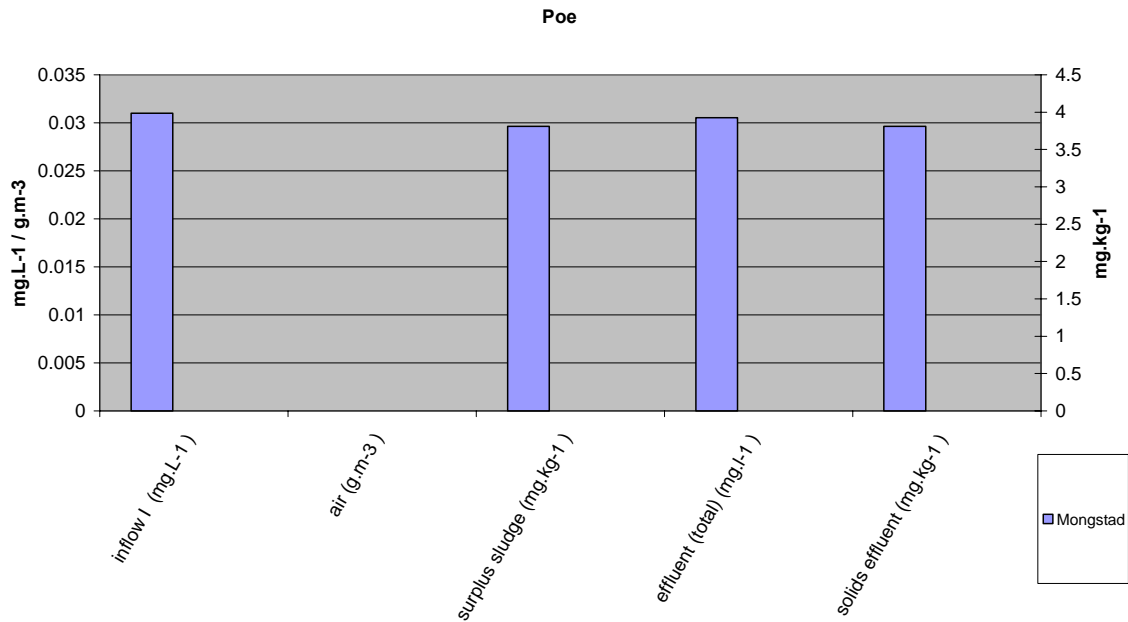


Figure 12 Performance the Mongstad WWTP for polyoxyethylene oleyl amine (6-box)

Polyoxyethylene oleyl amine is only used at Mongstad (Figure 12) almost all of the incoming compound is still present in the effluent.

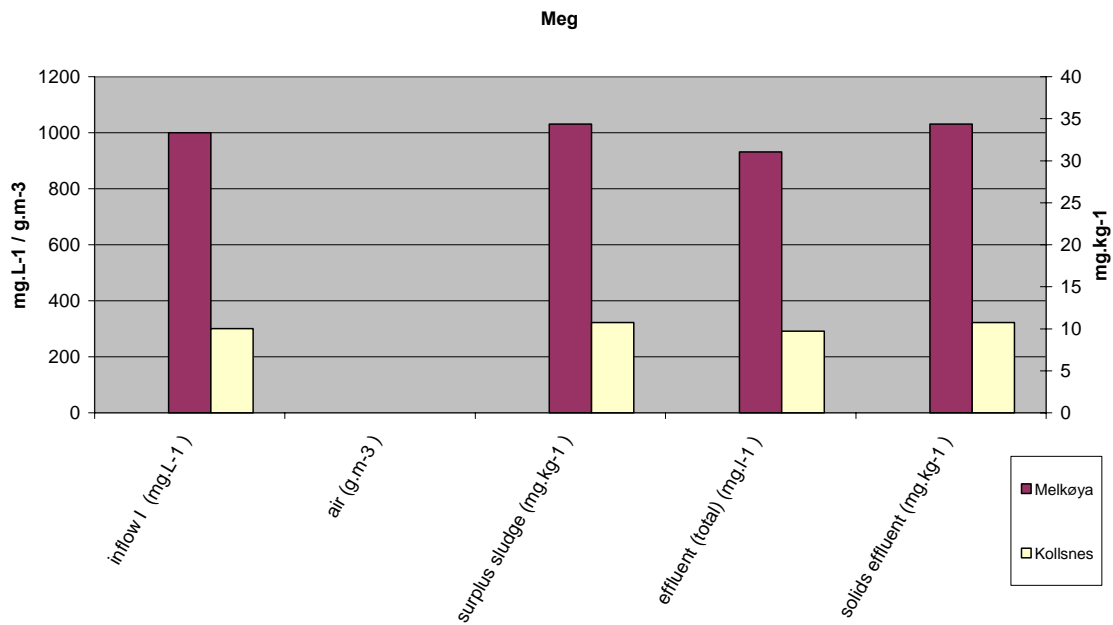


Figure 13 Comparison of monoethyleneglycol concentrations between the two WWTPs Melkøya en Kollsnes where this compound is present in the waste water (6-box)

Monoethyleneglycol (Meg) is used both at Melkøya and Kollsnes (Figure 13) it is not volatile or susceptible to biodegradation (similar to Mercury and Poe), as a result the majority of the incoming compound is still present in the effluent.

## 5 Influence of parameters on the model

### 5.1 Compound related

In total, five compound related parameters (physico-chemical properties) were varied individually using two variations next to the initial or best known value (base case).

The compound related parameters changed included

- molecular weight,
- $K_{ow}$ ,
- vapour pressure,
- solubility and the
- Henry constant (H).

The parameters were varied by setting at a lower value (95%) and at a higher value (105%) compared to the base case.

None of the variations made in the compound related parameters resulted in changes more than 5% in comparison to the base case. In conclusion, changing the compound related parameters does not affect the distribution or elimination of the compounds in the WWTP's beyond the expected change.

As an example the results for varying the value of the Henry constant are shown in Table 5, based on the Mongstad plant and Benzene. As the Henry constant influences volatilisation of the compound, the distribution across the compartments of the model changes accordingly. Also when more of the compound is left in the watercolumn (95% case), the importance of the biodegradation process increases somewhat relative to the base case. The changes found in the calculated concentration of benzene in the effluent are comparable with the changes in the input at about 5% or slightly less.

Table 5 Example calculation results for different values of the Henry constant. Results shown are for Mongstad, Benzene.

	Mo - B	Mo - B - 95%Hc	Mo - B - 105%Hc
<b>Changed parameter</b>			
Henry constant (H) =	557.3	529.4	585.2
<b>Elimination in the aerator (%)</b>			
stripping	48.3	46.4	50.1
biodegradation	6.7	7.0	6.5
total	55.0	53.3	56.6
<b>Elimination in the solids liquid separator (%)</b>			
volatilization	6.2	6.4	6.1
via surplus sludge	0.2	0.2	0.2
total	6.5	6.7	6.3
Total elimination from waste water (%)	61.4	60.0	62.8
Total emission via effluent (%)	38.6	40.0	37.2
% dissolved	38.6	40.0	37.2
% associated	0.0	0.0	0.0
balance	100.0	100.0	100.0
<b>Summary of distribution (%)</b>			
to air	54.5	52.8	56.1
to water	38.6	40.0	37.2
via surplus sludge	0.2	0.2	0.2
degraded	6.7	7.0	6.5
total	100.0	100.0	100.0
<b>Concentrations</b>			
in air (g/m <sup>3</sup> )	0.010	0.010	0.010
in surplus sludge (mg/kg)	4519	4685	4359
in effluent (total) (mg/L)	158	164	153
dissolved (mg/L)	158	164	153
associated (mg/L)	0.14	0.14	0.13
in solids effluent (mg/kg)	4519	4685	4359
<b>Operation of the plant</b>			
Sludge loading rate = (kg BOD/ (kg DWT.d))	0.121	0.121	0.121
HRT = (hr)	13.4	13.4	13.4
SRT = (d)	11.5	11.5	11.5
Aeration mode =	bubble aeration	bubble aeration	bubble aeration
Surplus sludge = (kg DWT/d)	342	342	342

## 5.2 Climate

For the three climate parameters default values were used for determining the base case:

- Air temperature,
- Water temperature,
- Wind speed.

Changes in climate were based on average wind speed and air temperatures given for several locations in Norway ([http://www.windfinder.com/wind-cgi/top\\_surfsports.pl?mode=statistic&country=no](http://www.windfinder.com/wind-cgi/top_surfsports.pl?mode=statistic&country=no)). This would give more realistic calculations for WWTP's in Norway. For speed of wind, the default value of 3 m/s reflects a light breeze, whereas variations used in the calculations reflect moderate breeze (6 m/s) to a fresh breeze (9 m/s). Average air temperatures measured in Norway range from 1-9°C. The default value of 15°C is, therefore, an overestimation of realistic temperatures. Variations calculated for the air and water temperature included 5 and 10°C. The climate parameters were calculated for all three WWTP's and all six compounds.

Varying the temperature did not show a clear difference compared to the base case. Variations in wind speed did show different concentrations of the compound in the air similar for all compounds and WWTP's. A moderate breeze resulted in 50% decrease of the concentration in air and the fresh breeze even decreased the concentration to 33% of the initial value. An illustration of this is given Table 6 for the Melkøya plant and Naphtalene



Table 6 Example calculation results for different values of windspeed. Results shown are for Melkøya, Naphtalene.

		Me - N	Me - N - wind6	Me - N - wind9
<b>Changed parameter</b>				
Windspeed =	(m/s)	3	6	9
<b>Elimination in the aerator (%)</b>				
stripping		33.7	33.7	33.7
biodegradation		26.6	26.6	26.6
total		60.4	60.4	60.4
<b>Elimination in the solids liquid separator (%)</b>				
volatilization		17.5	17.5	17.5
via surplus sludge		1.0	1.0	1.0
total		18.5	18.5	18.5
Total elimination from waste water (%)		78.8	78.8	78.8
Total emission via effluent (%)		21.2	21.2	21.2
% dissolved		21.0	21.0	21.0
% associated		0.2	0.2	0.2
balance		100.0	100.0	100.0
<b>Summary of distribution (%)</b>				
to air		51.2	51.2	51.2
to water		21.2	21.2	21.2
via surplus sludge		1.0	1.0	1.0
degraded		26.6	26.6	26.6
total		100.0	100.0	100.0
<b>Concentrations</b>				
in air	(g/m <sup>3</sup> )	2.1*10 <sup>-06</sup>	1.0*10 <sup>-06</sup>	6.8*10 <sup>-07</sup>
in surplus sludge	(mg/kg)	82.3	82.3	82.3
in effluent (total)	(mg/L)	0.3	0.3	0.3
dissolved	(mg/L)	0.3	0.3	0.3
associated	(mg/L)	2.5*10 <sup>-03</sup>	2.5*10 <sup>-03</sup>	2.5*10 <sup>-03</sup>
in solids effluent	(mg/kg)	82.3	82.3	82.3
<b>Operation of the plant</b>				
Sludge loading rate =	(kg BOD/ (kg DWT.d))	0.013	0.013	0.013
HRT =	(hr)	128.9	128.9	128.9
SRT =	(d)	127.2	127.2	127.2
Aeration mode =		bubble	bubble	bubble
Surplus sludge =	(kg DWT/d)	11.7	11.7	11.7

### 5.3 Sewage

For the sewage related parameters, it was expected that the compounds and their behaviour would be most important to study. Therefore, the five sewage related parameters were differed individually and calculations were performed for all compounds and WWTP's. Sewage related parameters changed included:

- total daily sewage inflow,
- concentration of compound inflow,
- concentration of suspended solids of the raw sewage,
- sludge loading rate and
- type of aeration.

Variations were performed by setting the parameters at a lower value (95%) and at a higher value (105%) compared to the base case. For the sludge loading rate, only seven options are possible for input and therefore, a lower and a higher available value were used for the calculations. The type of aeration was varied between bubble and surface aeration.

Sludge loading rate was dropped from the final analysis based on the changes implemented in version 3.3, the exact SLR is now calculated. It is no longer possible to manipulate the SLR within the model as a separate parameter. Changing either total daily sewage inflow or the volume of the aerator basin, will result in a different SLR being used in the calculations.

Changing the total daily sewage inflow did not change distributions of compounds, or the effectiveness of the WWTP. The results for total daily sewage flow are shown in Table 7 for Mercury in the Kolsness plant. The only influence shown was in the operation of the plant, where the amount of surplus sludge changed with a percentage similar to the change in input. Adding a primary sedimentation system in the WWTP showed a shift in the results where the changed inflow was visible in the primary sludge and not anymore in the surplus sludge.

Variations made for the compound inflow showed similar changes in the concentrations in air, sludge and effluent. It did not affect the operation of the plant or the distributions. Including a primary sedimentation system had no effect.

Phenol was influenced by variations of the concentration suspended solids in raw sewage, although for Melkoya and Kollsness the absolute values were very low. Sample results for phenol and the Mongstad plant are available in Table 8. Similarly, changed percentages were noticed for concentrations in sludge and effluent. For other compounds, no change was detected in the output after varying the concentration suspended solids. Including a primary sedimentation system, resulted in changes for the primary sludge for all compounds.

Non-volatile compounds are not affected by changing the aeration from bubble aeration into surface aeration. The volatile compounds benzene, naphthalene and phenol are affected. Phenol, which has the highest Henry constant (H), shows a decrease in effectiveness of the stripping in the plant with a decrease of 4%. Benzene and naphthalene on the other hand, show an increase in efficiency of the stripping process in the plant of circa 35% and 12% respectively. These changes are reflected on the percentage biodegraded and volatilized in the plant as less substance was available for these processes. A small decrease was noticeable for benzene and naphthalene, but in total circa 28% more compound was removed for benzene and 10% more for naphthalene. Similar changes were visible in the distribution of the compounds. In the case of phenol, less ends up in the air and more goes towards the outflowing water, vice versa for benzene and naphthalene. Besides changes in distribution and efficiency of the plant, changes in the output of the concentrations in air, sludge and effluent are visible. See Table 9 for results from calculations switching the aeration mode between bubble and surface aeration for the Melkøya plant and the compounds benzene and phenol.

Table 7 Example calculation results for different values of total daily sewage flow. Results shown are for Kolsness, Mercury.

	Ko - M	Ko - M- 95%Q1	Ko - M- 105%Q1
<b>Changed parameter</b>			
Sewage flow daily total l = (m <sup>3</sup> /d)	120000	114000	126000
<b>Elimination in the aerator (%)</b>			
stripping	0.002	0.002	0.002
biodegradation	0.000	0.000	0.000
total	0.002	0.002	0.002
<b>Elimination in the solids liquid separator (%)</b>			
volatilization	0.000	0.000	0.000
via surplus sludge	0.018	0.018	0.018
total	0.019	0.019	0.019
Total elimination from waste water (%)	0.02	0.02	0.02
Total emission via effluent (%)	99.98	99.98	99.98
% dissolved	99.98	99.98	99.98
% associated	0.0	0.0	0.0
balance	100.0	100.0	100.0
<b>Summary of distribution (%)</b>			
to air	0.00	0.00	0.00
to water	99.98	99.98	99.98
via surplus sludge	0.02	0.02	0.02
degraded	0.00	0.00	0.00
total	100.00	100.00	100.00
<b>Concentrations</b>			
in air (g/m <sup>3</sup> )	6.3*10 <sup>-13</sup>	6.3*10 <sup>-13</sup>	6.3*10 <sup>-13</sup>
in surplus sludge (mg/kg)	0.005	0.005	0.005
in effluent (total) (mg/L)	0.004	0.004	0.004
dissolved (mg/L)	0.004	0.004	0.004
associated (mg/L)	1.4*10 <sup>07</sup>	1.4*10 <sup>07</sup>	1.4*10 <sup>07</sup>
in solids effluent (mg/kg)	0.005	0.005	0.005
<b>Operation of the plant</b>			
Sludge loading rate = (kg BOD/ (kg DWT.d))	0.032	0.031	0.034
HRT = (hr)	50.2	52.8	47.8
SRT = (d)	46.4	49.0	44.1
Aeration mode =	bubble aeration	bubble aeration	bubble aeration
Surplus sludge = (kg DWT/d)	18.0	17.1	19.0

Table 8 Example calculation results for different values of the set of raw sewage parameters of input solids and carbon content of suspended solids. Results shown are for Mongstad, Phenol.

	Mo - Ph	Mo - Ph- 95%[SS]	Mo - Ph- 105%[SS]
<b>Changed parameter</b>			
Input solids in raw sewage = (kg <sub>dwt</sub> /(PE.d))	0.01	0.0095	0.0105
C susp solids raw sewage = (kg <sub>dwt</sub> /m <sup>3</sup> )	0.05	0.0475	0.0525
<b>Elimination in the aerator (%)</b>			
stripping	100.0	100.0	100.0
biodegradation	0.0	0.0	0.0
total	100.0	100.0	100.0
<b>Elimination in the solids liquid separator (%)</b>			
volatilization	0.0	0.0	0.0
via surplus sludge	0.0	0.0	0.0
total	0.0	0.0	0.0
Total elimination from waste water (%)	100.0	100.0	100.0
Total emission via effluent (%)	0.0	0.0	0.0
% dissolved	0.0	0.0	0.0
% associated	0.0	0.0	0.0
balance	100.0	100.0	100.0
<b>Summary of distribution (%)</b>			
to air	100.0	100.0	100.0
to water	0.0	0.0	0.0
via surplus sludge	0.0	0.0	0.0
degraded	0.0	0.0	0.0
total	100.0	100.0	100.0
<b>Concentrations</b>			
in air (g/m <sup>3</sup> )	1.9	1.9	1.9
in surplus sludge (mg/kg)	32.3	30.7	33.9
in effluent (total) (mg/L)	5.0*10 <sup>-03</sup>	4.7*10 <sup>-03</sup>	5.2*10 <sup>-03</sup>
dissolved (mg/L)	4.0*10 <sup>-03</sup>	3.8*10 <sup>-03</sup>	4.2*10 <sup>-03</sup>
associated (mg/L)	9.7*10 <sup>-04</sup>	9.2*10 <sup>-04</sup>	1.0*10 <sup>-03</sup>
in solids effluent (mg/kg)	32.3	30.7	33.9
<b>Operation of the plant</b>			
Sludge loading rate = (kg BOD/ (kg DWT.d))	0.12	0.12	0.12
HRT = (hr)	13.4	13.4	13.4
SRT = (d)	11.5	11.5	11.5
Aeration mode =	bubble aeration	bubble aeration	bubble aeration
Surplus sludge = (kg DWT/d)	338.1	338.1	338.1

Table 9 Example calculation results for both possible values of the aeration setting. Results shown are for Melkøya, Benzene and Phenol.

	Me - B	Me - B- surfacebubble	Me - Ph	Me - Ph- surfacebubble
<b>Changed parameter</b>				
Bubble or surface aeration: b/s	b	s	b	s
<b>Elimination in the aerator (%)</b>				
stripping	46.1	69.7	100.0	94.5
biodegradation	31.7	17.8	0.0	1.6
total	77.8	87.5	100.0	96.1
<b>Elimination in the solids liquid separator (%)</b>				
volatilization	12.1	6.8	0.0	2.2
via surplus sludge	0.1	0.0	0.0	0.0
total	12.2	6.9	0.0	2.2
Total elimination from waste water (%)	90.0	94.4	100.0	98.3
Total emission via effluent (%)	10.0	5.6	0.0	1.7
% dissolved	10.0	5.6	0.0	1.7
% associated	0.0	0.0	0.0	0.0
balance	100.0	100.0	100.0	100.0
<b>Summary of distribution (%)</b>				
to air	58.2	76.5	100.0	96.7
to water	10.0	5.6	0.0	1.7
via surplus sludge	0.1	0.0	0.0	0.0
degraded	31.7	17.8	0.0	1.6
total	100.0	100.0	100.0	100.0
<b>Concentrations</b>				
in air (g/m <sup>3</sup> )	1.2*10 <sup>05</sup>	0.0	6.7*10 <sup>05</sup>	0.0
in surplus sludge (mg/kg)	28.6	16.1	1.2*10 <sup>05</sup>	4.7
in effluent (total) (mg/L)	0.6	0.3	7.8*10 <sup>09</sup>	0.3
dissolved (mg/L)	0.6	0.3	7.4*10 <sup>09</sup>	0.3
associated (mg/L)	0.0	0.0	3.7*10 <sup>-10</sup>	0.0
in solids effluent (mg/kg)	28.6	16.1	1.2*10 <sup>05</sup>	4.7
<b>Operation of the plant</b>				
Sludge loading rate = (kg BOD/ (kg DWT.d))	0.013	0.013	0.013	0.013
HRT = (hr)	128.9	128.9	128.9	128.9
SRT = (d)	127.2	127.2	127.2	127.2
Aeration mode =	bubble	surface	bubble	surface
Surplus sludge = (kg DWT/d)	11.7	11.7	11.7	11.7

## 5.4 Biodegradation

Values for biodegradation were provided by StatoilHydro for the compounds. These values were varied using two alternatives next to the initial or best known value (base case). Additionally the temperature dependence was either set to 'no (default value)' or to 'yes', while the temperature of the water was changed as described earlier for the climate parameters.

The model does not appear to be sensitive for biodegradation in these cases. Only limited changes are shown when the combination of factors is set on most extreme values (varied biodegradation, lowest temperature and temperature dependence set to yes). Table 10 shows model results for the Kolsness plant and naphthalene.

Table 10 Example calculation results for different settings influencing biodegradation. Results shown are for Kolsness, Naphtalene.

		<b>Ko - N</b>	<b>Ko - N- 95%k biodeg</b>	<b>Ko - N- 105%k biodeg</b>	<b>Ko - N- 95%k biodeg T5</b>
<b>Changed parameter</b>					
T water =	(°C)	15	15	15	5.0
Temperature dependence (y/n)		n	n	n	y
k biodeg1 =	(1/d)	0.005833	0.005542	0.006125	0.005542
<b>Elimination in the aerator (%)</b>					
stripping		30.3	30.6	30.1	33.8
biodegradation		15.3	14.6	15.9	5.7
total		45.6	45.2	46.0	39.5
<b>Elimination in the solids liquid separator (%)</b>					
volatilization		3.4	3.5	3.4	3.8
via surplus sludge		1.7	1.7	1.7	1.9
total		5.1	5.2	5.1	5.7
Total elimination from waste water (%)		50.8	50.4	51.1	45.2
Total emission via effluent (%)		49.1	49.6	48.9	54.8
% dissolved		48.9	49.3	48.5	54.5
% associated		0.3	0.3	0.3	0.4
balance		100.0	100.0	100.0	100.0
<b>Summary of distribution (%)</b>					
to air		33.8	34.0	33.5	37.6
to water		49.2	49.6	48.9	54.8
via surplus sludge		1.7	1.7	1.7	1.9
degraded		15.3	14.6	15.9	5.7
total		100.0	100.0	100.0	100.0
<b>Concentrations</b>					
in air	(g/m3)	1.4*10 <sup>-06</sup>	1.4*10 <sup>-06</sup>	1.4*10 <sup>-06</sup>	1.5*10 <sup>-06</sup>
in surplus sludge	(mg/kg)	68.4	68.9	67.9	76.2
in effluent (total)	(mg/L)	0.3	0.3	0.3	0.3
dissolved	(mg/L)	0.3	0.3	0.3	0.3
associated	(mg/L)	0.0	0.0	0.0	0.0
in solids effluent	(mg/kg)	68.4	68.9	67.9	76.2
<b>Operation of the plant</b>					
Sludge loading rate =	(kg BOD/ (kg DWT.d))	0.032	0.032	0.032	0.032
HRT =	(hr)	50.2	50.2	50.2	50.2
SRT =	(d)	46.4	46.4	46.4	46.4
Aeration mode =		bubble aeration	bubble aeration	bubble aeration	bubble aeration
Surplus sludge =	(kg DWT/d)	18.0	18.0	18.0	18.0

## 5.5 Extra: size of the primary settler

As a primary settler was not included in the WWTP's, but shown to be an improvement as described by Struijs (1996) a small system was included in the 9-box, throughout all previous calculations. Influence of the size of a primary settler, however, was not included. Therefore, extra calculations with changing settler size were performed.

Varying the size of the primary settler shows changes in both the distribution as the efficiency of the plant, resulting in different output concentrations for the volatile compounds (phenol, benzene and naphthalene). A shallow system allows high volatilization in the settler, while deep systems do not affect the distribution or the efficiency of the plant.



## 6 Conclusions and recommendations

The final conclusion of the sensitivity analysis is that SimpleTreat.i does not have a specific sensitivity towards any of the parameters. For all investigated cases the resulting change in the output closely matches with the applied change to the input parameters expressed as a percentage. When considering sensitivity, changing an input value by a single percentage point will have a larger effect when it is a larger number. From this point of view more confidence regarding the larger numbers being used as input to the model may seem desirable.

However this does touch on the next point to consider when working with models: uncertainty.

Uncertainty is often larger for smaller numbers (certainly on a relative scale) and/or for quantities that are more difficult to measure accurately.

For a given plant sewage flows and compound concentrations are likely to qualify as values that can be known accurately and with a high degree of certainty. A provision that has to be made here is that a reliable technique for measuring the compound needs to exist. Compound characteristics such as  $K_{ow}$ , vapour pressure and biodegradation values fall into the category of values that are harder to quantify.

## 7 Quality Assurance

IMARES utilises an ISO 9001:2000 certified quality management system (certificate number: 08602-2004-AQ-ROT-RvA). This certificate is valid until 15 December 2009. The organisation has been certified since 27 February 2001. The certification was issued by DNV Certification B.V. Furthermore, the chemical laboratory of the Environmental Division has NEN-AND-ISO/IEC 17025:2005 accreditation for test laboratories with number L097. This accreditation is valid until 27 March 2009 and was first issued on 27 March 1997. Accreditation was granted by the Council for Accreditation, with the last inspection being held on the 5<sup>th</sup> of October 2007.

## References

EC (2004) European Union System for the Evaluation of Substances 2.0 (EUSES 2.0). Prepared for the European Chemicals Bureau by the National Institute of Public Health and the Environment (RIVM), Bilthoven, The Netherlands (RIVM Report no. 601900005). Available via the European Chemicals Bureau, <http://ecb.jrc.it>

StatOilHydro (2008). Going north Sustainable development 2007. StatoilHydro ASA, Oslo, Norway

Struijs, J. (1996). SimpleTreat 3.0: a model to predict the distribution and elimination of chemicals by sewage treatment plants. RIVM-report no. 719101025, National Institute of Public Health and the Environment (RIVM), Bilthoven, The Netherlands

Wal, J.T. van der (2008). SimpleTreat 3.1 Industrial User Manual. TNO-IMARES Report number 08.010, TNO-IMARES, Den Helder, The Netherlands

# Justification

Rapport C058/09  
Project Number: 4305100201

The scientific quality of this report has been peer reviewed by the a colleague scientist and the head of the department of Wageningen IMARES.

Approved: Dr. N.H.B.M. Kaag  
Scientist

Signature:

A handwritten signature in blue ink that reads "Maas Kaag".

Date:

16-06-2009

Approved: J.H.M. Schobben MSc  
Head of department Environment

Signature:

A handwritten signature in blue ink that reads "J.H.M. Schobben".

Date:

16-06-2009

Number of copies: 5  
Number of pages 36 excluding appendices  
Number of tables: 10  
Number of graphs: 13  
Number of appendix attachments: 2

# Annex A: Listing of sensitivity analysis results

Number of pages: 27

## **Coding of cases**

### **Plants: (part 1) :**

Mo = Mongstad, Me = Melkoya, Ko = Kollsnes

### **Compound: (part 2) :**

B = Benzene, N = Naphtalene, Ph = Phenol, M = Mercury (Hg), Poe = Polyoxyethylene oleyl amine

### **Parameters: (part 3)**

MM = Molecular weight, Kow = Kow (octanol-water partitioning coefficient), Vp = vapour pressure,

Sol = Solubility, Hc = Henry constant,

Txair = Air temperature, Txwater = Water temperature, windx = Wind speed

Q1 = Sewage flow daily total, [c]inflow= compound concentration in inflow, SLR = sludge loading rate,

[SS] = concentration suspended solids in raw sewage, surfacebubble = aeration type (surface or bubble)

k biodeg = biodegradation rate constant

PSS = primary settling basin size

Table Identifier >	Characterisation of the chemical			Emission scenario			Sewage			Biodegradation			
	Name compound = (C)	Molecular weight = g mol <sup>-1</sup>	Vapour pressure = Pa	Kow = log <sub>10</sub> K <sub>ow</sub>	Solubility = mg L <sup>-1</sup>	Henry constant = Pa m <sup>3</sup> mol <sup>-1</sup>	Waste = kg day <sup>-1</sup>	Waste = kg day <sup>-1</sup>	Waste = kg day <sup>-1</sup>	Waste = kg day <sup>-1</sup>	Waste = kg day <sup>-1</sup>	Waste = kg day <sup>-1</sup>	Waste = kg day <sup>-1</sup>
Phase 0: Basis data 3 WWTP (Mongstad, Mølva, Kollarna)													
Mo-B	Benzene	78.11	134.886	9999	1770	557.2875	15	15	15	15	0.0125	0.0125	0.0125
Mo-M	Phenol	94.111	198.12	317	3.04E+12	6.00E-04	15	15	15	15	0.0028167	0.0028167	0.0028167
Mo-M	Mercury (Hg)	200.59	29	48	70000	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-Pow	Phyoxanth/yene oily amine	190	19000	1	0.0264	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-B	Benzene	78.11	135	9999	1770	557.2875	15	15	15	15	0.0125	0.0125	0.0125
Mo-M	Phenol	94.111	198.12	317	3.04E+12	6.00E-04	15	15	15	15	0.0028167	0.0028167	0.0028167
Mo-M	Mercury (Hg)	200.59	29	48	70000	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-Pow	Phyoxanth/yene oily amine	190	19000	1	0.0264	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-M	Mercury (Hg)	200.59	29	48	70000	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-M	Mercury (Hg)	200.59	29	48	70000	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-Pow	Phyoxanth/yene oily amine	190	19000	1	0.0264	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-B	Benzene	78.11	135	9999	1770	557.2875	15	15	15	15	0.0125	0.0125	0.0125
Mo-N	Naphtalene	128.19	1950	12	31.7	46.6095	15	15	15	15	0.0125	0.0125	0.0125
Mo-M	Mercury (Hg)	200.59	29	48	70000	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-Pow	Phyoxanth/yene oily amine	190	19000	1	0.0264	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-B	Benzene	78.11	135	9999	1770	557.2875	15	15	15	15	0.0125	0.0125	0.0125
Mo-N	Naphtalene	128.19	1950	12	31.7	46.6095	15	15	15	15	0.0125	0.0125	0.0125
Mo-M	Mercury (Hg)	200.59	29	48	70000	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-Pow	Phyoxanth/yene oily amine	190	19000	1	0.0264	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-B	Benzene	78.11	135	9999	1770	557.2875	15	15	15	15	0.0125	0.0125	0.0125
Mo-N	Naphtalene	128.19	1950	12	31.7	46.6095	15	15	15	15	0.0125	0.0125	0.0125
Mo-M	Mercury (Hg)	200.59	29	48	70000	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-Pow	Phyoxanth/yene oily amine	190	19000	1	0.0264	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-B	Benzene	78.11	135	9999	1770	557.2875	15	15	15	15	0.0125	0.0125	0.0125
Mo-N	Naphtalene	128.19	1950	12	31.7	46.6095	15	15	15	15	0.0125	0.0125	0.0125
Mo-M	Mercury (Hg)	200.59	29	48	70000	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-Pow	Phyoxanth/yene oily amine	190	19000	1	0.0264	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-B	Benzene	78.11	135	9999	1770	557.2875	15	15	15	15	0.0125	0.0125	0.0125
Mo-N	Naphtalene	128.19	1950	12	31.7	46.6095	15	15	15	15	0.0125	0.0125	0.0125
Mo-M	Mercury (Hg)	200.59	29	48	70000	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-Pow	Phyoxanth/yene oily amine	190	19000	1	0.0264	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-B	Benzene	78.11	135	9999	1770	557.2875	15	15	15	15	0.0125	0.0125	0.0125
Mo-N	Naphtalene	128.19	1950	12	31.7	46.6095	15	15	15	15	0.0125	0.0125	0.0125
Mo-M	Mercury (Hg)	200.59	29	48	70000	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-Pow	Phyoxanth/yene oily amine	190	19000	1	0.0264	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-B	Benzene	78.11	135	9999	1770	557.2875	15	15	15	15	0.0125	0.0125	0.0125
Mo-N	Naphtalene	128.19	1950	12	31.7	46.6095	15	15	15	15	0.0125	0.0125	0.0125
Mo-M	Mercury (Hg)	200.59	29	48	70000	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-Pow	Phyoxanth/yene oily amine	190	19000	1	0.0264	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-B	Benzene	78.11	135	9999	1770	557.2875	15	15	15	15	0.0125	0.0125	0.0125
Mo-N	Naphtalene	128.19	1950	12	31.7	46.6095	15	15	15	15	0.0125	0.0125	0.0125
Mo-M	Mercury (Hg)	200.59	29	48	70000	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-Pow	Phyoxanth/yene oily amine	190	19000	1	0.0264	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-B	Benzene	78.11	135	9999	1770	557.2875	15	15	15	15	0.0125	0.0125	0.0125
Mo-N	Naphtalene	128.19	1950	12	31.7	46.6095	15	15	15	15	0.0125	0.0125	0.0125
Mo-M	Mercury (Hg)	200.59	29	48	70000	6.00E-04	15	15	15	15	0.01	0.01	0.01
Mo-Pow	Phyoxanth/yene oily amine	190	19000	1	0.0264	6.00E-04	15	15	15	15	0.01	0.01	0.01

Table Identifier >	input	input	input	input	input	input	input	input	input	input	input	input	output	output	output	output	output	output							
Case Identifier	Name compound = (C)	Height air column = (m)	Fraction of air average = (kg/L)	Fraction of BOD in row average = (g BOD PE-1-h)	Depth aerator = (m)	Oxygen concentration = (mg/L)	Aeration rate = (1.3E-05 m/s-h)	Carbonaceous BOD = (kg/m <sup>3</sup> )	Fraction of solids = (kg/m <sup>3</sup> )	Depth = (m)	C-avg solids = (kg/m <sup>3</sup> )	Function of solids = (kg/m <sup>3</sup> )	Density of solids = (kg/L)	Elimination in the aerator (stripping)	Elimination in the solids liquid separator (volatilization)	Elimination in the solids liquid separator (biodegradation)	Total emission via effluent (% dissolved, % associated, % dissolved + associated)	Summary of distribution (to air, to water, surplus, degraded, total)							
Phase 0 - Basis case 3 WWTP (Mongstad, Malloya, Kolli)	Mo-B - 95%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	48.3	6.7	50.0	38.6	0.0	100.0	54.5	38.6	0.2	6.7	100.0	
	Mo-N - 95%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	106	6.2	168	72.4	71.9	0.5	100.0	186	72.4	2.6	6.2	100.0
	Mo-Ph - 95%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	1000	0.0	1000	0.0	0.0	0.0	100.0	1000	0.0	0.0	0.0	100.0
	Mo-M - 95%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	100.0
	Mo-Pe - 95%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	100.0
	Mo-B - 105%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	48.3	6.7	50.0	38.6	0.0	100.0	54.5	38.6	0.2	6.7	100.0	
	Mo-N - 105%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	106	6.2	168	72.4	71.9	0.5	100.0	186	72.4	2.6	6.2	100.0
	Mo-Ph - 105%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	1000	0.0	1000	0.0	0.0	0.0	100.0	1000	0.0	0.0	0.0	100.0
	Mo-M - 105%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	100.0
	Mo-Pe - 105%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	100.0
	Mo-B - 95%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	48.3	6.7	50.0	38.6	0.0	100.0	54.5	38.6	0.2	6.7	100.0	
	Mo-N - 95%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	106	6.2	168	72.4	71.9	0.5	100.0	186	72.4	2.6	6.2	100.0
	Mo-Ph - 95%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	1000	0.0	1000	0.0	0.0	0.0	100.0	1000	0.0	0.0	0.0	100.0
	Mo-M - 95%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	100.0
	Mo-Pe - 95%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	100.0
	Mo-B - 105%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	48.3	6.7	50.0	38.6	0.0	100.0	54.5	38.6	0.2	6.7	100.0	
	Mo-N - 105%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	106	6.2	168	72.4	71.9	0.5	100.0	186	72.4	2.6	6.2	100.0
	Mo-Ph - 105%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	1000	0.0	1000	0.0	0.0	0.0	100.0	1000	0.0	0.0	0.0	100.0
	Mo-M - 105%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	100.0
	Mo-Pe - 105%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	100.0
	Mo-B - 95%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	48.3	6.7	50.0	38.6	0.0	100.0	54.5	38.6	0.2	6.7	100.0	
	Mo-N - 95%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	106	6.2	168	72.4	71.9	0.5	100.0	186	72.4	2.6	6.2	100.0
	Mo-Ph - 95%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	1000	0.0	1000	0.0	0.0	0.0	100.0	1000	0.0	0.0	0.0	100.0
	Mo-M - 95%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	100.0
	Mo-Pe - 95%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	100.0
	Mo-B - 105%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	48.3	6.7	50.0	38.6	0.0	100.0	54.5	38.6	0.2	6.7	100.0	
	Mo-N - 105%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	106	6.2	168	72.4	71.9	0.5	100.0	186	72.4	2.6	6.2	100.0
	Mo-Ph - 105%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	1000	0.0	1000	0.0	0.0	0.0	100.0	1000	0.0	0.0	0.0	100.0
	Mo-M - 105%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	100.0
	Mo-Pe - 105%Kow	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	4.15	0.00013	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	100.0

Input		output		output		output		output		output		
Table Identifier >		Concentrations		in effluent		in air		in sludge		Operation of the plant without primary effluent		
Table Identifier	Name compound = (C)	in air sludge (total) 0 m-3	in air sludge (total) 0 m-3	in effluent (total) mg/L	in effluent (total) mg/L	in air sludge (total) mg/L	in air sludge (total) mg/L	in sludge (total) mg/kg-d	in sludge (total) mg/kg-d	Bubble leading time = log BOD log (initial/d) h	Surplus sludge = SRT * (C) kg dry weight/d	Total wastewater = mg/d
<b>Phase 0: Basis date 3 WWTP (Municipal, Mullya, Kollit)</b>												
Mo-B	Benzene	0.0	4518.7	158.3	198.2	1.4	4610.2	0.1	15.4	13.4	11.5 bubble aeration	3381
Mo-B	Naphtalene	0.0	4518.7	158.3	198.2	1.4	4610.2	0.1	15.4	13.4	11.5 bubble aeration	3381
Mo-B	Phend	1.9	32.3	0.0	0.0	0.0	32.3	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-M	Mercury (Hg)	0.0	0.6	0.5	0.5	0.0	0.6	0.0	0.6	11.5	11.5 bubble aeration	3381
Mo-Pse	Phyoxathylene oliv amine	0.0	3.8	0.0	0.0	0.0	3.8	0.0	3.8	13.4	11.5 bubble aeration	3381
Mo-B	Benzene	0.0	28.6	0.6	0.6	0.0	28.6	0.0	28.6	0.013	128.9	11.7
Mo-B	Naphtalene	0.0	89.5	0.3	0.3	0.0	89.5	0.0	89.5	0.013	128.9	11.7
Mo-B	Phend	0.0	46.7	0.0	0.0	0.0	46.7	0.0	46.7	0.013	128.9	11.7
Mo-M	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.013	128.9	11.7
Mo-M	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.013	128.9	11.7
Mo-Meg	Monocethin/methylol	0.0	33.1	898.8	898.8	0.0	33.1	0.032	50.2	0.032	50.2	11.7
Ko-B	Benzene	0.0	1078.9	339.9	39.7	0.0	1078.9	0.032	50.2	0.032	50.2	18.0
Ko-N	Naphtalene	0.0	68.4	0.3	0.3	0.0	68.4	0.032	50.2	0.032	50.2	18.0
Ko-N	Phend	0.0	0.0	0.0	0.0	0.0	0.0	0.032	50.2	0.032	50.2	18.0
Ko-M	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.032	50.2	0.032	50.2	18.0
Ko-Meg	Monocethin/methylol	0.0	10.6	287.1	287.1	0.0	10.6	0.032	50.2	0.032	50.2	18.0
<b>Phase 1: Compound filtered</b>												
Mo-B	Benzene	0.0	4518.7	158.3	198.2	1.4	4610.2	0.1	15.4	13.4	11.5 bubble aeration	3381
Mo-N	-95%AMM	0.0	4610.2	198.4	198.1	1.4	4610.2	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-Ph	-95%AMM	1.9	32.3	0.0	0.0	0.0	32.3	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-M	-95%AMM	0.0	0.6	0.5	0.5	0.0	0.6	0.0	0.6	13.4	11.5 bubble aeration	3381
Mo-Pse	-95%AMM	0.0	3.9	0.0	0.0	0.0	3.9	0.0	3.9	13.4	11.5 bubble aeration	3381
Mo-B	-105%AMM	0.0	4518.7	158.3	198.2	1.4	4610.2	0.1	15.4	13.4	11.5 bubble aeration	3381
Mo-Ph	-105%AMM	1.9	32.3	0.0	0.0	0.0	32.3	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-M	-105%AMM	0.0	0.6	0.5	0.5	0.0	0.6	0.0	0.6	13.4	11.5 bubble aeration	3381
Mo-Pse	-105%AMM	0.0	3.8	0.0	0.0	0.0	3.8	0.0	3.8	13.4	11.5 bubble aeration	3381
Mo-B	-95%Kow	0.0	4335.2	158.3	198.2	1.4	4335.2	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-N	-105%Kow	0.0	4335.2	198.6	198.3	1.4	4335.2	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-Ph	-95%Kow	1.9	32.3	0.0	0.0	0.0	32.3	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-M	-95%Kow	0.0	0.6	0.5	0.5	0.0	0.6	0.0	0.6	13.4	11.5 bubble aeration	3381
Mo-Pse	-95%Kow	0.0	3.6	0.0	0.0	0.0	3.6	0.0	3.6	13.4	11.5 bubble aeration	3381
Mo-B	-105%Kow	0.0	4700.4	158.3	198.1	1.4	4700.4	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-N	-105%Kow	0.0	4789.0	195.2	198.8	1.4	4789.0	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-Ph	-95%Kow	1.9	32.3	0.0	0.0	0.0	32.3	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-M	-95%Kow	0.0	0.6	0.5	0.5	0.0	0.6	0.0	0.6	13.4	11.5 bubble aeration	3381
Mo-Pse	-95%Kow	0.0	3.9	0.0	0.0	0.0	3.9	0.0	3.9	13.4	11.5 bubble aeration	3381
Mo-B	-95%Vp	0.0	4518.7	158.3	198.2	1.4	4518.7	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-N	-105%Vp	0.0	4610.2	195.4	194.1	1.4	4610.2	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-Ph	-95%Vp	1.9	32.3	0.0	0.0	0.0	32.3	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-M	-95%Vp	0.0	0.6	0.5	0.5	0.0	0.6	0.0	0.6	13.4	11.5 bubble aeration	3381
Mo-Pse	-95%Vp	0.0	3.8	0.0	0.0	0.0	3.8	0.0	3.8	13.4	11.5 bubble aeration	3381
Mo-B	-105%Vp	0.0	4518.7	158.3	198.2	1.4	4518.7	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-N	-105%Vp	0.0	4610.2	195.4	194.1	1.4	4610.2	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-Ph	-95%Vp	1.9	32.3	0.0	0.0	0.0	32.3	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-M	-95%Vp	0.0	0.6	0.5	0.5	0.0	0.6	0.0	0.6	13.4	11.5 bubble aeration	3381
Mo-Pse	-95%Vp	0.0	3.8	0.0	0.0	0.0	3.8	0.0	3.8	13.4	11.5 bubble aeration	3381
Mo-B	-95%SdI	0.0	4518.7	158.3	198.2	1.4	4518.7	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-N	-105%SdI	0.0	4610.2	195.4	194.1	1.4	4610.2	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-Ph	-95%SdI	1.9	32.3	0.0	0.0	0.0	32.3	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-M	-95%SdI	0.0	0.6	0.5	0.5	0.0	0.6	0.0	0.6	13.4	11.5 bubble aeration	3381
Mo-Pse	-95%SdI	0.0	3.8	0.0	0.0	0.0	3.8	0.0	3.8	13.4	11.5 bubble aeration	3381
Mo-B	-105%SdI	0.0	4518.7	158.3	198.2	1.4	4518.7	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-N	-105%SdI	0.0	4610.2	195.4	194.1	1.4	4610.2	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-Ph	-95%SdI	1.9	32.3	0.0	0.0	0.0	32.3	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-M	-95%SdI	0.0	0.6	0.5	0.5	0.0	0.6	0.0	0.6	13.4	11.5 bubble aeration	3381
Mo-Pse	-95%SdI	0.0	3.8	0.0	0.0	0.0	3.8	0.0	3.8	13.4	11.5 bubble aeration	3381
Mo-B	-105%SdI	0.0	4518.7	158.3	198.2	1.4	4518.7	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-N	-105%SdI	0.0	4610.2	195.4	194.1	1.4	4610.2	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-Ph	-95%SdI	1.9	32.3	0.0	0.0	0.0	32.3	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-M	-95%SdI	0.0	0.6	0.5	0.5	0.0	0.6	0.0	0.6	13.4	11.5 bubble aeration	3381
Mo-Pse	-95%SdI	0.0	3.8	0.0	0.0	0.0	3.8	0.0	3.8	13.4	11.5 bubble aeration	3381
Mo-B	-105%Kw	0.0	4335.2	152.7	152.5	1.4	4335.2	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-N	-105%Kw	0.0	4428.4	198.2	198.9	1.4	4428.4	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-Ph	-95%Kw	1.9	32.3	0.0	0.0	0.0	32.3	0.1	13.4	13.4	11.5 bubble aeration	3381
Mo-M	-105%Kw	0.0	0.6	0.5	0.5	0.0	0.6	0.0	0.6	13.4	11.5 bubble aeration	3381
Mo-Pse	-105%Kw	0.0	3.8	0.0	0.0	0.0	3.8	0.0	3.8	13.4	11.5 bubble aeration	3381



Case Identifier	Characterisation of the chemical			Emission scenario			Sewage			C-camp			Biotodegradation				
	Molecular weight =	K <sub>ow</sub> =	K <sub>oc</sub> = [K <sub>ow</sub> × (1 - f)] × 0.001	H <sub>w</sub> (mg/d) =	Wind speed =	W <sub>air</sub> =	default = 15	default = 15	default = 15	default = 0.15 (medium)	default = 0	default = 0	default = 0	default = 0	default = 0	default = 0	default = 0
Name compound =	K <sub>ow</sub> =	K <sub>oc</sub> =	H <sub>w</sub> (mg/d) =	Wind speed =	W <sub>air</sub> =	default = 15	default = 15	default = 15	default = 0.15 (medium)	default = 0	default = 0	default = 0	default = 0	default = 0	default = 0	default = 0	default = 0
Mo-B-T10air	78.11	135	9999	1770	557.2875	10	15	10	410	1150	1150	0.01	0.05 n	0.0125	0	0	0
Mo-N-T10air	128.19	1950	12	31.7	46.6095	10	15	10	270	1150	1150	0.01	0.05 n	0.00683333	0	0	0
Mo-P-T10air	94.111	29	48	7000	3.04E+12	10	15	10	4200	1150	1150	0.01	0.05 n	0.00329167	0	0	0
Mo-N-T5air	100	1000	1	0.0264	6.00E-04	5	15	5	0.031	150	150	0.01	0.05 n	0	0	0	0
Mo-B-T5air	78.11	135	9999	1770	557.2875	5	15	5	410	1150	1150	0.01	0.05 n	0.0125	0	0	0
Mo-N-T5air	128.19	1950	12	31.7	46.6095	5	15	5	270	1150	1150	0.01	0.05 n	0.00683333	0	0	0
Mo-P-T5air	94.111	29	48	7000	3.04E+12	5	15	5	4200	1150	1150	0.01	0.05 n	0.00329167	0	0	0
Mo-N-T10water	100	1000	1	0.0264	6.00E-04	15	10	15	0.031	150	150	0.01	0.05 n	0	0	0	0
Mo-B-T10water	78.11	135	9999	1770	557.2875	15	10	15	410	1150	1150	0.01	0.05 n	0.0125	0	0	0
Mo-N-T10water	128.19	1950	12	31.7	46.6095	15	10	15	270	1150	1150	0.01	0.05 n	0.00683333	0	0	0
Mo-P-T10water	94.111	29	48	7000	3.04E+12	15	10	15	4200	1150	1150	0.01	0.05 n	0.00329167	0	0	0
Mo-N-T5water	100	1000	1	0.0264	6.00E-04	15	10	15	0.031	150	150	0.01	0.05 n	0	0	0	0
Mo-B-T5water	78.11	135	9999	1770	557.2875	15	10	15	410	1150	1150	0.01	0.05 n	0.0125	0	0	0
Mo-N-T5water	128.19	1950	12	31.7	46.6095	15	10	15	270	1150	1150	0.01	0.05 n	0.00683333	0	0	0
Mo-P-T5water	94.111	29	48	7000	3.04E+12	15	10	15	4200	1150	1150	0.01	0.05 n	0.00329167	0	0	0
Mo-N-Wind9	100	1000	1	0.0264	6.00E-04	15	15	15	0.031	150	150	0.01	0.05 n	0	0	0	0
Mo-B-Wind9	78.11	135	9999	1770	557.2875	15	15	15	410	1150	1150	0.01	0.05 n	0.0125	0	0	0
Mo-N-Wind9	128.19	1950	12	31.7	46.6095	15	15	15	270	1150	1150	0.01	0.05 n	0.00683333	0	0	0
Mo-P-Wind9	94.111	29	48	7000	3.04E+12	15	15	15	4200	1150	1150	0.01	0.05 n	0.00329167	0	0	0
Mo-N-Wind9	100	1000	1	0.0264	6.00E-04	15	15	15	0.031	150	150	0.01	0.05 n	0	0	0	0
Mo-B-Wind9	78.11	135	9999	1770	557.2875	15	15	15	410	1150	1150	0.01	0.05 n	0.0125	0	0	0
Mo-N-Wind9	128.19	1950	12	31.7	46.6095	15	15	15	270	1150	1150	0.01	0.05 n	0.00683333	0	0	0
Mo-P-Wind9	94.111	29	48	7000	3.04E+12	15	15	15	4200	1150	1150	0.01	0.05 n	0.00329167	0	0	0
Mo-N-Wind9	100	1000	1	0.0264	6.00E-04	15	15	15	0.031	150	150	0.01	0.05 n	0	0	0	0
Mo-B-Wind9	78.11	135	9999	1770	557.2875	15	15	15	410	1150	1150	0.01	0.05 n	0.0125	0	0	0
Mo-N-Wind9	128.19	1950	12	31.7	46.6095	15	15	15	270	1150	1150	0.01	0.05 n	0.00683333	0	0	0
Mo-P-Wind9	94.111	29	48	7000	3.04E+12	15	15	15	4200	1150	1150	0.01	0.05 n	0.00329167	0	0	0

Table Identifier >	6-box															Elimination in the aeration stripping					Elimination in the solids liquid separator					Total emission via effluent					Summary of distribution										
Case Identifier	Density air average in row = average =	Height air column =	Fraction of air average in row = average =	Depth aeration =	Oxygen transfer concentration =	Aeration rate (L3E-05) =	Carbonaceous solids =	Fraction of carbonaceous solids =	Depth SLS =	C-avg solids =	Function of solids SLS =	Density of solids SLS =	Depth SLS =	Fraction of solids SLS =	Function of solids SLS =	Frictional coefficient of solids =	Depth SLS =	Fraction of solids SLS =	Function of solids SLS =	Depth SLS =	Fraction of solids SLS =	Function of solids SLS =	Frictional coefficient of solids =	Depth SLS =	Fraction of solids SLS =	Function of solids SLS =	Frictional coefficient of solids =	Depth SLS =	Fraction of solids SLS =	Function of solids SLS =	Frictional coefficient of solids =	Depth SLS =	Fraction of solids SLS =	Function of solids SLS =	Frictional coefficient of solids =						
Mo-B-TDair	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	61.6	6.7	55.2	6.2	0.2	6.4	61.6	38.4	0.0	100.0	38.4	0.0	100.0	54.7	38.4	0.2	6.7	100.0	54.7	38.4	0.2	6.7	100.0		
Mo-N-TDair	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	107	6.2	100.0	8.0	0.0	10.0	107	72.3	0.0	100.0	72.3	0.0	100.0	18.7	72.3	0.0	100.0	18.7	72.3	0.0	100.0				
Mo-M-TDair	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	100.0	0.0	100.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	100.0	0.0	100.0	100.0	0.0	100.0	0.0	100.0	100.0	0.0	100.0	0.0	100.0		
Mo-Por-TDair	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	0.0	0.0	0.0	0.0	0.0	0.0	100.0	98.0	0.0	100.0	98.0	0.0	100.0	0.0	100.0	0.0	100.0	98.0	0.0	100.0	0.0	100.0			
Mo-B-TSair	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	48.3	6.7	55.0	6.2	0.2	6.4	48.3	38.6	0.0	100.0	38.6	0.0	100.0	54.5	38.6	0.2	6.7	100.0	54.5	38.6	0.2	6.7	100.0		
Mo-N-TSair	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	108	6.2	168	8.0	0.0	10.0	108	72.4	0.0	100.0	72.4	0.0	100.0	18.6	72.4	0.0	100.0	18.6	72.4	0.0	100.0	18.6	72.4	0.0	100.0
Mo-M-TSair	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	100.0	0.0	100.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	100.0	0.0	100.0	100.0	0.0	100.0	0.0	100.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0
Mo-Por-TSair	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	0.0	0.0	0.0	0.0	0.0	0.0	100.0	98.0	0.0	100.0	98.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0
Mo-B-TDover	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	48.3	6.7	55.0	6.2	0.2	6.4	48.3	38.6	0.0	100.0	38.6	0.0	100.0	54.5	38.6	0.2	6.7	100.0	54.5	38.6	0.2	6.7	100.0		
Mo-N-TDover	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	108	6.2	168	8.0	0.0	10.0	108	72.4	0.0	100.0	72.4	0.0	100.0	18.6	72.4	0.0	100.0	18.6	72.4	0.0	100.0	18.6	72.4	0.0	100.0
Mo-M-TDover	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	100.0	0.0	100.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	100.0	0.0	100.0	100.0	0.0	100.0	0.0	100.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0
Mo-Por-TDover	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	0.0	0.0	0.0	0.0	0.0	0.0	100.0	98.0	0.0	100.0	98.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0
Mo-B-TSover	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	48.3	6.7	55.0	6.2	0.2	6.4	48.3	38.6	0.0	100.0	38.6	0.0	100.0	54.5	38.6	0.2	6.7	100.0	54.5	38.6	0.2	6.7	100.0		
Mo-N-TSover	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	108	6.2	168	8.0	0.0	10.0	108	72.4	0.0	100.0	72.4	0.0	100.0	18.6	72.4	0.0	100.0	18.6	72.4	0.0	100.0	18.6	72.4	0.0	100.0
Mo-M-TSover	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	100.0	0.0	100.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	100.0	0.0	100.0	100.0	0.0	100.0	0.0	100.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0
Mo-Por-TSover	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	0.0	0.0	0.0	0.0	0.0	0.0	100.0	98.0	0.0	100.0	98.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0
Mo-B-TDover	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	48.3	6.7	55.0	6.2	0.2	6.4	48.3	38.6	0.0	100.0	38.6	0.0	100.0	54.5	38.6	0.2	6.7	100.0	54.5	38.6	0.2	6.7	100.0		
Mo-N-TDover	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	108	6.2	168	8.0	0.0	10.0	108	72.4	0.0	100.0	72.4	0.0	100.0	18.6	72.4	0.0	100.0	18.6	72.4	0.0	100.0	18.6	72.4	0.0	100.0
Mo-M-TDover	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	100.0	0.0	100.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	100.0	0.0	100.0	100.0	0.0	100.0	0.0	100.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0
Mo-Por-TDover	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	0.0	0.0	0.0	0.0	0.0	0.0	100.0	98.0	0.0	100.0	98.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0
Mo-B-TSover	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	48.3	6.7	55.0	6.2	0.2	6.4	48.3	38.6	0.0	100.0	38.6	0.0	100.0	54.5	38.6	0.2	6.7	100.0	54.5	38.6	0.2	6.7	100.0		
Mo-N-TSover	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	108	6.2	168	8.0	0.0	10.0	108	72.4	0.0	100.0	72.4	0.0	100.0	18.6	72.4	0.0	100.0	18.6	72.4	0.0	100.0	18.6	72.4	0.0	100.0
Mo-M-TSover	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	100.0	0.0	100.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	100.0	0.0	100.0	100.0	0.0	100.0	0.0	100.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0
Mo-Por-TSover	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	0.0	0.0	0.0	0.0	0.0	0.0	100.0	98.0	0.0	100.0	98.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0
Mo-B-TDover	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	48.3	6.7	55.0	6.2	0.2	6.4	48.3	38.6	0.0	100.0	38.6	0.0	100.0	54.5	38.6	0.2	6.7	100.0	54.5	38.6	0.2	6.7	100.0		
Mo-N-TDover	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	108	6.2	168	8.0	0.0	10.0	108	72.4	0.0	100.0	72.4	0.0	100.0	18.6	72.4	0.0	100.0	18.6	72.4	0.0	100.0	18.6	72.4	0.0	100.0
Mo-M-TDover	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	100.0	0.0	100.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	100.0	0.0	100.0	100.0	0.0	100.0	0.0	100.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0
Mo-Por-TDover	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	0.0	0.0	0.0	0.0	0.0	0.0	100.0	98.0	0.0	100.0	98.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0	0.0	100.0
Mo-B-TSover	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.972656	0.03	0.37	1.3	6.4	48.3	6.7	55.0	6.2	0.2	6.4	48.3	38.6	0.0	100.0	38.6														

Table Identifier >	input	output	output	output	output	output	output	output	output	output	
Case Identifier	Name compound =	in air	in effluent	in effluent	in effluent	in effluent	in effluent	in effluent	in effluent	Total	
Phase 2b: Klimatis Kampur ari an		Concentrations	in sludge (total)	disolved	associated	in effluent	in effluent	in effluent	in effluent	wastewater =	
Mo-B-T0air	Benzene	0.0	4583.7	157.4	157.3	0.1	4497.7	0.121	13.4	11.5	381.1
Mo-N-T0air	Naphtalene	0.0	46098.9	195.2	195.8	1.4	46098.9	0.121	13.4	11.5	381.1
Mo-M-T0air	Phenol	0.0	32.3	0.0	0.0	0.0	32.3	0.121	13.4	11.5	381.1
Mo-Poc-T0air	Phyoxymethylenes dioly amine	0.0	3.8	0.0	0.0	0.0	3.8	0.121	13.4	11.5	381.1
Mo-B-T0air	Benzene	0.0	4470.2	156.6	156.4	0.1	4470.2	0.121	13.4	11.5	381.1
Mo-N-T0air	Naphtalene	0.0	46032.8	194.9	195.6	1.4	46032.8	0.121	13.4	11.5	381.1
Mo-M-T0air	Phenol	0.0	32.3	0.0	0.0	0.0	32.3	0.121	13.4	11.5	381.1
Mo-Poc-T0air	Phyoxymethylenes dioly amine	0.0	3.8	0.0	0.0	0.0	3.8	0.121	13.4	11.5	381.1
Mo-B-T10water	Benzene	0.0	4518.7	158.3	158.2	0.1	4518.7	0.121	13.4	11.5	381.1
Mo-N-T10water	Naphtalene	0.0	46100.2	195.4	194.1	1.4	46100.2	0.121	13.4	11.5	381.1
Mo-M-T10water	Phenol	1.9	32.3	0.0	0.0	0.0	32.3	0.121	13.4	11.5	381.1
Mo-Poc-T10water	Phyoxymethylenes dioly amine	0.0	3.8	0.0	0.0	0.0	3.8	0.121	13.4	11.5	381.1
Mo-B-T5water	Benzene	0.0	4518.7	158.3	158.2	0.1	4518.7	0.121	13.4	11.5	381.1
Mo-N-T5water	Naphtalene	0.0	46100.2	195.4	194.1	1.4	46100.2	0.121	13.4	11.5	381.1
Mo-M-T5water	Phenol	1.9	32.3	0.0	0.0	0.0	32.3	0.121	13.4	11.5	381.1
Mo-Poc-T5water	Phyoxymethylenes dioly amine	0.0	3.8	0.0	0.0	0.0	3.8	0.121	13.4	11.5	381.1
Mo-B-wind9	Benzene	0.0	4518.5	158.3	158.1	0.1	4518.4	0.121	13.4	11.5	381.1
Mo-N-wind9	Naphtalene	0.0	46098.4	195.4	194.0	1.4	46098.4	0.121	13.4	11.5	381.1
Mo-M-wind9	Phenol	1.9	32.3	0.0	0.0	0.0	32.3	0.121	13.4	11.5	381.1
Mo-Poc-wind9	Phyoxymethylenes dioly amine	0.0	3.8	0.0	0.0	0.0	3.8	0.121	13.4	11.5	381.1
Mo-B-wind9	Benzene	0.0	4518.4	158.3	158.1	0.1	4518.4	0.121	13.4	11.5	381.1
Mo-N-wind9	Naphtalene	0.0	46098.4	195.4	194.0	1.4	46098.4	0.121	13.4	11.5	381.1
Mo-M-wind9	Phenol	1.9	32.3	0.0	0.0	0.0	32.3	0.121	13.4	11.5	381.1
Mo-Poc-wind9	Phyoxymethylenes dioly amine	0.0	3.8	0.0	0.0	0.0	3.8	0.121	13.4	11.5	381.1



Table Identifier >															
Case Identifier	Name compound	Height air column =	Fraction of air sample in row	Density air (kg/m <sup>3</sup> )	Depth aerator =	Oxygen concentration =	Aeration rate (1/L/E-05) =	Carbonaceous BOD in row average =	Fraction of C in row =	Fraction of solids in sludge =	Depth SLS =	C ratio SLS =	Function of SLS =	Density of solids SLS =	
Phase 3: Sewage															
Mo-B-95%CI	Benzene	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-B-95%CI	Napthalene	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-B-95%CI	Phenol	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-M-95%CI	Mercury (Hg)	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-P-95%CI	Polychlorinated biphenyls	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-B-105%CI	Benzene	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-N-105%CI	Napthalene	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-P-105%CI	Phenol	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-M-105%CI	Mercury (Hg)	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-P-105%CI	Polychlorinated biphenyls	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-B-95%CI	Benzene	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-N-105%CI	Napthalene	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-P-105%CI	Phenol	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-M-105%CI	Mercury (Hg)	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-P-105%CI	Polychlorinated biphenyls	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-B-105%CI	Benzene	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-N-105%CI	Napthalene	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-P-105%CI	Phenol	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-M-105%CI	Mercury (Hg)	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-P-105%CI	Polychlorinated biphenyls	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-B-95%CI	Benzene	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-N-105%CI	Napthalene	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-P-105%CI	Phenol	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-M-105%CI	Mercury (Hg)	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-P-105%CI	Polychlorinated biphenyls	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-B-95%CI	Benzene	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-N-105%CI	Napthalene	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-P-105%CI	Phenol	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-M-105%CI	Mercury (Hg)	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-P-105%CI	Polychlorinated biphenyls	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-B-95%CI	Benzene	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-N-105%CI	Napthalene	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-P-105%CI	Phenol	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-M-105%CI	Mercury (Hg)	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-P-105%CI	Polychlorinated biphenyls	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-B-95%CI	Benzene	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-N-105%CI	Napthalene	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-P-105%CI	Phenol	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-M-105%CI	Mercury (Hg)	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-P-105%CI	Polychlorinated biphenyls	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-B-95%CI	Benzene	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-N-105%CI	Napthalene	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-P-105%CI	Phenol	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-M-105%CI	Mercury (Hg)	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37
Mo-P-105%CI	Polychlorinated biphenyls	10	1.5	0.3	54	7	0.002	1.30E-05	4	0.37	1.3	4.15	6.973056	0.03	0.37









Table Identifier >	input		output		input		output		input		output	
	in air	in sludge	in effluent (total)	dislolved	associated	in effluent	in sludge	in effluent (total)	dislolved	associated	in effluent	in sludge
<b>WWTP Makaya</b>	Operation of the plant without primary settler											
<b>Phase 1: Compound related</b>	Budget loading rate = HRT = SRT = Aeration mode = Surplus sludge = wastewater =											
Case Identifier	Name compound =											
Me-B - 95%MM	Benzene	0.0	28.6	0.6	0.6	0.0	28.6	0.6	0.6	0.0	28.6	0.6
Me-B - 95%N	Naphtalene	0.0	82.3	0.3	0.3	0.0	82.3	0.3	0.3	0.0	82.3	0.3
Me-B - 95%Ph	Phenol	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Me-M - 95%MM	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Me-M - 95%AM	Monochloro(methyl)	0.0	33.1	898.8	898.8	0.0	33.1	898.8	898.8	0.0	33.1	898.8
Me-B - 105%MM	Benzene	0.0	28.6	0.6	0.6	0.0	28.6	0.6	0.6	0.0	28.6	0.6
Me-B - 105%N	Naphtalene	0.0	82.3	0.3	0.3	0.0	82.3	0.3	0.3	0.0	82.3	0.3
Me-B - 105%Ph	Phenol	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Me-M - 105%MM	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Me-M - 105%AM	Monochloro(methyl)	0.0	33.1	898.8	898.8	0.0	33.1	898.8	898.8	0.0	33.1	898.8
Me-M - 105%SM	Monochloro(methyl)	0.0	33.1	898.8	898.8	0.0	33.1	898.8	898.8	0.0	33.1	898.8
Me-B - 95%Vp	Benzene	0.0	28.6	0.6	0.6	0.0	28.6	0.6	0.6	0.0	28.6	0.6
Me-N - 95%Vp	Naphtalene	0.0	82.3	0.3	0.3	0.0	82.3	0.3	0.3	0.0	82.3	0.3
Me-N - 95%Vp	Phenol	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Me-M - 95%Vp	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Me-M - 95%Vp	Monochloro(methyl)	0.0	33.1	898.8	898.8	0.0	33.1	898.8	898.8	0.0	33.1	898.8
Me-B - 105%Vp	Benzene	0.0	28.6	0.6	0.6	0.0	28.6	0.6	0.6	0.0	28.6	0.6
Me-N - 105%Vp	Naphtalene	0.0	82.3	0.3	0.3	0.0	82.3	0.3	0.3	0.0	82.3	0.3
Me-N - 105%Vp	Phenol	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Me-M - 105%Vp	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Me-M - 105%Vp	Monochloro(methyl)	0.0	33.1	898.8	898.8	0.0	33.1	898.8	898.8	0.0	33.1	898.8
Me-N - 95%Sol	Naphtalene	0.0	82.3	0.3	0.3	0.0	82.3	0.3	0.3	0.0	82.3	0.3
Me-N - 95%Sol	Phenol	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Me-M - 95%Sol	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Me-M - 95%Sol	Monochloro(methyl)	0.0	33.1	898.8	898.8	0.0	33.1	898.8	898.8	0.0	33.1	898.8
Me-N - 105%Sol	Naphtalene	0.0	82.3	0.3	0.3	0.0	82.3	0.3	0.3	0.0	82.3	0.3
Me-N - 105%Sol	Phenol	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Me-M - 105%Sol	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Me-M - 105%Sol	Monochloro(methyl)	0.0	33.1	898.8	898.8	0.0	33.1	898.8	898.8	0.0	33.1	898.8
Me-B - 95%HC	Benzene	0.0	28.6	0.6	0.6	0.0	28.6	0.6	0.6	0.0	28.6	0.6
Me-N - 95%HC	Naphtalene	0.0	82.3	0.3	0.3	0.0	82.3	0.3	0.3	0.0	82.3	0.3
Me-N - 95%HC	Phenol	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Me-M - 95%HC	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Me-M - 95%HC	Monochloro(methyl)	0.0	33.1	898.8	898.8	0.0	33.1	898.8	898.8	0.0	33.1	898.8
Me-B - 105%HC	Benzene	0.0	28.6	0.6	0.6	0.0	28.6	0.6	0.6	0.0	28.6	0.6
Me-N - 105%HC	Naphtalene	0.0	82.3	0.3	0.3	0.0	82.3	0.3	0.3	0.0	82.3	0.3
Me-N - 105%HC	Phenol	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Me-M - 105%HC	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Me-M - 105%HC	Monochloro(methyl)	0.0	33.1	898.8	898.8	0.0	33.1	898.8	898.8	0.0	33.1	898.8



Table Identifier >		6-box										Elimination in the aerator			Elimination in the solids liquid separator			Total emission via effluent			Summary of distribution						
Case Identifier	Name compound =	Height air column =	Density air average =	Fraction of air average in row =	Depth aerator =	Origin concentration =	Aeration rate =	Fraction of solids =	Depth SLS =	C-avg solids =	Function of solids SLS =	Density of solids =	biodegradation	stripping	total	volatilization	vs surplus sludge	total	from waste water	% dissolved vs effluent	balance	to air	to water	degraded	total		
Me-B-TDair	Benzene	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-N-TDair	Naphtalene	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-M-TDair	Phenol	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-P-TDair	Mercury (Hg)	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-M-TDair	Monochloromethylol	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-B-TDair	Benzene	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-N-TDair	Naphtalene	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-M-TDair	Phenol	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-P-TDair	Mercury (Hg)	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-M-TDair	Monochloromethylol	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-B-TDwater	Benzene	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-N-TDwater	Naphtalene	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-M-TDwater	Phenol	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-P-TDwater	Mercury (Hg)	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-M-TDwater	Monochloromethylol	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-B-TDwater	Benzene	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-N-TDwater	Naphtalene	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-M-TDwater	Phenol	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-P-TDwater	Mercury (Hg)	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-M-TDwater	Monochloromethylol	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-B-TDwater	Benzene	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-N-TDwater	Naphtalene	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-M-TDwater	Phenol	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-P-TDwater	Mercury (Hg)	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-M-TDwater	Monochloromethylol	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-B-TDwater	Benzene	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-N-TDwater	Naphtalene	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-M-TDwater	Phenol	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-P-TDwater	Mercury (Hg)	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000
Me-M-TDwater	Monochloromethylol	54	10	1.5	0.3	9	0.002	1.30E-05	4	0.37	0.03	0.37	462	316	778	900	100	100	900	100	0.0	1000	563	100	0.1	316	1000

Table Identifier >	input	output	output	output	output	output	output	output	output	output
Case Identifier	Name compound =	in air	in effluent	in sludge	(total)	disolved	associated	in effluent	in sludge	Total
Me-B-T0air	Benzene	0.0	28.5	0.6	0.6	0.0	0.0	28.5	0.0	28.5
Me-N-T0air	Naphtalene	0.0	82.1	0.3	0.3	0.0	0.0	82.1	0.0	82.1
Me-P-T0air	Phend	0.0	33.1	0.0	0.0	0.0	0.0	33.1	0.0	33.1
Me-M-T0air	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Me-B-T0air	Monochlorobenzene	0.0	33.1	898.8	898.8	0.0	0.0	33.1	898.8	931.9
Me-N-T0air	Naphtalene	0.0	81.9	0.3	0.2	0.0	0.0	81.9	0.0	81.9
Me-P-T0air	Phend	0.0	33.1	0.0	0.0	0.0	0.0	33.1	0.0	33.1
Me-M-T0air	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Me-B-T0air	Monochlorobenzene	0.0	33.1	898.8	898.8	0.0	0.0	33.1	898.8	931.9
Me-B-T0water	Benzene	0.0	28.6	0.6	0.6	0.0	0.0	28.6	0.0	28.6
Me-N-T0water	Naphtalene	0.0	82.3	0.3	0.3	0.0	0.0	82.3	0.0	82.3
Me-P-T0water	Phend	0.0	33.1	0.0	0.0	0.0	0.0	33.1	0.0	33.1
Me-M-T0water	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Me-B-T0water	Monochlorobenzene	0.0	33.1	898.8	898.8	0.0	0.0	33.1	898.8	931.9
Me-B-T0wast	Benzene	0.0	28.6	0.6	0.6	0.0	0.0	28.6	0.0	28.6
Me-N-T0wast	Naphtalene	0.0	82.3	0.3	0.3	0.0	0.0	82.3	0.0	82.3
Me-P-T0wast	Phend	0.0	33.1	0.0	0.0	0.0	0.0	33.1	0.0	33.1
Me-M-T0wast	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Me-B-T0wast	Monochlorobenzene	0.0	33.1	898.8	898.8	0.0	0.0	33.1	898.8	931.9
Me-B-T0wast	Benzene	0.0	28.6	0.6	0.6	0.0	0.0	28.6	0.0	28.6
Me-N-T0wast	Naphtalene	0.0	82.3	0.3	0.3	0.0	0.0	82.3	0.0	82.3
Me-P-T0wast	Phend	0.0	33.1	0.0	0.0	0.0	0.0	33.1	0.0	33.1
Me-M-T0wast	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Me-B-T0wast	Monochlorobenzene	0.0	33.1	898.8	898.8	0.0	0.0	33.1	898.8	931.9
Me-B-T0wast	Benzene	0.0	28.6	0.6	0.6	0.0	0.0	28.6	0.0	28.6
Me-N-T0wast	Naphtalene	0.0	82.3	0.3	0.3	0.0	0.0	82.3	0.0	82.3
Me-P-T0wast	Phend	0.0	33.1	0.0	0.0	0.0	0.0	33.1	0.0	33.1
Me-M-T0wast	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Me-B-T0wast	Monochlorobenzene	0.0	33.1	898.8	898.8	0.0	0.0	33.1	898.8	931.9
Me-B-T0wast	Benzene	0.0	28.6	0.6	0.6	0.0	0.0	28.6	0.0	28.6
Me-N-T0wast	Naphtalene	0.0	82.3	0.3	0.3	0.0	0.0	82.3	0.0	82.3
Me-P-T0wast	Phend	0.0	33.1	0.0	0.0	0.0	0.0	33.1	0.0	33.1
Me-M-T0wast	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
Me-B-T0wast	Monochlorobenzene	0.0	33.1	898.8	898.8	0.0	0.0	33.1	898.8	931.9

Table Identifier >	Characterization of the chemical		Emission scenario		Sewage		C-heap		Biodegradation		
	input	input	input	input	input	input	input	input	input	input	
<b>Phase 3: Sewage</b>											
Case Identifier	Name compound =	Molecular weight =	Vapour pressure =	Solubility =	K <sub>a</sub> =	K <sub>b</sub> =	H <sub>1</sub> =	K <sub>ow</sub> =	R <sub>p</sub> (low) =	R <sub>p</sub> (medium) =	R <sub>p</sub> (high) =
Me-B-95%Q1	Benzene	78.11	135	9999	1770	5572875	3	1	79800	6.1	451
Me-B-95%Q2	Napthalene	128.19	1950	12	31.7	466095	15	15	84000	1.2	451
Me-PH-95%Q1	Phenol	94.111	29	48	70000	3.04E+12	3	3	84000	19	451
Me-M-95%Q1	Monochlorobenzene	112.5	156	100	70000	6.08E-04	15	15	79800	0.0004	451
Me-M-95%Q2	Monochlorobenzene	62.07	0	8	100	6.08E-03	15	15	79800	1000	451
Me-B-105%Q1	Benzene	78.11	135	9999	1770	5572875	3	1	84000	6.1	451
Me-B-105%Q2	Napthalene	128.19	1950	12	31.7	466095	15	15	84000	1.2	451
Me-PH-105%Q1	Phenol	94.111	29	48	70000	3.04E+12	3	3	84000	19	451
Me-PH-105%Q2	Phenol	94.111	29	48	70000	3.04E+12	3	3	84000	19	451
Me-M-105%Q1	Monochlorobenzene	112.5	156	100	70000	6.08E-04	15	15	84000	0.0004	451
Me-M-105%Q2	Monochlorobenzene	62.07	0	8	100	6.08E-03	15	15	84000	1000	451
Me-B-95%Q3	Benzene	78.11	135	9999	1770	5572875	3	1	84000	6.1	451
Me-B-105%Q3	Napthalene	128.19	1950	12	31.7	466095	15	15	84000	1.2	451
Me-PH-105%Q3	Phenol	94.111	29	48	70000	3.04E+12	3	3	84000	19	451
Me-M-105%Q3	Monochlorobenzene	112.5	156	100	70000	6.08E-04	15	15	84000	0.0004	451
Me-M-95%Q3	Monochlorobenzene	62.07	0	8	100	6.08E-03	15	15	84000	1000	451
Me-B-95%Q4	Benzene	78.11	135	9999	1770	5572875	3	1	84000	6.1	451
Me-B-105%Q4	Napthalene	128.19	1950	12	31.7	466095	15	15	84000	1.2	451
Me-PH-105%Q4	Phenol	94.111	29	48	70000	3.04E+12	3	3	84000	19	451
Me-M-105%Q4	Monochlorobenzene	112.5	156	100	70000	6.08E-04	15	15	84000	0.0004	451
Me-M-95%Q4	Monochlorobenzene	62.07	0	8	100	6.08E-03	15	15	84000	1000	451
Me-B-105%Q5	Benzene	78.11	135	9999	1770	5572875	3	1	84000	6.1	451
Me-B-105%Q6	Napthalene	128.19	1950	12	31.7	466095	15	15	84000	1.2	451
Me-PH-105%Q6	Phenol	94.111	29	48	70000	3.04E+12	3	3	84000	19	451
Me-M-105%Q6	Monochlorobenzene	112.5	156	100	70000	6.08E-04	15	15	84000	0.0004	451
Me-M-95%Q6	Monochlorobenzene	62.07	0	8	100	6.08E-03	15	15	84000	1000	451
Me-B-105%Q7	Benzene	78.11	135	9999	1770	5572875	3	1	84000	6.1	451
Me-B-105%Q8	Napthalene	128.19	1950	12	31.7	466095	15	15	84000	1.2	451
Me-PH-105%Q8	Phenol	94.111	29	48	70000	3.04E+12	3	3	84000	19	451
Me-M-105%Q8	Monochlorobenzene	112.5	156	100	70000	6.08E-04	15	15	84000	0.0004	451
Me-M-95%Q8	Monochlorobenzene	62.07	0	8	100	6.08E-03	15	15	84000	1000	451
Me-B-95%Q9	Benzene	78.11	135	9999	1770	5572875	3	1	84000	6.1	451
Me-B-95%Q10	Napthalene	128.19	1950	12	31.7	466095	15	15	84000	1.2	451
Me-PH-95%Q10	Phenol	94.111	29	48	70000	3.04E+12	3	3	84000	19	451
Me-M-95%Q10	Monochlorobenzene	112.5	156	100	70000	6.08E-04	15	15	84000	0.0004	451
Me-M-95%Q11	Monochlorobenzene	62.07	0	8	100	6.08E-03	15	15	84000	1000	451
Me-B-95%Q12	Benzene	78.11	135	9999	1770	5572875	3	1	84000	6.1	451
Me-B-95%Q13	Napthalene	128.19	1950	12	31.7	466095	15	15	84000	1.2	451
Me-PH-95%Q13	Phenol	94.111	29	48	70000	3.04E+12	3	3	84000	19	451
Me-M-95%Q13	Monochlorobenzene	112.5	156	100	70000	6.08E-04	15	15	84000	0.0004	451
Me-M-95%Q14	Monochlorobenzene	62.07	0	8	100	6.08E-03	15	15	84000	1000	451
Me-B-95%Q15	Benzene	78.11	135	9999	1770	5572875	3	1	84000	6.1	451
Me-B-95%Q16	Napthalene	128.19	1950	12	31.7	466095	15	15	84000	1.2	451
Me-PH-95%Q16	Phenol	94.111	29	48	70000	3.04E+12	3	3	84000	19	451
Me-M-95%Q16	Monochlorobenzene	112.5	156	100	70000	6.08E-04	15	15	84000	0.0004	451
Me-M-95%Q17	Monochlorobenzene	62.07	0	8	100	6.08E-03	15	15	84000	1000	451
Me-B-95%Q18	Benzene	78.11	135	9999	1770	5572875	3	1	84000	6.1	451
Me-B-95%Q19	Napthalene	128.19	1950	12	31.7	466095	15	15	84000	1.2	451
Me-PH-95%Q19	Phenol	94.111	29	48	70000	3.04E+12	3	3	84000	19	451
Me-M-95%Q19	Monochlorobenzene	112.5	156	100	70000	6.08E-04	15	15	84000	0.0004	451
Me-M-95%Q20	Monochlorobenzene	62.07	0	8	100	6.08E-03	15	15	84000	1000	451
Me-B-95%Q21	Benzene	78.11	135	9999	1770	5572875	3	1	84000	6.1	451
Me-B-95%Q22	Napthalene	128.19	1950	12	31.7	466095	15	15	84000	1.2	451
Me-PH-95%Q22	Phenol	94.111	29	48	70000	3.04E+12	3	3	84000	19	451
Me-M-95%Q22	Monochlorobenzene	112.5	156	100	70000	6.08E-04	15	15	84000	0.0004	451
Me-M-95%Q23	Monochlorobenzene	62.07	0	8	100	6.08E-03	15	15	84000	1000	451
Me-B-95%Q24	Benzene	78.11	135	9999	1770	5572875	3	1	84000	6.1	451
Me-B-95%Q25	Napthalene	128.19	1950	12	31.7	466095	15	15	84000	1.2	451
Me-PH-95%Q25	Phenol	94.111	29	48	70000	3.04E+12	3	3	84000	19	451
Me-M-95%Q25	Monochlorobenzene	112.5	156	100	70000	6.08E-04	15	15	84000	0.0004	451
Me-M-95%Q26	Monochlorobenzene	62.07	0	8	100	6.08E-03	15	15	84000	1000	451
Me-B-95%Q27	Benzene	78.11	135	9999	1770	5572875	3	1	84000	6.1	451
Me-B-95%Q28	Napthalene	128.19	1950	12	31.7	466095	15	15	84000	1.2	451
Me-PH-95%Q28	Phenol	94.111	29	48	70000	3.04E+12	3	3	84000	19	451
Me-M-95%Q28	Monochlorobenzene	112.5	156	100	70000	6.08E-04	15	15	84000	0.0004	451
Me-M-95%Q29	Monochlorobenzene	62.07	0	8	100	6.08E-03	15	15	84000	1000	451
Me-B-95%Q30	Benzene	78.11	135	9999	1770	5572875	3	1	84000	6.1	451
Me-B-95%Q31	Napthalene	128.19	1950	12	31.7	466095	15	15	84000	1.2	451
Me-PH-95%Q31	Phenol	94.111	29	48	70000	3.04E+12	3	3	84000	19	451
Me-M-95%Q31	Monochlorobenzene	112.5	156	100	70000	6.08E-04	15	15	84000	0.0004	451
Me-M-95%Q32	Monochlorobenzene	62.07	0	8	100	6.08E-03	15	15	84000	1000	451
Me-B-95%Q33	Benzene	78.11	135	9999	1770	5572875	3	1	84000	6.1	451
Me-B-95%Q34	Napthalene	128.19	1950	12	31.7	466095	15	15	84000	1.2	451
Me-PH-95%Q34	Phenol	94.111	29	48	70000	3.04E+12	3	3	84000	19	451
Me-M-95%Q34	Monochlorobenzene	112.5	156	100	70000	6.08E-04	15	15	84000	0.0004	451
Me-M-95%Q35	Monochlorobenzene	62.07	0	8	100	6.08E-03	15	15	84000	1000	451
Me-B-95%Q36	Benzene	78.11	135	9999	1770	5572875	3	1	84000	6.1	451
Me-B-95%Q37	Napthalene	128.19	1950	12	31.7	466095	15	15	84000	1.2	451
Me-PH-95%Q37	Phenol	94.111	29	48	70000	3.04E+12	3	3	84000	19	451
Me-M-95%Q37	Monochlorobenzene	112.5	156	100	70000	6.08E-04	15	15	84000	0.0004	451
Me-M-95%Q38	Monochlorobenzene	62.07	0	8	100	6.08E-03	15	15	84000	1000	451
Me-B-95%Q39	Benzene	78.11	135	9999	1770	5572875	3	1	84000	6.1	451
Me-B-95%Q40	Napthalene	128.19	1950	12	31.7	466095	15	15	84000	1.2	451
Me-PH-95%Q40	Phenol	94.111	29	48	70000	3.04E+12	3	3	84000	19	451
Me-M-95%Q40	Monochlorobenzene	112.5	156	100	70000	6.08E-04	15	15	84000	0.0004	451
Me-M-95%Q41	Monochlorobenzene	62.07	0	8	100	6.08E-03	15	15	84000	1000	451
Me-B-95%Q42	Benzene	78.11	135	9999	1770	5572875	3	1	84000	6.1	451
Me-B-95%Q43	Napthalene	128.19	1950	12	31.7	466095	15	15	84000	1.2	451
Me-PH-95%Q43	Phenol	94.111	29	48	70000	3.04E+12	3	3	84000	19	451
Me-M-95%Q43	Monochlorobenzene	112.5	156	100	70000	6.08E-04	15	15	84000	0.0004	451
Me-M-95%Q44	Monochlorobenzene	62.07	0	8	100	6.08E-03	15	15	84000	1000	451
Me-B-95%Q45	Benzene	78.11	135	9999	1770	5572875	3	1	84000	6.1	451
Me-B-95%Q46											

Table Identifier >		input	input	input	input	input	input	input	input	input	output	output	output	output	output	output												
Case Identifier	Name compound =	Height air column =	Density air average =	Fraction of air in row =	Fraction of air average =	Fraction of air in row =	Fraction of air average =	Depth aerator =	Oxygen concentration =	Aeration rate =	C ramp solids =	Function of solids =	Density of solids =	Elimination in the aerator			Elimination in the solids liquid separator			Total emission via effluent			Summary of distribution					
Phase 1: Sewage														biodegradation	stripping	total	volatilization	vs surplus sludge	total	% dissolved	% associated	balance	to air	to water	surplus	degraded	total	
Me-B-95%Q1	Benzene	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	462	323	785	11.7	0.1	11.8	903	9.7	0.0	100.0	579	9.7	0.1	323	1000	
Me-B-95%Q1	Naphtalene	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	342	256	598	17.0	0.9	17.9	165	20.3	0.2	100.0	519	20.5	0.9	272	1000	
Me-B-95%Q1	Phenol	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	104	76	180	0.0	0.0	0.0	104	0.0	0.0	100.0	104	0.0	0.0	0.0	1000	
Me-M-95%Q1	Mercury (Hg)	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	1000
Me-M-95%Q1	Monochloroethylol	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	1000
Me-B-105%Q1	Benzene	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	460	321	771	12.5	0.1	12.6	897	10.3	0.0	100.0	585	10.3	0.1	311	1000	
Me-B-105%Q1	Naphtalene	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	331	261	592	18.0	1.0	19.0	782	21.8	0.2	100.0	511	21.8	1.0	261	1000	
Me-B-105%Q1	Phenol	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	104	76	180	0.0	0.0	0.0	104	0.0	0.0	100.0	104	0.0	0.0	0.0	1000	
Me-M-105%Q1	Mercury (Hg)	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	1000
Me-M-105%Q1	Monochloroethylol	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	1000
Me-B-85%Q1	Benzene	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	461	317	778	12.1	0.1	12.2	890	10.0	0.0	100.0	582	10.0	0.1	317	1000	
Me-B-85%Q1	Naphtalene	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	337	266	604	17.5	1.0	18.5	788	21.2	0.2	100.0	512	21.2	1.0	266	1000	
Me-B-85%Q1	Phenol	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	100.0	0.0	100.0	0.0	0.0	0.0	100.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	0.0	1000
Me-M-85%Q1	Mercury (Hg)	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	1000
Me-M-85%Q1	Monochloroethylol	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	1000
Me-B-100%Q1	Benzene	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	461	317	778	12.1	0.1	12.2	890	10.0	0.0	100.0	582	10.0	0.1	317	1000	
Me-B-100%Q1	Naphtalene	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	337	266	604	17.5	1.0	18.5	788	21.2	0.2	100.0	512	21.2	1.0	266	1000	
Me-B-100%Q1	Phenol	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	100.0	0.0	100.0	0.0	0.0	0.0	100.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	0.0	1000
Me-M-100%Q1	Mercury (Hg)	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	1000
Me-M-100%Q1	Monochloroethylol	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	1000
Me-B-95%Q1	Benzene	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	461	317	778	12.1	0.1	12.2	890	10.0	0.0	100.0	582	10.0	0.1	317	1000	
Me-B-95%Q1	Naphtalene	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	337	266	604	17.5	1.0	18.5	788	21.2	0.2	100.0	512	21.2	1.0	266	1000	
Me-B-95%Q1	Phenol	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	100.0	0.0	100.0	0.0	0.0	0.0	100.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	0.0	1000
Me-M-95%Q1	Mercury (Hg)	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	1000
Me-M-95%Q1	Monochloroethylol	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	1000
Me-B-105%Q1	Benzene	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	461	317	778	12.1	0.1	12.2	890	10.0	0.0	100.0	582	10.0	0.1	317	1000	
Me-B-105%Q1	Naphtalene	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	337	266	604	17.5	1.0	18.5	788	21.2	0.2	100.0	512	21.2	1.0	266	1000	
Me-B-105%Q1	Phenol	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	100.0	0.0	100.0	0.0	0.0	0.0	100.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	0.0	1000
Me-M-105%Q1	Mercury (Hg)	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	1000
Me-M-105%Q1	Monochloroethylol	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	1000
Me-B-95%Q1	Benzene	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	461	317	778	12.1	0.1	12.2	890	10.0	0.0	100.0	582	10.0	0.1	317	1000	
Me-B-95%Q1	Naphtalene	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	337	266	604	17.5	1.0	18.5	788	21.2	0.2	100.0	512	21.2	1.0	266	1000	
Me-B-95%Q1	Phenol	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	100.0	0.0	100.0	0.0	0.0	0.0	100.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	0.0	1000
Me-M-95%Q1	Mercury (Hg)	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	1000
Me-M-95%Q1	Monochloroethylol	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	1000
Me-B-100%Q1	Benzene	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	461	317	778	12.1	0.1	12.2	890	10.0	0.0	100.0	582	10.0	0.1	317	1000	
Me-B-100%Q1	Naphtalene	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	337	266	604	17.5	1.0	18.5	788	21.2	0.2	100.0	512	21.2	1.0	266	1000	
Me-B-100%Q1	Phenol	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	100.0	0.0	100.0	0.0	0.0	0.0	100.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	0.0	1000
Me-M-100%Q1	Mercury (Hg)	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	1000
Me-M-100%Q1	Monochloroethylol	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	1000
Me-B-95%Q1	Benzene	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	461	317	778	12.1	0.1	12.2	890	10.0	0.0	100.0	582	10.0	0.1	317	1000	
Me-B-95%Q1	Naphtalene	10	1.5	0.3	4	0.37	1.3	5	0.03142857	0.03	0.37	1.3	337	266	604	17.5	1.0	18.5	788	21.2								

Table Identifier >	input		output		input		output		input		output	
	in air	in effluent	in air	in effluent	in air	in effluent	in air	in effluent	in air	in effluent	in air	in effluent
<b>Phase 3: Sewage</b>	Operation of the plant without primary settler											
<b>Case Identifier</b>	Name compound =		in surplus in effluent		disposed associated		in surplus in effluent		in surplus in effluent		Total	
			in air	sludge (total)			in air	sludge (total)	in air	sludge (total)	in air	sludge (total)
			Budget loading rate = HRT = SRT = Aeration mode = Surplus sludge = wastewater =									
			134.4 bubble aeration									
Me-B-95%Cl	0.0	27.7	0.6	0.6	0.0	27.7	0.012	155.6	134.4	0.0	11.0	79.9
Me-B-95%Cl	0.0	78.8	0.2	0.2	0.0	78.8	0.012	155.6	134.4	0.0	11.0	79.9
Me-PH-95%Cl	0.0	0.0	0.0	0.0	0.0	0.0	0.012	155.6	134.4	0.0	11.0	79.9
Me-M-95%Cl	0.0	32.9	892.0	892.0	0.0	32.9	0.012	155.6	134.4	0.0	11.0	79.9
Me-M-95%Cl	0.0	29.4	0.6	0.6	0.0	29.4	0.013	122.7	120.7	0.0	12.3	88.2
Me-B-105%Cl	0.0	84.8	0.3	0.3	0.0	84.8	0.013	122.7	120.7	0.0	12.3	88.2
Me-B-105%Cl	0.0	0.0	0.0	0.0	0.0	0.0	0.013	122.7	120.7	0.0	12.3	88.2
Me-PH-105%Cl	0.0	0.0	0.0	0.0	0.0	0.0	0.013	122.7	120.7	0.0	12.3	88.2
Me-M-105%Cl	0.0	33.2	901.2	901.2	0.0	33.2	0.013	122.7	120.7	0.0	12.3	88.2
Me-M-105%Cl	0.0	27.1	0.6	0.6	0.0	27.1	0.013	128.9	127.2	0.0	11.7	84.0
Me-B-85%Cl+flow	0.0	78.2	0.2	0.2	0.0	78.2	0.013	128.9	127.2	0.0	11.7	84.0
Me-PH-85%Cl+flow	0.0	0.0	0.0	0.0	0.0	0.0	0.013	128.9	127.2	0.0	11.7	84.0
Me-M-85%Cl+flow	0.0	31.4	852.0	852.0	0.0	31.4	0.013	128.9	127.2	0.0	11.7	84.0
Me-M-85%Cl+flow	0.0	29.9	0.6	0.6	0.0	29.9	0.013	128.9	127.2	0.0	11.7	84.0
Me-B-100%Cl+flow	0.0	86.5	0.3	0.3	0.0	86.5	0.013	128.9	127.2	0.0	11.7	84.0
Me-N-100%Cl+flow	0.0	0.0	0.0	0.0	0.0	0.0	0.013	128.9	127.2	0.0	11.7	84.0
Me-PH-100%Cl+flow	0.0	0.0	0.0	0.0	0.0	0.0	0.013	128.9	127.2	0.0	11.7	84.0
Me-M-100%Cl+flow	0.0	30.1	898.8	898.8	0.0	30.1	0.013	128.9	127.2	0.0	11.7	84.0
Me-M-100%Cl+flow	0.0	28.6	0.6	0.6	0.0	28.6	0.013	128.9	127.2	0.0	11.7	84.0
Me-B-SL+low	0.0	82.3	0.3	0.3	0.0	82.3	0.013	128.9	127.2	0.0	11.7	84.0
Me-N-SL+low	0.0	0.0	0.0	0.0	0.0	0.0	0.013	128.9	127.2	0.0	11.7	84.0
Me-PH-SL+low	0.0	0.0	0.0	0.0	0.0	0.0	0.013	128.9	127.2	0.0	11.7	84.0
Me-M-SL+low	0.0	33.1	898.8	898.8	0.0	33.1	0.013	128.9	127.2	0.0	11.7	84.0
Me-M-SL+low	0.0	28.6	0.6	0.6	0.0	28.6	0.013	128.9	127.2	0.0	11.7	84.0
Me-B-SL+high	0.0	82.3	0.3	0.3	0.0	82.3	0.013	128.9	127.2	0.0	11.7	84.0
Me-N-SL+high	0.0	0.0	0.0	0.0	0.0	0.0	0.013	128.9	127.2	0.0	11.7	84.0
Me-PH-SL+high	0.0	0.0	0.0	0.0	0.0	0.0	0.013	128.9	127.2	0.0	11.7	84.0
Me-M-SL+high	0.0	33.1	898.8	898.8	0.0	33.1	0.013	128.9	127.2	0.0	11.7	84.0
Me-M-SL+high	0.0	28.6	0.6	0.6	0.0	28.6	0.013	128.9	127.2	0.0	11.7	84.0
Me-B-95%(SS)	0.0	0.0	0.0	0.0	0.0	0.0	0.013	128.9	127.2	0.0	11.7	84.0
Me-M-95%(SS)	0.0	33.1	898.8	898.8	0.0	33.1	0.013	128.9	127.2	0.0	11.7	84.0
Me-M-95%(SS)	0.0	28.6	0.6	0.6	0.0	28.6	0.013	128.9	127.2	0.0	11.7	84.0
Me-B-105%(SS)	0.0	82.3	0.3	0.3	0.0	82.3	0.013	128.9	127.2	0.0	11.7	84.0
Me-N-105%(SS)	0.0	0.0	0.0	0.0	0.0	0.0	0.013	128.9	127.2	0.0	11.7	84.0
Me-PH-105%(SS)	0.0	0.0	0.0	0.0	0.0	0.0	0.013	128.9	127.2	0.0	11.7	84.0
Me-M-105%(SS)	0.0	33.1	898.8	898.8	0.0	33.1	0.013	128.9	127.2	0.0	11.7	84.0
Me-M-105%(SS)	0.0	28.6	0.6	0.6	0.0	28.6	0.013	128.9	127.2	0.0	11.7	84.0
Me-B-surfacebubble	0.0	16.1	0.3	0.3	0.0	16.1	0.013	128.9	127.2	0.0	11.7	84.0
Me-N-surfacebubble	0.0	0.0	0.0	0.0	0.0	0.0	0.013	128.9	127.2	0.0	11.7	84.0
Me-PH-surfacebubble	0.0	0.0	0.0	0.0	0.0	0.0	0.013	128.9	127.2	0.0	11.7	84.0
Me-M-surfacebubble	0.0	33.1	898.8	898.8	0.0	33.1	0.013	128.9	127.2	0.0	11.7	84.0
Me-M-surfacebubble	0.0	28.6	0.6	0.6	0.0	28.6	0.013	128.9	127.2	0.0	11.7	84.0
<b>Phase 4: Biodegradation</b>	Operation of the plant without primary settler											
Me-B-95%Cl	0.0	29.0	0.6	0.6	0.0	29.0	0.013	128.9	127.2	0.0	11.7	84.0
Me-N-95%Cl	0.0	83.4	0.3	0.3	0.0	83.4	0.013	128.9	127.2	0.0	11.7	84.0
Me-PH-95%Cl	0.0	0.0	0.0	0.0	0.0	0.0	0.013	128.9	127.2	0.0	11.7	84.0
Me-M-95%Cl	0.0	33.2	901.4	901.4	0.0	33.2	0.013	128.9	127.2	0.0	11.7	84.0
Me-M-95%Cl	0.0	28.1	0.6	0.6	0.0	28.1	0.013	128.9	127.2	0.0	11.7	84.0
Me-B-105%Cl	0.0	81.3	0.3	0.3	0.0	81.3	0.013	128.9	127.2	0.0	11.7	84.0
Me-N-105%Cl	0.0	0.0	0.0	0.0	0.0	0.0	0.013	128.9	127.2	0.0	11.7	84.0
Me-PH-105%Cl	0.0	0.0	0.0	0.0	0.0	0.0	0.013	128.9	127.2	0.0	11.7	84.0
Me-M-105%Cl	0.0	32.9	892.2	892.2	0.0	32.9	0.013	128.9	127.2	0.0	11.7	84.0
Me-M-105%Cl	0.0	28.1	0.6	0.6	0.0	28.1	0.013	128.9	127.2	0.0	11.7	84.0
Me-B-85%Cl+flow T5	0.0	36.2	0.8	0.8	0.0	36.2	0.013	128.9	127.2	0.0	11.7	84.0
Me-N-85%Cl+flow T5	0.0	100.1	0.3	0.3	0.0	100.1	0.013	128.9	127.2	0.0	11.7	84.0
Me-PH-85%Cl+flow T5	0.0	0.0	0.0	0.0	0.0	0.0	0.013	128.9	127.2	0.0	11.7	84.0
Me-M-85%Cl+flow T5	0.0	35.5	952.5	952.5	0.0	35.5	0.013	128.9	127.2	0.0	11.7	84.0
Me-M-85%Cl+flow T5	0.0	28.6	0.6	0.6	0.0	28.6	0.013	128.9	127.2	0.0	11.7	84.0
<b>Phase 5: Sea primary sedimentation system</b>	Operation of the plant without primary settler											
Me-B-PSS	0.0	82.3	0.3	0.3	0.0	82.3	0.013	128.9	127.2	0.0	11.7	84.0
Me-N-PSS	0.0	0.0	0.0	0.0	0.0	0.0	0.013	128.9	127.2	0.0	11.7	84.0
Me-PH-PSS	0.0	0.0	0.0	0.0	0.0	0.0	0.013	128.9	127.2	0.0	11.7	84.0
Me-M-PSS	0.0	33.1	898.8	898.8	0.0	33.1	0.013	128.9	127.2	0.0	11.7	84.0
Me-M-PSS	0.0	28.6	0.6	0.6	0.0	28.6	0.013	128.9	127.2	0.0	11.7	84.0







Table Identifier >	input		output		input		output		input		output	
	in air	in effluent	in air	in effluent	in air	in effluent	in air	in effluent	in air	in effluent	in air	in effluent
<b>Case Identifier</b>	Operation of the plant without primary effler											
<b>Concentrations</b>	Budget loading rate = HRT = SRT = Anation mode = Surplus sludge = wastewater =											
<b>WWTP Pollinans</b>	Phase 1 Compound related											
Ko-B-95%MM	0.0	1078.9	39.8	39.7	0.0	1078.9	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-B-95%MM	0.0	50.0	0.0	0.0	0.0	50.0	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-Ph-95%MM	0.0	0.0	0.0	0.0	0.0	0.0	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-M-95%MM	0.0	10.6	297.1	297.1	0.0	10.6	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-B-105%MM	0.0	1078.9	39.8	39.7	0.0	1078.9	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-B-105%MM	0.0	68.4	0.3	0.3	0.0	68.4	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-Ph-105%MM	0.0	0.0	0.0	0.0	0.0	0.0	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-M-105%MM	0.0	10.6	297.1	297.1	0.0	10.6	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-B-95%low	0.0	1035.1	39.8	39.7	0.0	1035.1	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-N-95%low	0.0	65.7	0.3	0.3	0.0	65.7	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-Ph-95%low	0.0	0.0	0.0	0.0	0.0	0.0	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-M-95%low	0.0	10.2	297.1	297.1	0.0	10.2	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-B-105%low	0.0	1122.3	39.8	39.7	0.0	1122.3	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-N-105%low	0.0	71.1	0.3	0.3	0.0	71.1	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-Ph-105%low	0.0	0.0	0.0	0.0	0.0	0.0	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-M-105%low	0.0	11.0	297.1	297.1	0.0	11.0	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-B-85%Vp	0.0	1078.9	39.8	39.7	0.0	1078.9	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-N-85%Vp	0.0	68.4	0.3	0.3	0.0	68.4	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-Ph-85%Vp	0.0	0.0	0.0	0.0	0.0	0.0	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-M-85%Vp	0.0	10.6	297.1	297.1	0.0	10.6	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-B-100%Vp	0.0	1078.9	39.8	39.7	0.0	1078.9	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-N-105%Vp	0.0	68.4	0.3	0.3	0.0	68.4	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-Ph-105%Vp	0.0	0.0	0.0	0.0	0.0	0.0	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-M-105%Vp	0.0	10.6	297.1	297.1	0.0	10.6	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-B-85%Sd	0.0	1078.9	39.8	39.7	0.0	1078.9	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-N-85%Sd	0.0	68.4	0.3	0.3	0.0	68.4	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-Ph-85%Sd	0.0	0.0	0.0	0.0	0.0	0.0	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-M-85%Sd	0.0	10.6	297.1	297.1	0.0	10.6	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-B-105%Sd	0.0	1108.1	40.8	40.8	0.0	1108.1	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-N-105%Sd	0.0	68.4	0.3	0.3	0.0	68.4	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-Ph-105%Sd	0.0	0.0	0.0	0.0	0.0	0.0	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-M-105%Sd	0.0	10.6	297.1	297.1	0.0	10.6	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-B-95%Hc	0.0	1078.9	39.8	39.7	0.0	1078.9	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-N-95%Hc	0.0	68.4	0.3	0.3	0.0	68.4	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-Ph-95%Hc	0.0	0.0	0.0	0.0	0.0	0.0	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-M-95%Hc	0.0	10.6	297.1	297.1	0.0	10.6	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-B-105%Hc	0.0	1050.4	38.7	38.7	0.0	1050.4	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-N-105%Hc	0.0	68.0	0.3	0.3	0.0	68.0	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-Ph-105%Hc	0.0	0.0	0.0	0.0	0.0	0.0	0.032	50.2	46.4	bubble aeration	18.0	120.0
Ko-M-105%Hc	0.0	10.6	297.2	297.2	0.0	10.6	0.032	50.2	46.4	bubble aeration	18.0	120.0



Table Identifier >		input	input	input	input	input	input	input	input	input	output	output	output	output	output	output
Case Identifier	Name compound =	Height air column =	Density air average =	Fraction of air average in row =	Depth aerator =	Oxygen aerator =	Aeration rate =	C-avg solids =	Function cc solids SLS =	Density solids =	Fraction of solids in row =	Depth SLS =	C-avg solids =	Function cc solids SLS =	Density solids =	
<b>6-box</b>																
Ko-B-T0air	Benzene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-B-T10air	Naphtalene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-B-T20air	Phenol	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-M-T0air	Mercury (Hg)	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-M-T10air	Monochlorobenzyl	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-B-T5air	Benzene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-B-T15air	Naphtalene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-B-T25air	Phenol	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-M-T5air	Mercury (Hg)	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-M-T15air	Monochlorobenzyl	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-B-T0water	Benzene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-B-T10water	Naphtalene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-B-T20water	Phenol	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-M-T0water	Mercury (Hg)	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-M-T10water	Monochlorobenzyl	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-B-T5water	Benzene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-B-T15water	Naphtalene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-B-T25water	Phenol	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-M-T5water	Mercury (Hg)	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-M-T15water	Monochlorobenzyl	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
<b>10-Box</b>																
Ko-B-T0air	Benzene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-B-T10air	Naphtalene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-B-T20air	Phenol	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-M-T0air	Mercury (Hg)	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-M-T10air	Monochlorobenzyl	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-B-T5air	Benzene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-B-T15air	Naphtalene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-B-T25air	Phenol	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-M-T5air	Mercury (Hg)	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-M-T15air	Monochlorobenzyl	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-B-T0water	Benzene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-B-T10water	Naphtalene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-B-T20water	Phenol	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-M-T0water	Mercury (Hg)	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3
Ko-M-T10water	Monochlorobenzyl	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3





Table Identifier	Input					Input					Input					Input					Input					Output					Output				
	Name compound =	Height air column =	Density air =	Fraction of air flow =	Fraction of air flow in row =	Depth aerator =	Oxygen concentration =	Aeration rate =	C-emp solids =	Function of C-emp solids =	Fraction of solids =	Depth SLS =	HRTSLS =	C-emp solids =	Function of C-emp solids =	Fraction of solids =	Elimination in the aerator by stripping	Elimination in the aerator by total biodegradation	Elimination in the solids liquid separator via surplus sludge	Elimination in the solids liquid separator via total volatilization	Elimination in the solids liquid separator total	% dissolved vs effluent	% associated balance	Sum of distribution to air	Sum of distribution to water	Sum of distribution to sludge	Sum of distribution to degraded	Sum of distribution to total							
<b>Phase B: Sewage</b>																																			
Ko-B-95%G1	Benzene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	54.2	16.3	70.7	2.7	0.1	2.8	74.1	25.9	0.0	100.0	57.0	25.9	0.1	17.0	100.0				
Ko-B-95%G1	Naphtalene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	30.8	14.6	45.2	3.5	1.7	5.1	50.8	49.2	0.0	100.0	34.0	48.6	1.7	14.6	100.0				
Ko-B-95%G1	Phend	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	10.0	0.0	10.0	0.0	0.0	0.0	10.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	100.0				
Ko-M-95%G1	Mercury (Hg)	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0				
Ko-M-95%G1	Monochlorobenzol	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0				
Ko-N-105%G1	Benzene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	54.1	16.3	70.7	2.7	0.1	2.8	74.1	25.9	0.0	100.0	56.9	27.0	0.1	16.0	100.0				
Ko-N-105%G1	Naphtalene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	28.8	14.9	44.4	3.5	1.7	5.1	48.7	50.3	0.0	100.0	33.1	50.3	1.7	14.0	100.0				
Ko-N-105%G1	Phend	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	10.0	0.0	10.0	0.0	0.0	0.0	10.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	100.0				
Ko-M-105%G1	Mercury (Hg)	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0				
Ko-M-105%G1	Monochlorobenzol	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0				
Ko-B-95%G1flow	Benzene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	54.2	16.3	70.7	2.7	0.1	2.8	74.1	25.9	0.0	100.0	56.9	26.5	0.1	16.5	100.0				
Ko-N-95%G1flow	Naphtalene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	30.3	15.3	45.6	3.4	1.7	5.1	50.8	49.2	0.0	100.0	33.8	49.2	1.7	15.3	100.0				
Ko-N-95%G1flow	Phend	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	10.0	0.0	10.0	0.0	0.0	0.0	10.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	100.0				
Ko-M-95%G1flow	Mercury (Hg)	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0				
Ko-M-95%G1flow	Monochlorobenzol	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0				
Ko-B-105%G1flow	Benzene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	54.2	16.3	70.7	2.7	0.1	2.8	74.1	25.9	0.0	100.0	56.9	26.5	0.1	16.5	100.0				
Ko-N-105%G1flow	Naphtalene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	30.3	15.3	45.6	3.4	1.7	5.1	50.8	49.2	0.0	100.0	33.8	49.2	1.7	15.3	100.0				
Ko-N-105%G1flow	Phend	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	10.0	0.0	10.0	0.0	0.0	0.0	10.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	100.0				
Ko-M-105%G1flow	Mercury (Hg)	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0				
Ko-M-105%G1flow	Monochlorobenzol	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0				
Ko-B-95%G1flow	Benzene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	54.2	16.3	70.7	2.7	0.1	2.8	74.1	25.9	0.0	100.0	56.9	26.5	0.1	16.5	100.0				
Ko-N-95%G1flow	Naphtalene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	30.3	15.3	45.6	3.4	1.7	5.1	50.8	49.2	0.0	100.0	33.8	49.2	1.7	15.3	100.0				
Ko-N-95%G1flow	Phend	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	10.0	0.0	10.0	0.0	0.0	0.0	10.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	100.0				
Ko-M-95%G1flow	Mercury (Hg)	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0				
Ko-M-95%G1flow	Monochlorobenzol	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0				
Ko-B-95%G1flow	Benzene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	54.2	16.3	70.7	2.7	0.1	2.8	74.1	25.9	0.0	100.0	56.9	26.5	0.1	16.5	100.0				
Ko-N-95%G1flow	Naphtalene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	30.3	15.3	45.6	3.4	1.7	5.1	50.8	49.2	0.0	100.0	33.8	49.2	1.7	15.3	100.0				
Ko-N-95%G1flow	Phend	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	10.0	0.0	10.0	0.0	0.0	0.0	10.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	100.0				
Ko-M-95%G1flow	Mercury (Hg)	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0				
Ko-M-95%G1flow	Monochlorobenzol	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0				
Ko-B-95%G1flow	Benzene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	54.2	16.3	70.7	2.7	0.1	2.8	74.1	25.9	0.0	100.0	56.9	26.5	0.1	16.5	100.0				
Ko-N-95%G1flow	Naphtalene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	30.3	15.3	45.6	3.4	1.7	5.1	50.8	49.2	0.0	100.0	33.8	49.2	1.7	15.3	100.0				
Ko-N-95%G1flow	Phend	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	10.0	0.0	10.0	0.0	0.0	0.0	10.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	100.0				
Ko-M-95%G1flow	Mercury (Hg)	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0				
Ko-M-95%G1flow	Monochlorobenzol	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	0.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0	0.0	0.0	0.0	0.0	0.0	0.0	100.0				
Ko-B-95%G1flow	Benzene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	54.2	16.3	70.7	2.7	0.1	2.8	74.1	25.9	0.0	100.0	56.9	26.5	0.1	16.5	100.0				
Ko-N-95%G1flow	Naphtalene	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	30.3	15.3	45.6	3.4	1.7	5.1	50.8	49.2	0.0	100.0	33.8	49.2	1.7	15.3	100.0				
Ko-N-95%G1flow	Phend	10	1.5	0.3	54	5.8	0.002	1.30E-05	4	0.37	1.3	7.5	8	0.03	0.37	1.3	10.0	0.0	10.0	0.0	0.0	0.0													

Table Identifier >		input	output	input	output	input	output	input	output		
Case Identifier	Name compound =	in surplus in effluent		in surplus in effluent		in surplus in effluent		Total			
		in air	sludge (total)	disolved	associated	in air	sludge (total)	disolved	associated		
<b>Phase 3: Sewage</b>											
Ko-B-95%(Q1)	Benzene	0.0	1066.3	38.9	38.9	0.0	1066.3	0.031	52.8	48.0	1140.0
Ko-B-95%(Q1)	Naphtalene	0.0	66.8	0.3	0.3	0.0	66.8	0.031	52.8	49.0	1140.0
Ko-B-95%(Q1)	Phend	0.0	68.4	0.3	0.3	0.0	68.4	0.031	52.8	49.0	1140.0
Ko-M-95%(Q1)	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.031	52.8	49.0	1140.0
Ko-M-95%(Q1)	Monochloroethyloz	0.0	10.6	298.5	298.5	0.0	10.6	0.031	52.8	48.0	1140.0
Ko-B-100%(Q1)	Benzene	0.0	1100.2	40.5	40.5	0.0	1100.2	0.034	47.8	44.1	1260.0
Ko-B-100%(Q1)	Naphtalene	0.0	69.9	0.3	0.3	0.0	69.9	0.034	47.8	44.1	1260.0
Ko-B-100%(Q1)	Phend	0.0	71.5	0.3	0.3	0.0	71.5	0.034	47.8	44.1	1260.0
Ko-M-100%(Q1)	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.034	47.8	44.1	1260.0
Ko-M-100%(Q1)	Monochloroethyloz	0.0	10.6	297.7	297.7	0.0	10.6	0.034	47.8	44.1	1260.0
Ko-B-95%(clflow)	Benzene	0.0	1025.0	37.8	37.7	0.0	1025.0	0.032	50.2	46.4	1200.0
Ko-B-95%(clflow)	Naphtalene	0.0	65.0	0.3	0.3	0.0	65.0	0.032	50.2	46.4	1200.0
Ko-B-95%(clflow)	Phend	0.0	66.6	0.3	0.3	0.0	66.6	0.032	50.2	46.4	1200.0
Ko-M-95%(clflow)	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.032	50.2	46.4	1200.0
Ko-M-95%(clflow)	Monochloroethyloz	0.0	10.1	272.8	272.8	0.0	10.1	0.032	50.2	46.4	1200.0
Ko-B-100%(clflow)	Benzene	0.0	1132.9	41.7	41.7	0.0	1132.9	0.032	50.2	46.4	1200.0
Ko-B-100%(clflow)	Naphtalene	0.0	71.8	0.3	0.3	0.0	71.8	0.032	50.2	46.4	1200.0
Ko-B-100%(clflow)	Phend	0.0	73.4	0.3	0.3	0.0	73.4	0.032	50.2	46.4	1200.0
Ko-M-100%(clflow)	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.032	50.2	46.4	1200.0
Ko-M-100%(clflow)	Monochloroethyloz	0.0	10.6	297.1	297.1	0.0	10.6	0.032	50.2	46.4	1200.0
Ko-B-95%(S)	Benzene	0.0	1078.9	39.8	39.7	0.0	1078.9	0.032	50.2	46.4	1200.0
Ko-B-95%(S)	Naphtalene	0.0	68.4	0.3	0.3	0.0	68.4	0.032	50.2	46.4	1200.0
Ko-B-95%(S)	Phend	0.0	70.0	0.3	0.3	0.0	70.0	0.032	50.2	46.4	1200.0
Ko-M-95%(S)	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.032	50.2	46.4	1200.0
Ko-M-95%(S)	Monochloroethyloz	0.0	10.6	297.1	297.1	0.0	10.6	0.032	50.2	46.4	1200.0
Ko-B-100%(S)	Benzene	0.0	1078.9	39.8	39.7	0.0	1078.9	0.032	50.2	46.4	1200.0
Ko-B-100%(S)	Naphtalene	0.0	68.4	0.3	0.3	0.0	68.4	0.032	50.2	46.4	1200.0
Ko-B-100%(S)	Phend	0.0	70.0	0.3	0.3	0.0	70.0	0.032	50.2	46.4	1200.0
Ko-M-100%(S)	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.032	50.2	46.4	1200.0
Ko-M-100%(S)	Monochloroethyloz	0.0	10.6	297.1	297.1	0.0	10.6	0.032	50.2	46.4	1200.0
Ko-B-95%(SS)	Benzene	0.0	441.1	16.3	16.2	0.0	441.1	0.032	50.2	46.4	1200.0
Ko-B-95%(SS)	Naphtalene	0.0	58.8	0.3	0.3	0.0	58.8	0.032	50.2	46.4	1200.0
Ko-B-95%(SS)	Phend	0.0	60.4	0.3	0.3	0.0	60.4	0.032	50.2	46.4	1200.0
Ko-M-95%(SS)	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.032	50.2	46.4	1200.0
Ko-M-95%(SS)	Monochloroethyloz	0.0	10.6	297.1	297.1	0.0	10.6	0.032	50.2	46.4	1200.0
Ko-B-95%(SS)	Benzene	0.0	441.1	16.3	16.2	0.0	441.1	0.032	50.2	46.4	1200.0
Ko-B-95%(SS)	Naphtalene	0.0	58.8	0.3	0.3	0.0	58.8	0.032	50.2	46.4	1200.0
Ko-B-95%(SS)	Phend	0.0	60.4	0.3	0.3	0.0	60.4	0.032	50.2	46.4	1200.0
Ko-M-95%(SS)	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.032	50.2	46.4	1200.0
Ko-M-95%(SS)	Monochloroethyloz	0.0	10.6	297.1	297.1	0.0	10.6	0.032	50.2	46.4	1200.0
<b>Phase 4: Biodegradation</b>											
Ko-B-95%(bio)	Benzene	0.0	1087.9	40.1	40.0	0.0	1087.9	0.032	50.2	46.4	1200.0
Ko-B-95%(bio)	Naphtalene	0.0	68.8	0.3	0.3	0.0	68.8	0.032	50.2	46.4	1200.0
Ko-B-95%(bio)	Phend	0.0	70.4	0.3	0.3	0.0	70.4	0.032	50.2	46.4	1200.0
Ko-M-95%(bio)	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.032	50.2	46.4	1200.0
Ko-M-95%(bio)	Monochloroethyloz	0.0	10.6	297.7	297.7	0.0	10.6	0.032	50.2	46.4	1200.0
Ko-B-100%(bio)	Benzene	0.0	1070.1	39.4	39.4	0.0	1070.1	0.032	50.2	46.4	1200.0
Ko-B-100%(bio)	Naphtalene	0.0	67.9	0.3	0.3	0.0	67.9	0.032	50.2	46.4	1200.0
Ko-B-100%(bio)	Phend	0.0	69.5	0.3	0.3	0.0	69.5	0.032	50.2	46.4	1200.0
Ko-M-100%(bio)	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.032	50.2	46.4	1200.0
Ko-M-100%(bio)	Monochloroethyloz	0.0	10.6	298.5	298.5	0.0	10.6	0.032	50.2	46.4	1200.0
Ko-B-95%(bio)	Benzene	0.0	1211.7	44.6	44.6	0.0	1211.7	0.032	50.2	46.4	1200.0
Ko-B-95%(bio)	Naphtalene	0.0	78.2	0.3	0.3	0.0	78.2	0.032	50.2	46.4	1200.0
Ko-B-95%(bio)	Phend	0.0	80.0	0.3	0.3	0.0	80.0	0.032	50.2	46.4	1200.0
Ko-M-95%(bio)	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.032	50.2	46.4	1200.0
Ko-M-95%(bio)	Monochloroethyloz	0.0	10.9	295.6	295.6	0.0	10.9	0.032	50.2	46.4	1200.0
<b>Phase 5: Size fraction sedimentation system</b>											
Ko-B-PSS	Benzene	0.0	1078.9	39.8	39.7	0.0	1078.9	0.032	50.2	46.4	1200.0
Ko-N-PSS	Naphtalene	0.0	68.4	0.3	0.3	0.0	68.4	0.032	50.2	46.4	1200.0
Ko-N-PSS	Phend	0.0	70.0	0.3	0.3	0.0	70.0	0.032	50.2	46.4	1200.0
Ko-M-PSS	Mercury (Hg)	0.0	0.0	0.0	0.0	0.0	0.0	0.032	50.2	46.4	1200.0
Ko-M-PSS	Monochloroethyloz	0.0	10.6	297.1	297.1	0.0	10.6	0.032	50.2	46.4	1200.0



# Annex B: SimpleTreat.i (v. 3.3, 15 May 09), Using the Batch-tab

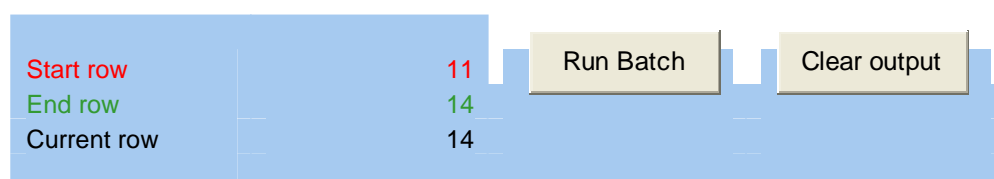
Number of pages: 1

A new addition has been made to the SimpleTreat-spreadsheet to assist in the use of the model during the sensitivity analysis. This new functionality can also be put to good use when assessing the performance of a WWTP for a set of compounds and/or different operating conditions.

The file with this new functionality is called: ST33i\_unprotected\_batch\_run.xls.

It is located on a tab called 'batch'.

A view of the top-right corner of this new tab 'batch' is given in Figure 1.



Tab-identifier >	input	input	input
Unit >	(-)	g mol-1	(-)
Case Identifier	Name compound	Molecular weight =	Kow =
base	Imidozaline	70.093	3.02E-01
high	Imidozaline	70.093	3.02E-01
low	Imidozaline	70.093	3.02E-01
choose your own	Imidozaline	70.093	3.02E-01

Figure 1 View of the 'batch'-functionality

A 'Start row' and 'End row' can be specified for the underlying macro's to operate on. By specifying these the user can control which cases, are to be calculated.

For the macro to return sensible results the user should start by specifying all inputs. In the 'batch'-tab these can be identified by the Tab-identifier in row 7. Please note that some inputs may also be required on the '9-box'- and '6-box'-tabs, when other values than the defaults are to be used in the calculations.

At the beginning of each row a 'Case Identifier' is available.

Once all the cases have been defined, the **"Run Batch"**-button will start a macro that will start to process all rows in the range specified by 'Start row' and 'End row'. 'Current row' can be used as a progress meter. For each case the macro will copy the specified inputs to the tabs 'input', '9-box' and '6-box', run the model and copy the results to the output range on the 'batch'-tab. All data is then available for analysis and evaluation.

The **"Clear output"**-button will clear all previously calculated results from the results-range to the right of the input-range. This button also runs a macro that processes the cases as defined by 'Start row' and 'End row'.

Calculating only new cases or only a subset of cases that have been modified can be achieved by appropriately adjusting the 'Start row' and 'End row'.